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NASA CONTRACTOR REPORT

NASA CR-143945

DEVELOPMENT OF THERMAL STRATIFICATION AND DESTRATIFICATION SCALING CONCEPTS - VOLUME II Stratification - Experimental Data

By T. N. Lovrich and S. H. Schwartz McDonnell Douglas Astronautics Company Huntington Beach, California

October 1975



Prepared for

N A S A - GEORGE C. MARSHALL SPACE FLIGHT CENTER Marshall Space Flight Center, Alabama 35812

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FOREWORD

This document is Volume II of the final report on NASA Contract NASS-24747, "Development of Thermal Stratification and Destratification Scaling Concepts." T. M. Lovrich, Program Manager, McDonnell Douglas Astronautics Company, performed the study for the George C. Marshall Space Flight Center of the National Aeronautics and Space Administration. The program was conducted under the technical direction of Mr. T. W. Winstead, Thermodynamics and Fluid Mechanics Branch, Propulsion Division, MSFC Propulsion and Vehicle Engineering Laboratory.

The author wishes to recognize Mr. L. A. Holmes, Engineering Instructor at Modesto Junior College in California, for initiating most of the initial scaling concepts analytical work and test design, and to Mr. T. W. Winstead, MSFC Contract Technical Supervisor, for his assistance during the performance of this research study.

The final report consists of two volumes:

Volume I Definition of Thermal Stratification Scaling Parameters and Experimental Investigations

Volume II Stratification—Experimental Data

Volume I is a report of the final results, conclusions, and recommendations of the study. It includes a presentation of the analytical methods used in defining the thermal stratification dimensionless scaling parameters and the experimental investigations performed with saturated Freon 113 PCA in three closed tanks geometrically scaled for determining the validity of these scaling parameters. Volume II contains a presentation of the experimental data collected and utilized in this stratification research study.

Work performed with the 6 inch and 18 inch diameter tanks was supported under this contract, while the work performed with a 12-inch-diameter tank was primarily supported by MDAC-West IRAD "Low-G Fluid Mechanics and Heat Transfer" funding.

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NOMENCLATURE

Specific heat at constant pressure D tank diameter Fourier number, $\mu_{\ell} \theta/\rho_{\ell} D^2$ Fo gravitational constant g Modified Grashof number, g $\beta q'' L^4/k v^2$ Gr* Modified Grashof number based on $q_{\mbox{\scriptsize H}}^{\mbox{\tiny II}}$ (e.g., theoretical Grashof number) Gr_{H}^{*} (Gr_{Fluid}^*) Modified Grashof number based on q_{ℓ}'' (i. e., q_{fluid}'') H tank height $\mathbf{h}_{\mathbf{fg}}$ latent heat of vaporization Interface number, q" DCp/hfg kl I Thermal conductivity L liquid height m mass pressure Prandtl number, $\mu c_{D}/k$ heat flux heat flux $(q_{fluid}^{"})$ heat flux to liquid heat flux to ullage

distance from bottom of tank

Greek Symbols

- β coefficient of thermal expansion
- 9 stratification test period
- μ viscosity
- ν kinematic viscosity, μ/ρ
- e density
- t dimensionless time, t/9

Section 1 INTRODUCTION

This volume of the final report contains temperature and pressure data obtained from the saturated Freon 113 PCA closed-tank stratification tests conducted during this study. These data are documented to provide the detailed stratification test data from which the analytical procedures and conclusions in Volume I were obtained, and to furnish data for further analyses as required.

The data presented in tabular form are the test conditions, sensible heat values, and Freon 113 PCA liquid and ullage (vapor) properties for the 37 tests conducted in this program. Also included, are graphical representations of the liquid and ullage temperature and delta-temperature profiles, ullage and liquid bulk temperature and pressure histories, and dimensionless liquid-ullage delta-temperature profiles. The Modified Grashof numbers (Gr_H^* and Gr_ℓ^*) and Fourier number-history data are also presented graphically.

Section 2 TEST MATRIX—HEATER AND THERMOCOUPLE LOCATIONS

The tests investigated in this program are identified in the Test Matrix shown in Table 2-1. Figures 2-1, 2-2, and 2-3 identify the test-tank wall heater arrangement, the tank wall and penetration structural thermocouple locations, and the ullage-liquid thermocouple positions on an internal tank rake, respectively. The liquid and ullage thermocouple locations relative to the tank height are given in Table 2-2.

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Table 2-1
TEST MATRIX - FREON 113 (PCA)

Fest Golumn #1	Fest Golumn #2	Test Column * 3 18 in. Dia Tank	
6 in. Dia Tank	12 in. Dia Tank		
8G - Acceleration - 27G	1G	1G	
1,000 Btu/hr ft ² (L) 87.5% FILL Gr# = 10 ¹⁵ TESTS #2,#12S	500 Btu/hr ft ² (L) 87. 5% FILL Gr= = 10 ¹⁵ TESTS #30,#25		
1,000 Btu/hr ft ² (L+U) 87.5% FILL Gr= = 10 ¹⁵ TESTS #3, #NS	500 Btu/hr (t ² (L+U) 87. 5% FILL Gr= = 10 ¹⁵ TESTS #31,#17		
700 Btu/hr ft ² (L) 50% FILL Gr# = 10 ¹⁴ TESTS #95, #15S	350 Btu/hr ft ² (L) 50% FHLL Gr= = 1014 TESTS #33, #32		
700 Btu/hr ft ² (L+U) 50 FILL Gr= 10 ¹⁴ TESTS #105, 'S	350 Btu/hr (t ² (L+U) 50% FILL Gr# = 10 ¹⁴ TESTS #34, #35		
600 Btu/hr ft ² (L) 87.5% FILL $Gr^{\pm} = 7 \times 10^{14}$ TESTS = 1, \pm 5, π 8.	300 Btu/hr (t ² (L) 87.5% FILL Gr# = 7 x 40 ¹⁴ RESTS #20, #22		
600 Btu/hr ft ² (L+U) 87.5% FILL Gr+ = 7 x 10 ¹⁴ TESTS #4.*•	300 Btu/hr ft ² (L+U) 87.5% FILL Gr= 7 x 10 ¹⁴ TESTS #23, #28		
90 Btu/hr (t ² (L) 87, 5% FILL Gro = .014 TEST #14	45 Btu/hr ft ² (L) 87. 5% FU.L Gr== 1014 TESTS #26, #15		
90 Btu/hr ft ² (L+U) 87, 5% FILL Gr* = 10.4 TEST #13	45 Btu/hr ft ² (L+U) 87.5% FILL Gr= 10 ¹⁴ TEST #27		
2,230 Btu/hr ft ² (L) 50% FILL $G_{\mathbf{r}^{\prime\prime}} = 10^{15}$ TEST #1S		748 Btu/hr (t ² (L) 50% FH.L Gr* = 10 ¹⁵ TESTS *BS, *D	
2, 860 Btu/hr (t ² (L) 87. 5% FILL Gr# = 10 ¹¹⁰ TEST #3S		960 Btu/hr ft ² (L) 87, 55; FILL Gr. 1010 TEST #15	

NOTES:

- (L), (L+U) ... Liquid, and I iquid + Ullage Heating.
- Tests horizontally across Table are scaling tests (i.e., tests having constant Modified Grashof no. Grass Group of the liquid depth)).
- 48 Ja. San tests number indicates no heating during destratification testing.

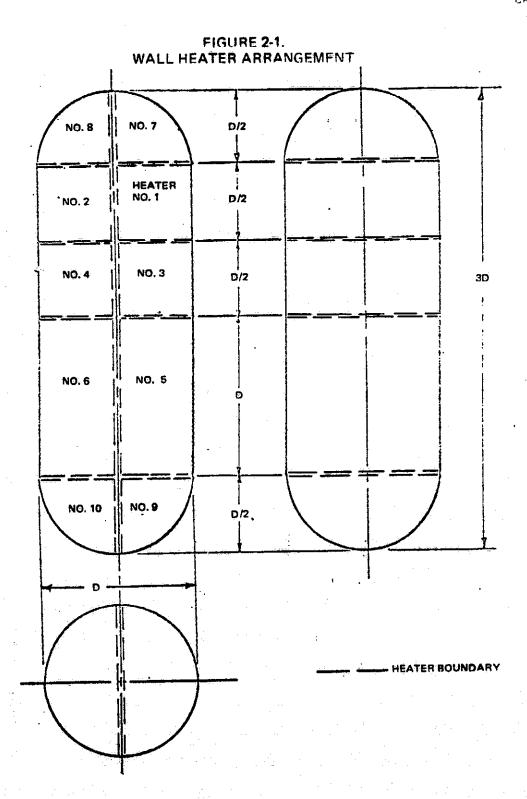


FIGURE 2-2.
TANK WALL AND PENETRATION THERMOCOUPLE LOCATIONS

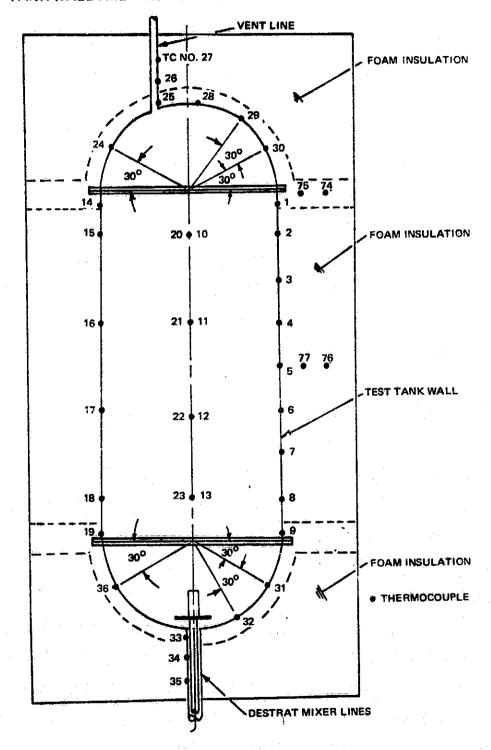


FIGURE 2-3.
LIQUID-ULLAGE RAKE THERMOCOUPLE LOCATIONS

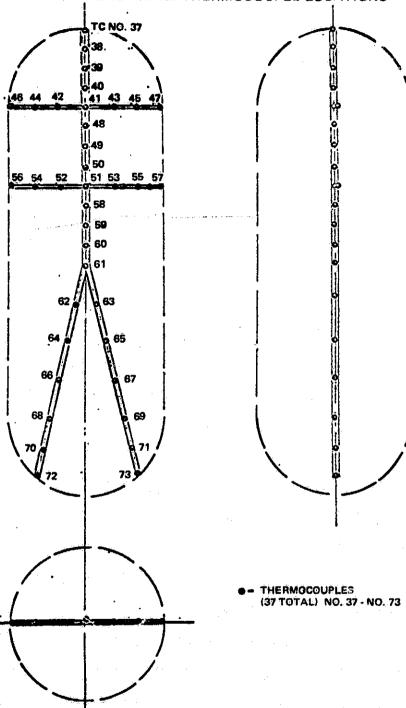
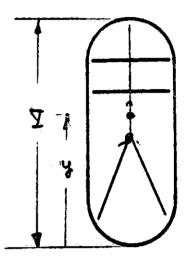


Table 2-2
LIQUID-ULLAGE THERMOCOUPLE - NORMALIZED TANK HEIGHT RATIOS

Thermocouple No.	Normalized Tank Height (y/文)
37	0.98
38	0.958
39	0.917
40	0.875
41-47	0.833
48	0.793
49	0.752
50	0.71
51-57	0.668
58	0.626
59 ·	0.584
60	0.542
61	0.5
62-63	0.42
64-65	0.339
66-67	0.259
68 -6 9	0.178
70-71	0.111
72-73	0.044



Section 3 TEST CONDITIONS AND TABULATED SENSIBLE HEAT DATA

This section contains the heat flux from the input neater, liquid (Freon 113 PCA) level, and stratification test time for each stratification test investigated. Included, are the tabulated sensible heat gains by the test liquid, ullage, and portion of the test tank structures; the tank wall; and silicone rubber heaters. This information is shown in Table 3-1.

Table 3
TEST CONDITIONS - SUPPI SENSIBLE HEAT GAI

Test No.	5 in, 8G	6 in. 8G	6 in. 8G
	No, 9 S	No. 2	No. 1
Liquid Level (percent) Heating Condition	50,0	87.5	87.5
	Liquid	Liquid	Liquid
Liquid Heater Electrical Source q ¹¹ (Btu/hr ft ²) Ullage Heater Electrical Source q ¹¹ (Btu/hr ft ²) Stratification Test Time (minute) Liquid Total Energy Supplied (Btu) Ullage Total Energy Supplied (Btu) Summation — Total Energy Supplied (Btu)	701, 569	1001.99	600,85
	0, 0	0.0	0.0
	3, 33	2.0	3.666
	45, 913	65.58	71.966
	0, 0	0.0	0.0
	45, 913	65.58	71.966
Liquid — Measured Heat Flux q'' (Btu/hr ft²)	368, 248	582, 284	389.008
Ullage — Measured Heat Flux q'' (Btu/hr ft²)	1, 744	2, 566	1.604
Tank - Stainless Wall - Measured Sensible Heat (Btu) Silicone Heaters - Measured Sensible Heat (Btu) Foam Insulation - Measured Sensible Heat (Btu) Freon 113 (PCA - Measured Sensible Heat (Btu) Ullage - Measured Sensible Heat (Btu) Summation - Measured Absorbed Sensible Heat (Btu)	6. 089	7.867	7.244
	4. 384	5.89	5.42
	8. 675	9.095	9.233
	24. 102	38.11	46.669
	0. 114	0.034	0.038
	43. 364	60.996	68.604
Percent - Measured Absorbed Heat/Total Energy Supplied	94.44	93.01	95.32
Test No.	12 in. 1G	12 in. 1G	12 in, 1G
	No. 25	No. 32	No. 22
Liquid Level (percent) Heating Condition	87.5	50, 0	87.5
	Liquid	Liquid	Liquid
Liquid Heater Electrical Source q ⁿ (Btu/hr ft ²) Ullage Heater Electrical Source q ⁿ (Btu/hr ft ²) Stratification Test Time (minute) Liquid Total Energy Supplied (Btu) Ullage Total Energy Supplied (Btu) Summation — Total Energy Supplied (Btu)	500.56	349.77	300.077
	0.0	0.0	0.0
	8.0	13.0	15.0
	524.188	357.123	589.2
	0.0	0.0	0.0
	524.188	357.123	589.2
3	328. 14	206.34	214, 021
	1. 194	0.723	0, 767
Liquid - Measured Heat Flux q'' (Btu/hr ft²) Ulfage - Measured Heat Flux q'' (Btu/hr ft²) Tank - Stainless Wall - Measured Sensible Heat (Btu) Silicone Heaters - Measured Sensible Heat (Btu) Foam Insulation - Measured Sensible Heat (Btu) Freon 113 PCA - Measured Sensible Heat (Btu) Ulfage - Measured Sensible Heat (Btu) Summation - Measured Absorbed Sensible Heat (Btu)	328.14		

Table 3-1
NS - SUPPLIED HEAT FLUXES HEAT GAINS (Page 1 of 2)

			· _				
6 in. 8G No. 1	6 in, 8G No. 14	6 in. 8G No. 10S	6 in. 8G No. 3	6 in. 8G No. 4	6 in, 8G No. 13	6 in. 27G No. 1S	6 in. 27G No. 3S
87, 5 Liquid	87.5 Liquid	50.0 Liquid and	87.5 Liquid and	97.5 Liquid and Ullage	87.5 Liquid and Ullage	50.0 Liquid	87.5 Liquid
600, 85	90, 127	Ullage 701,569	Ullage 1001.99	600.85	90. 127	2236, 686	2884. 422
် 0.0	0.0	701.569	1001.99	600, 85	90.127	0.0	0.0
3.666	25.0	2, 333	2.0	3,75	25.0	1.0	1.0
71,966	73.735	32, 142	65.58	73.735	73.735	43, 917	94.394
0.0	0.0	32, 142	13. 116	14,747	14.747	0.0	0, 0
71.966	73,735	64. 284	78, 696	88.482	88.482	43.917	94. 39 2
389.008	51,382	419.734	620, 367	386.81	59 . 366	1529.462	1880.114
1,604	0.249	14, 206	10,772	8,338	0.809	5.611	8. 264
7.244	5.421	18.8	15.867	15.067	8,756	5.91	10.355
5,42	3.892	13.396	9, 65	9.049	5,612	4. 146	7.8
9, 233	9, 116	12.54	11.16	11.099	10, 219	8.949	10.438
46.669	42,037	19.23	40,603	47.469	1 8.569	29.031	61.527
0,038	0,041	0.465	0.141	0, 206	0.132	0.107	0.054
68.604	60, 5 0 7	64. 4 31	77. 421	89.89	73, 288	48.143	90.174
95.32	82.06	1844、2等	98.37	93.68	82.82	109.62	95.53
12 in. 1G	12 in. 1G	12 10, 13	12 in. 1G	12 in, 1G	18 in. 1G		
No. 22	No. 15	No. 38	No. 17	No. 28	No. D		·
87.5	87.5	50,0	87.5	87.5	50.0		
Liquid	Liquid	Liquid and	Liquid and	Liquid and	Liquid		
A	•	Ullage	Ullage	Ullage			
300,077	45.012	349.77	500,56	300,077	753. 15		
0.0	0,0	350.35	500,56	300, 424	0.0		
15.0	99.0	9.0	8.0	15.0	9,0		
589.2	583,31	247. 239	524, 188	589.2	1197.835		
0.0	0.0	247.648	104.84	117.976	0.0		
589.2	583.31	494.887	629.028	707.176	1197.835		
214, 021	29.444	223.179	349.47	223, 311	409.627		÷
0.767	0.101	7.55	5.763	5.844	1.639		
61,65	39,912	168.205	109.404	125.084	201.998		
22. 237	14. 22	60.041	34.077	37.234	49.189		
72.869	68.84	105.571	86.48	89.537	238.016	•	
420, 229	381.562	157,756	365.964	438.47	651.483		
0.301	0.262	5.336	1.207	2. 295	2.607		•
577. 286	504.796	496. 909	597, 132	692.62	1143. 293		
97.97	86.53	100.4	94. 92	97.94	95.44		
20.5							

Table 3-TEST CONDITIONS - SUPPI SENSIBLE HEAT GAIL

			·
Test No.	6 in. 8G	6 in. 8G	6 in. 8G
	No. 15S	No. 12S	No. 5
Liquid Level (percent) Heating Condition	50.0	87.5	87.5
	Liquid	Liquid	Liquid
Liquid Heater Electrical Source q' (Btu/hr ft ²) Ullage Heater Electrical Source q'H (Btu/hr ft ²) Stratification Test Time (minute) Liquid Total Energy Supplied (Btu) Ullage Total Energy Supplied (Btu) Summation — Total Energy Supplied (Btu)	701.57	1001.99	600.85
	0.0	0.0	0.0
	3.333	2.0	3.667
	45.92	65.58	72.095
	0.0	0.0	0.0
	45.917	65.58	72.095
Liquid — Measured Heat Flux q'' (Btu/hr ft²) Ullage — Measured Heat Flux q'' (Btu/hr ft²)	395,894	603.703	387.535
	1,903	2.952	1.8
Tank - Stainless Wall - Measured Sensible Heat (Btu) Silicone Heaters - Measured Sensible Heat (Btu) Foam Insulation - Measured Sensible Heat (Btu) Freon 113 PCA - Measured Sensible Heat (Btu) Ullage - Measured Sensible Heat (Btu) Summation - Measured Absorbed Sensible Heat (Btu)	6.222	8.044	7.467
	4.464	5.977	5.523
	8.827	9.267	9.263
	25.911	39.512	46.5
	0.125	0.039	0.043
	45.549	62.839	68.796
Percent - Measured Absorbed Heat/Total Energy Supplied	99.19	95.82	95.42
Test No.	12 in. 1G	12 in. 1G	12 in, 1G
	No. 33	No. 30	No. 20
Liquid Level (percent) Heating Condition	50.0	87.5	87.5
	Liquid	Liquid	Liquid
Liquid Heater Electrical Source q'H (Btu/hr ft ²) Ullage Heater Electrical Source q'H (Btu/hr ft ²) Stratification Test Time (minute) Liquid Total Energy Supplied (Btu) Ullage Total Energy Supplied (Btu) Summation — Total Energy Supplied (Btu)	349.77	500.56	300.077
	0.0	0.0	0.0
	13.0	8.0	15.0
	357.123	524.188	589.2
	0.0	0.0	0.0
	357.123	524.188	589.2
Liquid — Measured Heat Flux q ¹¹ (Btu/hr ft ²)	208,707	362.662	205, 171
Ullage — Measured Heat Flux q ¹¹ (Btu/hr ft ²)	0,657	1.192	0, 74
Tank - Stainless Wall - Measured Sensible Heat (Btu) Silicone Heaters - Measured Sensible Heat (Btu) Foam Insulation - Measured Sensible Heat (Btu) Freon 113 PCA - Measured Sensible Heat (Btu) Ullage - Measured Sensible Heat (Btu) Summation - Measured Absorbed Sensible Heat (Btu)	41.338	64. 858	59.513
	14.729	23. 568	21.484
	66.745	73. 774	77.077
	213.093	314. 63	402.851
	0.671	0. 250	0.291
	336.576	477. 08	561.216
Percent - Measured Absorbed Heat/Total Energy Supplied	94, 24	91.01	95.25
		and the second s	

Table 3-1
NS - SUPPLIED HEAT FLUXES HEAT GAINS (Page 2 of 2)

2			and the second second					
6 in. 8G No. 5	6 in. 8G No. 16S	6 in. 8G No. 11S	6 in. 8G No. 6	6 in. 8G No. 8S	6 in. 1G No. 1	6 in. 1G No. 2		
87.5 Liquid	50.0 Liquid and	87.5 Liquid and	87.5 Liquid and	87.5 Liquid and	87.5 - Liquid and	87.5 Liquid and		
Diquid	Ullage	Ullage	Ullage	Ullage	Üllage	Üllage		
600.85	701.569	1001.99	600.85	600.85	600.85	600.85		
0.0	701.569	1001. 99	600.85	0.0	0.0	0.0		
3.667	2.333	2,0	3.8	3.667	3.7	3.7		
72.095	32. 142	65.58	74.718	72.095	72.752 0.0	72. 752 0. 0		
0.0	32.142	13.116	14.944	0.0 72.095	72.752	72, 752		
72.095	64.284	78.696	89. 662					
387,535	436.428	635.42	408.07	381,824	375.963	370.305	•	
1.8	10.662	10.178	9.723	1.517	1.356	1.594		
7,467	19,823	15.645	15, 91 2	6.978	8.4	8.488		
5,523	14. 182	9.535	9.607	5.167	6, 266	6, 233		
9, 263	12.896	11.26	11.375	9.031	9.633	9.758	•	
46.5	19.995	41.588	50.745	45.815	45.522	44,837		
0.043	0.488	0.133	0. 242	0.036	0.033	0.039	•	
68.796	67.384	78.161	87.881	67.027	69.854	69.355		
95.42	104.82	99.32	98.01	92. 97	96.01	95.33	•	<u> </u>
12 in. 1G	12 in. 1G	12 in. 1G	12 in. 1G	12 in. lG	12 in. 1G	18 in. 1G	18 in. 1G	
No. 20	No. 26	No. 34	No. 31	No. 23	No. 27	No. BS	No. IS	
87.5	87.5	50.0	87.5	87.5	87.5	50.0	87.5	
Liquid	Liquid	Liquid and	Liquid and	Liquid and	Liquid and	Liquid	Liquid	
		Ullage	Üllage	Ullage	Ullage			
300,077	45.012	349.772	500, 563	300,077	45.0116	753.151	965.0435	
0.0	0.0	350.35	500, 563	300. 424	45.0637	0.0	0.0	
15.0	99.0	9.0	8.0	15.0	99.0	9.0	9.0	
589.2	583.308	247.239	524. 188	589.2	583, 308	1197.835	2558, 06	
0.0	0.0	247.239	104, 838	117.976	116.797	0, 0	0, 0	
589.2	583.308	494.887	629.026	707. 176	700, 105	1197.835	2558.06	
205.171	30.664	237, 126	350.637	247.854	34. 946	400.823	578.124	
0.74	0.102	7.69	7, 732	5.459	0.472	1.723	2.73	
59.513	40.625	162.86	128.648	126.866	73.411	206.696	302.998	
21,484	14.514	57.597	38.45	37.778	22.89	49, 245	74. 144	
77.077	75.495	103.787	90.176	90.516	77.084	243.66	276. 177	
402,851	397.382	167.614	367. 186	486.661	452, 867	637, 481	1532.445	
0.291	0.264	5.436	1.619	2, 144	1.223	2.740	1.447	
561.216	528.28	497.294	626.079	743.965	627, 4 75	1139.822	2187, 211	
95.25	90.56	106, 48	99, 53	105.2	89.62	95.15	85.5	

Section 4 LIQUID AND ULLAGE (VAPOR) PROPERTIES

This section contains the test liquid (Freon 113 PCA) and ullage thermodynamic properties, and the characteristic temperature and pressures for each test investigated. Also shown, are the values for the three scaling parameters that were maintained constant for the scaling tests in this study. These parameters are the Modified Grashof number (Gr*), the Fourier number (Fo), and the Interface number (I). This information is shown in Table 4-1.

Notes:

r = 1 Normalized time at end of stratification test.

CHTMP Characteristic temperature, (qH D/k)

CHPRESS Characteristic pressure, (qH 0/D)

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Table 4-1
FREON 113 PCA LIQUID - ULLAGE PROPERT

Test No.		6 in. 8G #95	6 in. 8G #Z	6 in. 8G #1	6 in, 8G #14	6 in. 8
Characteris	stic Temperature (CHTMP) (*F)	8.861 + 03	1, 267 + 04	7.595 + 03	1. 140 + 03	8.867 + 0
Characteria	stic Pressure (CHPRESS) (lb(/in ²)	4.211 + 02	3, 609 + 02	3.96 + OZ	4.058 + 02	2.948 + 0
LIQUID:	density (lb/ft ³)	94. 431 - 93. 656	94. 382 - 93. 681	94. 387 - 93. 529	94. 335 - 93. 562	94. 394 -
	mass (lb)	12. 361 - 12. 259	21.621 - 21.46	21, 622 - 21, 425	21. 61 - 21, 433	12.356 -
	specific heat (Btu/lb °F)	0, 225 - 0, 227	0.225 - 0.227	0, 225 - 0, 227	0. 225 - 0. 227	0.225 - 0
	thermal conductivity (Btu/hr (t °F)	0.04 - 0.039	0.04 - 0.039	0.04 - 0.039	0.04 - 0.039	0.04 - 0.
	viscosity (lb/ft hr)	1,202 - 1,137	1. 198 - 1. 139	1, 198 - 1, 127	1. 194 - 1. 13	1.199 - 1
	kinematic viscosity (ft ² /hr)	0.012732 - 0.012139	0.01269 - 0.01216	0.012696 - 0.012049	0.01265 - 0.01207	0.0127 -
	Prandti No.	6. 834 - 6, 6116	6.819 - 6.6185	6. 82 - 6. 578	6. 805 - 6. 587	6,822 - 6
	Modified Grashof No. = $f(q_{H'}^{11}, \tau = 1.)$, Gr_{H}^{*}	1, 222 + 14	1, 342 + 15	8.217 + 14	1, 228 + 14	1.202 + 1
-	Modified Grashof No. = $f(q_{\ell}^{11}, \dot{\tau} = 1.), \bar{G}r_{\ell}^{*}$	6, 412 + 13	7.8 + 14	5. 32 + 14	6. 999 + 13	7, 193 + 1
٠	Interface No., I	0.03106	0.0218	0.0363	0. 242	0.03106
ULLAGE:	density (lb/ft3)	0.451 - 0.531	0.453 - 0.546	0.454 - 0.559	0.455 - 0.566	0.464 - (
	mass (lb)	0.059 - 0.07	0.015 - 0.018	0.015 - 0.018	0.015 - 0.019	0.061 - 0
	specific heat (Btu/lb °F)	0.158 - 0.16	0.158 - 0.16	0.158 - 0.16	0. 158 - 0. 16	0.159 - (
Test No.		6 in. 27G #3S	12 in. 1G #25	12 in. 1G #32	12 in. 1G #22	12 in.
Characteri	stic Temperature (CHTMP) (°F)	3,662 + 04	1. 267 + 04	8,861 + 03	7.6+03	1.14 + 03
Characteri	stic Pressure (CHPRESS) (lb _f /in, ²)	5. 195 + 02	3, 606 + 02	4.094 + 02	4.053 + 02	4.013 + (
LIQUID:	density (lb/ft ³)	94. 139 - 93. 009	94. 32 - 93, 53	93. 42 - 92. 39	94. 31 - 93. 34	94. 293 -
	mass (lb)	21, 565 - 21, 306	172. 85 - 171. 41	97. 83 - 96, 755	172. 83 - 171. 06	172.8 - 1
	specific heat (Btu/lb °F)	0, 226 - 0, 229	0.225 - 0.227	0.228 - 0.231	0. 225 - 0. 228	0.225 -
-	thermal conductivity (Btu/hr ft °F)	0.039	0.040 - 0.039	0.039 - 0.038	0.04 - 0.039	0.039
	viscosity (lb/ft hr)	1, 177 - 1, 088	1, 193 - 1, 127	1, 119 - 1, 044	1, 191 - 1, 113	1.19 - 1
	kinematic viscosity (ft ² /hr)	0.0125 - 0.01169	0.01264 - 0.01205	0.01197 - 0.0113	0.01263 - 0.01192	0.01262
	Prandtl No.	6. 746 - 6. 4478	6. 8 = 6. 579	6. 55 - 6. 308	6. 8 - 6. 53	6.792 -
	Modified Grashof No. = $f(q_H^{\prime\prime}, \tau = 1.)$, $Gr_H^{\prime\prime}$	1.431 + 16	1. 37 + 15	1.26 + 14	8. 422 + 14	1.251 +
•	Modified Grashof No. = $f(q_{*}^{ii}, \tau = 1.)$, Gr_{*}^{ii}	9, 324 + 15	8, 978 + 14	7, 431 + 13	6. 007 + 14	8. 186 +
	Interfacé No., I	0.00756	0.0218	0.03118	0.03633	02423
ULLAGE:	density (lb/ft ³)	0.451 - 0.594	0.459 - 0.546	0.451 - 0.516	0.455 - 0.559	0.458 -
	mass (lb)	0.015 = 0.019	0.12 - 0.143	0.472 - 0.541	0, 119 - 0, 146	0.12 - (
	specific heat (Btu/lb * F)	0. 158 - 0. 16	0.159 - 0.16	0.158 - 0.159	0, 158 - 0, 16	0.159 -
	specific heat (Btu/lb ° F)	0.158 - 0.16	0.159 - 0.16	0.158 - 0.159	0.158 - 0.16	0.1

EOLDOUT FRAME

Table 4-1
- ULLAGE PROPERTIES (Page 1 of 2)

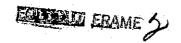
6 in. 8G #14	6 in. 8G #10S	6 in. 8G #3	6 in. 8G #4	6 in. 8G #13	6 in. 27G #1S
1, 140 + 03	8.867 + 03	1. 267 + 04	7, 598 + 03	1.14 + 03	2.838 + 04
4.058 + 02	2, 948 + 02	3, 609 + 02	4.058 + 02	4.058 + 02	4.028 + 02
94, 335 - 93, 562	94. 394 - 93. 775	94. 364 = 93. 618	94. 364 - 93. 491	93. 449 - 93. 66	94. 174 - 93. 241
21, 61 - 21, 433	12. 356 - 12. 275	21.616 - 21.445	21. 616 - 21. 416	21.407 - 21.455	12. 327 - 12. 205
0.225 - 0.227	0.225 - 0.227	0. 225 - 0. 227	0.225 - 0.228	0. 228 - 0. 227	0. 226 - 0. 228
0.01 - 0.039	0.04 - 0.039	G. 04 - 0. 039	0.04 - 0.039	0.039	0.039
1.194 - 1.13	1, 199 - 1, 147	1, 196 - 1, 134	1, 196 - 1, 124	1, 121 - 1, 137	1, 18 - 1, 105
0.01265 - 0.01207	0.0127 = 0.012226	0.012678 - 0.012112	0.012678 - 0.012022	0.01199 - 0.01214	0.01253 - 0.01185
6.805 - 6.587	6. 822 - 6. 644	6. 813 - 6. 60145	6, 813 - 6, 568	6, 557 - 6, 6126	6. 757 - 6. 504
1. 228 + 14	1,202 + 14	1. 354 + 15	8. 262 + 14	1. 247 + 14	1. 394 + 15
	7. 193 + 13	8, 385 + 14	5.319 + 14	8, 211 + 13	9. 531 + 14
	0.03106	0.0218	0. 0363	0. 242	0.00977
0.455 - 0.566	0.464 - 0.741	0.456 - 0.782	0.458 - 0.902	0.456 - 0.765	0.461 - 0.536
0.015 - 0.019	0.061 - 0.097	0.015 - 0.026	0.015 - 0.03	0.015 - 0.025	0.06 - 0.07
0. 158 - 0. 16	0.159 - 0.162	0.158 - 0.162	0. 159 - 0. 163	0. 158 - 0. 162	0.159 - 0.16
12 in. 1G #22	12 in. 1G #15	12 in. 1G #35	12 in. 1G #17	12 in. 1G #28	18 in. 1G #D
7, 6 + 03	1, 14 + 03	8, 851 + 03	1. 268 + 04	7. 597 + 03	2.859 + 04
4.053 + 02	4.013 + 02	2.835 + 02	3.606 + 02	4, 053 + 02	4.069 + 02
94. 31 - 93. 34	94, 293 - 93, 416	94. 34 - 93. 7	94, 29 - 93, 449	94. 306 - 93. 299	94. 326 - 93. 55
172, 83 - 171, 06	172.8 - 171.19	98. 79 - 98. 122	172, 795 - 171, 254	172. 825 - 170. 979	333, 377 - 330, 633
0.225 - 0.228	0,225 - 0,228	0.225 -0.227	0.225 - 0.228	0. 225 - 0. 228	0. 225 - 0. 227
0.04 - 0.039	0.039	0.04 - 0.039	0.039	0.039	0.040 - 0.039
1, 191 - 1, 113	1. 19 - 1. 118	1. 194 - 1. 14	1. 19 - 1. 121	1, 191 - 1, 109	1. 193 - 1. 129
0.01263 + 0.01192	0.01262 - 0.01197	0.01265 - 0.01217	0.01262 - 0.01199	0.01263 - 0.01189	0.01265 - 0.01206
6, 8 - 6, 53	6. 792 - 6. 549	6.8 - 6.623	6.79 - 6.557	6. 796 - 6. 519	6. 802 - 6. 584
8, 422 + 14	1, 251 + 14	1. 212 + 14	1.386 + 15	8. 473 + 14	1. 349 + 15
6.007 + 14	8, 186 + 13	7, 733 + 13	9.673 + 14	6. 305 + 13	7. 335 + 14
0.03633	0.2423	0.03118	0.0218	0. 03633	0.00966
t	1	0.453 - 0.827	0.480 - 0.828	0.458 - 1.037	0.445 - 0.513
0, 455 - 0, 559	0.458 - 0.549	37 . 37 = = 1			
0.455 - 0.559 0.119 - 0.146	0.458 - 0.549	0, 474 - 0. 866	0.126 - 0.217	0. 120 - 0. 272	1, 572 - 1, 814
	1. 140 + 03 4. 058 + 02 94. 335 - 93. 562 21. 61 - 21. 433 0. 225 - 0. 227 0. 04 - 0. 039 1. 194 - 1. 13 0. 01265 - 0. 01207 6. 805 - 6. 587 1. 228 + 14 6. 999 + 13 0. 242 0. 455 - 0. 566 0. 015 - 0. 019 0. 158 - 0. 16 12 in. 1G #22 7. 6 + 03 4. 053 + 02 94. 31 - 93. 34 172. 83 - 171. 06 0. 225 - 0. 228 0. 04 - 0. 039 1. 191 - 1. 113 0. 01263 + 0. 01192 6. 8 - 6. 53 8. 422 + 14	1, 140 + 03 4, 058 + 02 2, 948 + 02 2, 948 + 02 94, 335 - 93, 562 21, 61 - 21, 433 12, 356 - 12, 275 0, 225 - 0, 227 0, 04 - 0, 039 1, 194 - 1, 13 0, 01265 - 0, 01207 6, 805 - 6, 587 1, 228 + 14 6, 999 + 13 0, 242 0, 03106 0, 455 - 0, 566 0, 464 - 0, 741 0, 015 - 0, 019 0, 158 - 0, 16 12 in, 1G #22 12 in, 1G #15 7, 6 + 03 4, 053 + 02 94, 31 - 93, 34 172, 83 - 171, 06 0, 225 - 0, 228 0, 04 - 0, 039 1, 191 - 1, 113 0, 01263 - 0, 01192 6, 8 - 6, 53 6, 792 - 6, 549 8, 422 + 14 1, 294 + 93 1, 75 1, 14 + 03 4, 053 + 02 94, 31 - 93, 34 1, 191 - 1, 113 0, 01263 - 0, 01192 6, 8 - 6, 53 8, 422 + 14 1, 294 - 93, 775 1, 14 + 03 1, 14 + 03 1, 14 + 03 1, 14 + 03 1, 14 + 03 1, 14 + 03 1, 14 + 03 1, 14 + 03 1, 15 + 171, 19 1, 19 - 1, 118 1, 19 - 1, 118 1, 19 - 1, 118 1, 19 - 1, 118 1, 19 - 1, 118 1, 19 - 1, 118 1, 251 + 14	1, 140 + 03 4, 058 + 02 2, 948 + 02 3, 609 + 02 94, 335 - 93, 562 21, 61 - 21, 433 12, 356 - 12, 275 21, 616 - 21, 445 0, 225 - 0, 227 0, 04 - 0, 039 1, 194 - 1, 13 0, 01265 - 0, 01207 6, 805 - 6, 587 1, 228 + 14 1, 202 + 14 1, 354 + 15 0, 242 0, 03106 0, 455 - 0, 566 0, 464 - 0, 741 0, 0158 - 0, 16 0, 158 - 0, 16 12 in, 1G #22 12 in, 1G #15 12 in, 1G #22 12 in, 1G #15 172, 83 - 171, 06 172, 8 - 171, 19 0, 01265 - 0, 0219 0, 025 - 0, 228 0, 025 - 0, 228 0, 04 - 0, 039 1, 191 - 1, 113 1, 199 - 1, 147 1, 196 - 1, 134 0, 012678 - 0, 012112 6, 805 - 6, 587 6, 822 - 6, 644 6, 813 - 6, 60145 1, 354 + 15 8, 385 + 14 0, 0218 0, 456 - 0, 782 0, 015 - 0, 026 0, 158 - 0, 166 0, 158 - 0, 162 12 in, 1G #22 12 in, 1G #15 12 in, 1G #35 1, 14 + 03 4, 053 + 02 94, 31 - 93, 34 172, 83 - 171, 06 172, 8 - 171, 19 98, 79 - 98, 122 0, 225 - 0, 228 0, 04 - 0, 039 1, 191 - 1, 113 1, 19 - 1, 118 0, 01263 - 0, 01192 6, 8 - 6, 53 6, 792 - 6, 549 1, 212 + 14 6, 007 + 14 8, 186 + 13 7, 733 + 13	1, 140 + 03 4, 058 + 02 2, 948 + 02 3, 609 + 02 4, 058 + 02 94, 335 - 93, 562 94, 394 - 93, 775 94, 364 - 93, 618 94, 364 - 93, 491 21, 61 - 21, 433 0, 225 - 0, 227 0, 225 - 0, 227 0, 04 - 0, 039 1, 194 - 1, 13 1, 199 - 1, 147 1, 196 - 1, 134 1, 196 - 1, 134 0, 01265 - 0, 01207 6, 805 - 6, 587 1, 228 + 14 1, 202 + 14 1, 354 + 15 1, 202 + 14 1, 354 + 15 1, 204 + 14 1, 204 + 14 1, 204 + 14 1, 204 + 10 1, 205 + 10 1, 106 + 10 1, 107 1	1.140 + 03 1.161 + 03 1.058 + 02 2.948 + 02 3.609 + 02 4.058 + 02 4.058 + 02 4.058 + 02 3.609 + 02 4.058 + 02

Table 4-1
FREON 113 PCA LIQUID - ULLAGE PROPER

					•	
Test No.		6 in. 8G #15S	6 in. 8G # 12S	6 in. 8G #5	6 in. 8G #16S	6 in, 80
Characteri	stic Temperature (CHTMP) (°F)	8,88 + 03	1.269 + 04	7,592 + 03	8.86B + 03	1.2654 + 0
Characteri	stic Pressure (CHPRESS) (lbf/in ²)	4.212 + 02	3.609 + 02	3.968 + 02	2.948 + 02	3.609 + 02
LIQUID:	density (lb/ft ³)	94, 314 - 93, 48	94. 282 - 93. 556	94.411 - 93.556	94. 392 + 93. 749	94.457 - 9
	mass (15)	12. 346 - 12. 237	21. 598 - 21. 431	21. 627 - 21. 431	12, 356 - 12, 272	21.638 - 2
	specific heat (Btu/lb °F)	0.225 - 0.228	0.225 - 0.227	0.225 - 0.227	225 - 0. 227	0.225 - 0.
	thermal conductivity (Btu/hr ft °F)	0.04 - 0.039	0.039	0.04 - 0.039	(.04 = 0.039	0.04 - 0.0
	viscosity (lb/ft hr)	1, 192 - 1, 123	1. 189 - 1. 129	1.201 - 1.129	1.199 - 1.144	1, 205 - 1
	kinematic viscosity (ft ² /hr)	0.01264 - 0.01201	0,012613 - 0,012068	0.012716 - 0.012068	0.127 - 0.01221	0.01275 -
	Prandtl No.	6.798 - 6.565	679 + 6, 585	6, 827 - 6, 585	6. 823 - 6. 636	6, 84 - 6,
	Modified Grashof No. = $f(q_{H^*}^{ii}, \tau = 1.), Gr_{H}^{\pm}$	1.253 + 14	1, 367 + 15	8. 185 + 14	1.207 - 14	1,339 + 1
	Modified Grashof No. = $f(q_{ij}^n, \tau = 1.), Gr_{ij}^*$	7,069 + 13	8. 235 + 14	5. 279 + 14	7. 506 + 13	8.493 + 1
	Interface No., I	0.03106	0.0218	0,0363	0.03106	0.0218
ULLAGE:	density (lb/ft ³)	0.46 - 0.547	0.458 - 0.564	0.451 - 0.568	0.456 - 0.745	0.456 - 0
	mass (lb)	0.06 - 0.072	0.015 - 0.018	0.015 - 0.019	0.06 - 0.098	0.015 - 0
	specific heat (Btu/lb *F)	0.159 - 0.16	0. 159 - 0. 16	0.158 - 0.16	0. 158 - 0. 162	0.158 - 0
Test No.		12 in. 1G #33	12 in. 1G #30	12 in. 1G #20	12 in. 1G #26	12 in.
Characteri	stic Temperature (CHTMP) (*F)	8.859 + 03	1, 267 + 04	7.599 + 03	1.14 + 03	8, 858 + (
Characteri	stic Pressure (CHPRESS) (lb _f /in, ²)	4.094 + 02	3.606 + 02	4,053 + 02	4.013 + 02	2,835 +
LIQUID:	density (lb/ft ³)	94. 282 - 93, 426	94. 309 - 93. 517	94, 21 - 93, 364	94. 295 - 93. 382	94. 287 -
	mass (lb)	98. 732 - 97. 835	172, 83 - 171, 378	172, 795 - 171, 099	172, 805 - 171, 132	98. 738 -
	specific heat (Btu/lb °F)	0.225 - 0.228	0.225 - 0.227	0.225 - 0.228	0. 225 - 0. 228	0.225 -
	thermal conductivity (Btu/hr ft *F)	0.039	0.040 - 0.039	0.039	0.039	0.039
-	viscosity (lb/ft hr)	1. 189 - 1. 119	1, 191 - 1, 126	1. 19 - 1. 114	1, 19 - 1, 115	1.19 - 1
	kinematic viscosity (ft ² /hr)	0.01261 - 0.01254	0.01263 - 0.01204	0.01262 - 0.01193	0.01262 - 0.01194	0.01262
	Prandtl No.	6, 789 - 6, 551	6. 797 - 6, 575	6, 791 - 6, 535	6. 793 - 6. 54	6.79 - 6
	Modified Grashof No. = $f(q_{H^*}^{H}, \tau = 1.)$, Gr_{H}^{\pm}	1.259 + 14	1. 373 + 15	8.401 + 14	1. 257 + 14	1. 227 +
	Modified Grashof No. = $f(q_{\ell}^{ij}, \tau = 1,), Gr_{\ell}^{\pm}$	7.511 + 13	9.024 + 14	5.744 + 14	8, 563 + 13	8.319 +
	Interface No., I	0.03118	0.0218	0.03633	0. 2423	0.03118
ULLAGE:	density (lb/ft ³)	0.46 - 0.520	0.46 - 0.547	0.454 - 0.554	0.454 - 0.545	0.463 -
	mass (lb)	0.481 - 0.544	0. 121 - 0. 143	0.119 - 0.145	0.119 - 0.143	0.485 -
	specific heat (Btu/lb *F)	0.159	0.159 - 0.160	0.158 - 0.16	0. 158 - 0, 16	0.159 -
	and the same of th	<u> </u>	<u> </u>		<u> </u>	

Table 4-1
- ULLAGE PROPERTIES (Page 2 of 2)

6 in. 8G #16S	6 in, 8G #11S	6 in. 8G #6	6 in. 8G #8S	6 in, 1G #1	6 in. 1G #2	i
3: 868 + 03	1.2654 + 04	7. 603 + 03	7. 581 + 03	7. 596 + 03	7, 605 + 03	
, 948 + 02	3, 609 + 02	4. 112 + 02	3.968 + 02	4. 004 + 02	4.004 + 02	
4. 392 - 93, 749	94. 457 - 93. 692	94. 327 - 93. 394	94. 493 - 93. 651	94, 38 - 93, 544	94. 315 - 93, 491	
2, 356 - 12, 272	21, 638 - 21, 463	21, 608 - 21, 394	21. 646 - 21. 453	21. 62 - 21. 428	21.6 - 21.415	
. 225 - 0. 227	0.225 - 0.227	0.225 - 0.228	0.225 - 0.227	0. 225 - 0. 227	0, 225 - 0, 228	
.04 - 0,039	0.04 - 0.039	0.04 - 0.039	0.04 - 0.039	0.04 - 0.039	0.04 - 0.039	
199 - 1, 144	1. 205 - 1. 14	1. 193 - 1. 116	1.208 - 1.137	1, 198 - 1, 128	1, 192 - 1, 124	
0127 - 0.01221	0.01275 - 0.012166	0.01265 - 0.01195	0.01278 - 0.01214	0.01269 - 0.01206	0.01264 - 0.01202	
822 - 6.636	6.84 - 6.621	6. 802 - 6. 543	6. 852 - 6. 61	6. 818 - 6, 582	6.799 - 6.568	
207 + 14	1, 339 + 15	8. 373 + 14	8.073 + 14	1. 025 + 14	1.033 + 14	
506 + 13	8.497 + 14	5. 687 + 14	5. 13 + 14	6. 415 + 13	6. 36B + 13	
03106	0.0218	0.0363	0.0363	0.0363	0.0363	
456 - 0.745	0.456 - 0.767	0.458 - 0.764	0.453 - 0.554	0.449 - 0.54	0.455 - 0.561	
06 - 0.098	0.015 - 0.025	0.015 - 0.032	0.015 - 0.018	0.015 - 0.018	0.015 - 0.018	
158 - 0. 162	0.158 - 0.162	0, 159 - 0, 164	0.158 - 0.46	0. 158 - 0. 16	0. 158 - 0. 16	
12 in. 1G #26	12 in. 1G #34	12 in. 1G #31	12 in. 1G #23	12 in. 1G #27	18 in. 1G #BS	18 in. 1G #IS
14 + 03	8.858 + 03	1.267 + 04	7. 594 + 03	1. 14 + 03	2.863 + 04	3. 668 + 04
013 + 02	2.835 + 02	3. 606 + 02	4.053 + 02	4.013 + 02	4. 069 + 02	5. 214 + 02
295 - 93, 382	94. 287 - 93, 613	93.462 - 92.58	94. 333 - 93. 215	94. 276 - 93. 236	94. 253 - 93. 493	94. 261 - 93. 218
2, 805 - 171, 132	98. 738 - 98. 03Z	171. 278 - 169. 662	172. 874 - 170-826	172. 769 - 170, 863	333, 117 - 330, 432	583, 006 - 576, 556
22 5 - 0.228	0.225 - 0.227	0.228 - 0.23	0. 225 - 0. 228	C. 225 - 0. 228	0. 225 - 0. 228	0.225 - 0.228
)39	0.039	0.039 - 0.038	0.04 - 0.039	0.039	0.039	0.039
9 - 1.115	1. 19 - 1. 134	1, 122 - 1, 057	1. 194 - 1. 103	1. 189 - 1. 104	1. 187 - 1. 124	1. 187 - 1. 103
1262 - 0.01194	0.01262 - 0.012109	0.012 - 0.01142	0.01265 - 0.01183	0.01261 - 0.01184	0.01259 - 0.01202	0.0126 - 0.01183
93 - 6.54	6.79 - 6.6	6. 561 - 6. 349	6. 804 - 6. 498	6. 787 - 6, 503	6. 78 - 6. 569	6. 782 - 6. 498
57 + 14	1.227 + 14	1. 383 + 15	8. 565 + 14	1. 282 + 14	1, 36 + 15	1, 395 + 16
63 + 13	8.319 + 13	9. 686 + 14	7.075 + 13	9. 954 + 13	7. 238 + 14	8. 357 + 15
423	0.03118	0.0218	0.03633	0. 2423	0.00966	0.00754
54 - 0. 545	0.463 - 0.844	0.462 - 0.9	0.458 - 1.007	0. 463 - 0. 812	0.46 - 0.531	0.465 - 0.607
19 - 0. 143	0.485 - 0.884	0. 121 - 0. 236	0. 12 - 0. 264	0. 121 = 0, 213	1, 624 - 1, 878	0, 411 - 0, 536
58 - 0.16	0.159 - 0.163	0.159 - 0.163	0.159 - 0.164	0. 159 - 0. 163	0. 159 - 0. 16	0. 159 - 0. 16
2.1				and the second second		1



Section 5

EXPERIMENTAL TEMPERATURE, PRESSURE, AND COMPILED MODIFIED GRASHOF AND FOURIER NUMBERS DATA

This section is composed of the measured temperature and pressure data obtained during this program. The data are presented in sets corresponding to scaling tests in Sections 5.1 through 5.10. Scaled tests are represented by those tests listed in the same row of the test matrix (see Table 2-1). This represents tests where the dimensionless parameters, the Modified Grashof number Gr_H^* , the Fourier number Fo, and the liquid-vapor Interface number I defined in Volume I of this report, are held constant during each test. Three experimental variables were used to control the values of these dimensionless scaling parameters. These variables are the input heat flux $q_H^{''}$, the stratification test time θ , and the applied gravitational constant g. The test data in Section 5.11 do not represent scaling tests, but tests with constant wallheat flux $q_H^{''}$. These two tests, 6-in.-dia. tank test lg # l and # l2, have the same heat flux as the 6-in.-dia. tank test lg # l of Section 5.5.

The data from each set of scaling tests include:

- (1) Structural geometric tank weights wattmeter heat flux inputs.
- (2) Stratification temperature (°F) data for each thermocouple and at each recorded time slice.
- (3) Family of stratification temperature profile curves.
- (4) Family of stratification del-temp profile curves.
- (5) Family of stratification DT Norm (normalized del-temp) profile curves.
- (6) Bulk ullage and liquid temperature histories.
- (7) Tank pressure history.
- (8) Liquid Modified-Grashof number histories stratification.
- (9) Liquid Fourier number history.

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During the test program, the heaters #1 and #2, #3 and #4, #5 and #6, #7 and #8, and #9 and #10 (i.e., Figure 2-1) were connected in parallel. Under item (1) above, the supplied heater heat-flux values to the respective parallel heaters are identified as H12, H34, H56, H78, and H910 in Tables 5.1-1a through 5.11-1b.

Section 5.1 SCALING SET

6-in Dia Tank Tests	12-in Dia Tank Tests
8G	1G
Test #2	Test #30
Test #12S	Test #25

Table 5. 1-1a. 6 IN. DIA TANK TEST 8G#2 (Page 1 of 2) STRUCTURAL GEOMETRIC TANK LTS-WATTMETER HEAT FLUX INPUTS

THE KALL VOL 1 138	927 CYL AREA FT2= ,00131 1/2 CYL WALL	1,5708 VOLFT3= ,0	FLNGE ARE	A FT2= FLNGE VOI MASS=	,0365 F13= ,39058	.00076
I IG VOL FT3# ,229	OG7 ULLAGE VOL FT3=	.03272				
SUBINT HEAT FLUXES ((BTU/HR-FT2), AND ABSORBE	D HEAT AND TH	EMPERATURI	EESTIMAT	es 	
	=1001,9935 H56=1001,99	35 H910=10	01,9935	H/58 U	-4000	
EST HT FLUX IN LLGS	(BTU/HR-FT2)=1001.9935 E (BTU/HR-FT2)= 0.0000 FAT)&TU= 05.580 (S (STHAT)= 13.4616F	STRAT+DESTRAT (STRAT+DESTR)BTU= 12 AT)= 24	0:012 .6168F		
EST.HT INPUT ULLAGE			RAT)BTUS	0.000		
DOME AREA FT2=	Table 5.1-16. 6114. L-GEOMETRIC TANK WTS-WAT 3927	1.5708 VOLFT3= . 4= .81996	FLNGE AR	EA FT2=	.0365 L FT3= .38058	.00076
LIG VOL FT3= .22	1907 ULLAGE VOL FT3:	= ,03272	EMBERATUS	F FSTIMA	ES	
H12=1001.9935 H34	(BTU/HR-FT2)+AND ABSORB	935 H910=10	01.9935	H78= (0.0000	•
	The second section of the second seco					
EST. HT FLUX IN ULLG EST. HT INPUT LIG(ST EST. LIG TEMP INCRSE	(BTU/HR-FT2)=1001.9935 GE (BTU/HR-FT2)= 0.000 TRAT)BTU= 65.580 (E(STRAT)= 13.4594F	(STRAT+DEST				
EST. HT FLUX IN ULLG EST. HT INPUT LIG(ST EST. LIG TEMP INCRSE	E (BIONAKELIE)	(STRAT+DEST				

Table 5. 1-1c. 12 IN. DIA TANK TEST 1G#30 (Page 2 of 2) STRUCTURAL GEOMETRIC TANK WTS-WATTMETER HEAT FLUX INPUTS

DOME AREA FT2= 1,5708 DME WALL VOL FT3# .01047 DME MASS LBMe 5,24772	CYL AREA FT2# 1/2 CYL WALL Mass 1/2 Cyl Lum	VALETT-	44 744	EA FT2# .1458 FLNGE VOL FT3# Mass# 3.04465	.00606
LIQ VOL FT3# 1,83260	ULLAGE VOL FT3=	,26180			
INPUT HEAT FLUXES (BTU/HR-	FT2).AND ABSORDE	D HEAT AND	TEMPERATURE	ESTIMATES	· · · · · · · · · · · · · · · · · · ·
412= 500,5626 H34= 500,56					- ·
EST.HT FLUX IN LIG (STU/HR- EST.HT-FLUX IN ULIGE (STU/HR-	FT2)= 500.5626				į.
ST. HT INPUT LIG(STRAT)BTU= ST. LIG TEMP INCRSE(STRAT)=	524.188 (S	TUATABESTUA	T)BTU= 1179 RAT)= 30.	423 2103F	1, 1,
EST. HT INPUT ULLAGE (STRAT) 9	Tu= 0,000	(STRAT+DES	TRATIBIU=	0.000	
STRUCTURAL GEOMET		TMETER-HEAT	'-FLUX <mark>'-</mark> INP	•	
STRUCTURAL GEOMET DOME AREA F72= 1.5708 DME WALL VOL F73= .01047 DME MASS LBM= 5.24772	CYL AREA F72=	TMETER-HEAT	FLNGE ARE	• FT2=1458- FLNGE VOL FT3=	•0060
DOME AREA FT2= 1.5708 DHE WALL VOL FT3= .01047 DHE MASS LBM= 5.24772	CYL AREA FT2= 1/2 CYL WALL MASS 1/2 CYL LBM	TMETER HEAT	FLNGE ARE	• EA-FT2=1458	.00608
DOME-AREA-FT2=- 1.5708 DME WALL VOL FT3= .01047 DME MASS LBM= 5.24772 LIQ VOL FT3= 1.83260	CYL AREA FT2= 1/2 CYL WALL MASS 1/2 CYL LBM ULLAGE VOL FT3=	TMETER—HEAT	FLNGE ARE •01309 FLANGE	FT2= .1458- FLNGE VOL FT3= MASS= 3.04465	.0060
DOME AREA FT2= 1.5708 DME WALL VOL FT3= .01047 DME MASS LBM= 5.24772	CYL AREA FT2= 1/2 CYL WALL MASS 1/2 CYL LBM ULLAGE VOL FT3= FT2) AND ABSORBE	TMETER-HEAT -6.2832 VOLFT3= - 6.55965 -26180 D-HEAT-AND-	FLNGE ARE • 01309 FLANGE TEMPERATURE	FT2= .1458- FLNGE VOL FT3= MASS= 3.04465	.00601

	OF WORK HOLD SOLD SELECTION	<u> </u>			
1105(*1	3 3.000 .33	,650	1.000 1,330	1.660 2.000	
TAT:	* * * * * * * * * * * * * * * * * * *	. 110	11: • 607	17,011 11.00	•
	4 4 4 4 4 4 4 7 7 7 7	4 2 3 7 4 2 7 4 2 "	A TIME A PARTIE	A STATE OF THE PARTY OF THE PAR	
5	446 317 434 467	43n 792 434	.75P 437.91/	14111245 1411512	
3	447 A07 433 766	420 424 112	. A67 139./UG	1001000 1711010	
4	1.7 717 177 160	420 202 4.55	. 4/4 4.55.41/	130.000/ 17:11/20	
1 . 5	446 475 171 775	126 833 130	. 542 934. 1100	107,477 20/1746	
	446 718 414 647	426 244 450	1.490 9.500	1001046 100111	
	7 224 424 125	4 27 5 2 3 4 4 4 4	1.049 437.224	100000000000000000000000000000000000000	
ė –	75A 459 777	407 750 400	0000 130.000	10/1/72 1041 00	
9	111 202 116 706	118 698 12	797 121 . 22	TEGS TE STATE	
10	446 075 490 909	130 700 130	137.70	4/10/2 144124	
1.1	117,000 128,750	133,909 137	1,299 140,296	143,333 145,458	
12	117,333 120,417	135,208 137	7,958 140,000	142,333 144,625	/_/
1.3	115,500 127,775	132,667 134	1,005 135,000	137,503 130,083	-
14	116,125 118,792	122,042 14	762 437 167	130,542 133,125	
15	116,292 127,208	127,200 101	000 434 042	135,167 137,917 136,125 133,292	
_10	116,459 127,708	124 450 42	54C 420 583	131,700 133,792	
17	115,10/ 120,000	125 007 420	706 428 5h3	130,768 132,453	
_15	115,500 125,542	1224100 120	775 424 563	123,20 124,792	
¥19	114,999 116,983	4 40 703 43	\$ 206 430.500	142,375 144,953	
50	116,475 124,704	137 055 43	7 202 141.292	143,333 145,458	
21	117,000 12",/20	135,995 15	7 958 140 000	142,333 144,625	
55	1,17,333 127,317	132 467 13	4.058 135.083	137,583 139,083	
23	445 060 444 736	118 425 12	1. 998 123. DUU	1600010 160000	
24	445 997 446 777	117 737 11	3 467 110 91/	141-106-16-100	
25	411 167 115 667	114.575 11	A. DLO 11' . C/?	181,004c Terrien.	
26	405 750 400 975	115 167 11	6.333 110.000	TT / 8 TO / TT / 8 TE >	
27	144 017 114 77	117 642 11	7 837 118,583	_114,43516,130-	
_28 29	445 750 415 837	1 114 500 11	7.502 118.500	114 017 781 447	
30	4 15 017 114 625	118 425 12	1.042 123.400	185 1000 18 1000	
_31	444 700 408 061	1 120 425 45	0 0 0 1 1 1 1 1 1	13x4001 Prost	
32	444 703 435 350	1 129 425 13	0.958 131.0/2	195 001 1931701	
33	111 000 111 60	1 110 167 12	0.453 121.430	123.000 163.017	
_34	111,917, 112,58	113,959 11	5,333 114,417	117,739 115,667	

Table 5.1-2b. 6 IN. DIA TANK TEST 8G #12S (Page 1 of 2)
TEMPERATURE HATRIX-STRATIFICATION

4	•				
TIME (MIN)	0.000	.333	1.000	1.667	2.000
	0.000		500		1.000
		1217042-17			
		124.708 1			
		123.792 1.			
		124.333-1			
		122.833 13			
		123.208 1			~ · · ·
		123-500-1			
		123.792 11		-	
		119.125 1			· · ·
		129.458-13			
		130.042 1			
		130 667 13			
		128.917 13			
		20.000 12			
		123.417 13			
		123 -917-1 3			
- -		122.813 12			· = · • · · ·
		21.708 12			33.208
•		-17.792-12			
		29,458 13			
= ,		130.042 13 130.667—13			
		28.917 13			
		18.250 12			
		17-875-12			
		17.542 22			46.458
· _ ·		17.875 12			29.208
		18-000-12			-
		17.125 12			
		18.208 12			26.583
= -		27.931 13			
		28.792 13			
		18.375 12			
		Fadern TE		CADREN 1	674720

_				104	0.000
and the second	THE (MIN)	្រុបក្រក្	2.000 4.		8,00 0
TA			50 500		ាម្រា • ១០០
				667 131,042 15	
	1.1	L7-241-1-24	4 10 4 1 2 1 4 2	202 133,720 13	1 603
•	1)	17,342 12/	1000 101,3	500 134,542 13	7,203
	11	17,203 127	042 130.2	250 133,292 13	7,717
				183 133,95n 13	
				503 131,375 13	
77	/ 11			000 130,542 13	
V (292 130,792 13	
					9,542
1				750 147 783 14	
1				250-142-375 14	
_ 1					1,792
1		17,542 134			1.875
1				183 130 625 13	
1					, 958
1 (208 137,500 134	
1				792-136-708-13	
1				383 134,500 130	
1				158 126,292 12	
2	1	1 7.792 -135	, 375-148-6	567 <u>142,209 14</u>	5,125
2				250 141,542 14	
2				792 139,708 14	
2				333_138_750 14	
, 2	4 11	16,583 119	,000 122,1	167 125 375 12	A , 333
2	5 11	16,375 118	,333 120,7	750 123,375 12	5,792
-2	5 <u> </u>	16,208 11F	,201-120,5	5 87-127-125-12 1	5,500
2	7 11	16,292 118	,292 120,5	300 122,875 12º	5,125
2	9 11	17,458 118	.na3 119.6	667 121,750 12	3,917
2				100-122,417-12	
3	D 11	16,708 118	,917 122,n	183 125,292 12	A,250
3:	1 11	18,292 133	708 136,2	292 138 542 14	0.917
3	2	18,042 132	1467 134,2	209-134,542-13 1	9.000
3.				709 124,583 126	
3	4 11	15,500 115	,208 115,4	158 115 875 11	6,333
3		15.292 114	500-114-0	100-113-792-11	3.458
				and the second s	

Table 5.1-2d. 12 IN. DIA TANK TEST 1G #25 (Page 1 of 2)

TEMPERATURE MATRIX-STRATIFICATION

				•	
TIME (MIN)	0.000	2.000	4.000	6.000	8.000
TAU	0.000	.250	-500	.750 1.	000
1	116.958	123.583	127.542 1	30.625 13	3.542
2				33.292-13	
3	• • • • • • • • • • • • • • • • • • • •			34.542 13	=
4				33.375 13	
5				34.042 13	
6		-		31.333 13	
7				30.542 13	
8				30-292-13	
9				26.958 12	
10				41.958 14	
11				41.125 14	
15				38.875 14	
				39,583 14	
14				30-125-13	
15				38.667 14	
16				37.250 14	
17				36.625 13 34.167 13	
18				25.875 12	
19				41.583 14	
20				41.292 14	
55				39.417 14	
52				38.792-14	
24				25,167 12	
25				23.125 12	
				23.083 12	
27				22.833 12	
28			- , -, -	21.583 12	
	117.083	117.750	119.792-1	22.250 12	4.917
30				25.042 12	
31				38,167 14	
32	**			36-167-13	
33				24.292 12	
34	114.958	114.833	115.250 1	15.708 11	6.250

117.983 117.625 119.042 121.083 123.333

105,333 105,292 105,708 106,500 107,417

-95-000--94-875--94-833--94-958--95-125

89.417 89.375 89.250 89.292 89.167

100.500-100.333-100.333-100.500-100.792----

Table 5.1-2d. 12 IN. DIA TANK TEST 1G #25 (Page 2 of 2)

36

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-74

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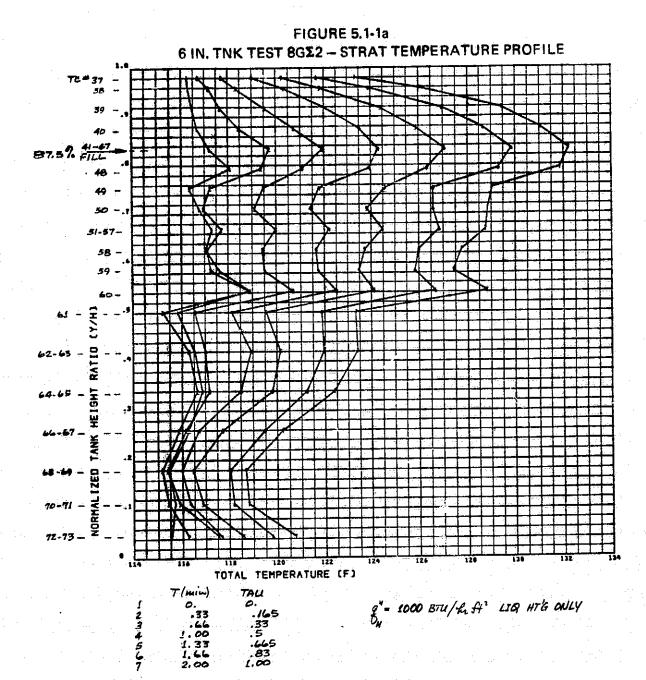
76

114.875 114.167 113.667 113.292 112.958 118.375 133.875 136.125 138.292 140.583

117.458 118.375 120.833 123.625 126.333

117.458 118.708 121.667 124.667 127.583

117.125 119.208 122.500 125.542 128.583



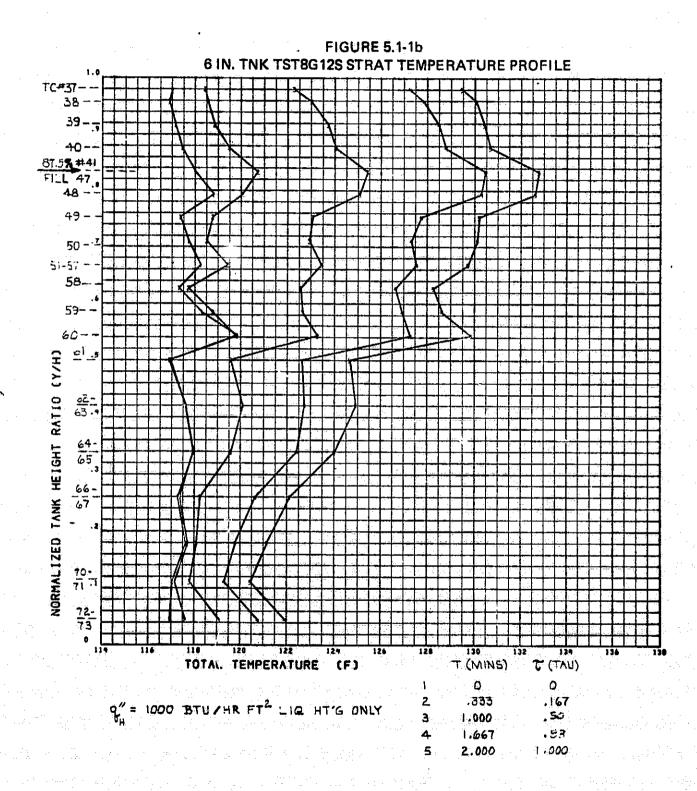
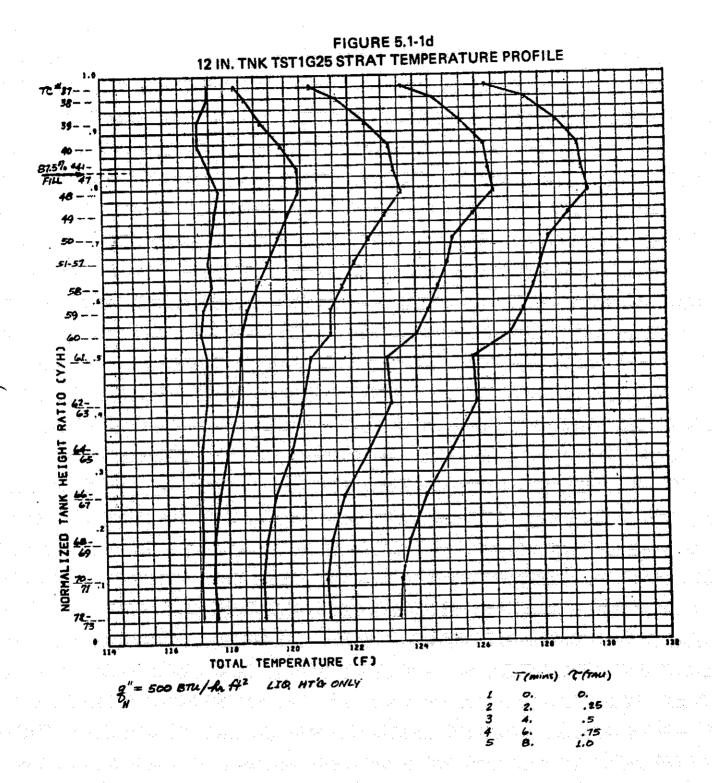
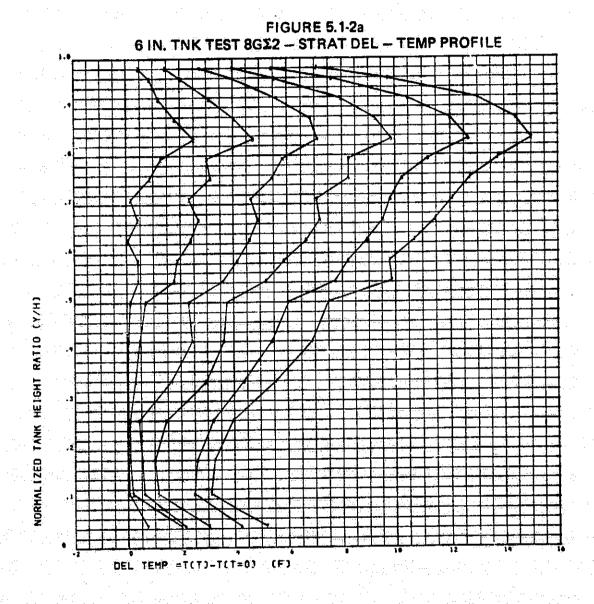


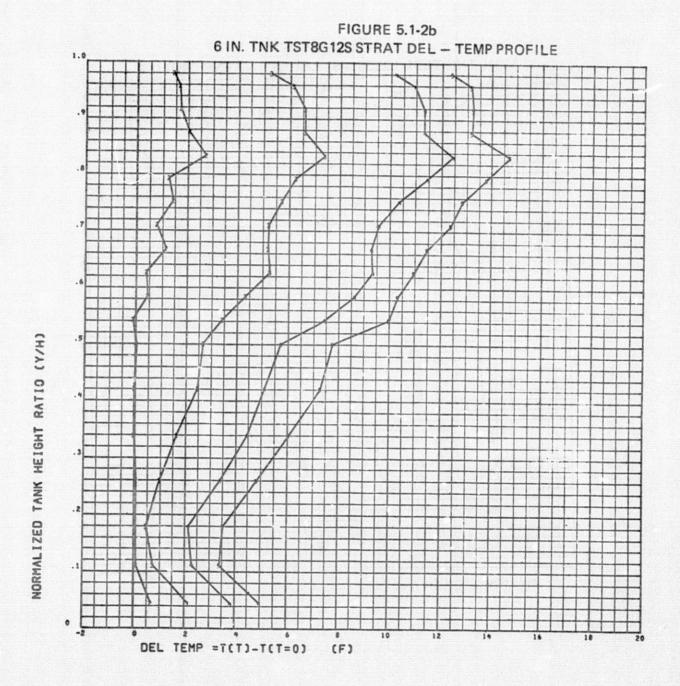
FIGURE 5.1-1c

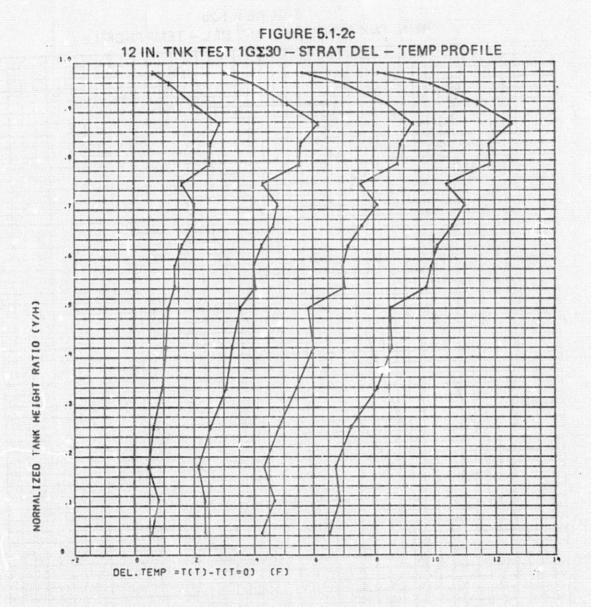
	2 02 me rele entre	(mint)	THAN	
8 =	= 500 BTU / th f+2 LIQ HT'S ONLY	c.	0.	
	2	. Z	,	
		4.	.5	
. Si		8.	1.0	

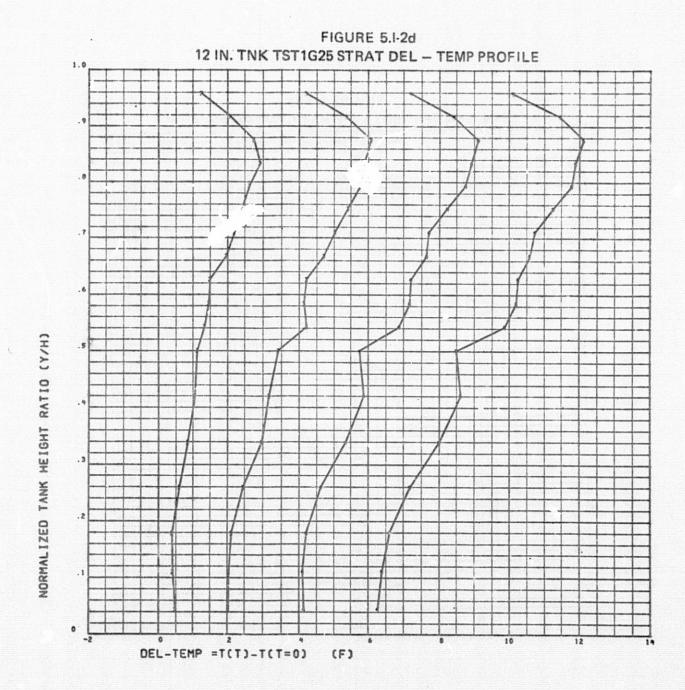
TOTAL TEMPERATURE (F)

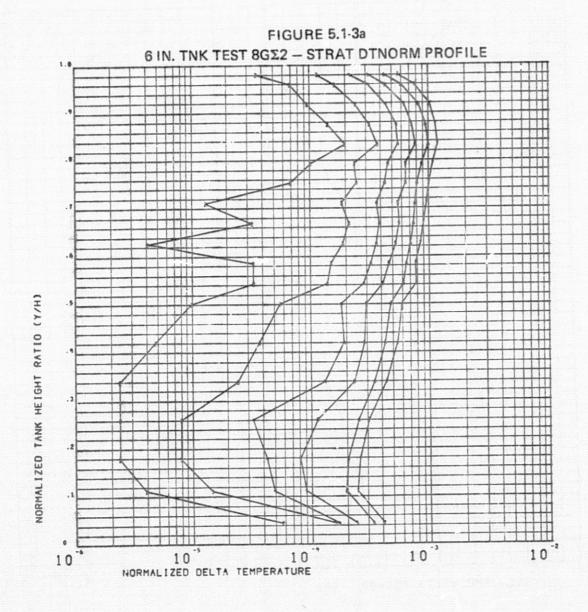


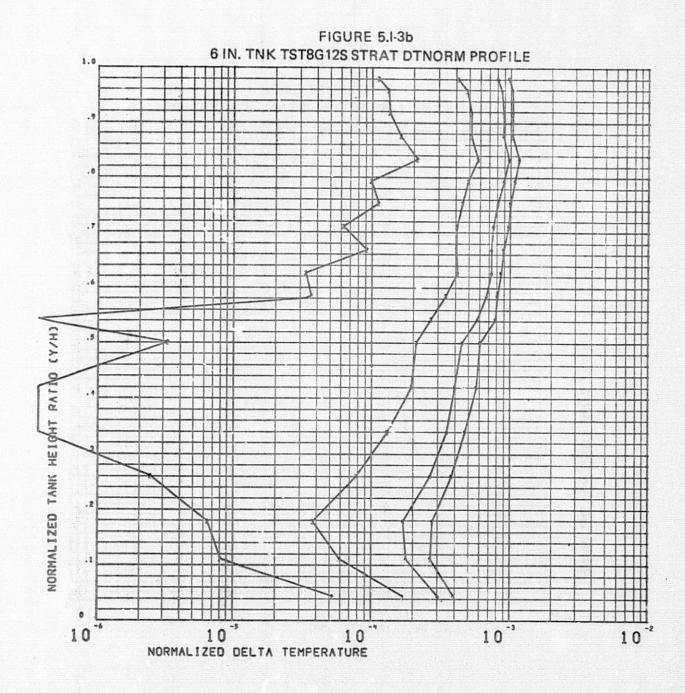


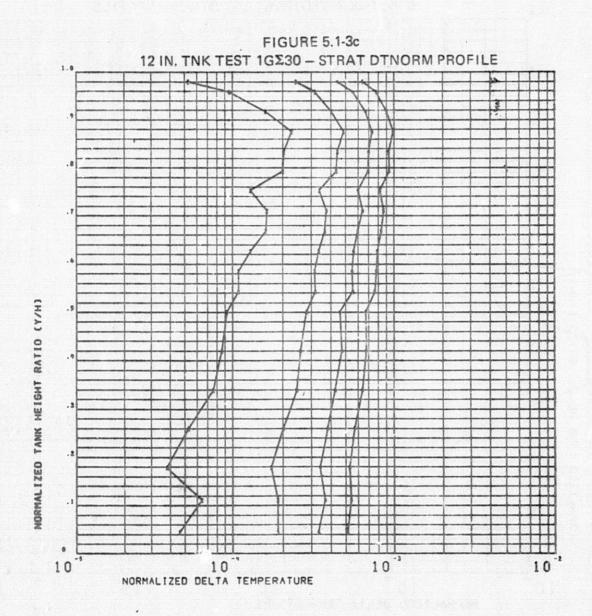


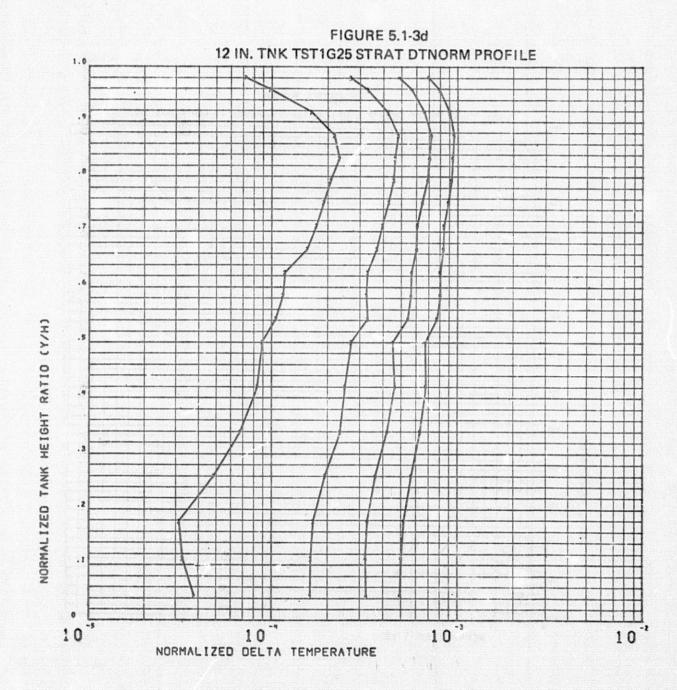












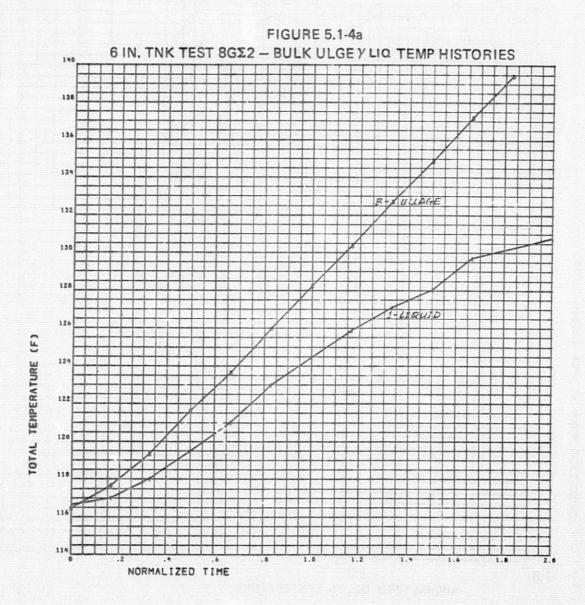


FIGURE 5.1-4b 6 IN. TNK TST8G12S BULK ULGE YLIQ TEMP HISTORIES 130 TOTAL TEMPERATURE NORMALIZED TIME

43

B - ULLAGE

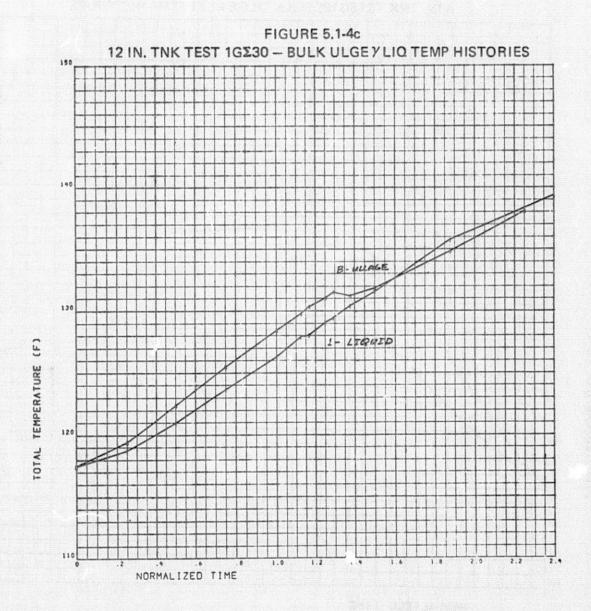
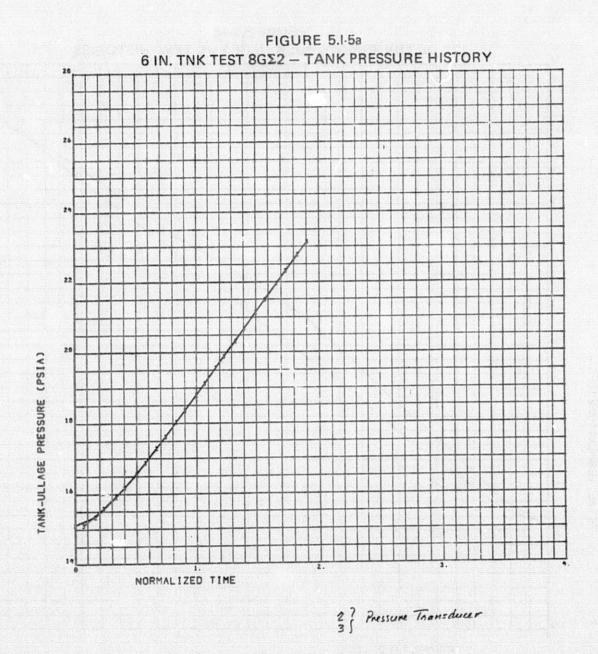
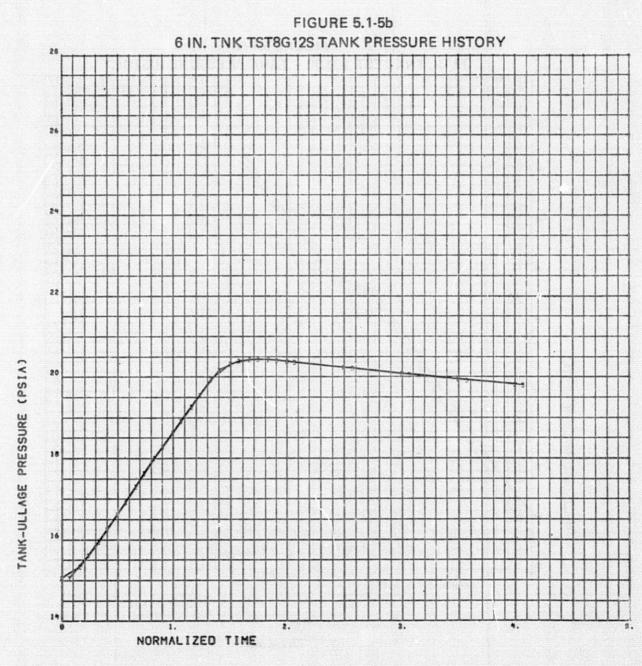


FIGURE 5.1-4d 12 IN. TNK TST1G25 BULK ULGEY LIQ TEMP HISTORIES 140 TOTAL TEMPERATURE (F) 120 NORMALIZED TIME

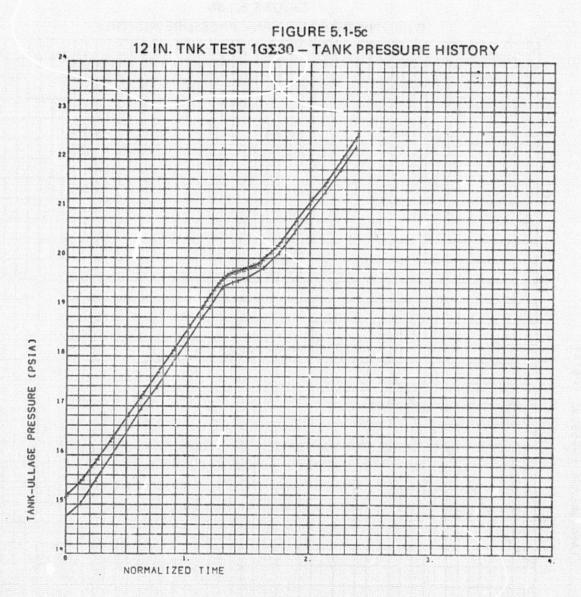
45

B - ULLAGE 1 - LIQUID





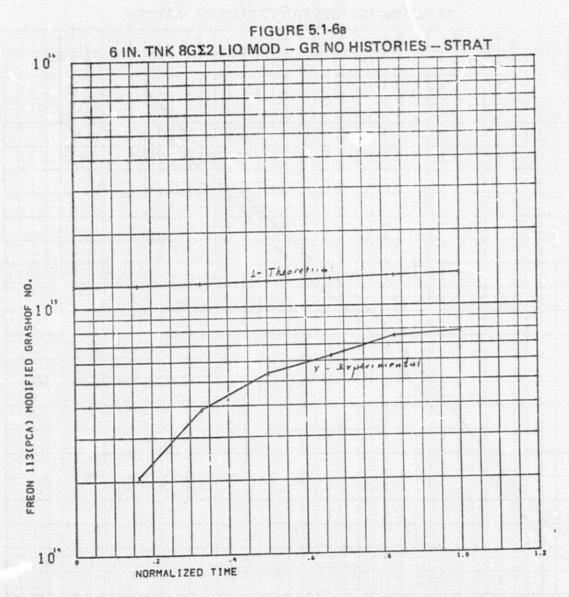
2 PRESSURE TRANSDUCER

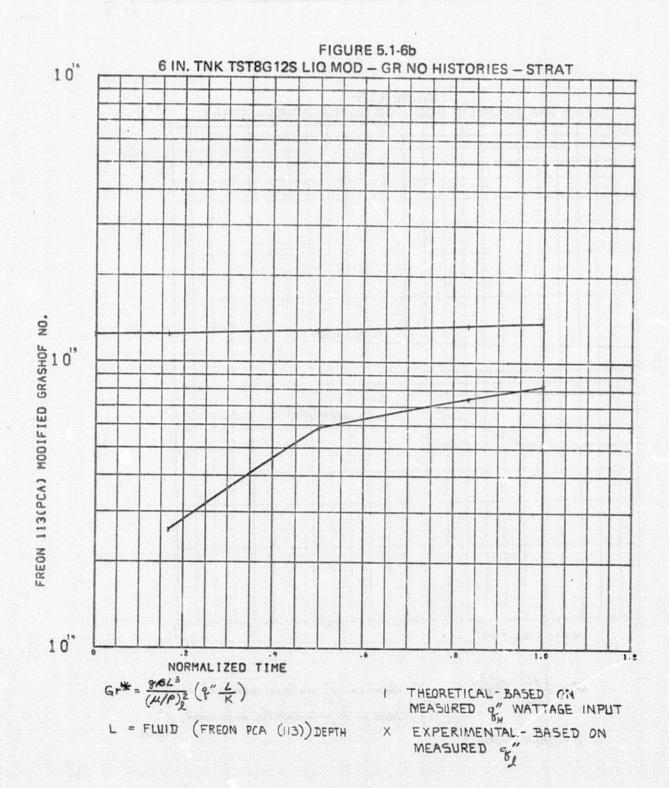


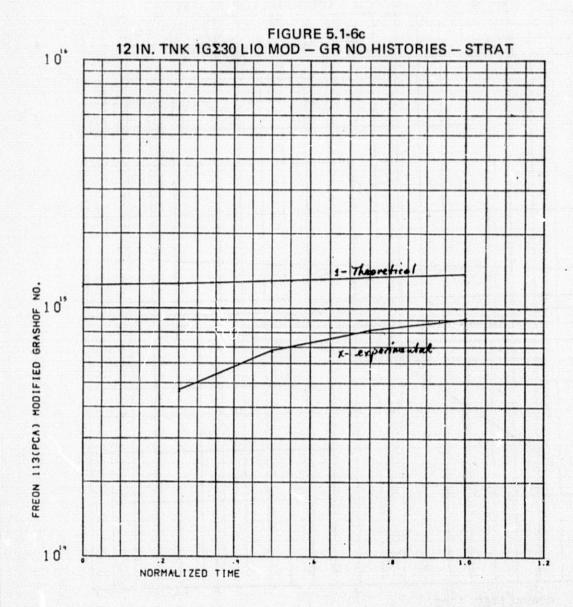
1- Gage 2}- Transducer

FIGURE 5.1-5d 12 IN. TNK TST1G25 TANK PRESSURE HISTORY 22 TANK-ULLAGE PRESSURE (PSIA) NORMALIZED TIME 1- Pressure Gage
2; Pressure Transducer

49







$$Gr^* = \frac{g \beta L^3}{(\mu/e)_j^2} \left(\frac{g^* L}{k}\right)$$

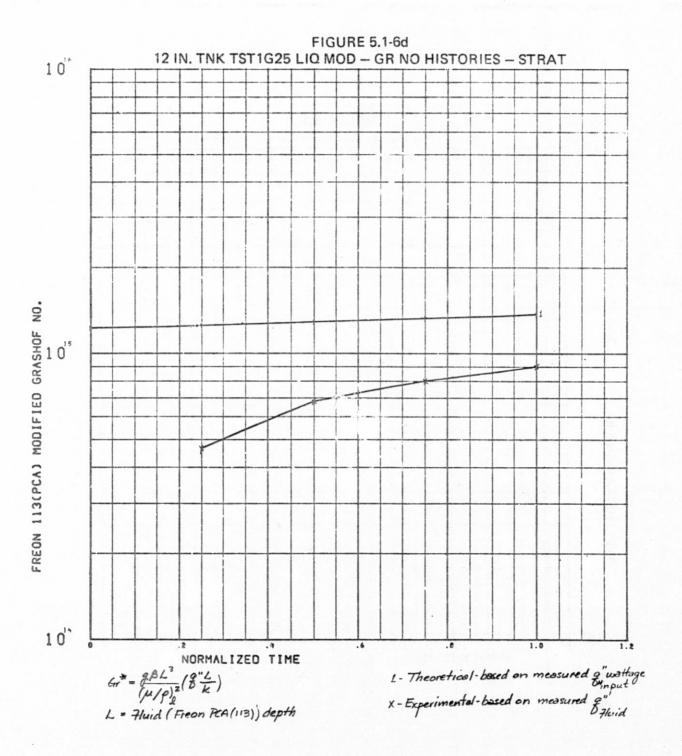
L - Aluid depth

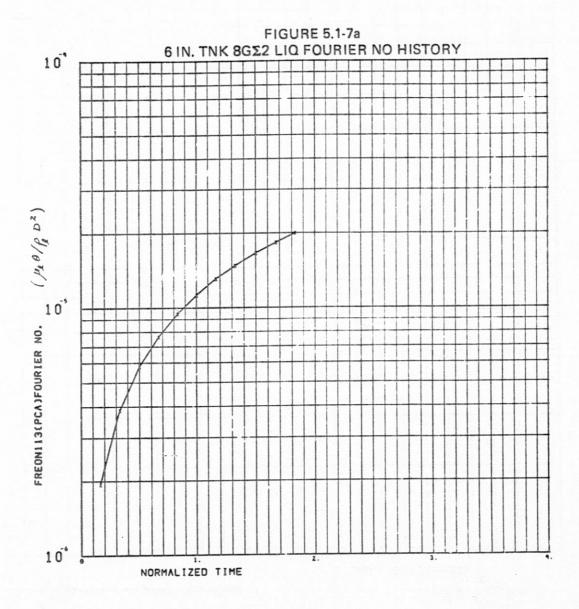
Gr = g AL3 (8 L)

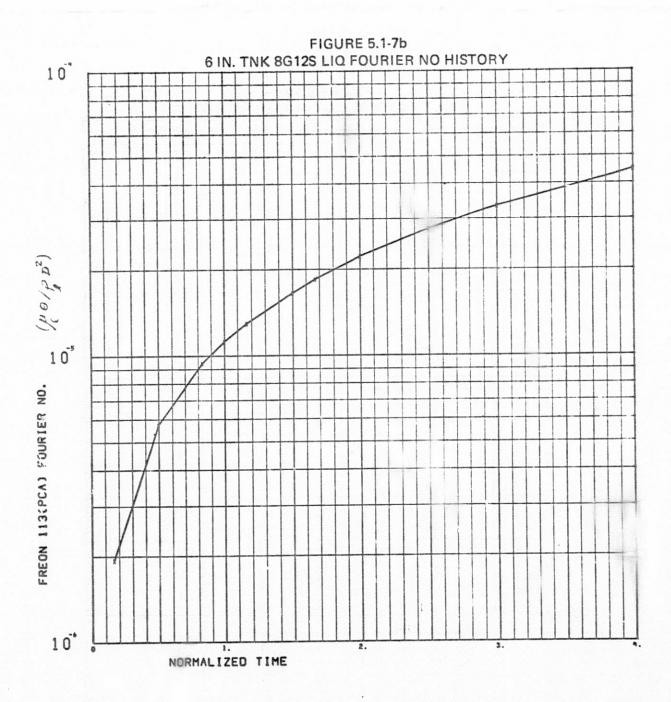
1 = Based on g" wattage measured impact

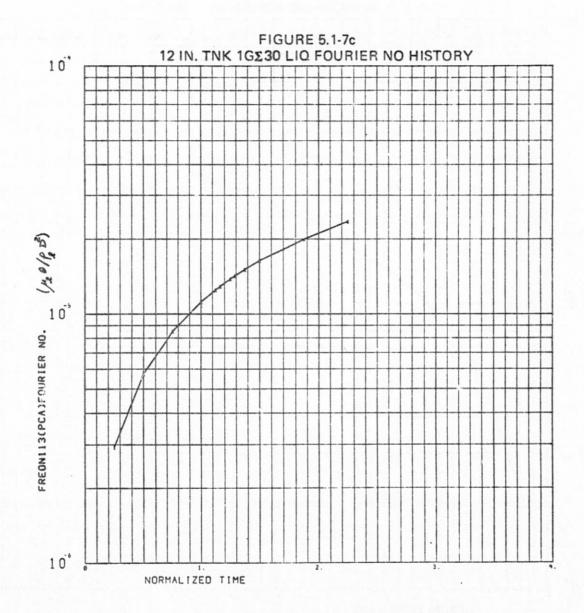
(4/p) = Based on experimentally determined; g"

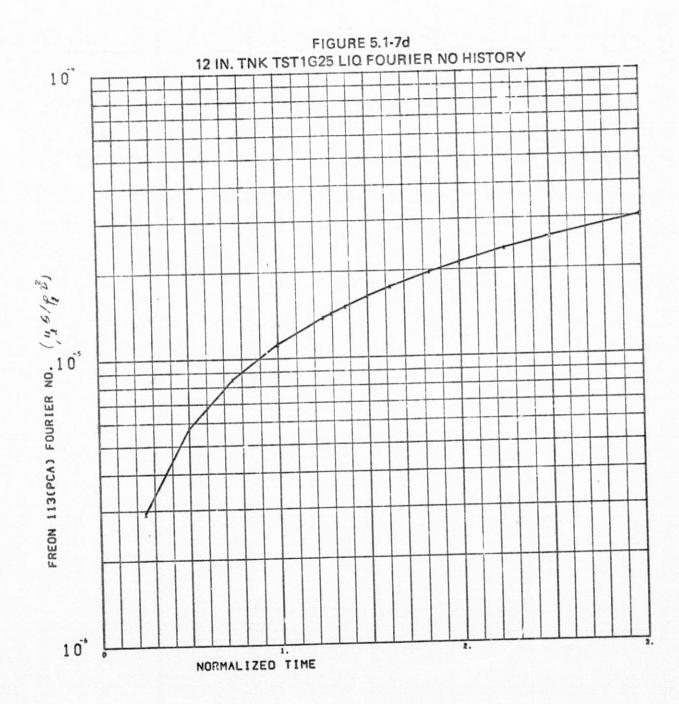
Third.











Section 5.2 SCALING SET

6-in Dia Tank Tests	12-in Dia Tank Tests
8G	1G
Test #3	Test #31
Test #11S	Test #17

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STRUCTURAL	GEOMETRI	TANK WTS	-WATTHETER	HEAT FLU	X INPUTS
VIII-019 75		,			

DOME-AREA FT28-3927-CYL AREA FT29-1:5708-FLNGE AREA FT29-:0365-1/2 CYL WALL VOLFTSS .00164 FLNGE VOL FT3# .00076 DME WALL VOL FT3# .00131 ,38058 DME MASS LBM# .65596 FLANGE MASSE MASS 1/2 CYL LBM# .81996 ULLAGE VOL FT3# .03272 LIG VOL FT3# .22907 INPUT HEAT FLUXES (BTU/HR=FT2), AND ABSORBED HEAT AND TEMPERATURE ESTIMATES-H12=1001,9935 H34=1001,9935 H56=1001,9935 H910=1001,9935 H76=1001,9935 EST. HT FLUX IN LIG (BTU/HR-FT2)=1001.9935 EST.HT FLUX IN ULLGE (BTU/HR=FT2) #1001.9935 EST.HT_INPUT_LIG(STRAT)BTU= 65.580 (STRAT+DESTRAT)BTU= 131.161 EST.LIQ TEMP INCRSE(STRAT) = 13,4605F (STRAT+DESTRAT) = 25.8956F EST HT INPUT ULLAGE(STRAT) BTUE 13.416 (STRAT+DESTRAT) BTUE 26.232 Table 5. 2-1b. 6 IN. DIA. TANK TEST 8G#11S STRUCTURAL GEOMETRIC TANK WTS-WATTMETER HEAT FLUX INPUTS DOME AREA FT2= .3927 CYL AREA FT2= 1.5708 FLNGE AREA FT2= .0365 -DME WALL VOL FT3= .00131 1/2 CYL WALL VOLFT3= .00164 FLNGE VOL FT3= .00076 DME MASS LBM= .65596 MASS 1/2 CYL LBM= .81996 FLANGE MASS= .38058

LIQ VOL FT3= .22907 ULLAGE VOL FT3= .03272

INPUT HEAT FLUXES (BTU/HR-FT2) , AND ABSORBED HEAT AND TEMPERATURE ESTIMATES

H12=1001.9935 H34=1001.9935 H56=1001.9935 H910=1001.9935 H78=1001.9935

EST.HT FLUX IN LIQ (BTU/HR-FT2)=1001.9935-EST.HT FLUX IN ULLGE (BTU/HR-FT2)=1001.9935

EST.HT INPUT LIG(STRAT)BTU= 65.580 (STRAT+DESTRAT)BTU= 0.000 -(ST.LIG TEMP INCRSE(STRAT)= 13.4618F (STRAT+DESTRAT)= 0.0000F

EST. HT INPUT ULLAGE (STRAT) BTU= 13.116 (STRAT+DESTRAT) BTU= 0.000

99

Table 5, 2-1c. 12 IN. DIA. TANK TEST 1G#31 (Page 2 of 2) STRUCTUPAL SEGMETRIC TANK STS-MATIMETER HEAT FLUX INPUTS

DOME AREA FT2= 1,5706 CYL AREA FT2= 6,2832 FLNGE AREA FT2= ,1458 -DME -ALL VOL FT3= ,01047 1/2 GYL WALL VOLFT3= ,01309 FLNGE VOL FT3= DME HASS LBM= 5,24772 MASS 1/2 CYL LBM= 6,55969 FLANGE MASS= 3,04465	
LIQ VOL ET3= 1.83260 ULLAGE VOL FT3= .26180	
INPUT HEAT FLUXES (BTU/HR-FT2), AND ABSORBED HEAT AND TEMPERATURE ESTIMATES	
H12= 500,5626 H34= 500,5626 H56= 500,5626 H910= 500,5626 H78= 500,5626	
EST.HT FLUX IN LID (BTU/HR=FT2)= 500,5626 EST.HT FLUX IN ULLGE (BTU/HR=FT2)= 500,5626 EST.HT INPUT LIC(STRAT)BTU= 524,488 (STRAT+DESTRAT)BTU= 982,852 EST.LID TEMP_INCRSE(STRAT)= 13,4462F (STRAT+DESTRAT)= 25,1829F	
EST. HT INPUT ULLAGE (STRAT) BTU= 104.838 (STRAT+DESTRAT) BTU= 196.570	ang and annual services an
Table 5.2-1d. 12 IN. DIA. TANK TEST 1G#17 STRUCTURAL GEOMETRIC TANK WIS-WATTMETER HEAT FLUX INPUTS	
DOME AREA FT2= 1,5708 CYL AREA FT2= 6,2832 FLNGE AREA FT2= ,1458 DME WALL VOL FT3= ,01047 1/2 CYL WALL VOLFT3= ,01309 FLNGE VGL FT3= DME MASS LBM= 5,24772 MASS 1/2 CYL LBM= 6,55965 FLANGE MASS= 3,04465	.00608
LIQ VOL FT3= 1,83260 ULLAGE VCL FT3= .20180	
INPUT HEAT FLUXES (RTU/FR-FT2), AND ABSCREED HEAT AND TEMPERATURE ESTIMATES	
H12= 500,5026 H34= 500,5626 H56= 500,5626 H910= 500,5626 H78= 500,5626	
EST. HT -FLUX IN LIQ (BTU/ R=FT2)=-500,5626	
EST, HT FLUX IN ULLCE (BTL/HR=FT2) = 500,5626 EST, HT INPUT LIG(STRAT) BTL = 524,188 (STRAT+DESTRAT) BTU = 906,406 EST, LIG TEMP INCRSE(STRAT) = 13,4459F (STRAT+DESTRAT) = 23,2291F	
EST. HT INPUT ULLAGE (STRAT) BTU= 104,838 (STRAT+DESTRAT) BTU= 181,281	

			The second secon
TIMPIMIN) 0,000 ,333 ,667	1,000 1,333 1,667	2.000
TAU	0,000 ,167 ,334	,500 ,666 ,834 1	.000
1	116,000 118,417 122,625	125,708 129,042 131,958 1	35,083
?	116,958 123,875 130,792	134,833 134,208 141,833 1	44,500
3		132,833 135,958 139,375 1	A1, 958
4			40.917
5	116,708 121,625 126,750		37,708
6	116,750 121,917 126,958		36,625
7	116,833 122,333 127,625	129,875 132,333 134,292 1	36,125
8	116,958 122,750 127,209	124,958 130,750 132,375 1	
9		121,250 122,500 123,625 1	25,125
10	116,833 127,917 132,542		45,292
11	116,875 128,708 133,875		45,125
12	117,250 129,417 134,917		44,453
13	116,542 127,875 132,833		39,042
14	116,000 118,917 122,625	125,708 120,042 131,958 1	
		130,750 132,958 135,917 1	
16	116,542 122,958 127,875		38,250
17	116,000 120,792 124,500		33,792
	115,375 120,500 124,833	126,708 129,750 130,917 1	
19	114,708 116,542 118,833		24,708
_20	116,833 127,917 132,542		45,292
₹21	116,875 129,708 133,975		45,125
22	117,250 129,417 134,917		44,459
23	116,542 127,875 132,833	134,917 136,417 137,417 1	39,042
2A	_116,292_134,167_153,792		19,167
25	115,958 119,583 123,042	126,917 131,542 139,208 1	49,583
26	115,833 118,958 122,125	125,375 128,833 132,083 1	
27	114,792 119,042 122,042	125,292 128,792 132,125 1	
28		130,917 137,917 145,625 1	54,125
29	116,000 125,792 135,958	145,458 155,292 164,958 1	74,542
30	-116,375-140,458-164,792-	186,750 204,875 224,625 2	
31	116,042 126,896 131,125	132,354 132,771 133,458 1	
32	116,750 127,708 132,125	133,333 133,542 134,250 1	35,000
33	114,750 117,083 119,708	121,125 122,333 123,083 1	24,000
34		114,917 116,708 117,917 1	

Та	ble 5.2-2a. 6 IN. DIA TANK TEST 8G #3 (Page 2 of 2)	
35	105,500 106,500 107,583 108,917 110,375 111,625	447 097
36	-115,333-126,083-130,125-131,375-132,000-132,667	173 1003
37		
38	116 667 110 501 120 650 120 708 170 405 170 140	166,583
39	116,667 119,583 122,958 127,375 133,125 138,667	124:375
40	116,833 110,058 123,125 127,833 132,875 140,333 117,250 120,125 123,167 126,833 132,583 137,417	
41		142,042
42	116,792 119,542 121,750 124,458 127,958 130,875	133,750
43	-116,917,119,375,121,875,124,500,127,958,130,875,	134,042
44	117,083 120,042 122,167 124,750 127,875 131,083	133,833
45	117,167 119,750 122,083 124,875 128,667 132,000	135,917
46	117,083 120,375 122,333 124,702 127,750 130,417	133,458
47	117,000 119,625 122,292 125,167 128,583 132,125	
48	117,375 120,792 123,333 126,25n 130,042 132,083	134,875
49	-117,792-119,167-121,625-124,208-127,667-130,167-	
50	116,458 117,917 119,833 122,583 125,125 127,750	130,542
51	116,750 117,750 119,542 122,333 124,458 127,500	129,667
52	117 188 117 125 120 667 121 417 123 708 126 375	
53	117,188 118,125 120,500 122,354 124,563 126,708	129,375
54	116,458 117,375 119,458 122,000 124,667 126,000	129,667
55	-117,875-118,625-120,333-123,292-125,417-127,042	130,208 -
56	117,708 118,750 120,750 123,042 125,292 129,042	130,167
57	117,875 118,625 120,333 123,292 125,417 127,042	130,209
58	117,708 118,750 120,750 123,042 125,292 128,042 116,542 116,833 119,250 121,542 123,208 125,375	
59		127,875
60		127,708
61	118,792-118,958-120,583-122,375-124,708-126,792 116,083 116,000 116,875 118,542 119,542 122,458	129,042
62		123,292
63		123,667
64	117,083 117,042 117,625 119,708 120,625 127,292 118,125 118,042 118,833 120,250 122,083 122,792	
65		124,542
66	115,917 115,958 116,000 117,292 118,208 119,833	
67	116,125-116,042-115,833-116,750-117,708 119,333 116,625 116,875 116,842 117,625 118,500 110,958	120.375
68		121,250
-69	117,583 117,667 117,750 118,583 119,167 120,042	121:007
70	-115,875 115,792 115,708 116,375 114,792 117,958	110-107
71	116,000 115,917 115,792 116,667 116,875 118,167	119,042
72	116,292 116,375 116,417 117,125 117,375 118,583 117,333 117,500 117,625 118,708 119,250 120,625	
73	AAC OF A LAR AOR AAA AAR AAR	
74		
		11,792
76	91,167 91,083 90,917 91,167 90,917 91,208	
77	104,292 104,333 104,333 104,833 105,042 105,625 1	
, ,	89,875 89,667 89,375 89,458 89,125 89,208	89,042

. .)

TEMPERATURE MATRIX-STRATIFICATION

	TIME	(MIN)	0.00	0 .33			7 2.000	
	TAU		0.000	.167	.500	.833	1.000	
	1		116.833	120.583	128.917	135.750	-139.542-	
	5			124.000				
	5			122.958			141.458	
	4		117.500	-123.583			140.292	•
	5		116.667	121.917		134.917		
	6		116,500	122.167	130.083			
	7 .		116.375	-122.250	129.563	-133,521	-135.833-	
	8		116.250			132.583		
	9		114.875			123.750		
	10		117.167	126.583	136.667	-142.333	145.208	
	11		117.042		137.250			
	12		116.583					
í	13		115.500	126.708	133.833			
	14		115.583	118.833	125.667			
	15		116.292	122,250	130.083			
	16-		116.792			135.333	137-917-	
	17		115.813		128.792			
	18		114.833		126,500			
	19		114.208			122:292	123.667	
	50		117.167	이렇게 하셨다 그런 게 게 되었다. 다하다	136,667			
	21		117.042		137,250			
	55		116.583	-129.000	137.583			
	23		115.500		133.833			
	24		116,417	135.542	172.708			
	- 25						138.708	
	26		111.313	119.458			그리는 사용을 하는 사람들은 사람들은 물을 잃었다. 전 사람들이 얼마나 보다는 그게	
	27		106.708	118.917	125.292	2 131.083		
	- 28-		116.167	-120.292	131.250	145.792	-154.042-	
	29		116.167	126.250	146.250	165.667		
	30		117.458	142.750	189.458	556.585	241.542	
	-31	-			-129.722	131-722	132.639	
	32		116.708				133,250	
	33		114.042	116.125	119.833	121.958		
	30		112.417	-113.083	-115.208	-117.167	117.875	

64

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Table 5. 2-2b. 6 IN. DIA TANK TEST 8G #11S (Page 2 of 2)
           110.917 110.917 111.750 112.750 113.208
  22
           115.417 124.667 129.292 131.292 132.333
  36
           116.667 120.792 135.167-154.417-166.833-
 -37
           116.667 119.833 127.875 141.500 154.250
  38
           117.000 120.042 127.708 139.250 147.667
  39
           -117.292-120.250-127.375-135.833-139.667--
-40
           117.208 119.292 124.833 130.375 133.083
  41
           117,208 119,208 124,833 130,667 133,625
  42
           -1-17-500-1-19-500-1-25-292-130-750-133-333 -
           117.583 119.708 125.542 132.500 135.167
           117.458 120.042 120.708 130.333 132.833
  45
           <del>-117.375-119.</del>708-126.208-131.000-134.042--
           117.958 120.917 126.125 132.208 134.625
  47
           118.167 119.500 124.917 130.208 132.417
  48
           115,875 117,042 122,083 126,833 129,125
  -49
           116.375 117.417 121.708 126.917 129.250
  50
           116.125 116.542 120.500 125.542 128.208
  51
           116.979 117.396 121.667 126.083 128.271-
 -52
           115.667 116.333 121.542 125.250 127.458
  53
           117.833 118.250 122.833 126.625 128.333
  54
           117.542 117.917 122.500 126.833 129.542
 -55
           117.833 118.250 122.833 126.625 128.333
  56
          . 117.542 117.917 122.500 126.833 129.542
  57
           115.833-116.208-121.375-124.875-126.875-
 -58
           117,083 117,542 121,208 124,958 127,333
  59
           118,500 119,042 122,083 126,458 128,208
  60
           115.042-115.375-117.167-120.625-122.667-
  61
           114.875 115.542 117.542 120.833 122.417
  62
           115.958 116.458 118.542 122.042 123.917
  63
           117-167-117-792-119-542-122-375-123-750
           114.167 114.667 115.750 118.625 120.667
  65
           114.250 114.500 115.542 118.125 119.500
  66
           115.292-115.417-116.417-118.917-120.292-
 -67
           116.167 116.208 116.875 119.042 120.167
  68
           113.458 113.792 114.917 116.792 118.042
  69
           113.792-114.000-115.208 116.667 117.958 ---
  70
           114.375 114.750 115.708 117.417 118.875
  71
           115.500 116.292 117.667 119.708 120.667
  72
           -113.167-114.083-115.875-117.542-119.250---
--73
           109,250 110,125 112,125 115,500 117,500
  74
            97.125 97.708 98.292 99.292 100.042
  75
           104.917 105.250 105.542 106.500 107.208
  76
            90.625 90.792 90.542 90.292 90.500
  77
```

	TIM	EIHIN	')	0.000		2.00	a	4,00	0	6.000	8	.000	
	TAU		0,0		, 2			01	, 7		1.00		
	1_		-117	1292	124	202			131	1833	1351		
	5			458		292		,583	133	,958	137.	333	
	5			792		583		. 667		917	139,	042	
	4			958		417		. 525		1667	134	P. 33	
	5			833		792	1,31	.333	133	917	134		
	6			875		,183		, A75	131	,417	134		
	77			,875	125	. 275	128	, 375	130	.70F	133,		
	18		117	875		.125	123	.542	130	· 833	133,		
	ç			,542	121	, 256	124	, 567	127	,250	129		
	10		117	,503-	135	,20A	101	, 757	1,42		145		
	11			, 557	135	142	134	. 167	141	1235	141,	333	
	12			000		553	135	,542	137	,200	142:	042	
	-13-		_117	792	135	125	1.37	1333	139	542	141	750	
	14			,000		.000	127	.792	131	,5un	135		
	15			583		, A33	1.56	.042	139	625	142,	792	
	16		117	.748-					137	.500	140		
	17		117	,625	130	058	1.33	. 375	136	,70°	139,	542	
	18			542		417	131	,750	134	.333	137,		
	-19-			167	121	333	123	,750			125	625_	
	20			917		.083		,142	142	,5un	145		
	21			750		,417	139	,583	141	,792	144	503	
	22			,125		208	135	,753	-139		142,		
	23			,042		583	136	,750	138	. 475	141,	705	
	24			500		.417		.000	171	,250	177		
	-25		116	208	125	542		+17	145	1042	154	125_	
	26		115	000	122	,750	129	,875	137	452	144		
	27		115	375	122	.703	123	,750		, 45R	145	950	
-	_28-			1208		417	101	, 217	1 187	,292	213:	000-	-
	29			.333		375		. 417	162	.792	177	667	
	30			1142		417		542		959	224	208	
_	_31_			625		1333		542	132	542	141	167_	
	32			375		. 458	134	.375	136	.738	139,	958	
	33			292		. 333		5,083		.7UP	125,	A67	
	34			792						1042	116;	708	

Table !	5.2-2c. 12 IN.	DIA TANK	TEST 1	G NO. 31 (Page 2 of 2)
35	115,542			113,875 113,625
36	119,167		36,667	138,708 141,083
37		132 125 15	4 167	179,667 202,292
38		127,000 14	12,167	154,167 169,208
39			30,333	
40_			50.292	137,792 144,125
41	117,542	120,708 12	23,667	126,833 130,292
42		120,750 12	24,375	127,792 131,125
43	117,708		4 375	127,750 131,083
44	117,792		4,542	128,042 131,417
45	117,667	120,542 12	4,333	127,625 131,417
46	117,542	121,250 12	25,333-	128,583-132,125
47	117,750		4,375	
48		121,000 12	3,875	127,250 130,792
49	117,894			126,708 131,125
50	117,750		2,833	126,208 129,458
51	117,667		1,525	124,583 127,333
52		119,500 12		
53	117,458		3,083	126,208 129,417
54	117,750		2,792	126,000 129,167
55		110,833 12		125,050 120,208
56	117,625		2,583	125,792 128,875
57	117,54.2	•	3,042	126,042 129,250
58			2,333	125,458-128,750
59	117,500		1,917	125,000 128,083
60	117,333		1,708	124,708 127,542
62	117,417	118,667 12	-	123,702 124,542
63	117,625		1.042	123,792 126,583
- 64	117,333		0.875	123,500 126,292
65		118,292 12		122,958-125,708
60	117,417			123,125 125,792
67		118,042 12	0,000	122,333 124,917
68	117,250	117,975 11		122,333 124,917
69	117,333			
70				
71	117,208		9,417	121,625 124,000 121,625 124,000
_72	117,250			
¥73	117,292			
74	96,250		6,875	
75	106,083			97,542 98,250 110,292 112,292
76	68,792		8,875	88,875 88,917
77	99.458		9.583	99.792 100.208
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							4.000	8,000	
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7 4 11	-3.000		125	. 25 0	- ,5	00	750		
- ! AU	117 2	08 12		123,5	83 127	,625	131,500	135,333	
1	11/16	117 12	2.708	126,4	17 136	1.667	134,333	137,667	
2	11/10	83 12	7 043	127 4	58-135	.333-	-134.625	1371792	
3	-11719	17-12	0 7072	107 0	42 13	250	133,583	136,583	
4	117.7	108 12	3,700	14/14	45 701	003	134,125	137,083	
5	117.4	158 12	3,742	127,1	0/ 10	1.063	132.042	1341625	
6	-117.4	117-12	3,333	125,9	58 12	958	132 503	153,292	
ž	117,	42 12	3,208	125,5	83 12	250	130,583	133,083	
	117		2,958	120.0	00 12	8,542	130,708	1001000	
8	1171	13-11	9,750	-121.5	42 12	4,250	126,917	1291375	
9	-117		1,542	135,6		9,917	143,000	146,625	
10	117,	41/ 10	4 075	130,0		9,125	141,667	1441875	
11	117,	24% 10	1,875	137	160. 13	6.417	139,417		
12	-117		9,625	133,	100 43	7.292			
13	1171	417 13	1,167	134	100 13	7 1 4 7 6	130,833		
14			0,458	123,	250 12	7.167	130,000	-1421083	-
15	-117	458-17	6,208	-130	500-13	21520	136,667		
16	117	542 12	5,708	129	420 Tu	01200	1001-		
	117		6,208		292 13	3,375	136,333	139,125	_
17	-117		4 875	-128	292 13	1,208	133,45	136,250	
18	11/1		9,250	120.	750 12	3,375	125,792	1281272	
19	116,		14 875	135	750 13	9,667	143,208	1401/00	
20	118,	042 1	11,875	4.415	702-13	9.205	-142,200	-145,042	-
21	-1171	60/-1	221120	1991	792-13	6.833	139,958	142,375	
22	117.	625 1	5U 420	7041	EUD TO	0 100		141,500	
23	117.	625 1	30,792	134,	025 10	6.792	168,95	-177,292	-
24	-117	500-1	301042	140,	208-15	700	100,72		
25	117	583 1	21,10/	1501	8/5 1	4,95	143.16		
26			40 450	1 122	500 17	8,83	135,33	143 375	_
	-117	167-1	19,542	-122	542-17	28,797	7 191.41	3-1431375	
27	125	083 1	34.708	144	CO/ T	30177			
28	107	000 1	29.37		125 1	50.45	8 166,20	8 182,542	
29	120	000 1	35.75	1-152	750-1	82.79	2-165,25	0-1841042	
30	120	125-1	30 66	7 133		36,29	2 138.62	5 1411042	
31		083 1		7 47"	475 4	74 5A	3 134.54	2 138,875	
32	117	708 1	28,83	3 1021	708-4	22.50	3-124-25	0-126,042	-
33	-114	1928-1	10154	1.50	500 4	14 66	7 114.87	5 115,292	
34	114	625 1	14,41	/ 114	200 1	14100	, 71410,		

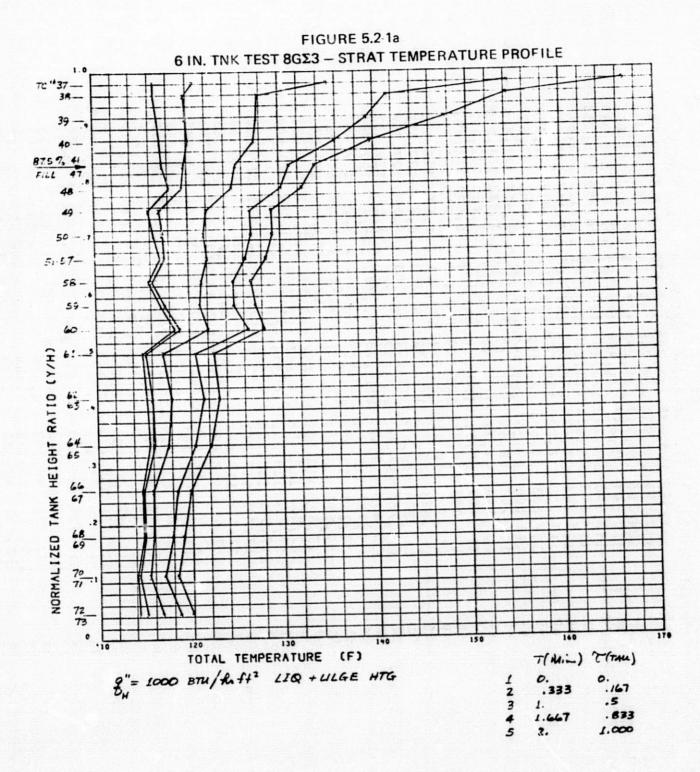
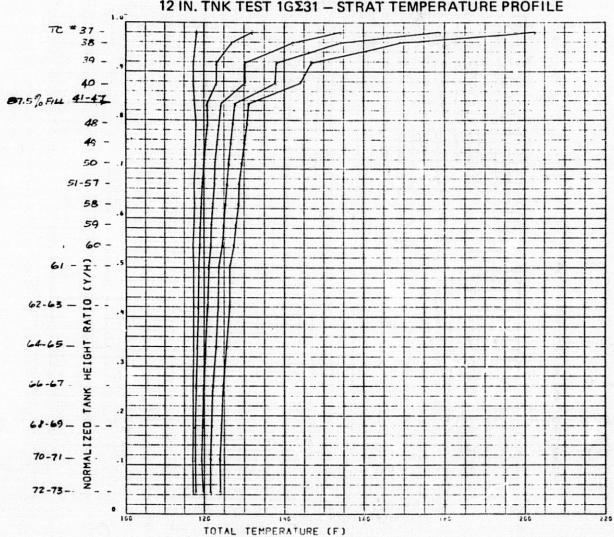


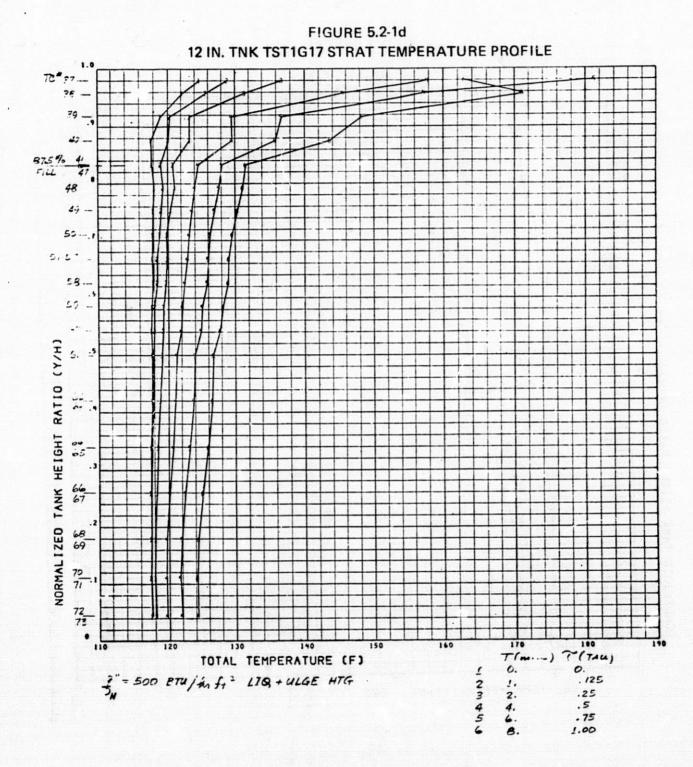
FIGURE 5.2-1b 6 IN. TNK TST8G11S STRAT TEMPERATURE PROFILE TC # 27 38 40 87.5 % FILL 41-47 49 50 51.57 58 59 -RATIO 70-71 - VA-TOTAL TEMPERATURE (F) T/min.) 8"= 1000 BTU/ A ST 2
8H LIQUID+ ULLAGE HT'G

71

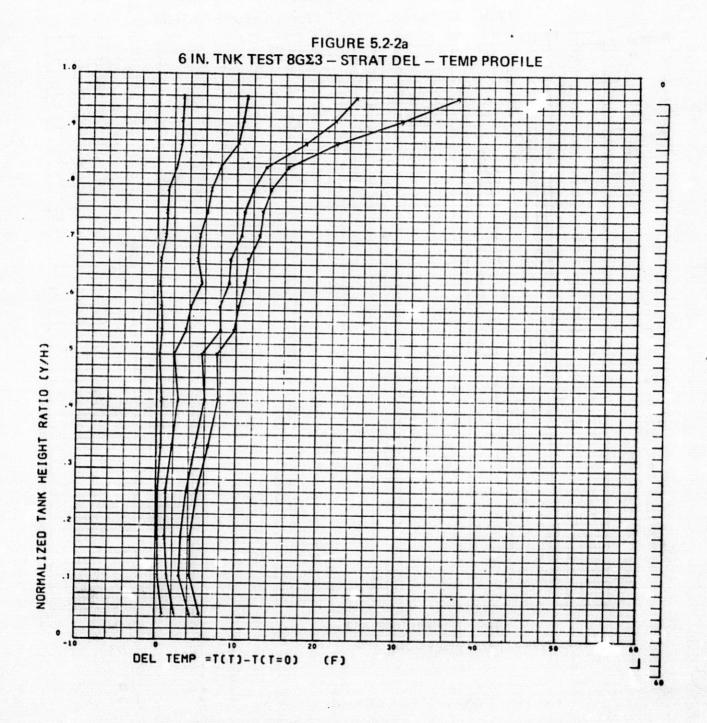
FIGURE 5.2-1c
12 IN. TNK TEST 1GΣ31 — STRAT TEMPERATURE PROFILE

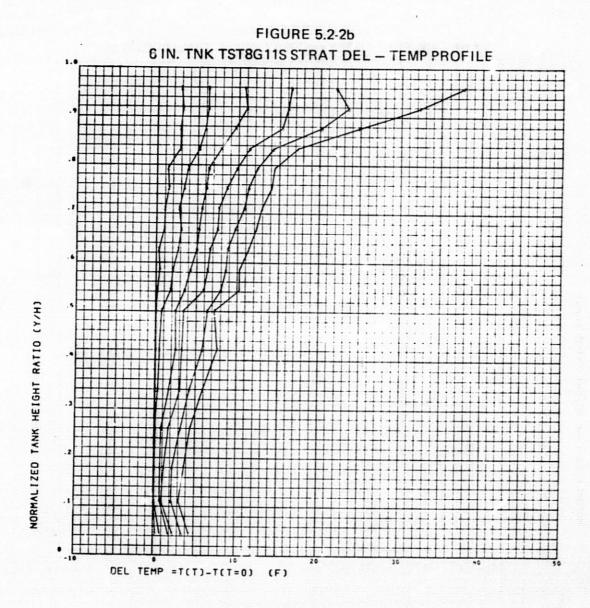


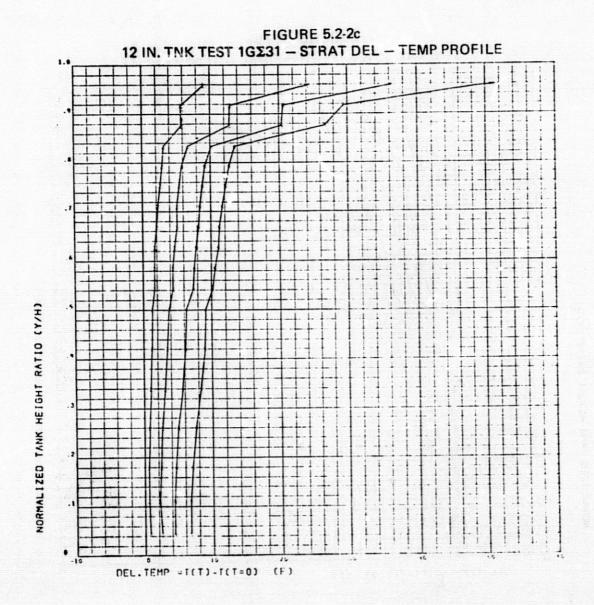
2"= 500 B	TU/An AZ LIQ + LILLAGE HTG		T(min)	TITAL
		1	0.	0.
		2	2.	.25
		3	4.	.50
		4	6,	.75
		-	8.	1.0

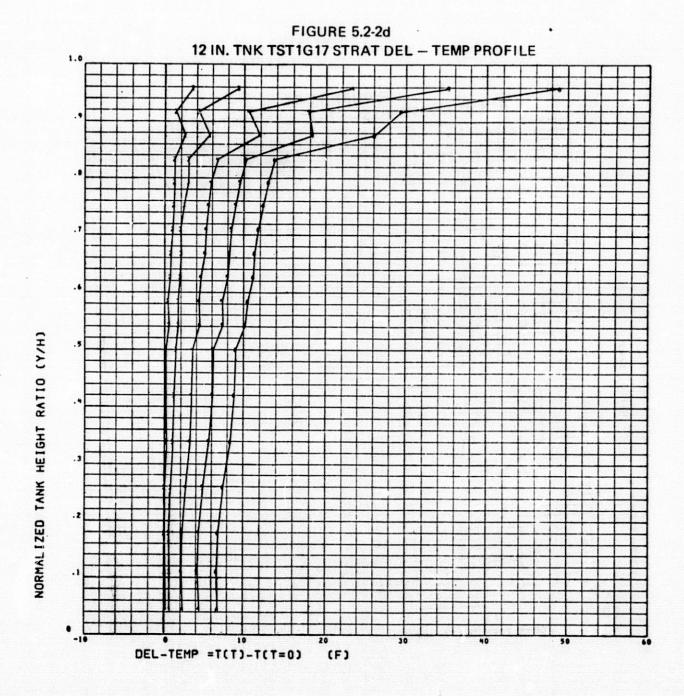


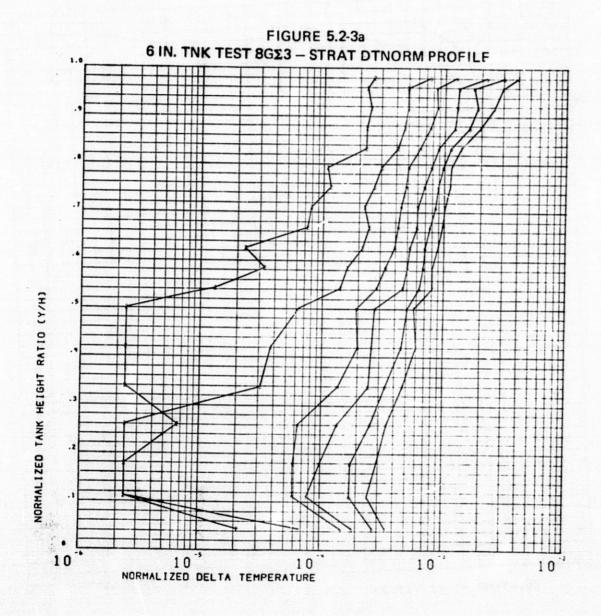
73

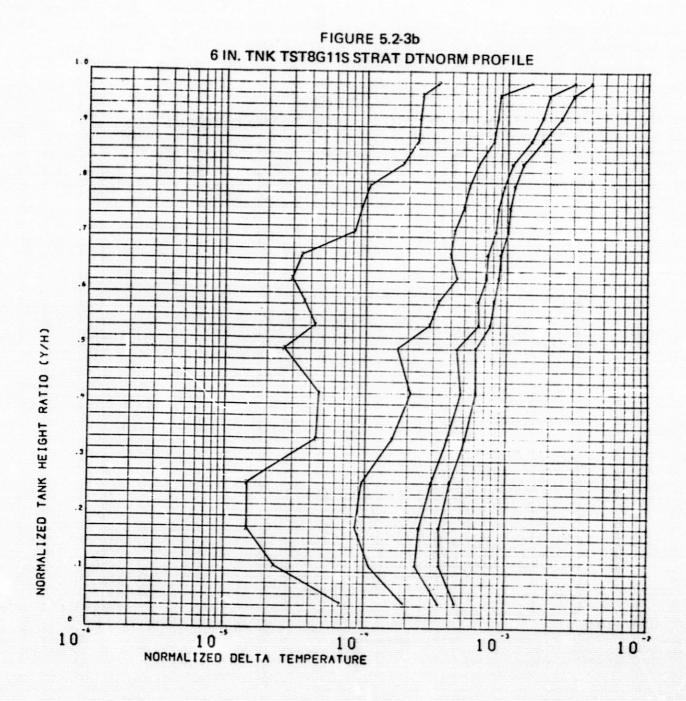


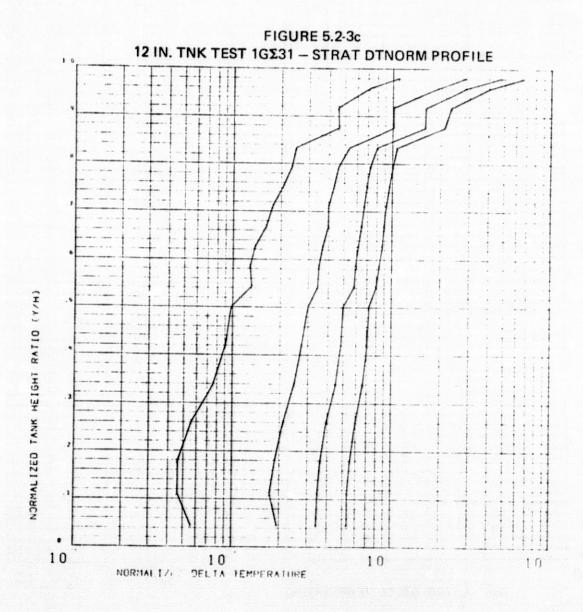


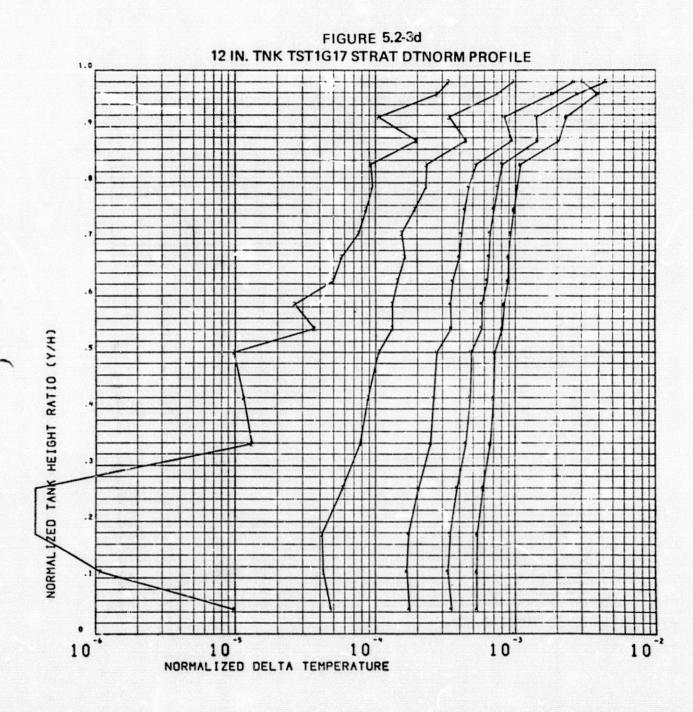


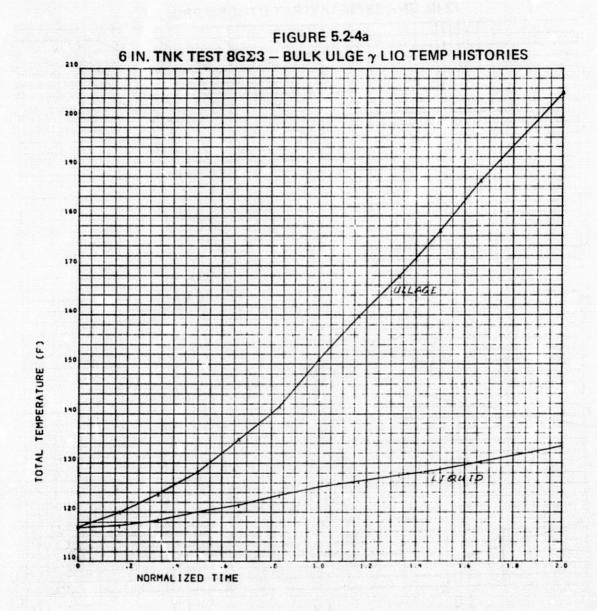


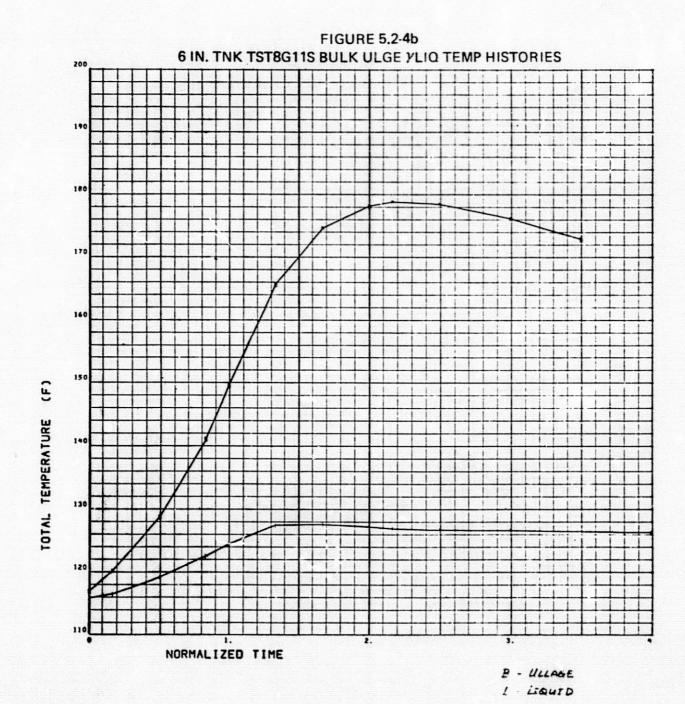


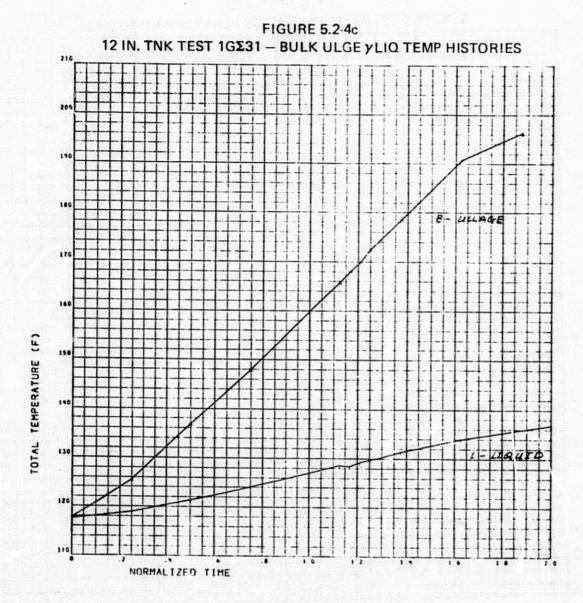


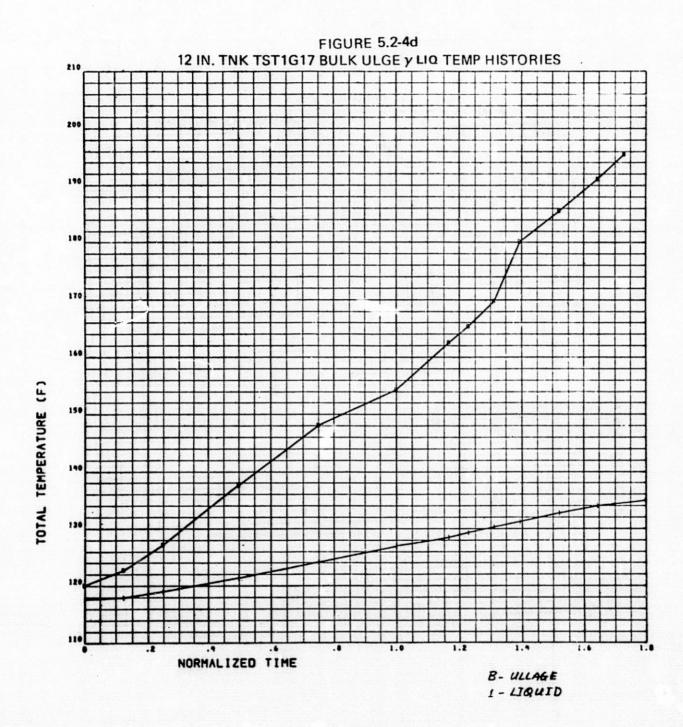


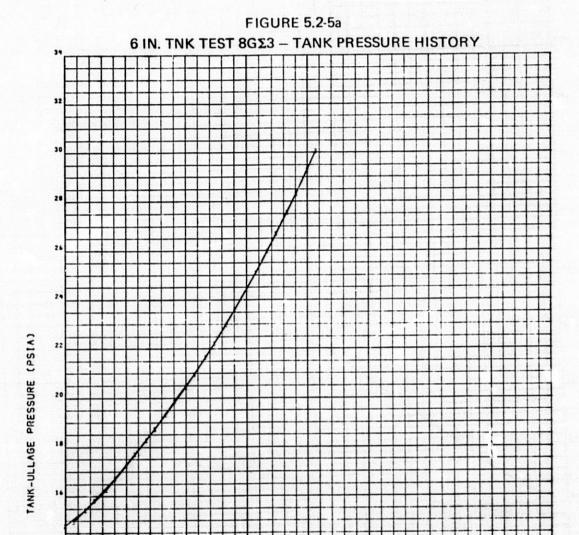




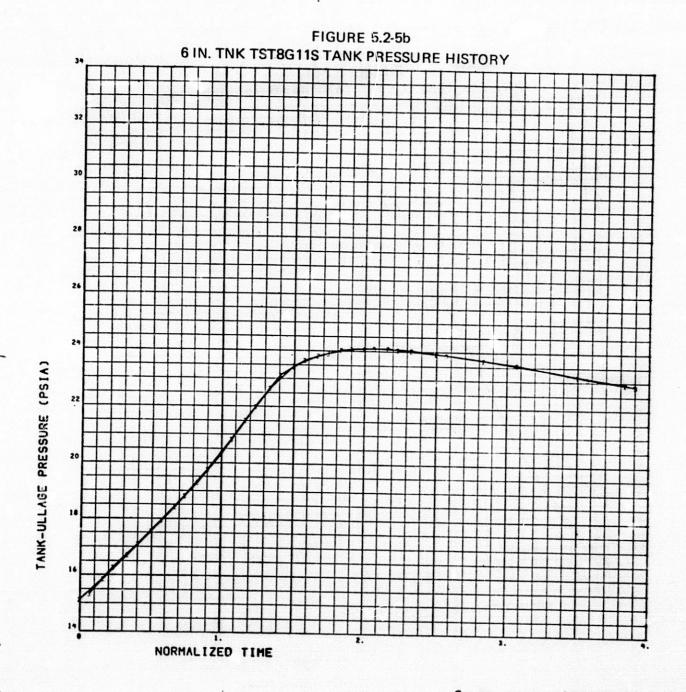




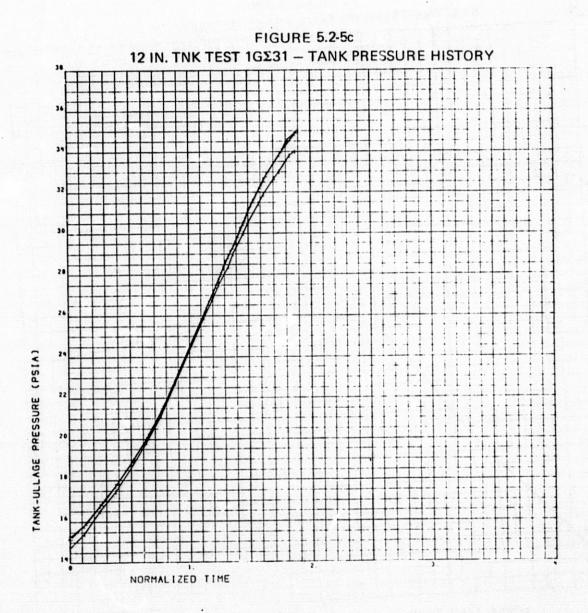




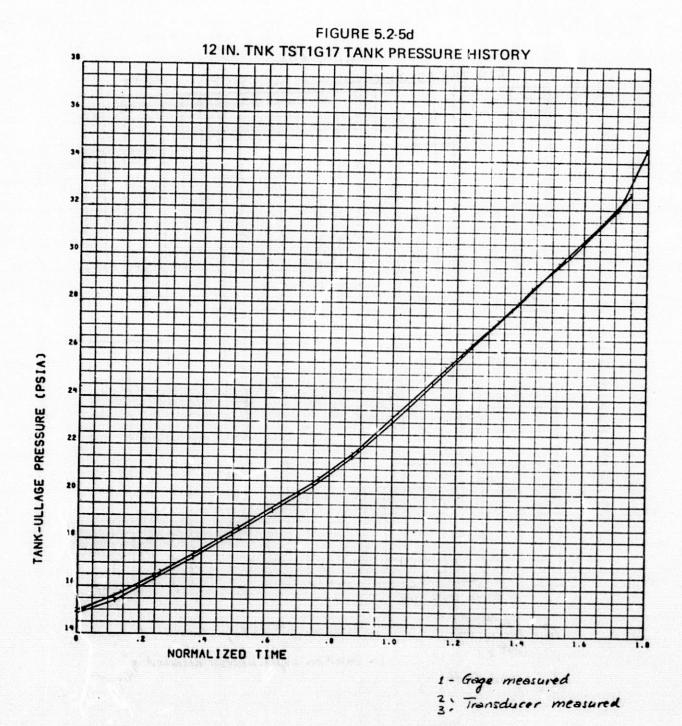
NORMALIZED TIME

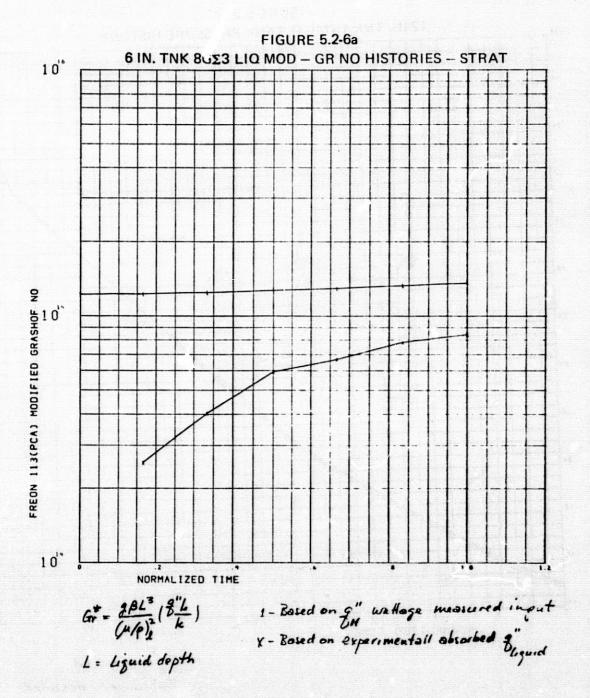


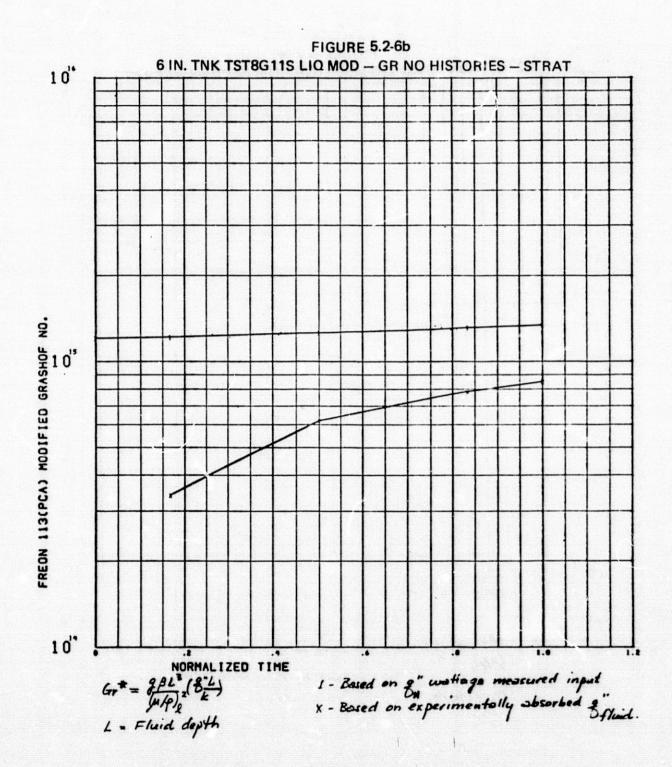
2: Tronsducer Measured

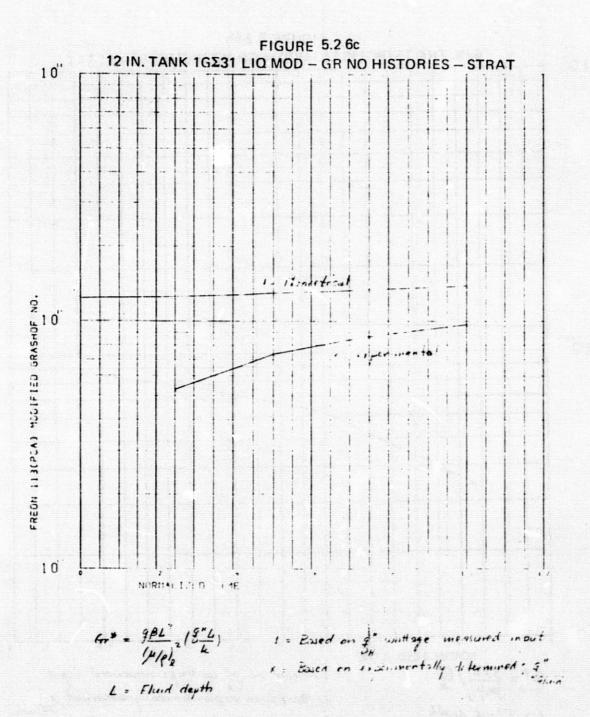


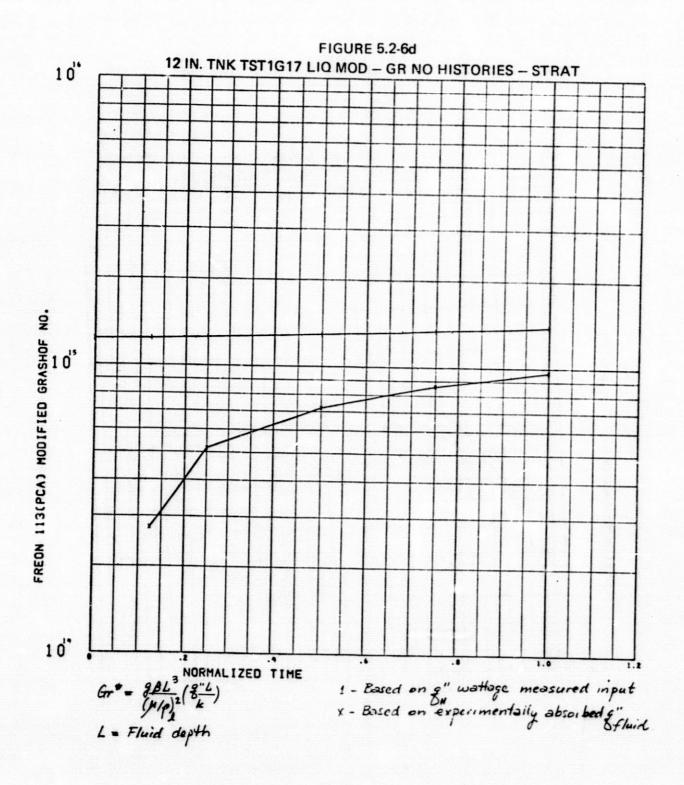
1 - Gage 2) - Transducer 3)

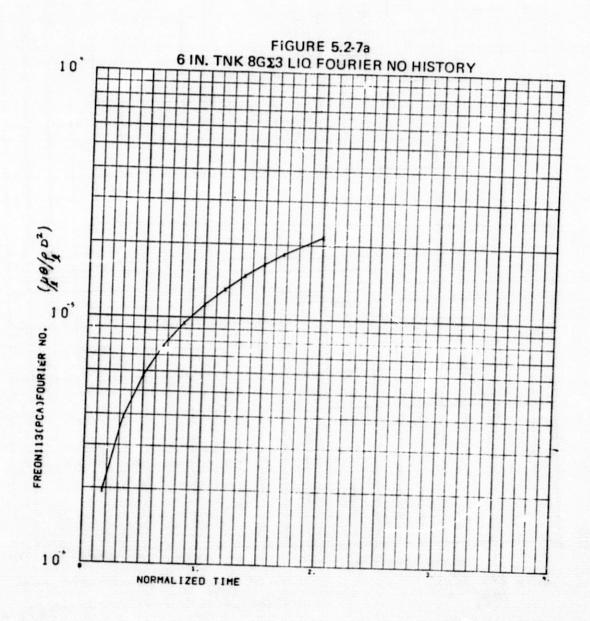


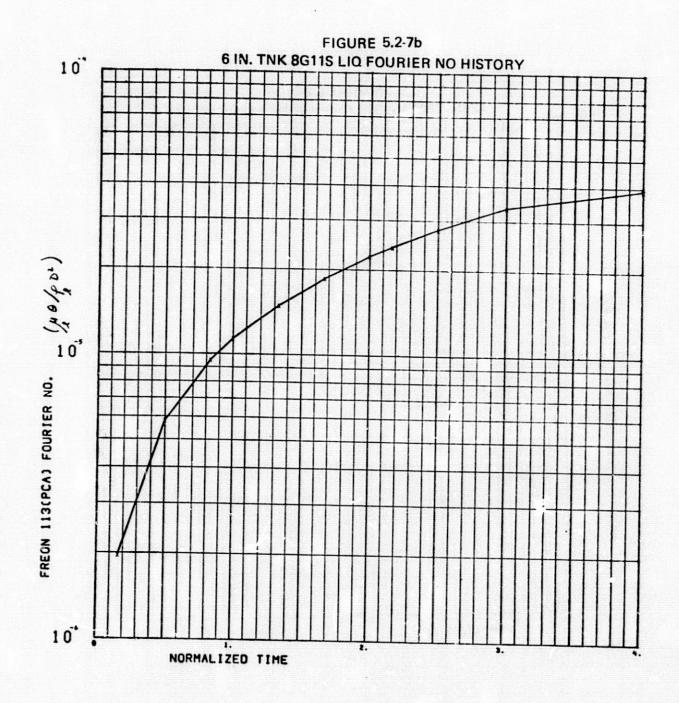


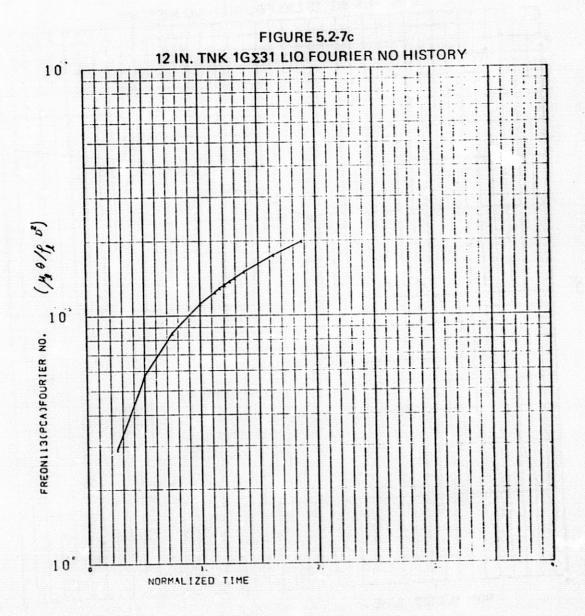


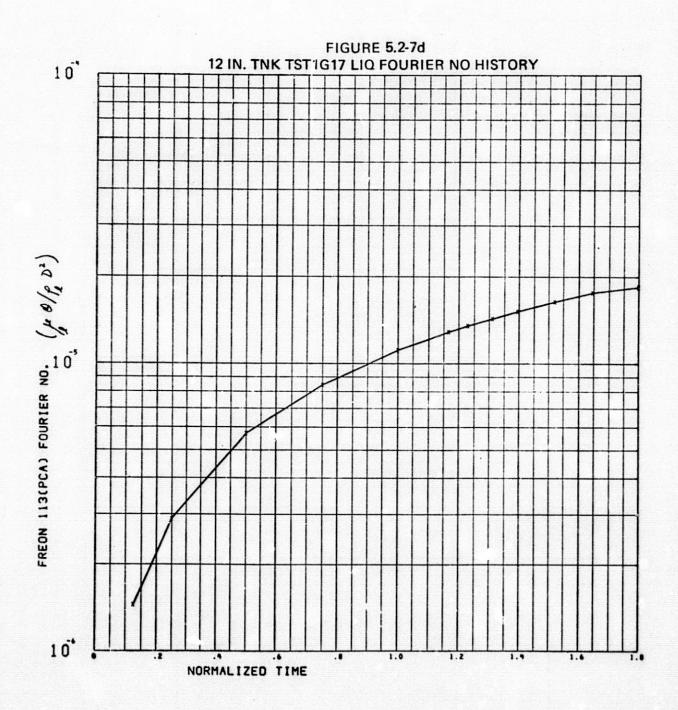












Section 5.3 SCALING SET

6-inDia Tank Tests	12-in Dia Tank Tests
8G	1G
Test #9S	Test #33
Test #15S	Test #32

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Table 5.3-1a. 6 IN. DIA. TANK TEST 8G#9S (Page 1 of 2) STRUCTURAL GEOMETRIC TANK WIS-WATTMETER HEAT FLUX INPUTS

	= .3927 73= .00131 .65596	CYL AREA FY 1/2 CYL W Mass 1/2 CYL	2= 1.5708 ALL VOLFT3= LBM= .81996	.00164	FLNGE	VOL FT3=	,00076
LIG VOL FT3=	.13090	ULLAGE VOL F	T3= ,13090				
INPUT HEAT FL	UXES (BYUZHR	-FT2) AND ABSO	RBED HEAT AND	TEMPERATU	RE ESTIM	ATES	
H12= 0.0000	H34= 0.0	000 H56= 701	.5691 H910=	701.5691	H78=	0.0000	
EST.HT FLUX IN	ULLGE (BTU/	HR-FT2)= 0.0	000				
EST. HT INPUT L EST. LIQ TEMP I	19(STRAT) BTU NCRSE(STRAT)	= 45,913 = 16,4923F	(STRAT+DESTR	AT)BTU= Trat)=	0.000 0.000F		
EST. HT INPUT U	LLAGE (STRAT)	BTU= 0.000	(STRAT+DE	STRAT)BTU=	0.00	0	
	CTORAL GEORE	:1010-1488-415-	\ 	T FLUX IN	PUTS-		
DOME AREA FT2	= ,3927 T3= ,00131		2= 1;5708	FL\GE_A	FEA FT2=	VCL -FT3#	:00076
DOME AREA FT2 DHE WALL VOL F DME MASS LHM=	= ,3927 T3= ,00131 ,65596	CYL AREA FT	2= 1,5708 ALL VOLFT3= LEM= ,81996	FL\GE_A	FEA FT2=	VCL -FT3#	,00076
DOME AREA FT2 DHE HALL VOL F DHE HASS LHM=	= ,3927 T3= ,00131 ,65596	CYL AREA FT 1/2 CYL k "ASS 1/2 CYL ULLAGE VCL F	2= 1,5708 ALL VOLFT3= LEM= ,81996 T3= ,13090	FLAGE_A 100164 FLANG	FEA FT2= FLNGE E MASS=	VCL -F13= ,38058	:00076
DOME AREA FT2 DME WALL VOL F DME MASS LHM= LIQ VOL FT3= INFLIT HEAT FL	= ,3927 T3= ,00131 ,65596 ,13090 HXES (BTU/FR	CYL AREA FT 1/2 CYL k "ASS 1/2 CYL ULLAGE VCL F	2= 1,5708 ALL VOLFT3= LEM= ,81996 T3= ,13090 REED HEAT AND	FLAGE_A 100164 FLANG	FEA FY2= FLNGE E MASS=	VCL -F13# ,38058	,00076
DOME AREA FT2 DHE HALL VOL F DME HASS LHM= LIQ VOL FT3= INFLIT HEAT FL H12= 0,0000 EST, FT FLUX IN	= ,3927 T3= ,00131 ,65596 ,13090 HXES (BTU/FR H34= 0,0 LIG (RTU/FR ULLGE (RTU/FR ULLGE (RTU/FR	CYL AREA FY 1/2 CYL h "ASS 1/2 CYL ULLAGE VCL F -FT2), AND ABSC 000 +56= 701 -FT2)= 701.569 +R=FT2)= 0.0	2= 1,5708 ALL VOLFT3= LEM= ,81996 T3= ,13090 REED HEAT AND ,5691 H910= 1 000 (STRAT+DESTR	FLAGE A 100164 FLANG	FEA FY2= FLNGE HASS= RE ESTIM	,38058 -ATES 0,000	,00076

31,400

Table 5.3-1c. 12 IN. DIA. TANK TEST 1G#33 (Page 2 of 2)
STHUCTURAL GEOMETRIC TANK WTS-WATTMETER, HEAT FLUX INPUTS

FLNGE AREA FT2= .1458 CYL AREA FT2# 6,2832 DOME AREA FT2= 1.5708 .01309 FLNGE VOL FT3= .00608 1/2 CYL WALL VOLFT3= DIE WALL VOL FT38 ,01047 LIO VOL FT3# 1.04720 ULLAGE VOL FT3# 1.04720 INPUT HEAT FLUXES (BTU/HR-FT2), AND ABSORBED HEAT AND TEMPERATURE ESTIMATES -H12= -0,0000--H34= -0,0000 -H56= 349,4822 -H910= 350,3504-- H78= -0,0000-----EST. HT FLUX IN LIG (BTU/HR-FT2)# 349.7716 EST. HT FLUX IN HELGE (GTU/HR-FT2) = 0,0000 (STRAT+DESTRAT)BTU# 934.014 EST. HT INPUT LIGISTRATIBIUS 357,123 (STRAT+DESTRAT) = 41,8531F EST.LIQ TEMP INCRSE(STRAT)= 16,0305F (STRAT+DESTRAT)BTU# 0.000 EST. HT INPUT ULLAGE (STRAT) BTU= 0.000 Table 5.3-1d. 12 IN. DIA. TANK TEST 1G#32 STRUCTURAL GEOMETRIC TANK HTS-HATTMETER HEAT FLUX "INPUTS----FLNGE AREA FTE -1456 DOME AREA FT2= 1.5708 CYL AREA FT2= 6.2852 FLNGE VOL FT3= .00608 1/2 CYL WALL VOLFT3= .01309 DME WALL VOL FT3= ..01047 FLANGE MASS= 3.04465 MASS 1/2 CYL LBM= 6.55965 DME MASS LBM= 5.24772 LIQ VOL FT3= 1.04720 ULLAGE VOL FT3= 1.04720 INPUT HEAT FLUXES (BTU/HR-FT2) AND ABSORBED HEAT AND TEMPERATURE ESTIMATES 0.0000 H56= 349.4822 H910= 350.3504 H78= 0.0000 H12= 0.0000 H34= EST. HT FLUX IN LIQ (BTU/HR-FT2) = 349.7716 EST.HT FLUX IN ULLGE (BTU/HR-FT2)= 0.0000 EST. HT INPUT LIG(STRAT) BTU= 357.123 --- (STRAT+DESTRAT) BTU= 824.130 EST.LIQ TEMP INCRSE(STRAT) = 16.0304F (STRAT+DESTRAT) = 36.9441F EST. HT INPUT ULLAGE (STRAT) BTUE ... 0.000 ... (STRAT+DESTRAT) BTUE ... 0.000

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TIME	(MIN)		0	. 0	n n			. 6		7		•	7	33	2		,	. 0 0			2		447	,		7	7	7.7	
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į				33			7.				19							83		1000				2275		1177			
		25,000,000,000 6	205 0.75	54		_	7.				19				100		C 13 (1)	192		TO 100 THE	3.		The second second				45		
4				70			7.				19							08			4.					-	52	1000	
5				41			2.				56						0.00	25			2.				7017	-	25		
6				79		-	5.				30							100			5 .			-		-	79	7.	
7		13000000000		91	25 12 15 10		5.				29							29	1.		5.				7.3.1	-	11		
8				04			5.				28							58			5.					0.00	4		
9				62			9.				21							25	17. 10.0		6.					- 17	0		
10				91			7.				18							75			3,						250		
11				000			7.				19							08			4.					77	11		
12			2000	25(1000	0.			77	34	100						08		0.000	0.		12 2 2 C				5		
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14				625		A CONTRACTOR	6.				18	2712 32						75			3.						158		
15				917		T - T	7.				7				CONTRACTOR OF		100	42	310 (1)	General Property	3.	1200 to 10	A-1550 X 112	1015	5 (5.4)	-	151		_
16		11	6.	250			7.				19							08	a constant		4.			1870		-	67		
17				167			2.				26							50	7	950	2.			3.75			117		
18		11	5.	417			2.				26							33			1.					*	33		
19		11	4.	797	?	11	7.	66	7		90							58	100		4.					-	17		
20	1.0	11!	5.0	117	•	11	7.	00	0	1	18	. 9	1	7				75			3.					7	50		
21		11	5.0	100)	T	7.	37	5	T	9	• 4	15	8			7	08	17.07		1.					20100	17		-
55		11	7 . 2	250) !	13	0.	29	5	13	54	. 4	1	7				08									50		
23		11	5.6	125		12	8.	50	0	13	30	. 8	7	5				75			5.					3	33		
24		11	5.5	542	!	11	6.	87	5	1 1	8	. 7	9	2				17			5.						08		
25		115	5.5	500	۱ !	1 1	6.	62	5	11	8	. 5	0	0	12	20	. 5	83			2.						25		
26		11!	5.4	158	1	11	6.	62	5	11	8	. 4	5	8	12	0	. 5	42									04		
27				17			6.			11					10	0	,5	υŬ									83		-
28		115	5.7	92	! !	11	6.	71			8				12	0	. 2	50	1	22	2.	08					83		
29				158	200	11	6.	80		11					11	9	. 1	25	1	21		0 0	0	12	3	. 0	83		
30		5 1 CO TE 1 1 C		17	C2137		6.			11								67	1	22		95					00		
31				17			6.			12					12	9	. 4	17			.:			7 T 120 C	- 1000	Target Sales	88		
32				58	3.0		7 . 5			12				0	12	9	9	58			. (67		
33				08			8 . 6			12	0	, 3	33	3-	12	1	4	58	1	22		71	7	12	4	, 5	00		-
34		1 2	2.2	92	1	1	3 .	33.	3	11	5,	, 4	17	7	1 1	6	7	50	1	17	•	75					75		

	Table 5 3-22 6 11	V DIA MANTE	
35	110 000 11	N. DIA TANK	TEST 8G #9S (Page 2 of 2)
36	***************************************	U.303 111.16	7 111 017 113 754 117 117
37	115.750 11	7 135 148 000	0 128,875 130.917 132.208
38	115-750 11	7.125 118.91	
39	116.042 11	7.125 119.167 7.333 119.292	
40	116,208 11	7.583 119.629	
41	로 The Children (1996) 10 10 10 10 10 10 10 10 10 10 10 10 10	7.125 119.375	
42		.333 119,458	
43	116.333 117	.583 119.750	
y. 44	그 그 그리고 그리는 그리고 있는데 그리고 있다면 그런 사람이 얼마나 아니는 어떻게 된 생각이 되었다. 그리고 있는데 그리고 있다는데 그리고 있다면 그리고	.708 119.750	사용을 보다면 보다면 하는데 이번 그리고 있는데 그리고 있다면서 모임하는데 하다면서 하는데
45	116.458 117		
46		.792 119.625	121.917 124.375 126.917
47	116.917 117	.875 119.958	122-333 12/ 625 127 254
48	116.708 118	.250 120.417	122.750 125.042 127.425
50	1124101 110	.333 118.292	120.625 123.042 125:250
51		.833 118.833	121.083 123.542 125.917
52		.625 118.625	120.833 123.458 125.708
53		.438 119.438	121.771 124.354 126.563
54		417 118 167	120.375 122.750 125.250
55		.250 120.250	122.708 125.250 127.417
56	보기 : : : : : : : : : : : : : : : : : : :	.042 120.000 .250 120.250	122,250 124,958 127,333
57			122.708 125.250 127.417
58		708 118.625	
59	116.750 117		120.750 123.208 125.542 122.125 124.667 127.125
60		625 121.625	
61		250 120.708	그리고 하는 그는
62	116.042 117		
63	116.833 118.	875 121.458	
64	118.042 119.	792 121.708	123.833 125.708 127.833 123.417 125.875 127.875
65	115.542 116.	042 117.917	120.250 122.417 124.333
66		542 117.250	118.833 120.875 122.833
67 68	116.417 116.	458 118.375	120,042 122,000 124,000
69	116.625 117.	458 118.042	119,958 122,000 123,917
70	115.125 115.		117.625 119.458 121 777
71	115.458 115.	542 116.125	117.625 119.542 121.542
72	115.958 116. 116.708 117.	1100411	110.10/ 120.292 122.542
73	114.708 116.		120.125 121.792 124.042
74	108.042 108.		118.500 120.417 122.375
75	94.208 94.		108.875 109.958 111.417
76	103.792 103.	700 404	95.500 96.083 96.875
77	88.458 88.		104.542 105.500 106.500
		0/10/3	67.625 87.625 87.792

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Table 5.3-2b. 6 IN. DIA TANK TEST 8G #15S (Page 1 of 2)

TEMPERATURE MATRIX-STRATIFICATION

TIME (MIN)		,000		, A3		.00		,60		. 333	
TAU			. 2'								
1	117.	748	119.	042	123,	083	125	708	128	505	
2			119,								
3			-1-1-9-								
4	118.	042	119,	750	123.	95B	126.	5 F 3	128	275	
5			125.			208	134.	167	136	667	
· · · · 6 · · · · · · · · · · · · · · ·	118	167-	127,	167	-135	750	-136,	375	140	625	
7	118,	354	128,	438	135	250	137.	938	140	063	
8	118,	542	127.	708	134,	75C	137.	500	139	500	
9	117	335	-171	7-18				455	130	547-	
10	117.	417	118,	375	123,	250	125,	833	126	125	
11			119,				126.				
12	118	750-	-132								
15			131,								
14			116.		122		125.		127		
15			119						120		
16			119		123,				122		
17			125.				133	715	136		
1 1			125								
19			120								
20			118		123						
			-115						125		
22			132		139,					500	
23			131		134	CER	137.		139		
- 24			-118,								
25			116.		122		124.		126		
26			116		122		124.		125		
27			112				123		125		
28			118.				123.		125		
29											
			117.		120,	117	122.		124.		
발표합니다 : 1일 이번에 중에만 모든 [[시기] [[시기] [[시기] [[[시기] [[[[[[[[[[[[[[[[[[114				124.		127.		
31			129,		131,		133.		135		
32	119,				131,		133.		135,		
			120+				CONTRACTOR OF STREET		1241		100
34	113,	245	114,	675	117,	158	117.	063	121.	250	

	Table 5	3-2b. 6 IN. DIA TANK TEST 8G #15S (Page 2 of 2)
	35	109,625 110,250 111,750 112,756 113,583
	36	118,250 128,917 131,250 133,167 135,000
	37	117,333 119,083 122,417 124,333 126,292
		117,333 119,083 122,667 124,958 127,083
	38	117,563 119,250 123,125 125,625 126,000
	40	117,792 119,503 123,625 126,167 128,625
	41	117,542 119,333 123,417 126,125 128,625
	42	117,542 119,500 123,500 126,292 128,768
	43	117,667 119,667 123,708 126,458 128,675
	44	117,956 119,792 123,875 126,583 129,125
	45	117,625 119,625 123,667 176,583 129,642
	46	117,563 119,500 123,792 126,583 129,000
	47	117,956 119,917 124,042 126,833 126,125
	48	110,250 120,250 124,667 127,417 129,750
	49	116,375 118,250 122,667 125,000 127,208 .
	50	116,833 118,625 123,208 125,417 127,792
	51	116,675 118,500 123,000 125,250-127,542
	52	117,354 119,333 123,875 126,104 128,375
	53	116,250 118,003 122,708 125,000 127,200
195	54	118,043 120,167 124,750 126,958 129,206
	55	117,917 120,000 124,458 126,750 129,042
	56	118,083 120,167 124,750 126,956 129,208
	57	117,917 120,000 124,456 126,750 129,0-2
	58	116,417 118,542 123,083 125,292 127,500
	59	117,667 119,875 124,333 126,625 128,875
		11/100/ 11/10/2 124,000 120,022 120,072
	60	119,000 121,292 125,917 126,292 130,583
	61	116,833 120,250 125,542 127,917 129,917
	▼ 62	116,750 119,563 124,750 126,750 128,917
	63	118,083 120,792 126,125 128,333 130,292
	64	119,125 121,563 126,167 127,633 130,167
	65	116,792 117,958 122,500 124,375 126,333
	66	
	67	117,875 118,375 122,125 123,792 125,625
	68 -	118,792 118,917 121,633 123,708 125,708
		116,629-116,792-119,625-121,458-123,167-
	70	116,792 117,125 119,593 121,500 123,292
	71	117,333 117,633 120,458 122,208 124,292
	72	118,000-119,375-122,292-123,792-125,625
	73	115,958 117,792 120,917 122,500 124,292
	.74	109,792 110,125 111,333 112,250 113,292
	75	97,503 97,958 99,042 99,375 99,792
	76	106,792 106,958 108,333 108,917 109,583
	77	
	//	93,042 92,792 92,792 92,625 92,458

TIME ("I")		U,	000	1	3	.0	n,)		Ó.	00	0		0	. 0	00	1	1	0	. (001)	1	2	. 0	00)	1	3	.000	0
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1	11.6	. 4	SA				n									3														542	
7	116			11									12														1	25		875	
3	117	. 1						12	20	. 1	53		122	٠.	16	7	1:	2 1		11 8	33						1	24		233	
4																														16.1	
	117												129																	333	
f ·	117			12									12											, 1						142	
7	117			12									125											. 7						708	
8	117			12									2											. 7						375	
_ 9	11/	, 5		12									24								12			. 7					7	563	
710	115	. 6		11									21											, 5					7	734	
11	117	. 4		11									23								7			. (7	750	
	119	10.00											35											. 0						952	
	119			13									3											, 8						117	
	116												19											. 4						292	
	116							11	9	. 4	17	1	21		74	2	1 2	22	:	7 9	2			,7						33	
	131																														
	110																							. 4						375	
	118												31											.4					7	92	
- 19	117	.3.	33 -	12	٠.	16	7	16	4	. 1	00	. 1	3.		10	13	12	27		41	7			.0					7	92	
20	117	. 2	00	11	7 :	54.	3	11	9	Γ,	00	1	21	i	16	7		3	. 1	٠.,	G			, 9					•	17	
	117																							, 8						50	
	120																														
	120																							, 2						50	
	116																							. 3					7	5=	
	115																							, 0						58	-
	113																							,7						58	
	110												14				11							, 2					7	50	
	116																													مر	
	115																:1							. 7					A SEC	25	
	115																													03	
	120																														
	120	.0	10	120	,'	12	;	1.3	1	5	nn	1	33	1	6	7	4 3	4	. 7	, 5	5			. 4						67	
	115																							, 3						8	
	1.4																														

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Table 5.3-2c. 12 IN. DIA TANK TEST 1G #33 (Page 2 of 2)
          114,667 113,425 113,083 112,792 112,500 112,208 112,167
 35
          121,250 130,792 133,042 134,917 136,500 138,042 138,833
 36
         116,917 117,000 117,417 118,250 118,917 119,625 120,042
 37
          116,917 117,000 117,833 118,750 119,458 120,375 120,750
 36
          116,792 116,917 118,167 119,292 120,250 121,292 121,792
          117,208 117,250 118,542 110,625 120,833 122,083 122,706
          117,125 117,125 118,623 119,917 121,208 122,667 123,500
 41
          117,208 117,250 118,750 120,000 121,292 122,792 123,667
 42
          116,708 117,250 118,033-120,125 121,375 122,958 123,667
          116,750 117,458 119,083 120,333 121,667 123,167 123,958
          117,208 117,292 118,750 120,083 121,333 122,792 123,563
         116,542 117,167 118,792 120,083 121,417 123,000 123,750
         117,375 117,458 118,833 120,167 121,375 122,833 123,667
          117,583 117,875 119,667 121,208 122,958 124,708 125,750
 48
         117,667 118,000 119,917.121,708 123,500 125,333 126,292
         117,708 118,125 120,208 122,167 124,042 125,958 126,792
50
          117,708 118,208 120,708 122,667 124,333 126,042 127,042
51
         117,500 118,125 120,792 122,563 124,417 126,000 127,083
          117,167 117,917 120,625 122,500 124,167 125,792 126,875
53
          117,417 118,292 120,917 122,833 124,500 126,167 127,167
54
         117,750-118-125-120,792-122,625-124,292 125,917 127,042
- 55
          117,375 118,107 120,792 122,542 124,333 126,000 127,042
56
          118,042 117,167 120,708 122,667 124,208 125,917 127,042
57
         117,625 118,542 121,417 123,167 124,667 126,250 127,250
58
          117,625 119,042 121,750 123,200 124,583 126,083 127,083
59
         117,708 119,875 122,833 124,500 126,000 127,542 125,625
60
         117,917-119,709 122,667-124,250 128,792 127,375 126,333
61
          117,958 119,625 122,667 124,542 126,042 127,708 128,667
62
          117,708 119,417 122,625 124,208 125,792 127,333 124,458
63
         117,708 118,033 121,750 123,458 125,000 126,500 127,750
          117,708 118,917 121,917 123,625 125,083 126,750 127,833
65
          117,667 118,542 121,250 122,833 124,250 125,958 126,958
66
         -117,667-118,542-121,250-122,833-124,250 121,958 126,959
67
          117,708 118,208 120,833 122,333 123,792 125,417 126,542
68
          117,750 118,333 120,792 122,333 123,792 125,500 126,500
69
         117,625 118,167 120,500 122,000 123,542 125,208 126,250
          117,625 118,167 120,500 122,000 123,542 125,208 126,250
71
          117,667 118,167 120,667 122,292 123,708 125,208 126,250
72
          117,667-118,208-120,625-122,000-123,542-125,083 126,167-
73
          95,625 95,375 95,667 95,708 95,583 95,667 95,917
74
          105,792 105,333 105,833 106,000 106,083 106,417 106,875
75
¥76
                          68,125 88,000 87,833 87,708 88,042
           88.042 87.750
                          98,917 99,000 99,083 99,250 99,583
           98,750 99,500
77
```

-TEMPERATURE MATRIX-STRATIFICATION

			•
TIME(MI	IN) 0.000 3.000 6.000		12.000 13.000
TAU	0.000 .231 .462	.615 .769	.923 1.000
1	114.875-115.958-117.458-	-118.833 120.542 1	22.250-123.125-
ž	115.417 116.875 119.000	120.875 123.125 1	25.083 126.083
3	116.292 117.792 120.375		26.083 126.875
4	117.083 118.917-121.292		26.292 127.042-
5			32.708 133.375
6	117.583 125.208 127.917		33.292 134.000
7			32.792-133.667-
B	117.792 125.333 127.750		32.917 133.583
9	117.375 121.833 124.667		30.042 130.875
10	115.333 116.792 118.875		24.958 125.958 -
11	116.792 118.708 121.042		26.000 126.750
12	117.750 130.958 133.708		39.000 139.792
13		-135.542-137.583-1	38.917-139.875-
14			21.958 122.875
15	115.375 116.875 119.000	120.875 123.167 1	25.208 126.042
16	116.958 118.917 121.167	- B. B. T.	26.167-126.917-
17	117.458 129.250 132.083		37.458 138.458
16	요즘 없는 그들은 사람이 있다면 가입니다. 이 사람이 없는 이 가게 되었다면 하는 것이 없다면 하는데 하는데 사람이 되었다면 하는데 되었다면 하는데 되었다면 하는데 없다.		35.417 136.042
19	117-167-121-417-124-083-		[[[[[[[] : [[[] : [[] : [[] : [] : [[] : [] : [[] : [] : [] : [[] : [] : [[] : [] : [[] : [] : [] : [] : [[] :
20			25.208 126.125
21	116.708 118.708 120.958		25,917 126,667
- 55 -	117.500-130.917-133.875		39.333 140.125
23	117.500 131.083 133.333	다른 (조건) 하게 하는 것을 하고 있는 것이 없었다. 그렇게 되는 사람들이 가장 보고 있는 것이 없는 것이 없는 것이 없는 것이 없는 것이다.	38.500 127.208
24	114.125 115.107 116.417		19,542 119,958
25	그는 사람들은 이 이 사람들은 이 아이들은 그는 사람들은 사람들은 사람들은 사람들은 사람들은 사람들은 사람들은 사람들은	B - '' '	17.208-117.542-
26	112.917 113.500 114.167	사이지를 하다. (1) 회사는 다른 이번 사이를 가득하고 하는 사람들은 사람들은 사람들이 하는 경기를 보고 있다.	15.542 115.708
27	112.458 112.417 113.000	H (2017년 - 1917년	13.542 113.417
88	113.958-114.458 114.875	이 마음이 가지 않는 것이 되었다. 그리고 있다면 얼마 없는 그는 그리고 있다. 그리고 있다면 그렇게 되었다면 그리고 있다.	16.750 117.0-2 -
29	113.708 114.250 114.792		17.000 117.292
30	113.833 114.958 116.167		19.353 119.792
31	117.542 131.000 133.208		38.292-139.042-
32	로마 그는 그는 얼마를 하고 있었다. 한국 회사 연락 전쟁에 있는 보다 그리고 생각되고 있다. 이루 시간에 살게 살게 먹는데 그리고 말라고 하는데 가지 않는데 살아 보다 보다.	133.375 135.208-1	경기 없는 사람이 되게 (사회)에 하이라면 있는 것이 되었다면 하게 되었다면 하는 것이 되었다면 하는데 하는데 그 없는데 그렇게 되었다면 하는데 하는데 하는데 그렇게 되었다면 하는데
33	115.625 120.750 122.542	요즘 마음 시민이 회에서 약 경영하는 대회 학생들은 다른 사 규칙에 대접 어디지면 하지만 내려는 이렇게 되었다.	26.625 127.333
34	115.333 115.333 115.292	[1] [7] [2] [2] [1] [2] [2] [2] [2] [2] [2] [2] [2] [3] [3] [4] [4] [4] [4] [4] [4] [4] [4] [4] [4	16.500 116.708
	BELTO TO SERVER SEE SEE SEE SEE SEE TE TO SEE TO SEE TO SEE TO SEE SEE SEE SEE SEE SEE SEE SEE SEE SE		

109

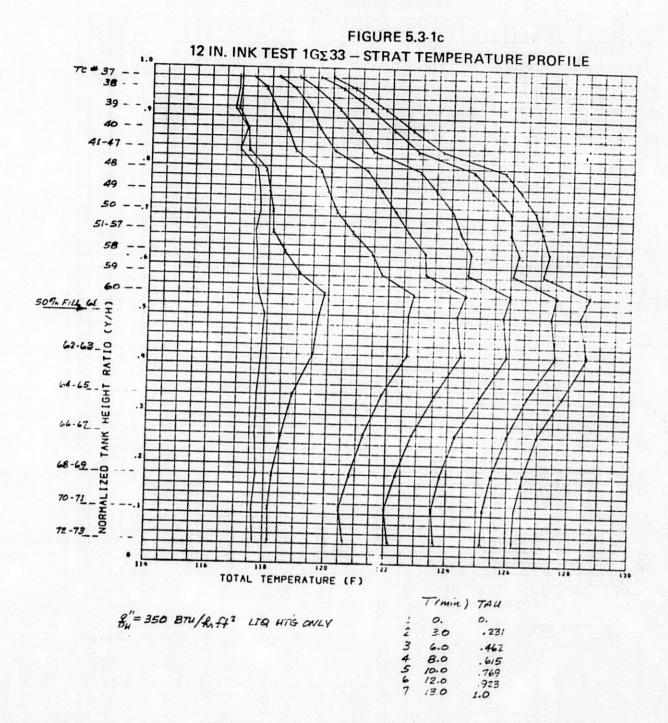
FIGURE 5.3-1a 6 IN. TNK TEST 8G 29S - STRAT TEMPERATURE PROFILE 4 47 -51-57 -59 60 -NORMALIZED TANK HEIGHT RATIO (YZH) TOTAL TEMPERATURE (F) T(m...)

0.
.667
1.333
2.
2.667 EN TOO BILL/ R. AZ LIQ HT'G ONLY

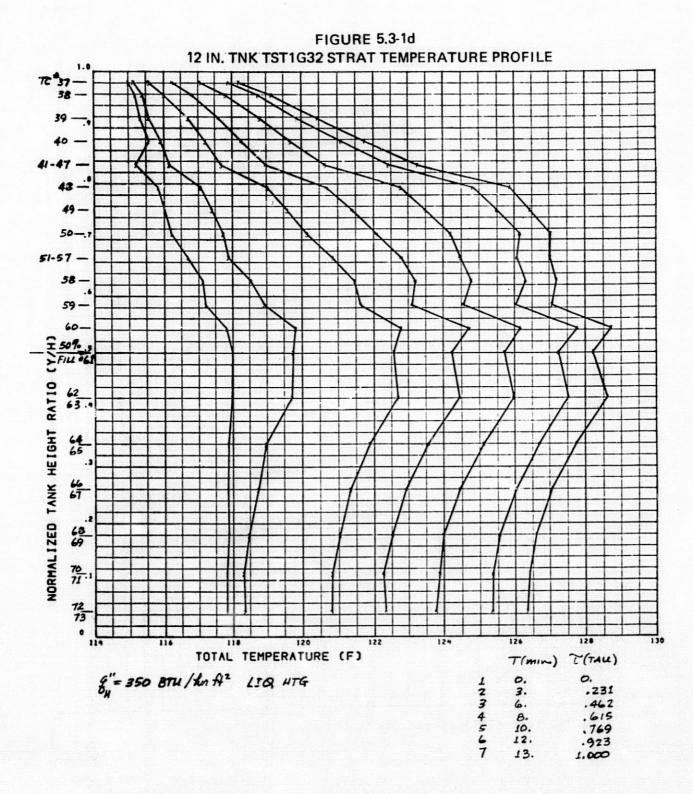
110

FIGURE 5.3-1b 6 IN. TNK TST8G15S STRAT TEMPERATURE PROFILE NORMAL IZED TANK HEIGHT RATIO (Y/H) 110 120 122 124 120 TOTAL TEMPERATURE (F) T(min) T(TAU) 9"= 700 BTU/ \$ fi LIQ HTG o. .833 0. .250 .600 .800 1.000 2.667 3.333

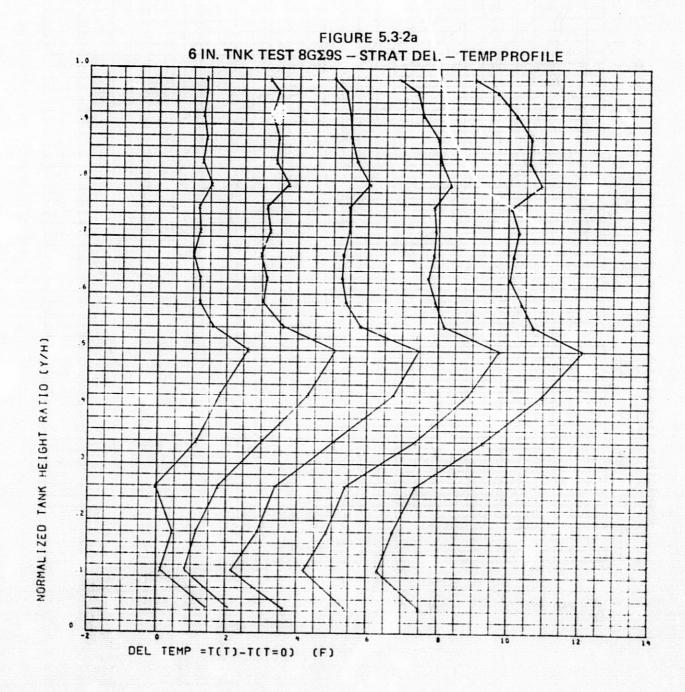
111

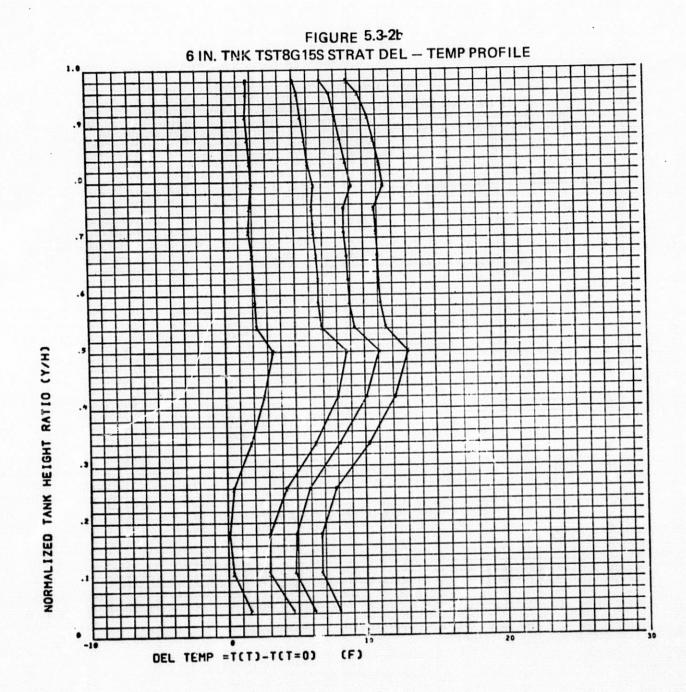


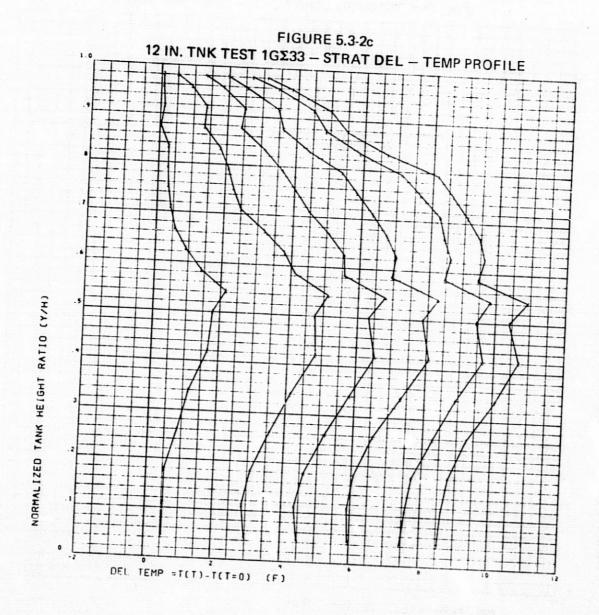
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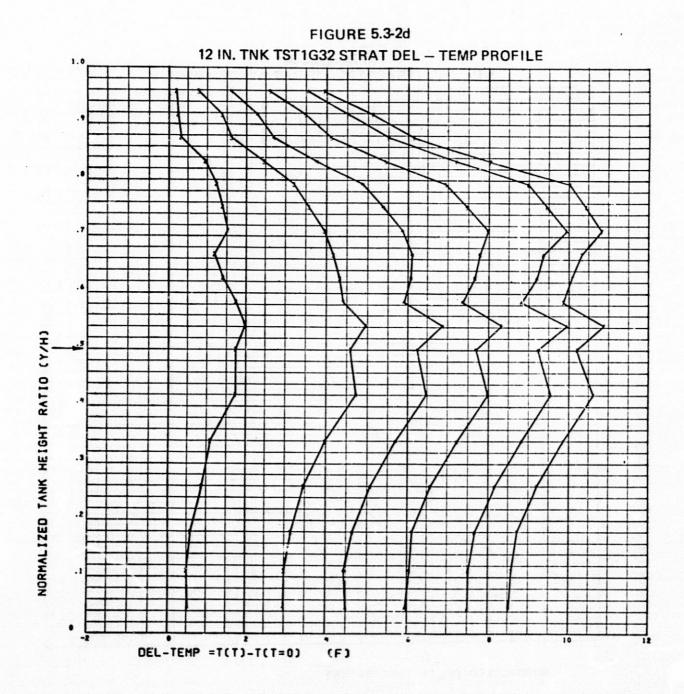


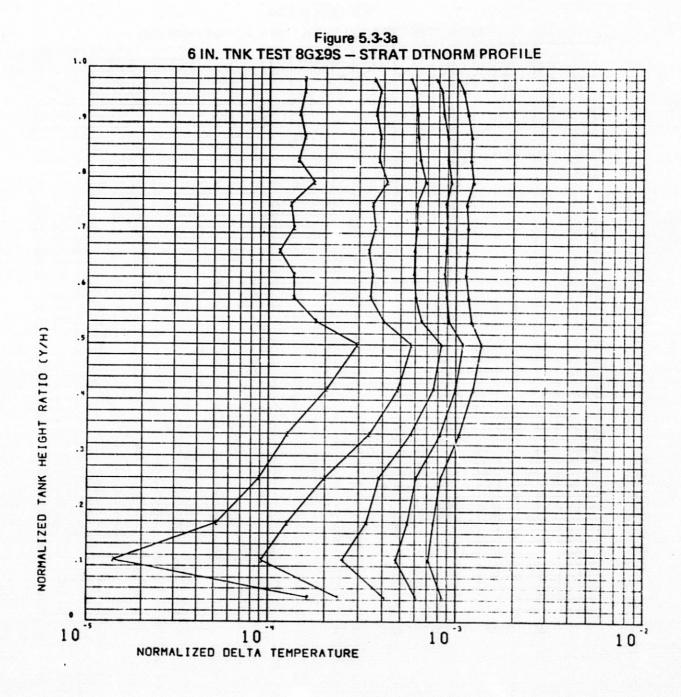
113

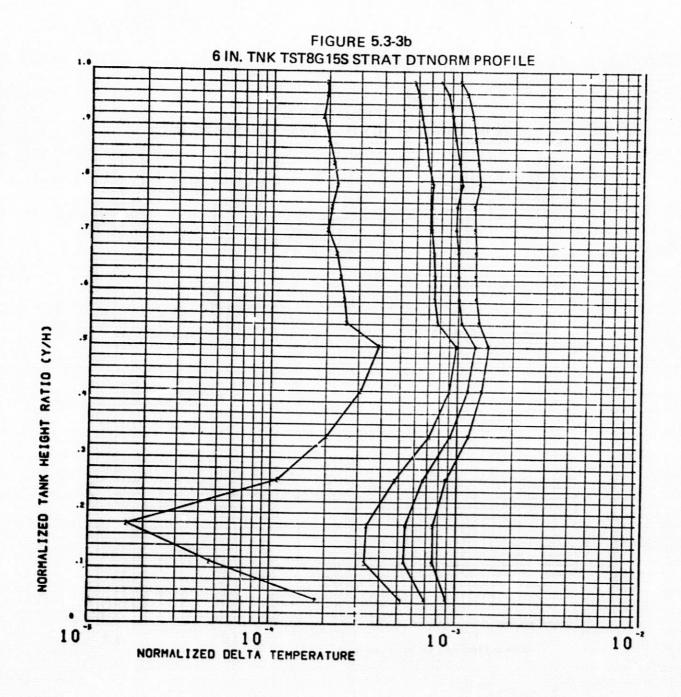


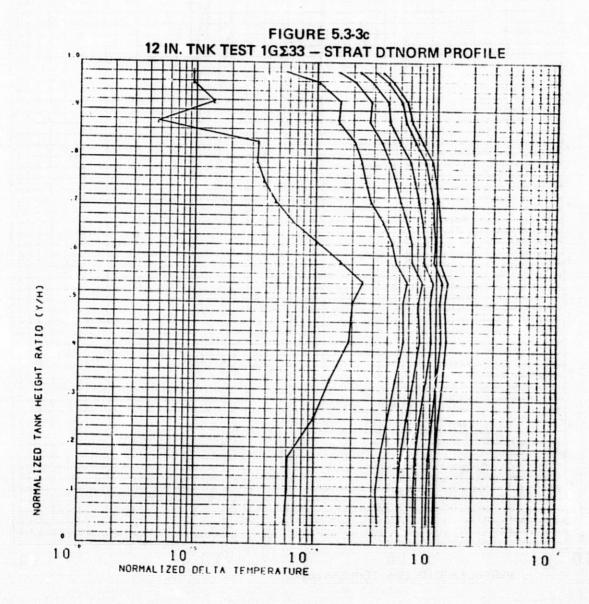


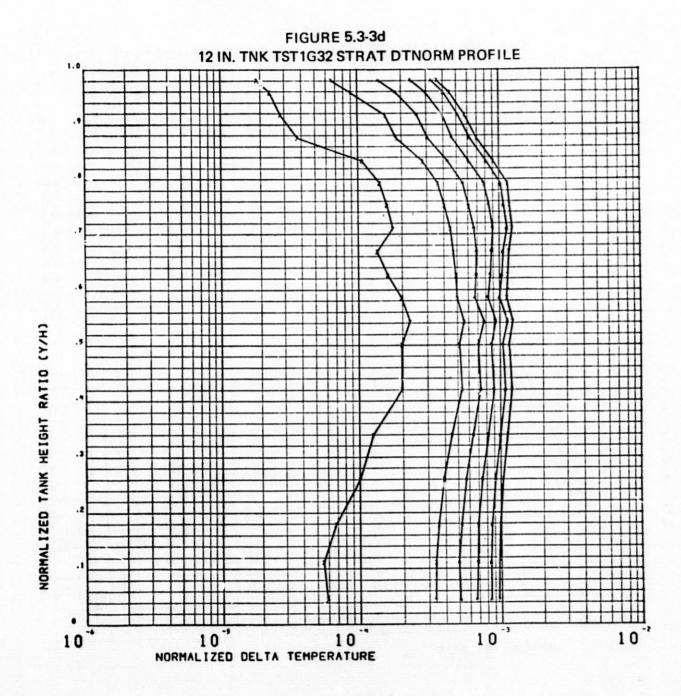


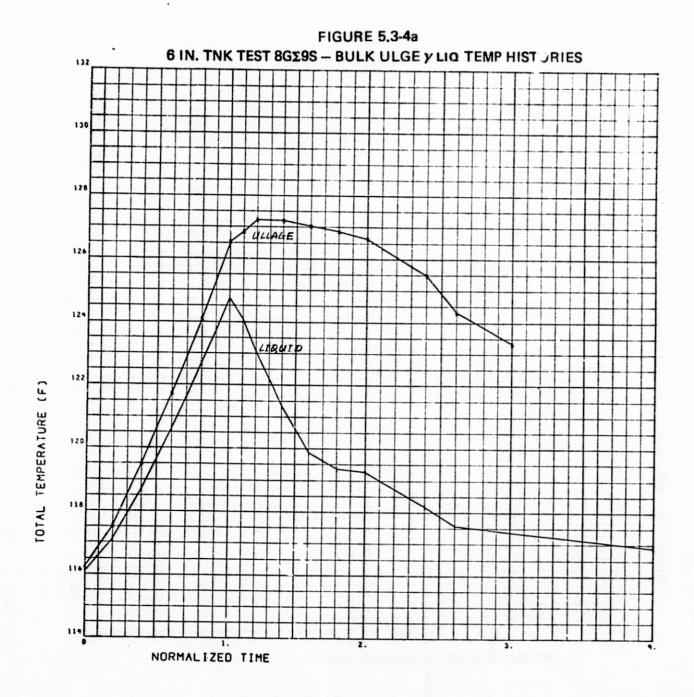




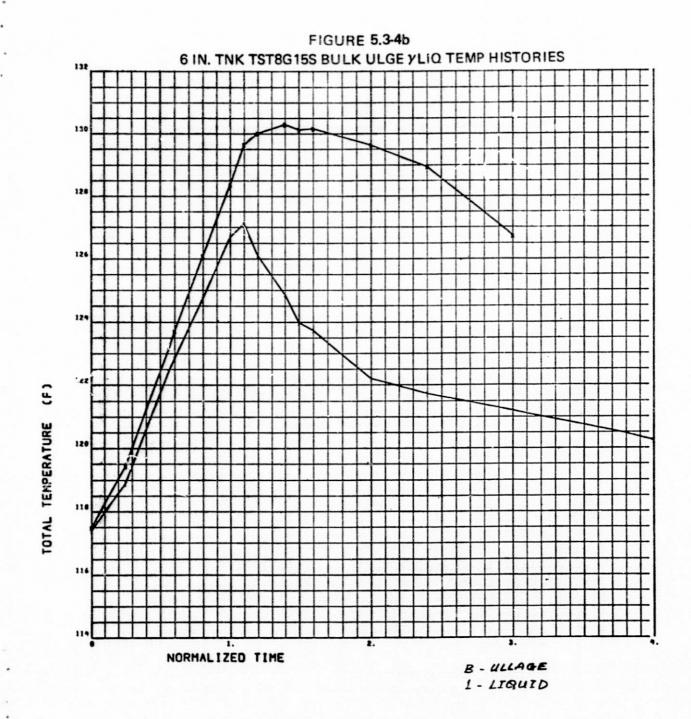


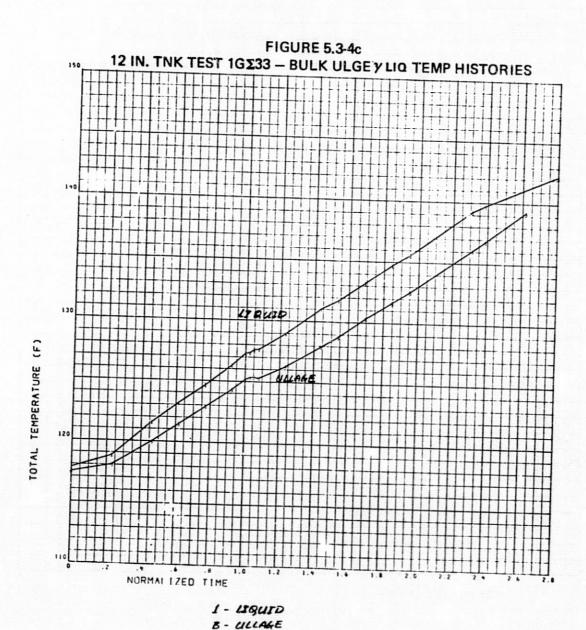




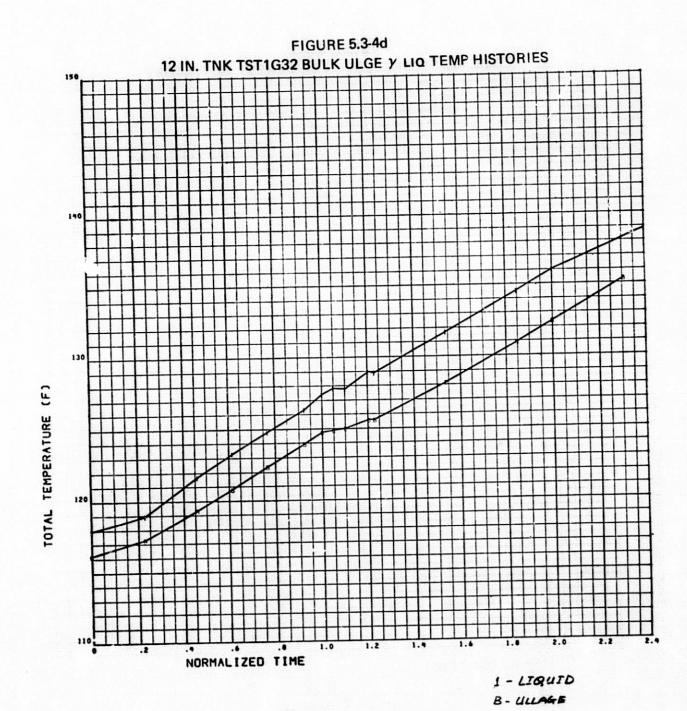


1 - LIQUID B - ULLAGE

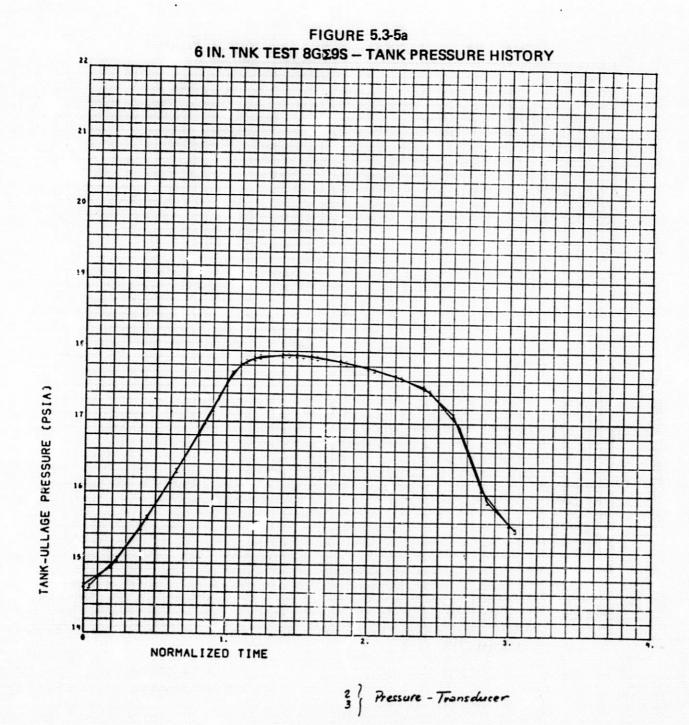


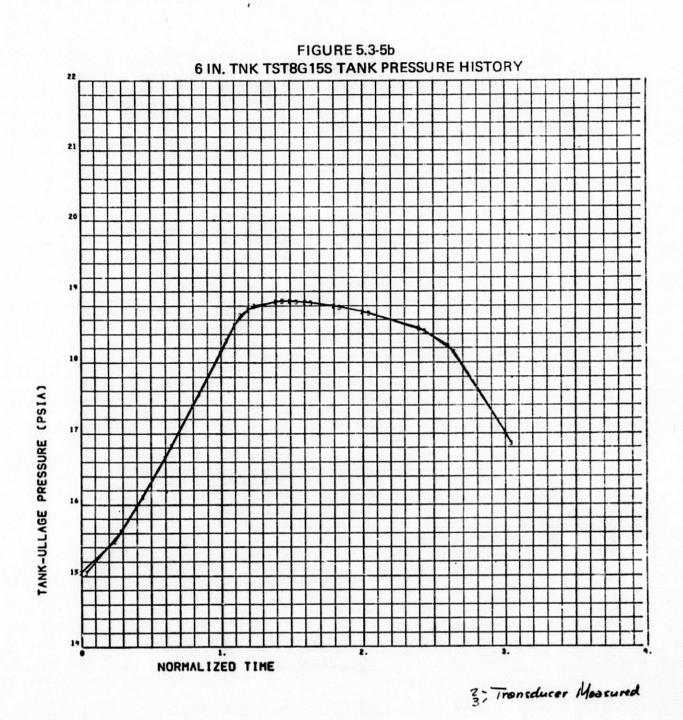


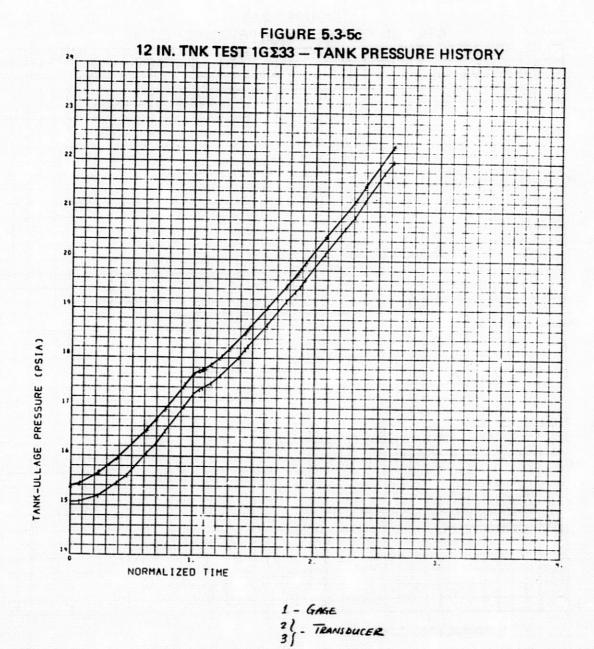
124

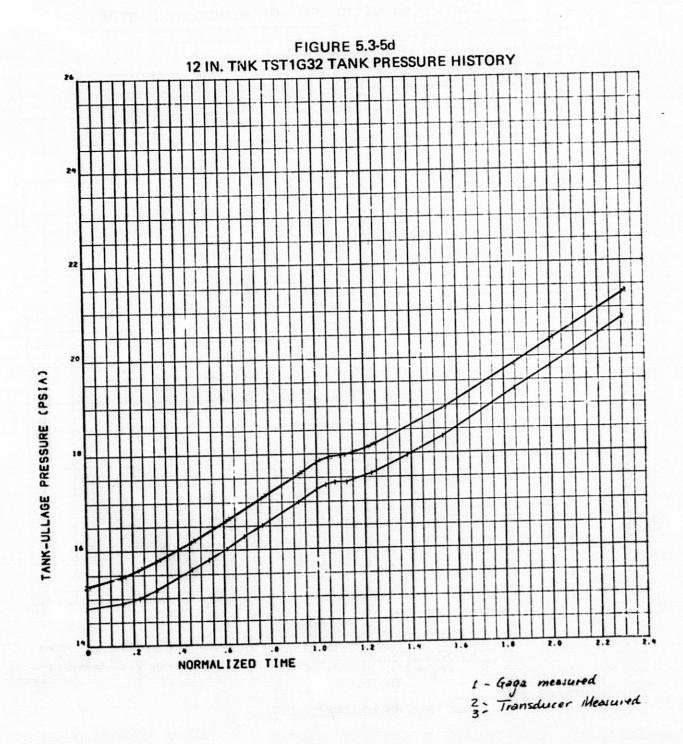


125

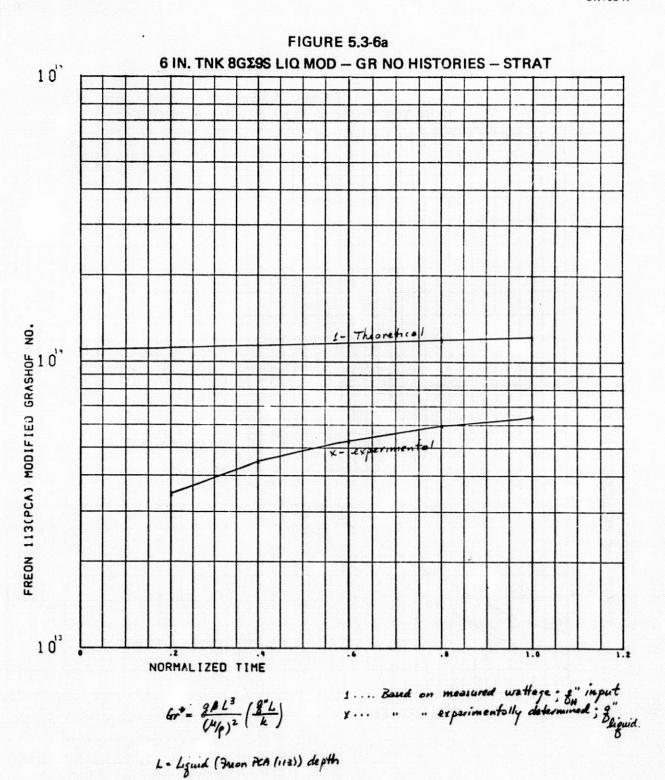


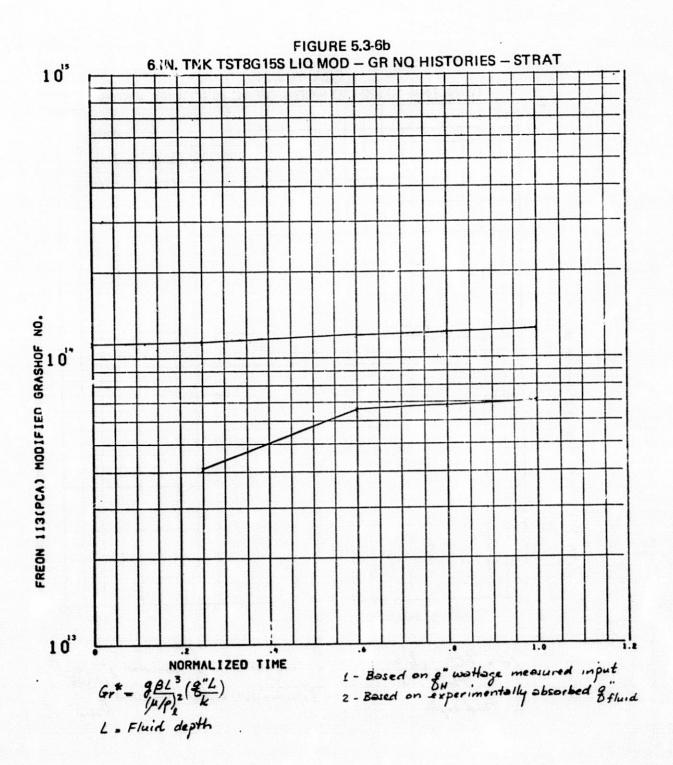




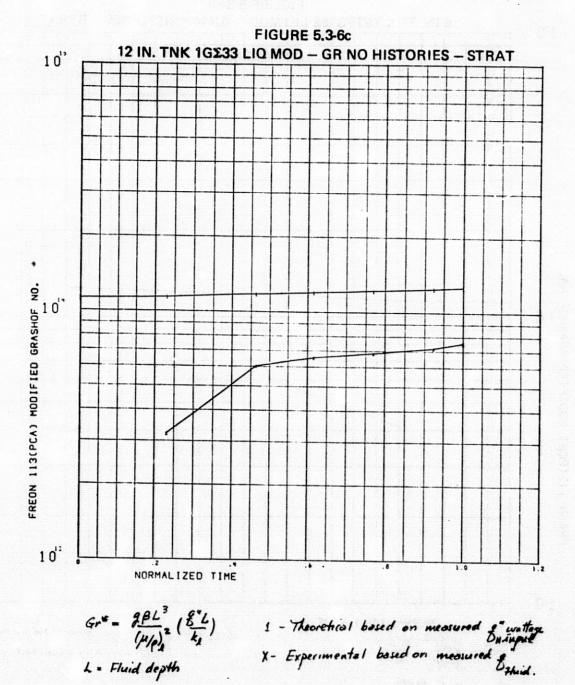


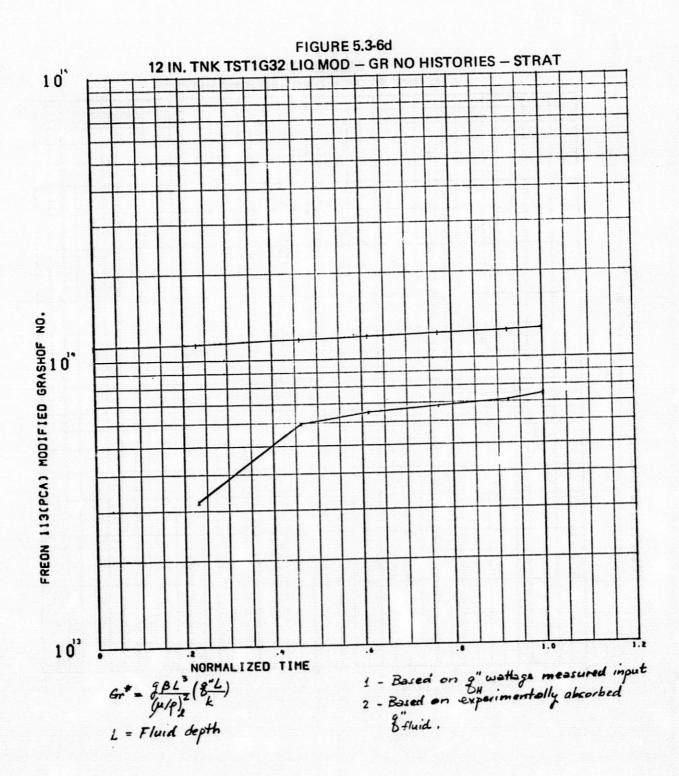
CR108-II

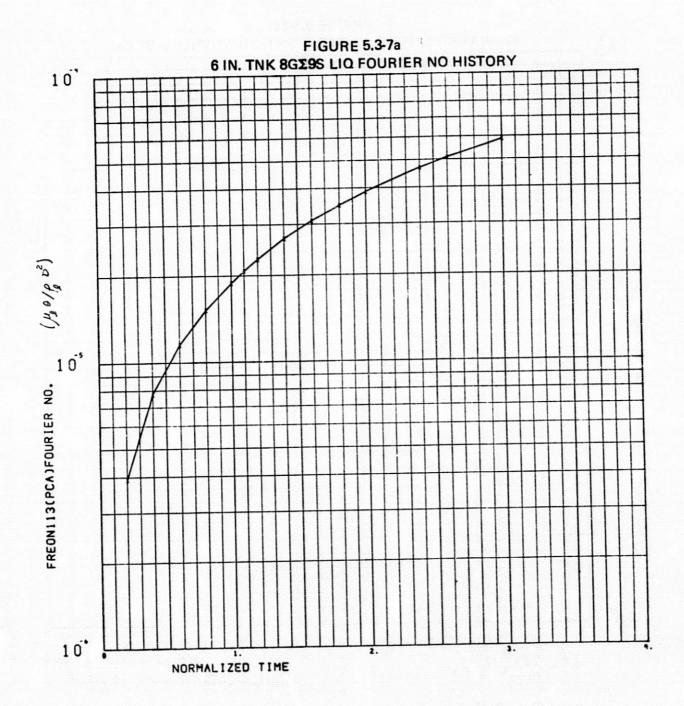


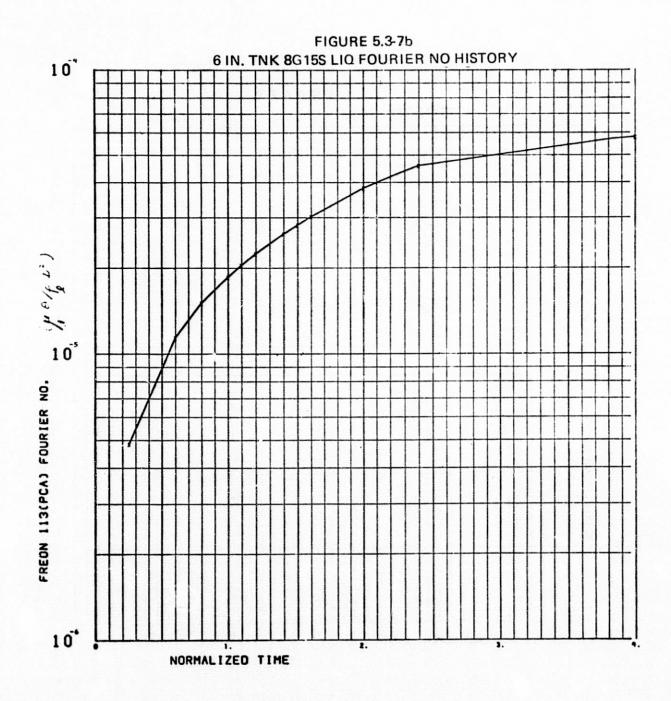


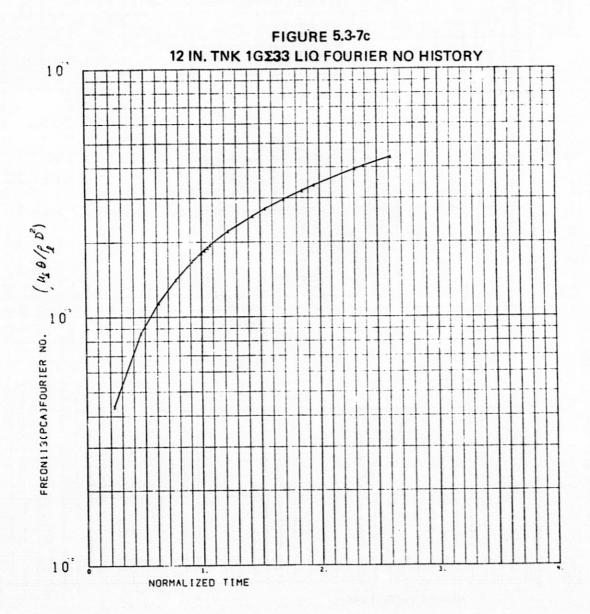
CR108-11

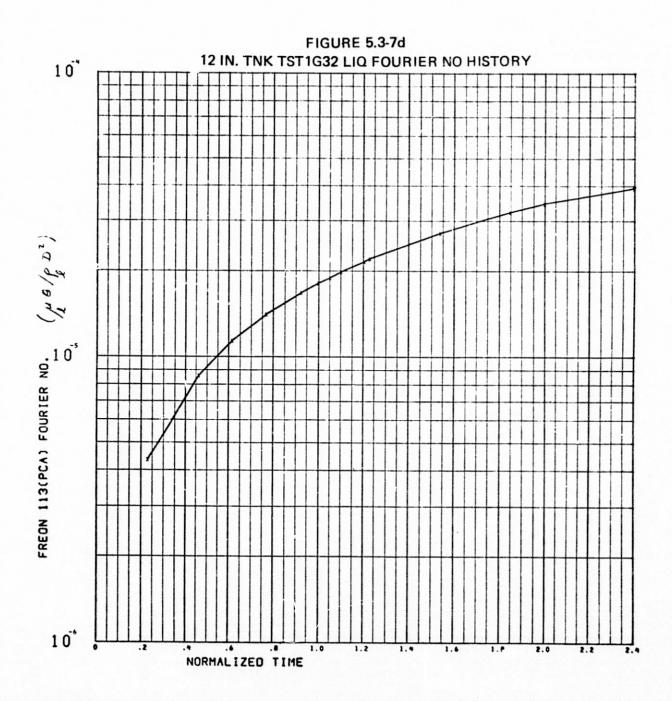












Section 5.4 SCALING SET

6-in Dia Tank Tests	12-in Dia Tank Tests
8G	1G
Test #16S	Test #34
Test #10S	Test #35

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Table 5.4-la. 6 IN. DIA. TANK TEST 8G#16S (Page 1 of 2) STRUCTURAL GEOMETRIC TANK WTS-WATTMETER HEAT FLUX INPUTS

DME MASS LBMI	165596	MASS 1/2 CYL	LBM= .81996	LFUNGE	MASS# 138056	
LIO VOL FT3	12090	ULLAGE VOL F	T3# 113090			•
INPUT HEAT	LUXES (BTU/HR	R-FŢŻ),ĀNŅ ĀBSO	REED HEAT AND	TEMPERATUR	RE ESTIMATES -	
H12= 701.5691	H34= 701.5	691	.,5691 H910#	701,5691	H78= 701,5691	
		FT2) - 7011569				
EST. HT FLUX I	LIG(STRAT)RTU	HR*FT2)# 701.5		AT)BTU=	0.000	
		1115470F			1 0 0 0 0 F	
			4655.5.5	CTRATIOTHE	0.000	
EST HT INPUT	ULLAGE (STRAT)	BTU: 32,142	(STRAT+DE	SIKA I / BIU-	0.000	
	Tal	ble 5.4-1b. 6 IN	DIA. TANK T	EST 8G#10S		
STR	Tal UCTURAL GEOME	ble 5.4-1b. 6 IN TRIC TANK WIS- CYL AREA FY	DIA. TANK T. WATTMETER HEA	EST 8G#10S T FLUX INP FLNGE AR	UTS EA FT2= .0365	-0007
STR DOME AREA FT DME WALL VOL	Tal UCTURAL GEOME 2= .3927 FT3# .00131	ble 5.4-1b. 6 IN TRIC TANK WIS- CYL AREA FY	DIA. TANK TO WATTMETER HEAD	EST 8G#10S T FLUX INP FLNGE AR .00164	UTS	.00076
STR DOME AREA FT DME WALL VOL	Tal UCTURAL GEOME 2= .3927 FT3# .00131 .65596	CYL AREA FY 1/2 CYL W MASS 1/2 CYL	DIA. TANK T. WATTMETER HEA 2= 1.5708 ALL VOLFT3= LBM= .81996	EST 8G#10S T FLUX INP FLNGE AR .00164	EA FT2= .0365 FLNGE VOL FT3=	.00076
STR DOME AREA FT DME WALL VOL DME MASS LBM= LIG VOL FT3=	Tal SUCTURAL GEOME 2= .3927 FT3# .00131 .65596 .13090	CYL AREA FY 1/2 CYL W MASS 1/2 CYL	DIA. TANK TO WATTMETER HEAD TO SERVICE TO SE	EST 8G#10S T FLUX INP FLNGE AR .00164 FLANGE	EA FTZ= .0365 FLNGE VOL FT3= MASS= .38058	.00076
STR DOME AREA FT DME WALL VOL DME MASS LBM= LIG VOL FT3= INPUT HEAT F	Tal UCTURAL GEOME 2= .3927 FT3# .00131 .65596 .13090 LUXES (BTU/HR	TRIC TANK WIS- CYL AREA FT 1/2 CYL W MASS 1/2 CYL ULLAGE VOL F FT2), AND ABSO	DIA. TANK TO WATTMETER HEAD 22 1.5708 ALL VOLFT3= LBH= .81996 T3= .13090 RBED HEAT AND	EST 8G#10S T FLUX INP FLNGE AR .00164 FLANGE	EA FTZ= .0365 FLNGE VOL FT3= MASS= .38058	.0007
STR DOME AREA FT ME WALL VOL ME MASS LBM= LIQ VOL FT3= INPUT HEAT F H12= 701.5691	Tal UCTURAL GEOME 2= .3927 FT3# .00131 .65596 .13090 LUXES (BTU/HR H34# 701.5	CYL AREA FT 1/2 CYL W MASS 1/2 CYL W LLAGE VOL F FT2), AND ABSO 691 H56= 701	DIA. TANK T. WATTMETER HEA 22 1.5708 ALL VOLFT3= LBM= .81996 73= .13090 RBED HEAT AND .5691 H910=	EST 8G#10S T FLUX INP FLNGE AR .00164 FLANGE TEMPERATUR	EA FT2= .0365 FLNGE VOL FT3= MASS= .38058	.0007
STR DOME AREA FT DME WALL VOL DME MASS LBM= LIO VOL FT3= INPUT HEAT F H12= 701.5691 EST.HT FLUX I	Tal UCTURAL GEOME 2= .3927 FT3# .00131 .65596 .13090 LUXES (BTU/HR H34# 701.5	CYL AREA FT 1/2 CYL W MASS 1/2 CYL W ULLAGE VOL F -FT2), AND ABSO 691 H56= 701	DIA. TANK T. WATTMETER HEA 2= 1.5708 ALL VOLFT3= LBM= .81996 T3= .13090 RBED HEAT AND .5691 H910=	EST 8G#10S T FLUX INP FLNGE AR .00164 FLANGE TEMPERATUR 701.5691	EA FT2= .0365 FLNGE VOL FT3= MASS= .38058	.0007

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Table 5.4-1c. 12 IN. DIA. TANK TEST 1G#34 (Page 2 of 2) STRUCTUPAL GEOMETRIC TANK WIS-MATTMETER HEAT FLUX INPUTS

GYL AREA FT2=			EA FT2= ,1458	
1/2 CYL WALL			FLNGE VOL FT3=	.00608
ULLAGE VOL FT3:	1,04720			
FT2) AND AFSORGE	ED HEAT AND	TEMPERATUR	E ESTIMATES	
04 H56= 349,48	322 H910#	350,3504	H78= 350,3504	
FT2)= 349.7716				
R-FT2)= 350,3504				
247,239 (8	STRAT+DESTR	AT)BTU= 35	6,271	
			,4362F	•
TU= 247.648	(STRAT+DE	STRATIBIU=	_366,877	
1	MASS 1/2 CYL LAN ULLAGE VOL FT3: FT2).AND APSORGE 04 H56: 342.48 FT2): 349.7716 R=FT2): 350.3504 247.239 (S 11,1007F	MASS 1/2 CYL LRM= 6,55965 ULLAGE VOL FT3= 1,04720 FT2):AND APSORBED HEAT AND 04 H56= 342,4822 H910= FT2)= 349.7716 R=FT2)= 350,3504 247,239 (STRAT+DESTR 11,1007F (STRAT+DES	MASS 1/2 CYL LRM= 6,55965 FLANGS ULLAGE VOL FT3= 1,04720 FT2).AND APSORGED HEAT AND TEMPERATUR 04 H56= 349,4822 H910= 350,3504 FT2)= 349.7716 R=FT2)= 350,3504 247,239 (STRAT+DESTRAT)BTU= 36 11,1007F (STRAT+DESTRAT)= 16	MASS 1/2 CYL LRM= 6,55965 FLANGE MASS= 3,04465 ULLAGE VOL FT3= 1,04720 FT2).AND APSORGED HEAT AND TEMPERATURE ESTIMATES 04 H56= 349,4822 H910= 350,3504 H78= 350,3504 FT2)= 349.7716 R=FT2)= 350,3504 247,239 (STRAT+DESTRAT)BTU= 356,271

Table 5.4-1d. 12 IN. DIA. TANK TEST #35 STRUCTURAL GEOMETRIC TANK WIS-WATTMETER HEAT FLUX INPUTS

DOME AREA FT2= 1,5703 CYL ARE DME WALL VOL FT3= ,01047 1/2 C DME MASS LBM= 5,24772 MASS 1/2	YL WALL VOLFT3=	FLNGE AREA FT2= , .01309 FLNGE VOL FLANGE MASS= 3.0	FT3= .00608
LIQ VOL FT3= 1.04720 ULLAGE V	OL FT3= 1.04720		
INPUT HEAT FLUXES (STU/HR-FT2), AND	ABSORBED HEAT AND	TEMPERATURE ESTIMATES	3
H12= 350,3504 H34= 350,3504 H56=	349,4822 H910=	350,3504 H78# 350,3	3504
EST.HT FLUX IN LIQ (BTU/HR-FT2)= 349 FST.HT FLUX IN ULLGE (PTU/HR-FT2)= 3			
ESTINT INPUT LIG(STRAT)BTU= 247.239 ESTILIG TEMP [NCRSE(STPAT)= 11.101	(STRAT+DESTR	AT)BTU# 476,163 TRAT)# 21,3619F	
EST, HT INPUT ULLAGE (STRAT) BTU= 247.	648 (STRAT+DE	STRAT)BIU= 476,951	

TIME(HI	N) 0.000	, 333	,667	1,333	1,667	2,000	2,333
TAU	0.000	1143	1286	1571	1714		000
1	116.333	118.042-	23.125-	135.458-	142,167-1	48.058	6.425-
2	116.542	122.667	37.125	164.667	177,667 1	80 768 20	1 200
3	116.625	121.583	34 208	164.792	175,625 1	99 700 20	11200
4	116.917	122.702	76 777	142.447	173,025 1	041/45 50	11420
5	116.708	120 077	136 147	10%100	174,500 1	041411 14	4,/08
6	446 975	120,000	20.107	1951450	135,458 1	38:042 14	0,958
7	110.075	121 1220 1	501503	101171/	133,750 1	35,542 13	7,500
8	-11/-000-	121+4/9-3	201333-	1301750-	133,125-1	34,917-13	6,750-
	11/1125	121,708 1	26,083	1291583	132,500 1	34,292 13	6.000
9	110,000	117,8/5 1	19.917	122.292	123.542 1	24.917 12	6.500
-10		120+4PB1	44-3/2-	1/4+333-	188.292.2	D4-587-24	4-282-
11	116.250 1	129.000 1	45.292	73.875	186,458 1	97.790 00	0.200
12	117.458	26.375	30.708	35.292	137,250 1	70 047 20	01200
13	-116-750-	25.000 1	20 042	34 447	13/12/01	301717 14	0,242
14	115 047	47 700	271072	1911001-	132,917-1	33,958-13	5,295-
15	112,917	11/1/00 1	20.242	1011/20	137,042 1	12.208 14	7,875
15	110.10/	20,91/ 1	31.000	1531417	164,583 1	75,417 18	6,083
-16	11-0+270-1	121-0-2-1	32-503-	-54+10/-	164-542-47	74-467-48	7-667
17	110./00]	122.044 1	30.615	43.885	150.021 15	55.60R 46	1.344
18	112:/00 1	17,8/5 1	23.333	26.875	128.75n 13	30.417 43	1.375
19	112+200-1	10-428-1	18-10/-	20.750-	22.n49_12	27-425-424	4-549-
20	116.167 1	28,458 1	44.375	74.333	88,292 20	14 . 583 24	1.202
21	116.250 1	29.000 1	45.292	73.875	86,458 19	77 700 20	11676
22	117.458-4	26-175-1	30-708	35.292	37-250-13	7 7 7 7 200	1200
23	116.750 1	25.000 1	39 643	34.447	70 047 47	101717-140	11242
24	116.292 1	29 017 1	47 076	60 777	32,917 13	3,758 135	1245
25	110,5,5 1	47 050 1	4010/2	001333	79,125 18	9 208 199	,000
	1101000 1	17,900-1	201/00-1	201420-1	29,625-13	3-750-139	,583-
26	110.021 1	1/,000 1	20.41/ 1	25,958 1	28.854 13	12.274 136	. 583
27	110.042 1	17,700 1	20.125 1	25,458 1	28.n83 13	10.790 437	. 587
28	-110+41 /-1	14-545-1	22-792-1	32-1250-1	37-750-14	3-875-150	1375
29	110,000 1	23,420 1	30.503 1	44.333 1	51.125 15	7.917 164	-667
30	116,542 1	34.667 1	52.5nn 1	83.042	96.417 20	8.587 220	447
31	-117-014-1	24.764 1	28.083	29.500	20 754 47	0 450 170	40.
32	117.625 1	25 775 4	20 000 4	70 467	27/20-13	01420-131	1044
33	117.625 1	17 000 1	27.000 1	30110/ 1	30,41/ 13	1.042 132	.083
34	115.083 1 112.000 1	1/:000 1:	19,000 1	21:10/ 1	21.708 12	2.250 123	.167

.

	Table 5.4-2a. 6 IN. DIA TANK TEST 8G #16S (Page 2 of 2)
35	108,250 108,583 109,125 110,292 110,833 111,542 112,417
36	116,708 124,458 127,625 129,107 129,417 130,167 131,500
37	116.583 120.042 124.458 140.458 149.333 158.208 167.792
38	116.667 118,458 121,917 129,458 140,792 149,417 158,000
39	116,792 118,583 121,333 128,833 133,750 143,000 149,125
40	117.042 118.792 122.708 130.208 135.125 140.375 145.958
41	116,667 118,500 121,125 128,292 131,708 136,042 142,250
42	116,917 118,792 121,958 130,1875 137,000 146,375 154,042
43	117-125-118-792-122-375-1301458-134-792-145-167-152-167-
44	117, 375 119, 083 122, 083 129, 292 137, 375 145, 208 153, 458
45	117.083 119.083 122.542 1301542 138,083 145,792 154,500
-46-	116.833 119.667 123.042 132.583 142.292 151.333 161.000
47	117,542 122,500 129,042 147,292 157,750 167,917 178,792 116,396 118,104 121,375 129,021 132,604 136,708 145,833
48	
49	116,667 118,042 120,917 128,750 132,500 136,375 146,958
50	116.417 117.917 120.833 127.917 132.167 136.167 147.917
51	116.41/ 11/191/ 1201633 12/191/ 132/1083 136:000 144:458
52	11/100 110//00 121/21 1201120 1021000 100/000 144/42
53	116.083 117.750 120.375 128.708 133.792 137.417 147.792 117.708 119.500 122.208 128.333 132.000 135.833 141.000
54	117,760 119,560 122,200 1281333 132,000 133,033 1411003
55 56	117.708 119,500 122,208 128,333 132,000 135,833 141,000
57	117.583 119,292 122,875 130,458 134,333 139,917 148,917
58	116-292-117-958-120-750-128-625-132-875-136-708-144-917
59	117,292 119,167 121,667 128,333 131,958 135,250 139,625
	118.708 120,583 123,208 128,500 131,417 133,875 136,833
60	-116,042-117,042-118,625-122,292-124,667-125,833-128,333-
62	116,083 116,875 118,625 121,250 123,125 124,583 126,458
63	117,125 117,708 120,000 122,625 124,875 126,083 127,792
64	118.333 118.042 120.292 1221458 123,792 124.500 126.792
65	115.917 115.750 116.708 1191042 120,583 121.875 123.500
66	116.083 115,875 116,458 118,250 119,167 119,833 121,292
67	116.833-116.625-117.292-1191208-120,125 120,667 122,250
68	117.917 117.625 117.958 118.625 119.633 120.458 122.000
60	115,792 115,583 116,042 116,792 118,000 118,542 117,833
¥ 70	115,917 115,750 116,250 1171042 117,675 118,500 120,042
71	146.333 116.417 116.750 117,583 118,375 119,042 120,458
72	116.958 117.583 118.375 119.208 120.167 121.208 122.542
73	
74	108,917 109,208 110,333 112,917 115,167 117,333 120,542
75	95.917 96.125 96.792 97.708 98.417 98.875 100:167
76	105,208-105,167-105,458-105,917-106,500-106,797-107,667-
77	91.208 91.125 91.208 901958 901792 90,708 90.917

TIME (MI	N) 0.000	.333	666 1.00	0 1,333	1,666	2,000	
TAU	0.000	.143 .285		.571	.714	857	1.000
ī		18.417 120.9		131.083	136,333 1	41.583	146.667
- ż		24.792 139.2		스 시에 없는 것 같아요. "이 보이지 않아요. 이 중에 나를 다 되었는데 없다"는 것 같아.		90.917	201.042
3	117.833	23.125 135.6				88.792	200.417
4	117.833	23.917 136.7	08 149.875	162.375	173.792 1	84.292	193.792
5	117.250	21.167 126.0	83 129.417	132,583	135.583 1	38.250	140.792
6	117.542	21.500 126.4	158 129.667	131.833	133.667 1	35.625	137.083
7	117.625	21.917 126.5	63 128.792	130.604	132.896 1	34.750	136.000
8	117.700 1	22.333 126.6	67 127,917	129,375	132.125 1	33.875	134.917
9	116.333	118.000 119.8	375 121.000	122.042	123.458 17	24.792	125.958
10	116-792	29.333 144.2	250 159.417	173.375	186.792 1	99.583	211,333
11	117.000	30.125 145.6	67 160.333	173,375	185,208 1	96.083	205.792
12	117.917	26.667 130.5	642 133,083	135.125	137,083 1	38,625	139,917
13	117.250	25.167 128.7	192 130.667	131.458	132,500 1	33,667	134.792
14	116.500	18.417 120.9	17 125.000	131.083	136.333 1	41.583	146.667
15	116.750	21.708 131.4	117 142.333	153.083	164,000 1	74.500	184,125
16	117.042	22.625 133.1	25 144.250	154.833	165.083 1	74.625	183,542
17	117.542	21.500 126.4	58 129.667	131.833	133,667 1.	35,625	137.083
18	116.375	20.042 123.5	42 125.208	126,917	128,917 13	30.167	131.083
19	115.750	16.917 118.2	50 119.708	120.625	122,000 18	23.208	124.375
20	116.792		50 159.417	173.375	186.792 19	99.583	211.333
21	117.000 1	30.125 145.6	67 160.333				
55	117.917	26.667 130.5	42 133.083	135.125	137.083 13	38,625	139.917
23	117.250 1	25.167 128.7	92 130,667	131,458	132,500 13	33,667	134,792
24	116.792	28.083 140.8	75 153,583	165,167	176.250 18	36,583	195.792
25	116.583		75 124.417	127,333	130.500 13	33.708	136.875
26	116,563	18,583 121.0	63 124.021	126.813	129,792 13	32,896	135.875
27	116.542	18.417 120.7	50 123.625	126.292	129.083 13	\$2.083	134.875
28		19.542 122.6	67 127.000	131.875	137.458 14	13.458	149,583
29		22.542 129.1	67 135,958	142.667	149.542 1	56,417	163.000
30	116.792 1	32.208 148.4	58 164.583	179.167	192.792 20	5,125	216.458
31	116.667 1		63 128,979				
32	117.167	24.375 127.4					
33	115.208 1	16.667 118.5	42 120.167	120,917	121.542 17	22.167	122.792
34	113.208 1	13.458 114.3	33 115.167	115.792	116.708 1	17.375	117.833

Table 5.4-2c. 12 IN. DIA TANK TEST 1G #34 (Page 1 of 2)
TEMPERATURE MATRIX-STRATIFICATION

117,292 125,458 130,292 140,417 150,917 162,6 117,290 135,083 148,000 172,917 195,458 216,6 117,417 136,417 149,375 175,125 193,625 219,4 117,500 136,750 147,583 165,333 170,833 189,6 117,792 125,542 127,625 130,875 133,708 136,3 117,708 124,083 125,458 127,833 130,083 132,0 117,875 124,375 125,417 127,208 128,917 130,7 117,833 124,083 125,417 127,208 128,917 130,7 117,453 120,033 121,875 124,883 124,000 127,7 10 117,250 147,500 161,000 185,250 208,750 230,7 11 17,333 146,250 158,083 177,083 191,625 203,4 117,958 120,542 131,250 133,583 135,958 138,1 117,750 130,500 131,750 133,208 136,500 145,5 117,167 144,167 150,250 163,667 171,500 180,7 117,433 141,667 152,333 168,250 180,500 190,4 117,625 127,958 129,708 132,167 134,417 136,5 117,542 126,833 128,083 129,917 131,792 133,58 117,250 146,792 157,792 175,250 188,750 199,40 117,1250 146,792 157,792 175,250 188,750 199,40 117,125 132,125 137,042 150,958 150,977 166,62 117,125 132,125 137,042 150,958 150,977 166,92 117,125 132,125 137,042 150,958 150,977 166,62 117,125 132,125 137,042 150,958 150,977 166,92 117,125 132,125 137,042 150,958 150,977 166,92 117,125 132,125 137,042 150,958 150,977 166,92 117,125 132,125 137,042 150,958 150,977 166,92 117,125 132,125 137,042 150,958 150,977 166,92 117,125 132,125 137,042 150,958 150,977 166,92 117,125 132,125 137,042 150,958 150,977 166,92 117,127 120,500 123,000 128,500 134,083 139,48 117,042 125,977 131,292 143,083 155,708 168,83 117,042 125,977 131,292 143,083 155,708 168,83 117,042 125,977 131,292 143,083 155,708 168,83 117,042 125,977 131,292 143,083 155,708 168,83 117,042 125,977 131,292 143,083 155,708 168,83 117,042 125,977 131,292 143,083 155,708 168,83 117,042 125,977 131,292 143,083 155,708 168,83 117,042 125,977 131,292 143,083 155,708 168,83 117,042 125,977 131,292 143,083 155,708 168,83	.000
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1	1	116	.20	8 1	44	667	1 1	56	292	17	1.1	67	190	0.0	42	202	2.8	75	
1	2	117	, 45	8 1	28	708	1	30	292	132	2.4	58	134	1,5	83	136	5.9	17	
	3		25			833			708					5,9		13	5 . 8	75	
	4								917										
	5		.62			167			375					0.0		23	73.0 M. COST		
	6		.37			917			250	170			184			19	100000		
1	7								917										
	8		08			583			667				13(13			
•	9		.66			917			875				12			120			
	ó								375				212			23	300		
	1		. 29			333			375					1,1		199	1 1000000		_
																137	A The Colors		
	2		. 20			208			375				134		20	0.000			
	3		. 25						292							13	The state of the state of		-
	4		,66	3.59 M. P. S. T. T.		000				155				, 9	TO 15	17:			
	5		.50			500			917				140			147			
	6								458										_
	7		,95	100	STATE LAND	583			333	128	The State of the State of	District Control	134	A 11 11 11 11 11 11 11 11 11 11 11 11 11		140			
	A		,54			565				155			173			193			
	9	The state of the s	IN WITH THE THE						667							167			
3	0		.91			292			042				192			212		STATES OF STATES IN	
3	1	117	. 41	7 1	29	125	1	30 .	250	131	7	80	133	. 12	25	135	. 0	42	
	2								833							133	1.3	75	_
3	3	113	.00	0 1	17	583	1	18.	875	120	.2	6 0	121	,58	33	123	. 0	0 a	
3	4		.37													112	. 4	58	

Table 5.4-2d. 12 IN. DIA TANK TEST 1G #35 (Page 2 of 2) 110.333 109.875 109.542 109.042 108.708 108.625 35 117,833 129,542 130,417 131,958 133,500 135,250 36 37 116,083 125,458 133,625 153,125 173,750 195,042 38 116.250 123.125 128.583 144.792 160.750 178.542 39 116.292 120.042 122.750 131.667 145.875 159.500 40 116,500 120,250 123,375 131,458 144,208 157,292 116,292 119,833 122,625 128,417 135,875 144,917 41 116,000 120,042 122,833 130,042 144,500 158,667 42 43 116.250 120.042 122.792 129.208 138.167 158.042 116.333 120.292 123.125 129.875 146.083 159.792 44 45 116,333 120,125 122,958 130,292 144,250 157,667 46 116.083 120.167 122.875 128.917 135.083 155.625 47 116.250 120.208 123.000 134.250 148.833 164.167 48 116,542 120,292 123,043 129,458 137,458 153,875 116,417 120,208 122,979.129,750 137,979 153,437 49 50 116.292 120.125 122.875 130.042 138.500 153.000 51 116,208 119,667 122,667 128,500 134,708 141,250 52 116,125 119,833 122,833 129,417 140,000 153,625 53 116,042 119,667 122,708 128,875 135,917 152,218 54 116,333 119,958 122,917 129,167 136,917 153,125 55 116.292 119.792 122.750 129.083 137.958 152.033 56 116,292 119,833 122,792 128,750 136,250 150,033 57 116,125 119,792 122,750 129,625 142,333 156,125 58 116,583 119,917 122,875 129,042 136,203 145,833 116,667 117,667 122,708 128,708 135,250 142,833 59 117,042 119,458 121,292 124,333 127,750 131,167 60 117,333 118,792 119,875 122,083 124,417 126,875 61 62 117.417 118.458 119.500 121.667 123.833 125.875 63 117,208 118,208 119,458 121,417 123,625 125,667 64 117.083 117.917 118,958 120.750 122,667 124,542 65 117,208 117,917 119,042 120,750 122,750 124,583 117,069 117,653 118,583 120,181 121,931 123,667 66 67 117,125 117,667 118,542 120,083 121,792 123,542 68 117.000 117.375 118.250 119.708 121.333 122.917 69 117,125 117,542 118,333 119,792 121,458 123,042 117,042 117,375 118,181 119,611 121,236 122,792 70 71 117.083_117.292_118.083_119.542_121.125_122.667 72 117.042 117.458 118.208 119.583 121,250 122,792 73 117,042 117,458 118,292 119,458 121,167 122,750 ¥ 74 94,708 94,833 95,292 96,000 96,917 98,167 75 105,208 105,875 106,956 109,292 112,542 116,250 76 85.083 85,208 A5,583 85,667 85,708 85.708 77 95.792 96,167 96,333 96,625 96,875 95.750

CR 108-11

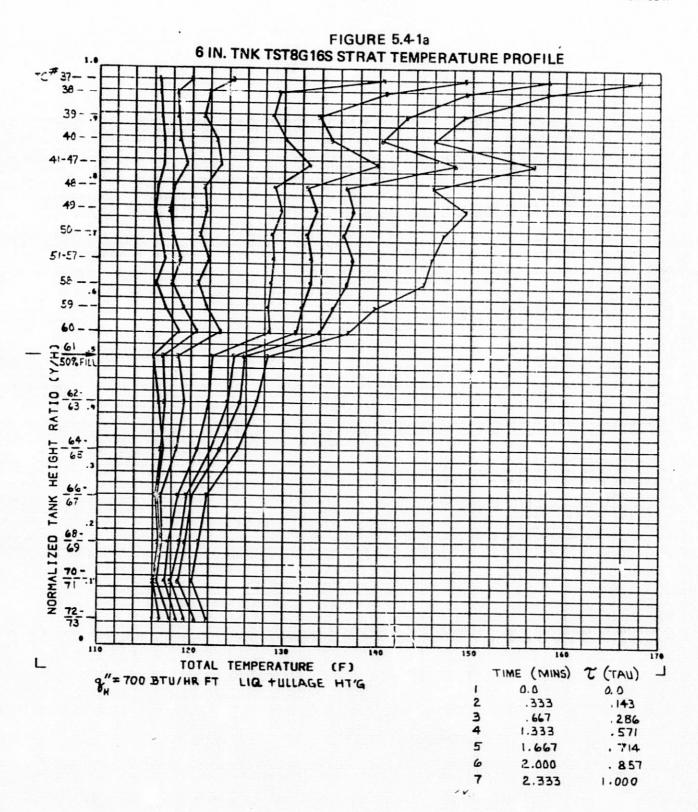
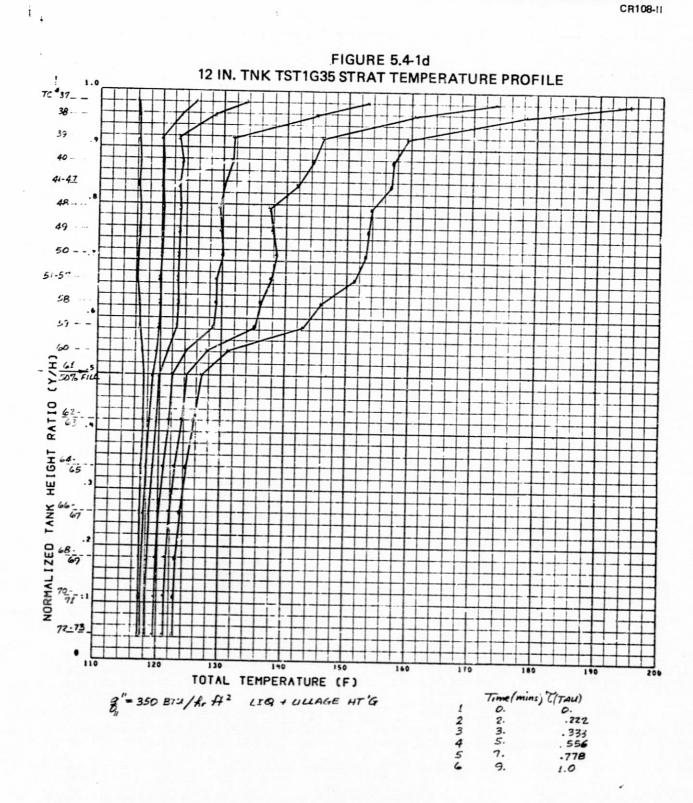


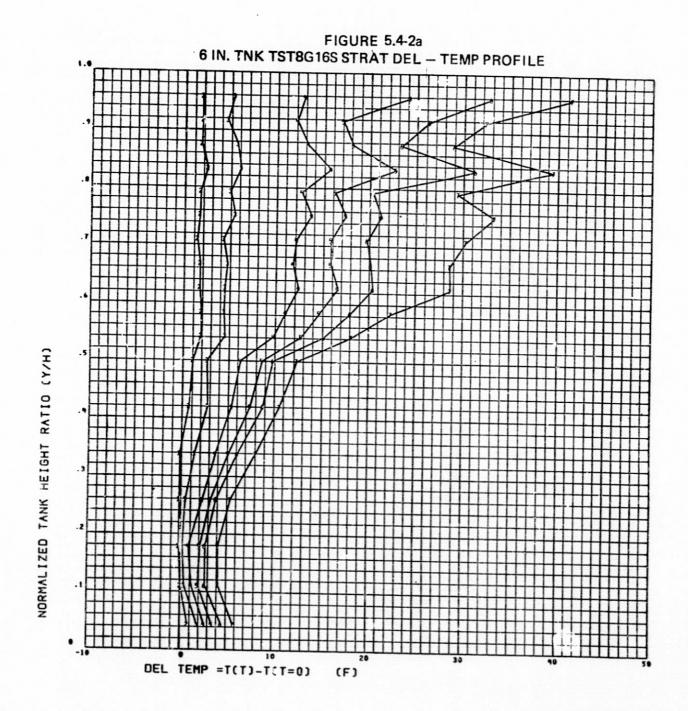
FIGURE 5.4-1b 6 IN. TNK TEST 8GΣ 1 OS-STRAT TEMPERATURE PROFILE NORMALIZED TANK HEIGHT RATIO (YZH) TOTAL TEMPERATURE (F) T(min) TAU .143 .285 .429 .571 .714 0. g"= 700 BTU/fL ft LIQ + ULL AGE HT'G 1. 1.333 2.333

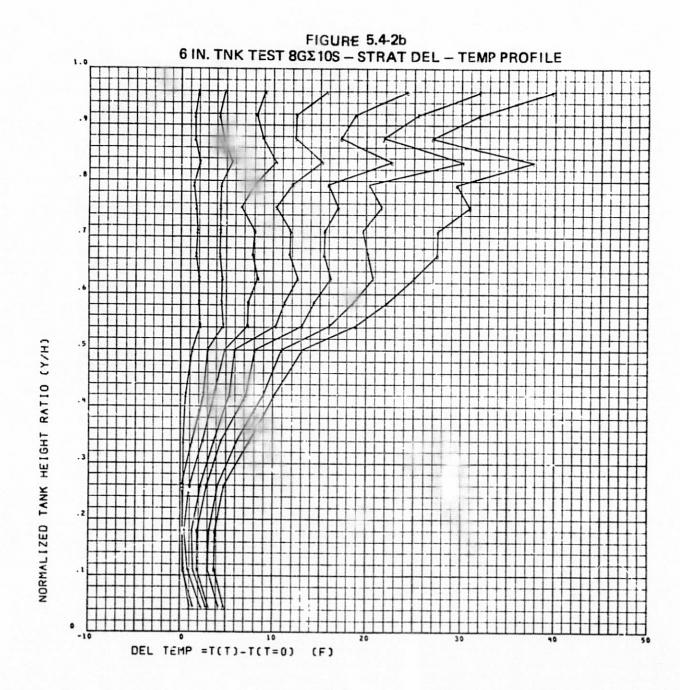
151

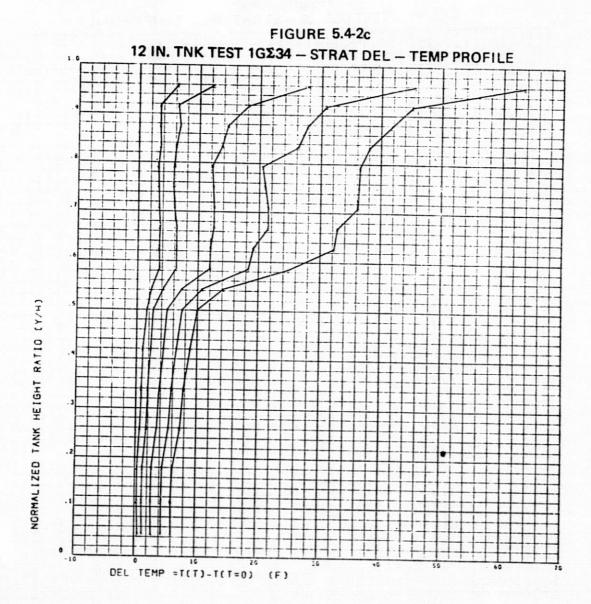
Figure 5.4-1c 12 IN. TNK TEST 1G\$34 - STRAT TEMPERATURE PROFILE TC #37 64-65_-H TOTAL TEMPERATURE (F) Time (min.) TAU 9"= 350 BTU/h ff2

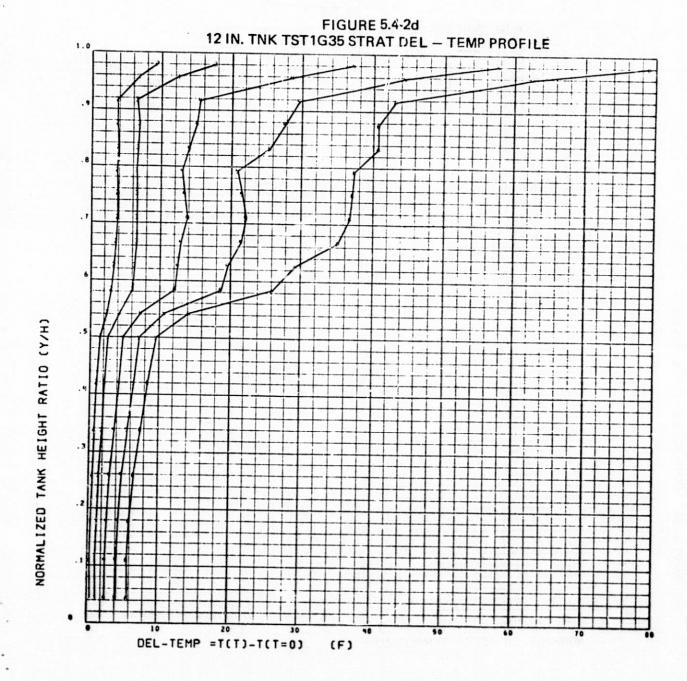
CH LIQ+ULLAGE HT'G .778

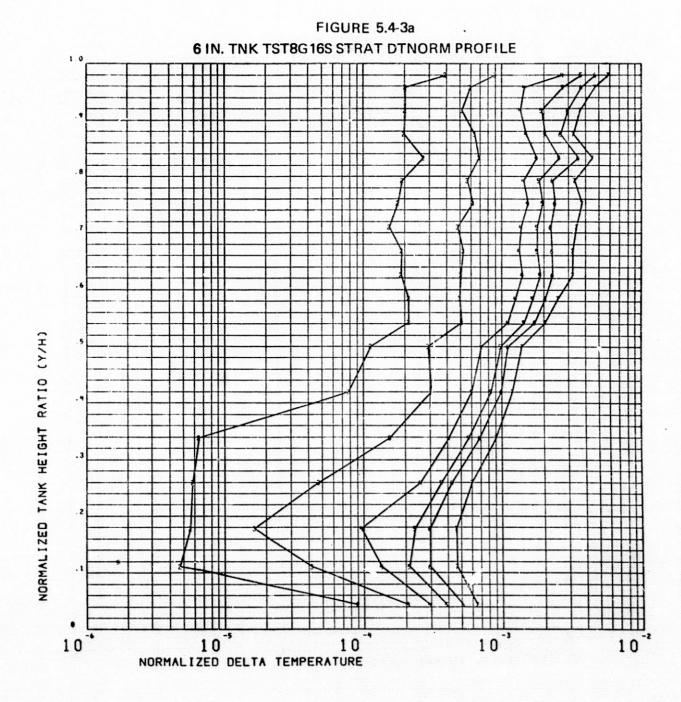


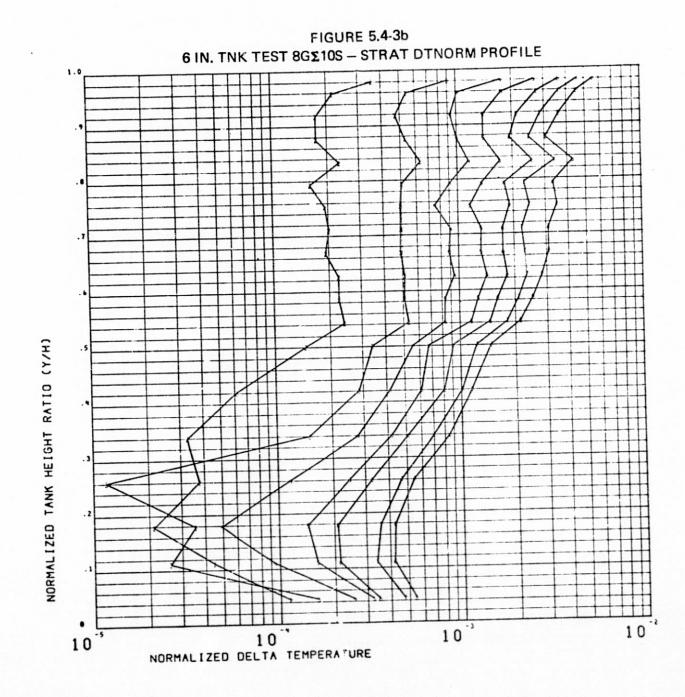


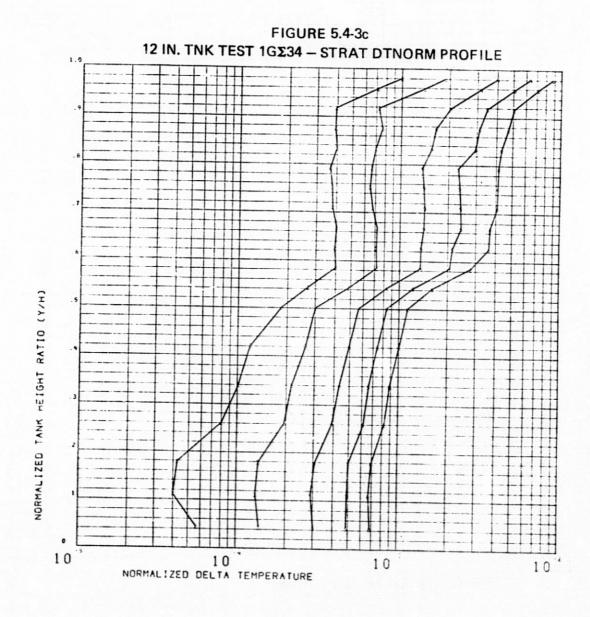


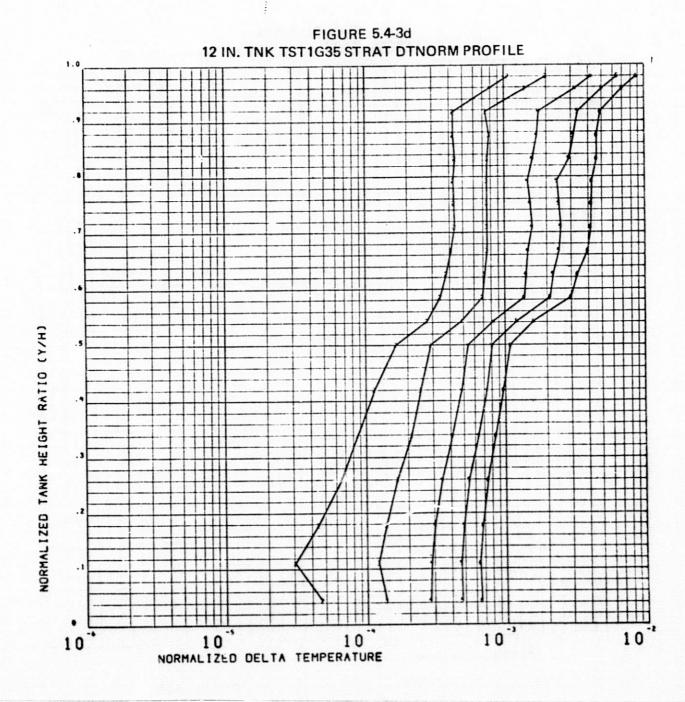


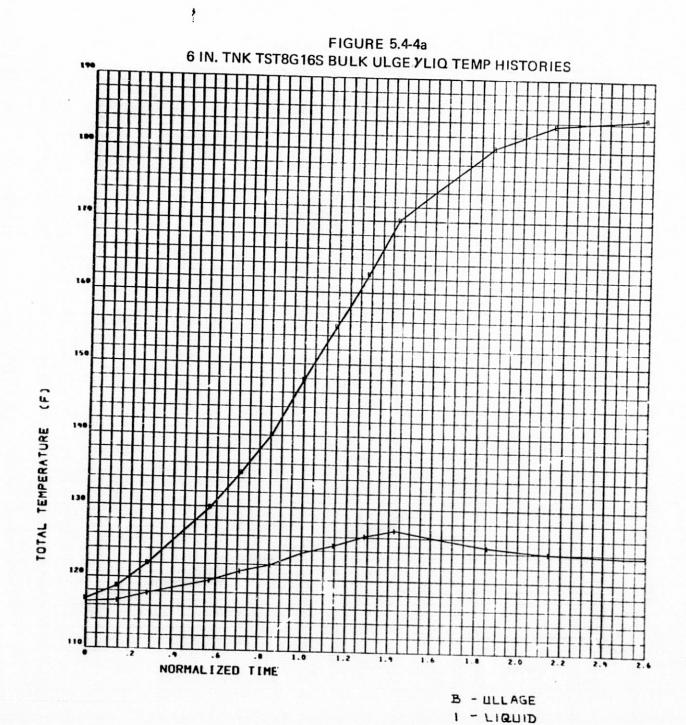




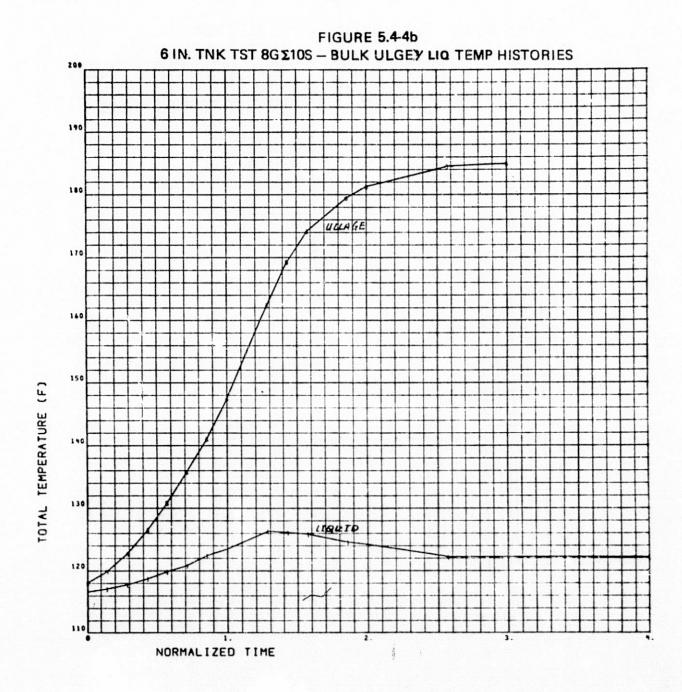








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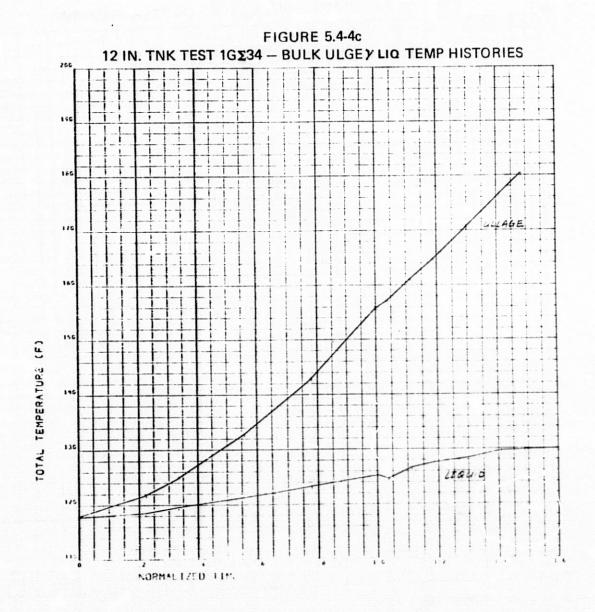


FIGURE 5.4-4d 12 IN. TNK TST1G35 BULK ULGE Y LIQ TEMP HISTORIES 210 200 180 170 160 TOTAL TEMPERATURE (F) 150 130 120 NORMALIZED TIME B - ULLAGE 1 - LIQUID

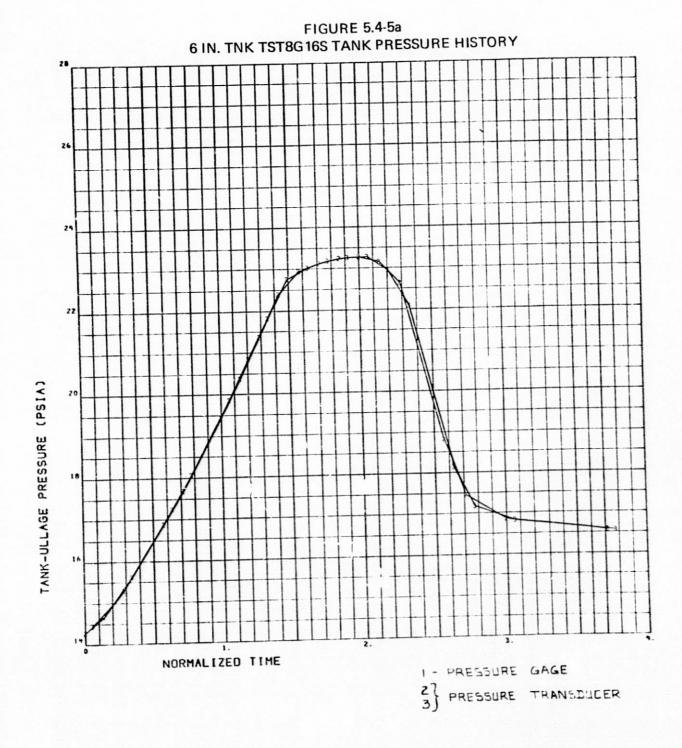
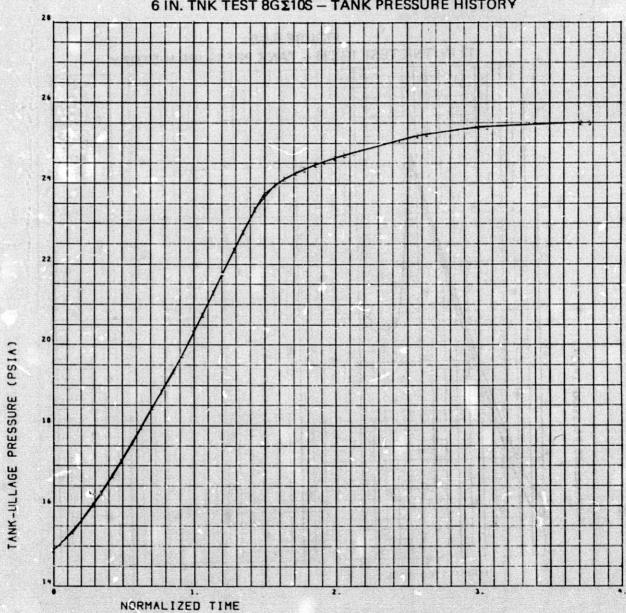
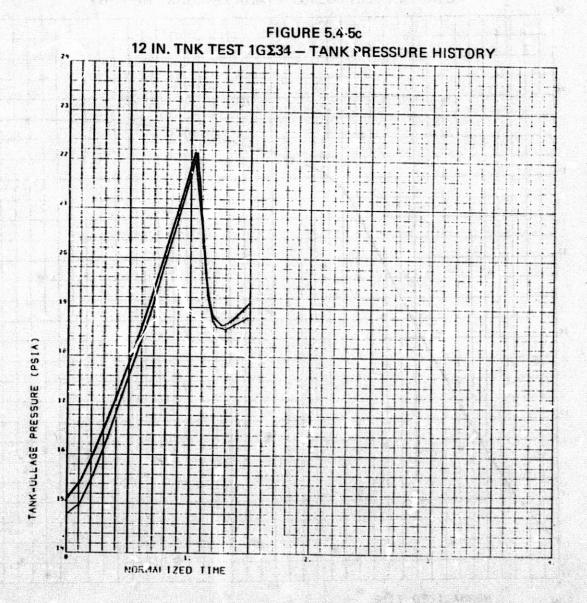


FIGURE 5.4-5b
6 IN. TNK TEST 8G∑10S — TANK PRESSURE HISTORY



2 Pressure - Transdurer

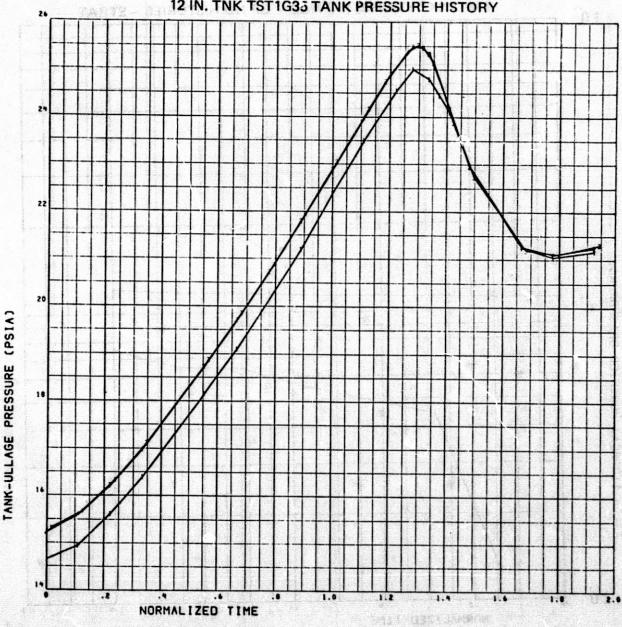
(1)



GALTE

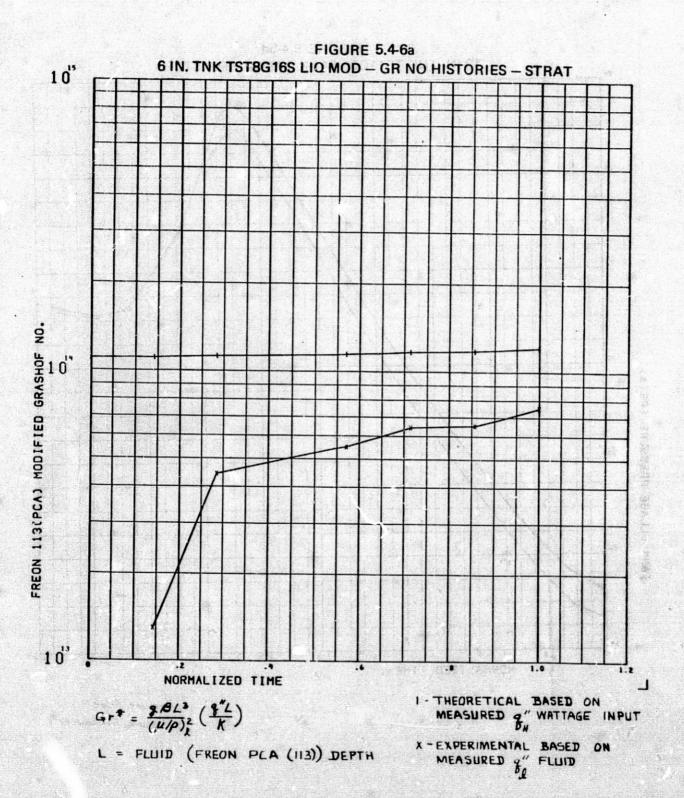
- TRANSDUCER

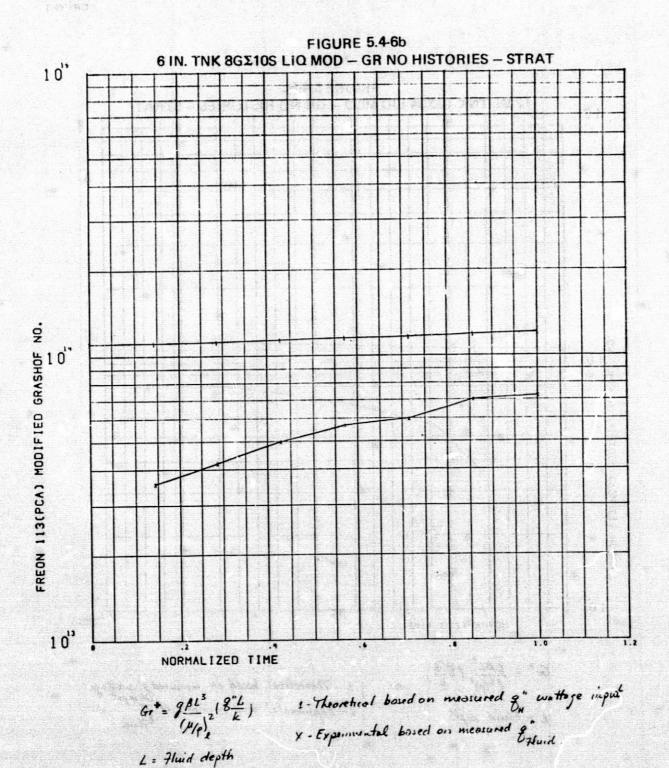
FIGURE 5.4-5d 12 IN. TNK TST1G33 TANK PRESSURE HISTORY

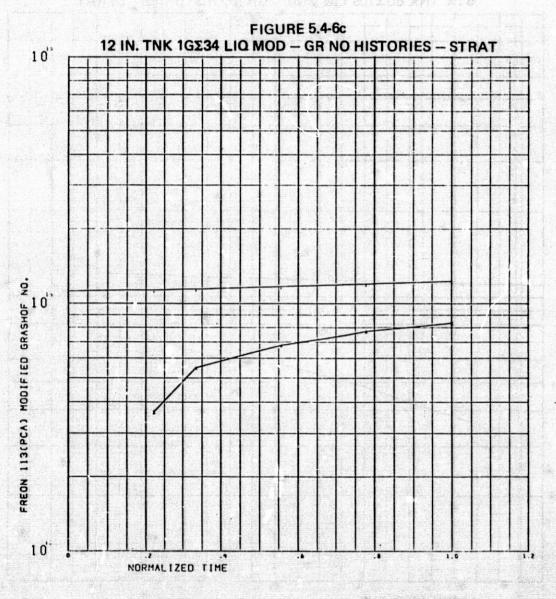


1 - Pressure Goga: 2 > Pressure Transducer

The Company of the Co

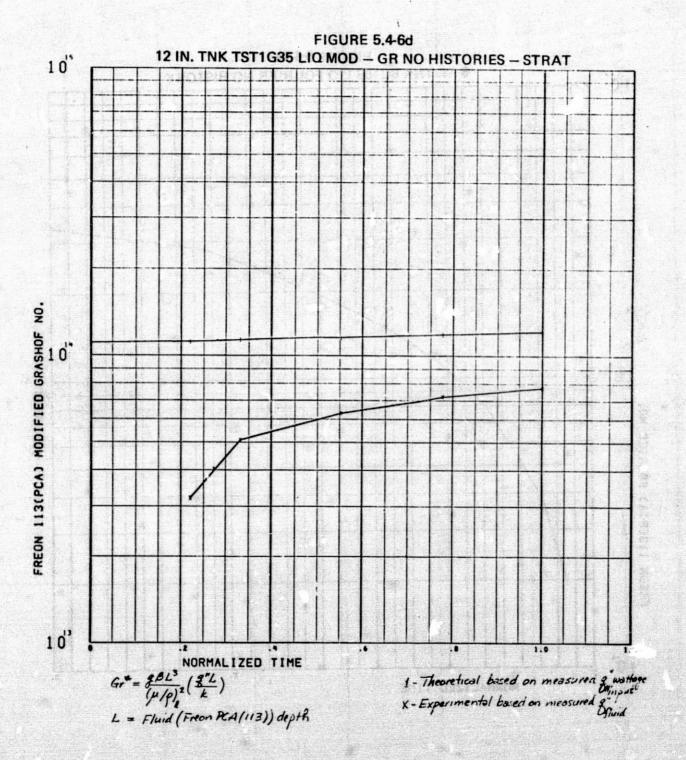


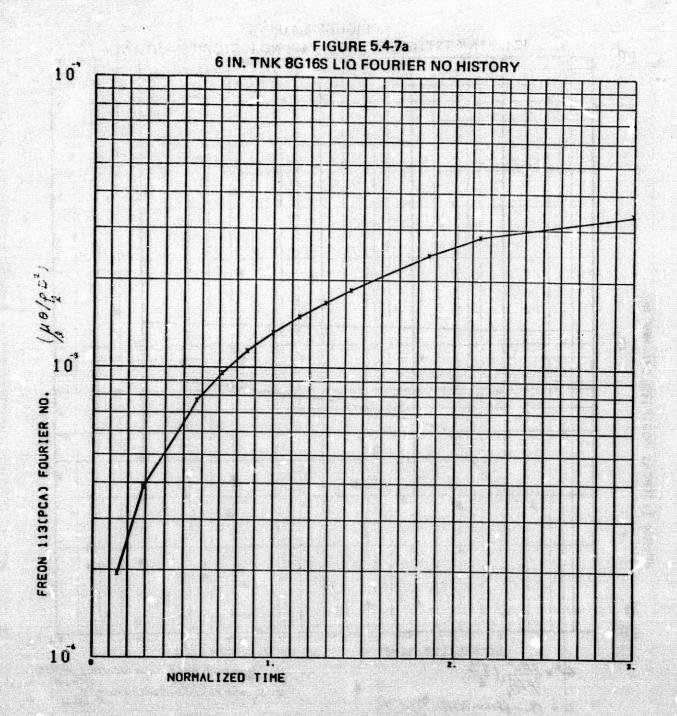


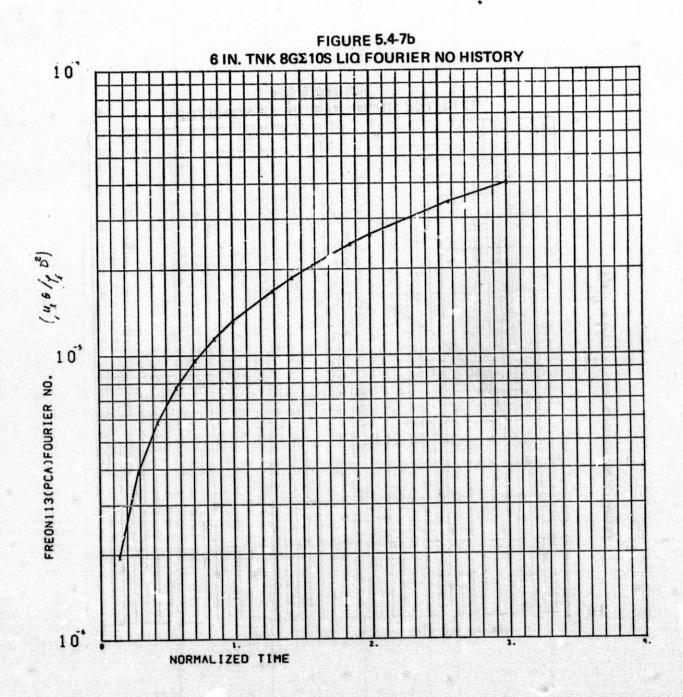


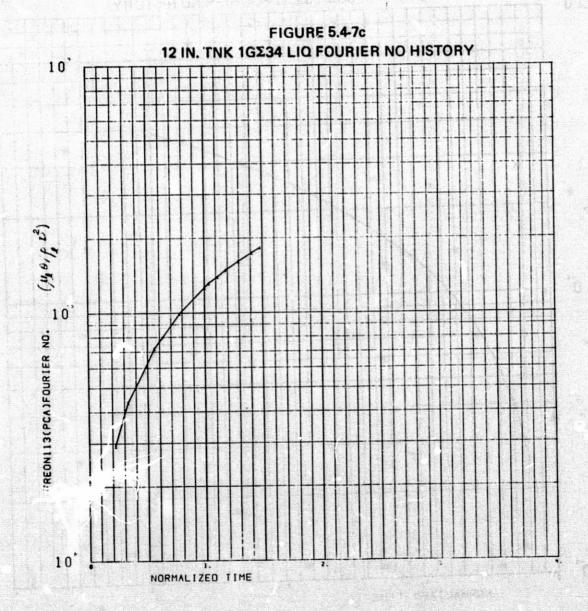
$$Gr^{4} = g \frac{\beta L^{3}}{(\mu_{f})_{3}^{2}} (\frac{g^{\mu}L}{k})$$

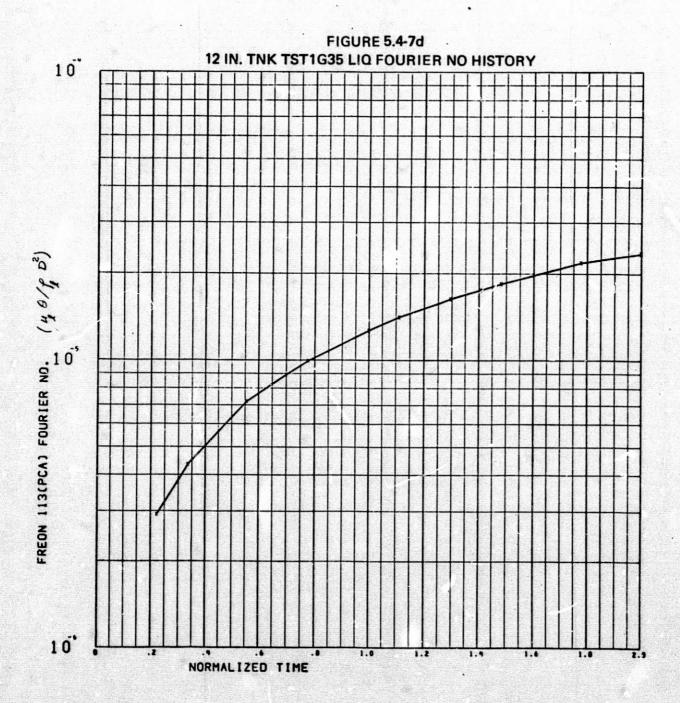
$$L = Fluid depth$$











Section 5.5 SCALING SET

6-in Dia Tank Tests		12-in Dia Tank Tests
gillin.	8G	1G
	Test #1	Test #20
	Test #5	Test #22
	Test #8S	1690 1122

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Table 5.5-la. 6 IN. DIA. TANK TEST 8G#1 (Page 1 of 3) STRUCTURAL GEOMETRIC TANK WTS-WATTMETER HEAT FLUX INPUTS

.0007	.0365 OL FT3= .38058	AREA FT2= FLNGE V(GE MASS=	FLNGE .00164 Flan	1.5708 L VOLFT3= BM= .81996	CYL AREA FT: 1/2 CYL H 35 1/2 CYL H	: .3927 73= .00131 .65596 MA	DOME AREA FT2= DME WALL VOL FT DME MASS LBM=
	•			.03272	LAGE VOL F	.22907 U	LIQ VOL FT3=
	TES	URE ESTIMAT	TEMPERAT	ED HEAT AND	2) + AND ABSOI	IXES (BTU/HR=FT	INPUT HEAT FLU
	0.0000	H78# (600.8488	488 H910#	H56= 600	H34= 600.8488	112= 600.6488
							ST.HT FLUX IN
		111,409 22,8544F	AT)BTU= (RAT)=	STRAT+DESTR	71.966	ULLGE (BTU/HRP (Q(STRAT)BTU=	EST.HY FLUX IN EST.HY INPUT LI EST.LIQ TEMP IN
		= 0,000	TRAT)BTU	(STRAT+DE	0,000	LAGE(STRAT)BTU	EST. HT INPUT UL
				I. DIA. TANK			
						TABI HRTHMOGOLARIF	STRUG
.0007	,0265 OL F13#	AREA FT2=-	FLNGE	1,57U8	TANK-WTS-P TANK-WTS-P TANK-WTS-P TANK-WTS-P	3927 .00131	DOME AREA FT2=
	,0265 OL F13#	AREA FT2=-	FLNGE	1,5708 L VOLFT3= MR .01990	YL AREA FTE 1/2 CYL N SS 1/2 CYL L	3927 38 .00131 65596 MA	DOME AREA FT2# DME WALL VOL FT DME MASS LUMB
	.0365 OL FT3# .38558	AREA FT2=- FLNGE VO GE MASS=	FLAGE .00164 FLAN	1,>708 L VULF 13= MR .81996	TARK HTS-1 TARK HTS-1 TARE OF HAMES 1/2 CYL HAMES 1/2 CYL HAMES OF THE	3927 30131 65596 MA	DOME AREA FT2= DME WALL VOL FT DME MASS LEME LIG VOL FT3=
	.0365 OL FT3# .38558	AREA FT2=- FLNGE VO GE MASS#	FLAGE .00164 FLAN	1,5708 L VULFT3= M= .01990 = .03272 EC HEAT AND	TANK HTS-H T/2 CYL H/ SS 1/2 CYL H/ LAGE VOL FY	3927 3= .00131 .65596 MA	DOME AREA FT2# DME WALL VOL FT DME MASS LUMB
	,0365 OL F13# ,38558	AREA FT2=- FLNGE VO GE MASS#	FLAGE .00164 FLAN	1,5708 L VULFT3= M= .01990 = .03272 EC HEAT AND	TANK-WIS-N TANK-WIS-N TANK WIS-N TANK AFROM TANK AFROM HEGE 600	3927 38 .00131 65596 MA ,22907 UI XES (BTU/) R=FT	DOME AREA FT2= DME WALL VOL FT: DME MASS LEME LIG VOL FT3= INPUT HEAT FLU
	,0365 OL F13# ,38558	AREA FT2=- FLNGE VO GE MASS= URE ESTIMAT H78= 0	FLAGE ,00164 FLANI TEMPERATION	1,5708 L VULFT3= M= .01996 = .03272 ED HEAT AND	TANK-HTS-H TANK-H	3927 3= .00131 .65596 MA .22907 UI XES (BTU/:R=FT) H34= 600.6488 LIQ (BTU/:R=FT) ULLGE (BTI/:R=FT)	DOME AREA FT2= DME WALL VOL FT3 DME MASS LEM= LIG VOL FT3= INPUT HEAT FLUX 112= 600,8488 EST, HT FLUX IN I
	,0365 OL F13# ,38558	AREA FT2=- FLNGE VO GE MASS= URE ESTIMAT H78= 0	FLAGE .00164 FLANI TEMPERATION 600.8488	1,5708 L VULFT3= M= .01996 = .03272 ED HEAT AND 488 M910=	TANK-HTS-H TANK-HTS-H T/2 CYL H S 1/2 CYL H LAGE VOL FY LAGE VOL FY H56# 600. 1) = 600.8468 T2) = 0.00	3927 3= .00131 .65596 HA .22907 UI XES (BTU/: R=FT) H34= 600.6488 LIQ (BTU/: R=FT) ULLGE (BTI/: R=FT) C(STRAT) RTL=	DOME AREA FT2= DME WALL VOL FT3 DME MASS LEME LIG VOL FT3= INPUT HEAT FLUX 112= 600,8488

Table 5.5-1c. 6 IN. DIA. TANK TEST #8S (Page 2 of 3) STRUCTURAL GEOMETRIC TANK WIS-WATINGTEN HEAT FLUX INPUTS FLAGE AREA FT2= DCHE AREA FT28 .3027 CYL AREA FT28 115706 FLAGE VOL FT3= 1/2 CYL HALL VOLFT3= .00076 .00164 DHE LALL VLL FT32 . CO171 , 81996 FLANGE MASSE .38056 MASS 1/2 CYL LEMB DEE MASS LEME .65596 ULLAGE VCL FT3= ,03272 ,22907 LIG VOL FT3= ILFUT HEAT FLUXES (ETU/LE-FT2) AND ABSCREED HEAT AND TEMPERATURE ESTIMATES H12= 600,8488 H34= 600,8488 H56= 600,8486 . H910= 600,8488 H78= 0,0000 EST, HT FLUX IN LIQ (BTU/IR-FT2)= 600.8488 EST. PT FLUX IN ULLIFE (BTL/FFFT2)= 0.0000 ESTINT INPUT LIGISTRATIETUS 72,095 (STRATADESTRATIETUS 0,000 EST, LIR TEMP INCRSE(STRAT)= 14,7983F (STRAT+DESTRAT)= 0.000DF (STRAT+DESTRATORTUR 0.000 EST. ET INPUT ULL AGE (STRAT) ETUE 0.000 Table 5.5-1d. 12 IN. DIA. TANK TEST 1G#20 -STRUCTURAL-GEOMETRIC-TANK-WTS-WATTMETER-HEAT FLUX-INPUTS-FLNGE AREA FYRE 1458 TOWE AREA FT2= 1.5708 - CYL AREA FT2# 6.2832 .01309 FLNGE VOL FT3# :00608 1/2 CYL WALL VOLFT3= DE WALL VOL FT3= .01047 FLANGE: MASSE 3.04465 MASS 1/2 CYL LBM# 6.55965 DME MASS LBMs 5,24772 LIC VOL FT3= 1.83260 ULLAGE VOL FT3= 26180 - INPUT HEAT FLUYES (STU/HR=FT2), AND ADSORRED HEAT AND TEMPERATURE ESTIMATES H12= 300,4244 H34= 300,4244 H56= 299,5561 H910= 300,4244 0.0000 H78= EST. HT FLUX IN LIO (BTU/HR-FY2) = 300.0771 EST. HT FLUX IN ULLGE (BTU/HR#FT2)= 0,0000 EST, HT INPUT LIG(STRAT)BTU= 589,200 (STRAT+DESTRAT)BTU= 1103,768 EST, LIG TEMP INCRSE(STRAT)= 15,1119F (STRAT+DESTRAT)= 25,2792F EST.HT INPUT ULLAGE(STRAT)BTU= -- 0.000 -- (STRAT+DESTRAT)BTUE -- 0.000-

Table 5.5-le. 12 IN. DIA. TANK TEST 1G#22 (Page 3 of 3) SIFUTURAL GENELIRIC TANK WIS-WATTHETER PEAT FLUX INPUTS

		00608
	ULLAGE VOL FT3= ,26100	
TOPUT HEAT FLUXES (STUVERS)	FT2), AND ABSORBED HEAT AND TEMPERATURE ESTIMATES	
H12= 300,4244 H34= 300,424	44 H56= 299,5561 H910= 300,4244 H78= 0,0000	
ESTANT FLUX IN LIG (BTU/FR-F	FT2)= 300:0771	
ESTILID TEMP INCREE(STRAT)	15.1115F (STRAT+DESTRAT)BTU: 1531,920 15.1115F (STRAT+DESTRAT): 39.2100F	
EST, HT INPUT ULLAGE (STRAT) BT	TU= C.000 (STRAT+DESTRAT)BTU= 0.000	

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TIME (MIN)	0.000	1.000	1,666	2,333	3.000	3,666
TAU	0.000	.273	.455	.637	.820	1.002
1	116.417	122.125	125.750	129.000	131.667	134.792
. 5	117.042	129.583-	133.333	136,500	139,708	142,875
3			132.500	135.375	138,042	140.750
Ū,	117.417	128.542	131.833	134.458	137.292	139.708
5 5	116.958	126.417	129.750	132.167	134.417	136,875
6	116,833	126.208	129.417	131.792		136.042
7	117.083	127.000				135.625
8	116.958	126.708	128,250	130,333	132,750	134,583
9	114.792	119.708	121.000	122,500	124,292	126,000
10		128,667	132.500	135.458	138,417	141.542
- 11	117.333	129.167	132.292	135.125	137.542	140.083
12	117.375	129.750		134.208	136,583	138.792
13		128.208		131.042		134.458
14	116,417	122.125	125,750	129,000	131.667	134.792
15	116.625	126.625	130.167	132,500	135,042	137,958
16	116.833			132.500		137.250
17	116.417	123.625	126,667	128.875	131.083	133,208
18	115,833	123.875	125.667	127,625	129.708	131,375
19	115.292	118.917	120.625	122.458	124.167	125.917
20		128,667	132,500	135,436	138,417	141.542
21		129.167		135,125	137.542	140.083
22		129.750		134.208	136.583	138,792
23	116.667	128.208	129.583	131.042	132,625	134.458
24				124,333		129.792
25				120.750	122,583	124.625.
26				118,125		119,292
27			그리아 얼마나 그래요 얼마를 가지하다. 그런 나는 그리나 그래를 다	111.333	(4) (1) (1) (1) (1) (1) (1) (1) (1) (1) (1	110,333
28	116.000					122.750
29		116,833				123,625
30	116.292	118.875	121.750	124.458	127.375	130,125
31						130.075
32	116.500	128.250				
33	114.500	119.125	120.792	121.583	122,667	124,083
34	111.917					119.750

	Table 5.5-2a.	6 IN. D	ANK TEST 8G#	1 (Page 2 of 2)
35	108.375	109.792 11	1.208 112.292	113.292 114.542
36	115.167	126.708 12	7.625 128.125	129,250 130,875
37	116.375	117.875 11	9.500 121.20A	123,125 125,333
38	116.375	118-458 12	0-585 122-780	125,042 127,456
39	116.708	119.792 12	2.542 125 777	128,000 130,875
40	116.833	130 ATT 12	000 127 000	120,000 130,075
41	117,128	121 042 12	4.000 127.000	129.750 132.625
42	117.350	121 125 12	1 777 126 04E	129,792 132,417
43	117 507	121 777 12	160001	130,333 133,083
	117.583		4.458 127.292	
44	117.542	151.145 15:	0.125 128,417	131.625 134.250
45	117.458	121.458 124	1.292 127.042	130.125 132.542
46	117.250	121.792 125	.208 128,167	
47		122,375 126	.292 129,125	132,125 134,083
48	118.083	121.500 124	1,458 127,583	130.500 133.417
49	116.167	118,833 121	.625 124.917	127.833 130.458
50	116,625	118,958 122	.208 125.333	128,208 130,500
51	116.292	118.750 121	.333 124,333	126.917 129.250
52	116.896	119.375 122	.021 124.667	127.063 129.646
53		118,458 120		126,375 129,125
54		120.292 123		127.750 130.167
55	117.667	120.250 122	-875 125-708	128,375 130,833
56	117.917	120.292 123	.083 125.292	127.750 130.167
57	117.667	120.250 122	.875 125.708	128.375 130.833
58	116,833	119.063 121	.646 124.313	127.083 129.250
59	117,375	119,375 121	.958 124.292	127.250 129.250
60	118.750	120,292 122	.875 125,250	127,583 129,833
61	115,625	116.708 118	.292 120.292	122,792 124,667
65	115.875	116.542 118	.500 120.792	122,875 124,708
63	116.917	117.625 119	.375 121.792	123.956 125.792
64		118,792 120		124.417 125.750
65	115.458	115.542 117	.208 118.958	21.000 122.750
66	115.583	115.750 116	.583 118.708	119.875 121.250
67	116.542	116.667 117	.708 119.417	121.250 122.792
68	117.542	17.917 118	.583 120-042	21,458 123,042
69	115.000	115.375 115	.958 117.292	119.125 120.017
70	115.292	115.708 116	250 117.458	118,875 120,333
71	115.750	16.375 116		119.750 121.000
72	[10]			121.167 122.667
73				
74 -	106.542			119.750 121.375 112.500 114.042
75	92.625	나이면 살아지지 않아야 하면 있는 것이 가끔하는 때 이번 살아야 없어지지 않아?	917 93,417	
76		: (150 NO 150 NO POLITICO E SE 150 NO POLITICO E POLIT	50 BB (1955 BB) 12 THE STREET STREET STREET	94.000 94.208
77	89.375		나는 사람이 되었다면 하는 사람들이 되었다.	06.875 107.583
	0743/3	UT1676 04	042 89,208	89,292 89,208

	(MIN) 0.000 ,333 1,667 3.010	3,667
!_AU	0,000 ,091 ,455 ,818 1.	00
1	116,458 118,583 127,208 133,375 136	5.417
2	116,750 121,708 133,042 189.417 142	2.204
3	116,917 120,625 131,333 137,292 14	,0H3
4	117,107 121,292 131,417 136.667 139	.292
5	116,583 119,833 129,292 134,125 136	5.5nc
6	<u> </u>	-563
7	116,875 120,625 128,875 133.000 135	.25"
8	116,833 120,875 127,938 132.625 135	.167
9		1542
10	116,583 123,625 132,042 138,083 141	.167
11	116,708 123,708 131,542 136,958 139	.501
12	116,875 124,292 131,500 136,375 138	,50:
13	116,333 123,125 129,333 132,417 134	.250
14	115,833 117,333 124,500 137,625 133	.753
15	116,342 119,750 129,250 134,50 137	1292
16	116,792 121,375 128,708 135.667 137	,667
17	115,875 118,750 126,208 130,667 132	.833
18	115,333 118,333 125,167 128,875 130	750
19	114,833 115,917 120,167 123,792 125	,583
20	116,583 123,625 132,042 138.083 141	.167
- 21	116,708 123,708 131,542 136,958 139	
22	116,875 124,292 131,500 136.375 138	,50C
23		,250
24	115,917 116,417 122,125 127,750 13	.792
25	115,708 116,042 120,500 125,250 127	.917
26	115,292 115,958 120,042 124.458 126	.875
- 27	112,543 115,750 119,383 122,625 124	
28	116,042 116,250 119,417 123,583 126	.042
29	115,667 115,625 118,958 123,458 126	.000
_30	115,708 116,167 122,042 127,875 13.	1792
31	115,972 122,514 127,722 129,458 131	,111
32	116,583 123,125 128,917 130,125 131	,833
33 34	114,542 115,792 120,083 121,792 123	1530
	110.625 110.917 114.125 116.417 117	

	Table	5.5-2b. 6 IN. DIA TANK TEST 8G #5 (Page 2 of 2)
	35	106,208 106,208 108,208 119,125 111,250
	36	115,607 122,208 127,125 129,125 130,750
	37	116,000 116,625 120,667 125,333 127,958
	38	116,000 116,500 121,542 126.875 129,625
tion of the second	39	116,250 116,958 122,833 128,542 131,417
	/ 40	116,458 117,250 123,625 129.417 132,292
	41	116,500 118,208 124,542 130,000 133,000
tak seren una	42	116,458 118,083 124,208 130,083 133,063
	43	116,458 117,917 124,833 130,625 133,000
	44	116,750 118,292 124,792 130.583 133,500
St. Establish Land	45	116,417 117,917 125,167 130,042 132,875
	46	116,792 118,250 124,633 130,500 133,542
	47	117,107 119,417 125,958 131,292 134,375
La company	48	117,583 118,250 123,792 129,833 132,875
	49	116,003 116,083 121,633 127,625 13.,042
	50	116,375 116,583 121,875 127,583 13.,542
and the second of the second o	51	116,042 116,208 121,167 126,708 129,083
	52	116,729 116,958 121,979 127,125 129,453
	53	116,042 116,000 121,167 126.333 128.583
4	54	117,417 117,708 122,792 127,542 129,833
	55	117,107 117,500 122,583 128.042 13 417
	56	117,417 117,708 122,792 127.542 129.833
	57	117,147 117,700 122,792 127,592 124,633 117,147 117,500 122,583 128,042 13 ,417
and the second second	58	115,958 115,917 121,042 125.875 128.167
	59	116,875 117,208 121,375 126.25 128.583
A STATE OF THE STA	<u> 60 </u>	
	61	445 500 445 405 447 052 400 405 404 977
	62	115,500 115,625 117,958 122,625 124,833
	63	115,667 115,833 118,208 122,167 123,959
	64	
	65	117,625 117,625 120,167 123,583 125,667
	66	115,375 115,667 116,875 120,708 122,583
	67	
		116,125 116,458 117,292 127.667 122,375
#	68 69	117,208 117,208 117,917 120.875 122,203
		115,208 115,292 115,667 118,833 12:,203
	70	115,417 115,583 116,000 118.833 121,200
	71 72	115,750 116,083 116,542 119.292 12 .792
	73	116,500-117,042-118,208-120-917-122,292
	74	114,542 115,250 116,583 119.208 12.,792
	75	106,833 107,208 109,208 112.417 114.167
	76	92,708 92,875 92,917 93,792 94,083
		104,292 104,417 105,167 106.958 107.917
	77	90,417 90,500 89,917 90,000 89,958

IAU	(FIN) 0.989 .333 1.000 3.020 3.667
	0.000 .091 .273 .618 1.000
1	117,708 117.833 123,917 133.458 136.083
——- <u>\$</u> —	110171/11/11/129.667-139.000-144-875
3	110,420 122,042 128,042 136,958 139,550
4	118,303 122,167 128,042 136,375 138,792
	12/10/2 1201220 126-250-133-667-136-333
6	117,000 119,717 125,750 132,500 134,792
?	11/,949 119,998 127,208 131,375 134,125
	112,71/ 120,042-124,675-132,009-134,375
ý	134,420 115,708 116,209 123,958 125,625
10	117,722 124,792 128,875 137,833 145,563
	110,770 120,717 120,667 134,542 132,958
12	112,428 123,083 128,292 135,542 137,625
13	115,292 121,067 126,125 131,333 133,042
14	116,625 118,125 121,375 130,000 132,542
15	11/,3/2 120,958 125,583 134,042 134,583
16	118,503 121,323 126,833 134,000 136,042
17	110, 11/ 117, 042 123, 252 135, 003 134, 959
16	114,700 117,792 122,125 128,167 126,792
19	114,125 114,875 117,083 122,667 124,292
20	117,750 124,792 126,675 137,833 140,563
21	116,958 123,917 128,667 136,542 138,958
2.2	115,958 123,063 126,292 135,542 137,625
23	115,272 121,667 126,125 131,333 133,042
24	115,792 116,167 118,375 126,333 128,875
25	114,042 116,083 117,375 123,125 125,167
26	1:7,146 108,202 111,125 116,375 117,375
27	100,25: 100,500 104,875 109,625 109,583
35	115,408 115,542 117,000 121,333 123,167
29	115.007 115.792 116,667 121,706 123,792
30	116,272 116,750 118,563 126,542 129,292
31	114,750 121,903 124,528 126,292 129,847
32	115 1007 121,708 125,417 128,958 130,458
33	113,542 115,125 117,750 121,292 122,542

Table 5	.5-2c. 6 IN. DIA TANK TEST 8G #8S (Page 2 of 2)
	7.11, 917 111, 873 112, 000 114, 000 114, 500
36	114,272 120,500 124,053 127,958 129,542
37	116,167 116,542 117,792 123,375 125,408
	116,250 116,333 118,417 125,042 127,542
39	116,542 117,292 119,208 127,375 126,917
40	117,000 117,833 120,333 128.753 131,375
41	- 117,0.0 119,125 120,875 135,625 138,900
42	117,000 118,003 120,875 130,500 133,125
43	117,2-8 118,375 121,083 131,042 133,417
44	117,458 118,567 122,125 135,708 133,417
45	117,353 118,375 121,208 130,917 133,123
46	117,417 119,125 122,125 130,633 133,542
47	118,500 170,125 123,000 131,542 134,750
48	116,729 117,104 119,750 122.563 131,021
49	146,476 116,083 118,625 126,500 129,042
50	116,675 116,667 118,700 126,750 129,417
51	116,625 116,458 118,167 126,042 128,292
52	117.3/6 117.260 110 147 106 643 100 774
53	117,3/5 117,250 119,167 126,563 128,771
54	115,792 115,917 116,208 125,633 127,792
55	118,125 118,042 120,167 127,083 129,250
56	117,875 117,542 119,667 127,542 129,833
57	118,125 118,042 120,167 127,083 129,250
58	117,8/5 117,542 119,667 127,542 129,833
59	115,998 116,167 118,125 125,083 127,333
	117,000 117,083 118,333 126,000 127,058
60	118,208 118,417 119,792 126,958 126,167
61	114,542 114,292 115,250 121,667 123,208
62	114,250 114,333 115,333 121,500 123,375
63	115,375 115,375 116,500 122,667 124,583
64	116,417 116,625 118,042 122,875 124,542
<u> 45</u>	113,003 113,167 114,208 119,250 121,208
66	113,200 113,042 114,042 118,292 119,917
67	114,272 114,042 115,042 119,706 121,125
68	115,542 115,202 115,217 112,625 121,123
69	112,917 112,708 113,167 117,208 118,750
70	113,272 113,000 113,458 117,292 118,633
71	113,217 113,833 114,292 118,083 110,750
72	115,292 115,292 115,958 119,750 121,417
73	112,917 113,250 113,875 117,917 116,375
74	107,2:4 109,500 110,667 116,083 117,517
75	95.833 95.917 96.458 99.000 90.917
76	103,607 103,500 103,709 106,208 106,708
77	47,45a 87,202 87,202 87,417 87,250

)

Table 5.5-2d. 12 IN. DIA TANK TEST 1G #20 (Page 1 of 2)
TEMPERATURE MATRIX-STRATIFICATION

TIME (0002.0	00- 4.0	006.0	009.0	00- 12.0	00-43,000-15,0
TAU	11 6 0 0 11	1100	160/	. 400	. 600	.800	267 4 000
1	117,1	25 121.29	2 123.34	125.54	2 129.25	131.04	2 131,917 133,75
2	117.1	25 123 00	0 125 70	27 Bit	7 130 33	1 1 17 04	134,000 135,625
3	117.5	UO 124.04	2 126 451	128.25	130 70	437 406	134,375 135,200
4	117.5	03 123 79	2 126 04	127 75	130 04	130,02	133,542 135,333
. 5 .	-117.4	58_123.70	2 125 050	127 70	130,070	102,750	-133,417-135,125
6	117.4	17 122 58	3 124 456	425 07	1 20 25	-132430	-103,417-435,12
7	117.5	UN 122 58	3 124 467	1 425 45	3,24,750	130,007	131,500 133,167
- 8	117.4	58 122 05	2 124 776	120,400	127,500	129,91/	130,667 132,292
9	117.1	67 110 87	5 424 450	120,54	1.27 58	129,875	130,500 131,958
10	117 3	33 420 62	2 121,426	122,917	125,042	127,250	127,917 129,417
_ii	111	00 150.05	2 101.10/	107.85	4.44.7NH	432.250	470 200 444 644
12	117 5	17 127 14	2-131-142	-132,795	135,167	137,750	138,583 140,750
13		AN TEL MI	/ 167.205	100.007	4.30.875	4 36. 333	474 637 477 669
_14		4/ 15/ 473	0 149.905	1011.007	1 10 667	474 750	475 449 .77
15	THE RESIDENCE OF THE PARTY AND ADDRESS.				100 .040	478 768	474 495 497 544
16	**' !	1 160 1 13	1 169.2311	101.208	4 3 7 7 5 0	4 77 000	4 70 A4A 473 EAR
_17				1 1 1 1 1 1 2 2 2		THE SHE	4 4 4 7 7 7 7 7 7 4 4 4
18	CONTRACTOR OF A SECOND STATE OF THE	The second of the second of the second		7 / M . M / N			474 EAT . 74 A
	*** ***		1 160.0/2	16/./90	120.708	1.44 . 017	4 10 BAA 474 944
19			1504/9/	167.107	124.16/	124 375	477 475 470 4/4
		10-10-17		132 017	135 542	130.417	4 30 40E 444 10E
21	14/17	0 169.10	101.250	133.040	476 773	477 700	474 764 4-4
22	*** 100	10 16/106:	167.10/	130.7UA	132.875	135.333	134 007 477 049
23			TEA - 11 11 11	-1011-1/5	_1.32.375	134.583	4 TE DEA 476 449
24	11000	170.000	119.917	121.667	124.167	124.708	127 540 400 4/9
25	110,00	0 11/16/	110.007	920.000	124.058	124 000	124 447 454 400
26	HARMONIAL A. Bull Bull.			-114.417	124 125	122.750	127 417 424 EAT
27	117,00	O TTO TT	110.046	118.917	120.125	121.333	174 700 477 447
28	440,00	E TTU . 5/3	11/ 41/	119.053	120.855	122.750	199 507 494 766
29		2 110./92	118.042	110.333	124.208	127.250	127 050 425 449
30	110101	2 11/1/20	119./97	121.747	424.nnn	124.450	437 777 408 048
31	11/100	1 16/.400	129.41/	130.542	132.500	134.605	445 777 476 049
32	DESCRIPTION OF THE PARTY OF THE				1 4 2511	4 4 7 7 7 7 7 7	ITA NAN A AND
33	447.00	0 -7.042	160.333	121.250	477 707	124 EAA	432 447 484 448
34	114,95	8 114.750	114.750	114.700	116.023	115 675	115,875 115,458
				74-1125	1121100	1721052	115,0/5 115,458

	Table 5, 5-2	d. 12 IN. DLA	A TANK T	EST 1G #20	(Page 2	of 2)
35	414 750 414	97 113 458	112.056	112,417 11	2.000-	112,000 111,875
36	448 000 426	SEN 120 425	130.833	132.00/ 10	4./20	107,246 107,000
37	446 375 417	125 419 AAA	120.417	122.3/2 12	4.41/	127.129 129.00/
	446 500 447	162 110 425		7 477		
39	416 708 418	ISA 120.250	122.042	124.583 12	7.094	12/1/1/ 127,00/
40	446 017 116	277 420 A75	429.749	125.546 12	M.10/	129,000 130,000
41	117 458 118	117 120 708	122.292	125.000 12	1,396	1511 430 130 530
42	417 RRT 410	121 121 000	122.792	125.542 12	8.200	124,420 100,720
43	117.667 119	142 121 125	123.000	125.525 12	8,292	129,125 130,792
Y44	117 799 410	09 120 375	122.708	125.375 12	8.208	129,125 130,792
경기를 전혀하다 하루 하면 내 전기를 하는데 집 때문에게	117,667 119,	50 120 583	122.458	128.083 12	7.833	128,833 130,542
45	117,007 117,	49 121 BOO	123.450	124.500 12	A. 917	129,750 131,708
46	117 447 410	27 424 737	123.417	125.958 12	8.542_	129,333 131,167
47	117 050 110	200 424 777	427 426	126 750 12	8.417	129,333 131,125
48	117,990 119,	107 121 353	122.700	125,208 12	7.833	128,833 130,500
49	117,093 119,	103 120,993	122 042	124 625 12	7.250	29,292 129,875
50	11/1/09 11/1	12/ 140 447	134 300	127 708 12	4.250	127,208 125,958
51	117,833 118,	125 119,007	122 007	124 425 12	7.167	129.125 129.875
52	117,792 118,	92 120,333	122,000	124 047 12	7.625	129,125 129,875
53	117,625 118,	17-120-792	1421424	124 443 12	7.167	123,208 130,000
54	117,792 118,	175 120,542	122,209	124,007 12	7 1107	128,167 129,875
55	117,792 118.	792 120,50	122,250	1241/00 12	7 4 25	128.042 127.833
-56	117,708 118,	750 120 333	153,042	124,023 42	7 003	129,125 129,833
57	117,667 118.	17 120,500	125,508	124,792 12	4 047	127 933 447 667
58	117,833 118,	750 120,125	121,917	124,3/5 12	0171/	127,833 127 567
59	117,667-118,	100-119,917	121,542-	124,005-12	01101-	127,250 129,300-
60	117,583 114,	792 119,792	121,417	123,025 12	5 050	127,125 128,792
61	117,750 118,	250 119,333	120,625	123,083 12	51220	126,375 127,875
- 63	417 750 110	200 110 A17	126 705	127 044 14	4.3/3-	140-474-14-1-1
63	117 625 118	142 119.292	120.667	122.033 12	4. 425	120,000 127,007
64	117.583 117.	958 119.N83	120.250	127.294 16	4.0/2	123,000 127,000
65	117.583_117.	958 119.042-	120,292	122,542-12	4,500	125,000-127,000-
66	117.583 117.	833 118.708	119.792	121,870 12	3171	124,000 122,000
67	417.563 417.	833 118.708	119.792	121.875 12	3.71/	124,833 125,333
68	117 549 117	7.18 118 500-	110.583	121 500 32	-HCP+1	144-339-143-144
69	417 847 417	700 41R 5A3	119.667	121.622 12	3.500	124,3/7 127,470
70	447 460 417	447 11R 417	110.375	121.3/2 12	3 . 2 0 5	164,600 167,067
- 71	117,458-117.	667 118.417	119.375	121.0/2 16	01200	1541500 1521052
72	117,542 117.	792 118,417	119,500	1511145 19	01000	1541101 1521001
73	117,500 117,		119,458	121,458 12	3,250	124,250 125,708
74	92,042 92		92,467	-64-508-6		94,167 94,667
75	103,458 103.		106,208	105,708 10		107,583 109,525
76	80,875 81.	083 81,958	82,083	82,292 8	2,292	82,583 82,750
_ 77	91.542 91	792 - 91,958	92,167		3,250	93,750 95,500

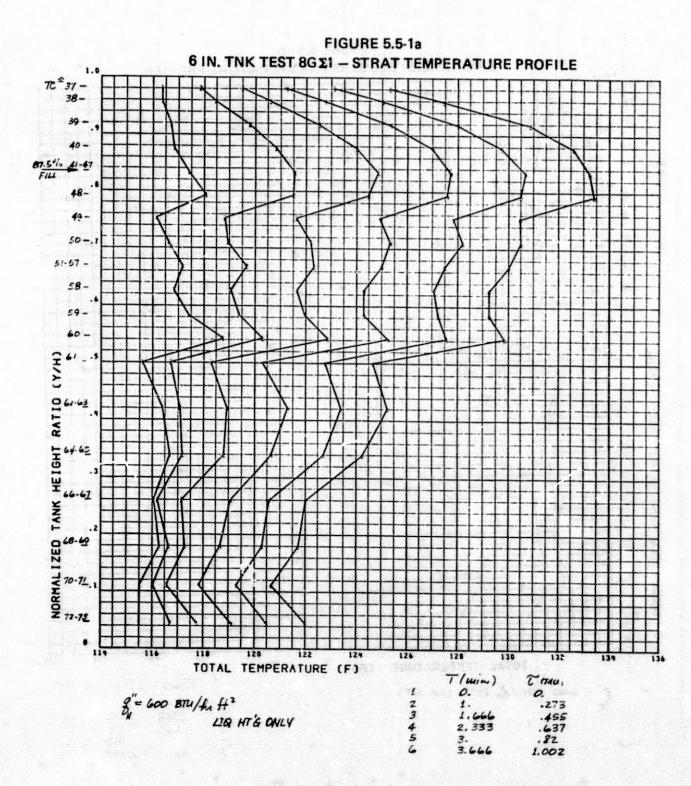
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Table 5.5-2e. 12 IN. DIA TANK TEST 1G #22 (Page 1 of 2)

TEHPERATURE	AHTS-XIHTAN	TIFIGATION

TINECH	11N) 0.000 2.600 6.000 9.000 12.000 15.66
TAU	0.000 .133 .400 7600 .800 1.000
_1	116.875 121.042 125.458 128.167 130.958 133.625
2	116,875 122.956 127.45H 130.417 133,042 135,792
3	117,250 123.625 123,125 130,958 133,667 136,250
	117,458 123,750 127,667 130,167 133,066 135,417
5	117,208 123,956 128,053 130,458 133,083 135,700
6	117,208 122,792 126,292 128,667 131,125 133,778
	117,292 122.667 125,667 127,917 130,375 132,875
8 9	117,458 123,125 126, 42 128,000 130,333 132,750
	117,125 119,917 123,208 125,450 127,708 129,953
10	117,042 123,750 132,667 135,543 138,417 141,042
11	117,206 128,750 132,500 135,125 137,667 140,333
12	117,417 127,708 131,003 133,563 136,125 138,625
-13	117,167 128,917 131,2 ⁹ 2 133,250 135,458 138,893
14	116,667 121,033 125,208 127,958 130,667 133,375
15	117,083 127,125 131,292 134,375 137,000 139,873
-16	117,250 126,417 130,542 133,125 135,75: 138,250
17	117,167 126.417 129,792 132,083 134,583 137,203
18	116,958 125,292 124,533 130,667 132,959 135,500
19	116,583 119.375 122,417 124,683 126,792 129,142
20	117,333 129.042 133,000 135,917 133,459 141,250
21	117,167 128,708 132,708 135,375 137,759 140,542
_22	117,230 127,833 131,443 133,583 136,004 130,542
23	117,292 123.208 130,750 132,958 135,042 137,458
24	116,625 117,875 121,625 124,333 126,958 129,667
25	116,250 117,292 120,333 122,7%0 125,208 127,792
20	116,042 117,125 120,125 122,373 124,792 127,292
27	116,083 117,167 119,917 122,167 124,417 126,933
28	110,458 117,167 119,533 121,792 124,167 126,503
29	110,167 116,958 119,708 122,083 124,500 127,042
30	116,333 117,667 121,417 124,125 126,750 129,458
31	117 417 127 583 130 417 132 500 134 625 137 083
32	117,125 126.500 129,083 131,083 133,167 135,500
33	114,708 118,500 120,750 122,292 124,083 126,000
34	114 125 113,708 113,750 114,042 114,500 115,125

	Table 5. 5-2e. 12 IN DIA TANK THEFT A. T.
35	Table 5. 5-2e. 12 IN. DIA TANK TEST 1G #22 (Page 2 of 2)
36	***************************************
37	117,792 127,875 136,667 132,833 134,917 137,206
38	116,625 117,625 120,667 123,063 134,917 137,206 110,706 117,633 121,292 123 703 125,542 128,033
39	110.708 117.633 121.292 123.792 126,375 129,000
40	
41	117,000 116,75; 122,563 125,542 128,206 130,000 117,333 118,625 122,200 124,766 127,292 130,000
42	**/ . UVU 110.0/2 122 250 424 and
	** * * * * * * * * * * * * * * * * * *
- 43	100 100 100 100 100 100 100 100 100 100
44	11/10/2 110.91/ 122.500 125 202 127 055
45	+1/17/0 110./92 122.208 404 700 702 474
46	11/1/22 11/2.10/ 197 (47 478 198 90
47	117,583 115.675 122,875 125,667 128,500 131,455
48	41/1/76 114,125 105 USB 438 / A CA CA CA CA
49	11/2009 110.020 122.58% 425 0.0 .02
50	41/1200 110.00/ 122 206 404 755
51	44/4062 110441/ 124.000 429 448 04
52	117 503 440 447 474 475 475 4767 120,167 129,167
53	11/40/2 11/14/31 122 467 404 DEC
54	117 625 412 750 1261407 1241872 127,417 130,500
55	
56	117 625 442 75 124 127 124 175 127 243 130 200
57	
58	117.500 118.875 122.883 124.833 127.167 130.042 117.708 118.583 121.708 124.833 127.167 130.043
59	
60	
61	74/10/2 44/11/1/ 121/292 127, 967 474 20, 404
62	
63	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
64	
65	117,292 117,792 120,208 122,583 124,708 127,375
66	117.292 117.792 120.125 122.625 124.833 127.375 117.333 117.681 119.736 122.625 124.833 127.417
67	117.333 117.681 119.736 122.028 124.069 126.694
68	117.333 117.708 119.625 121.950 123.953 126.625
69	
<u>70</u>	
71	123.375 125 054
72	17. 17. 17. 17. 17. 17. 17. 17. 17. 17.
73	74 140 11/1/05 119:005 121:379 123 203 126 016
74	17,375 117,625 110,125 121,417 123 542 124 223
	76,917 93,453 93,703 04 750
75	104.417 104.625 105.125 106.292 107 200 107
76	85,042 85.060 04.628 84.702 04.600 109.000
77	97,000 97,000 94 917 07 777
	77.333 97.542 98.375



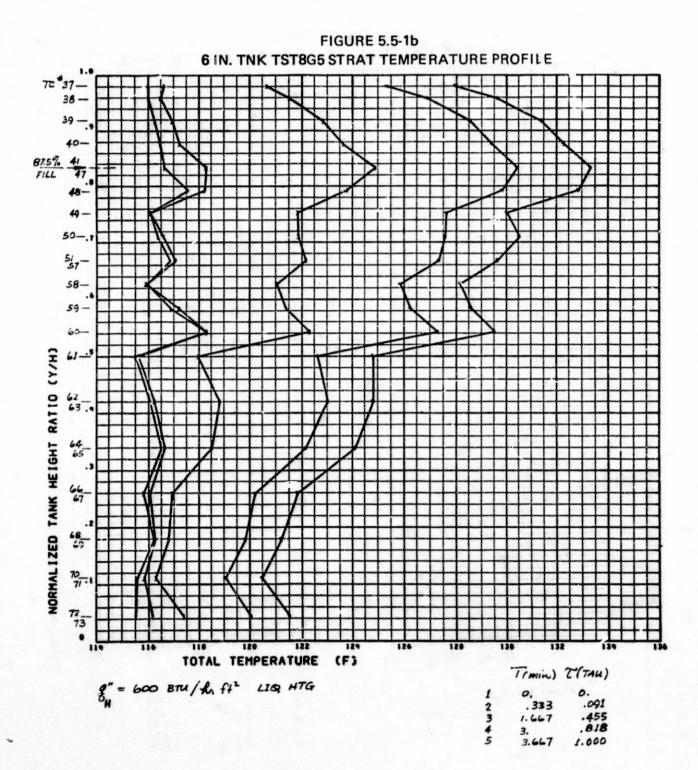
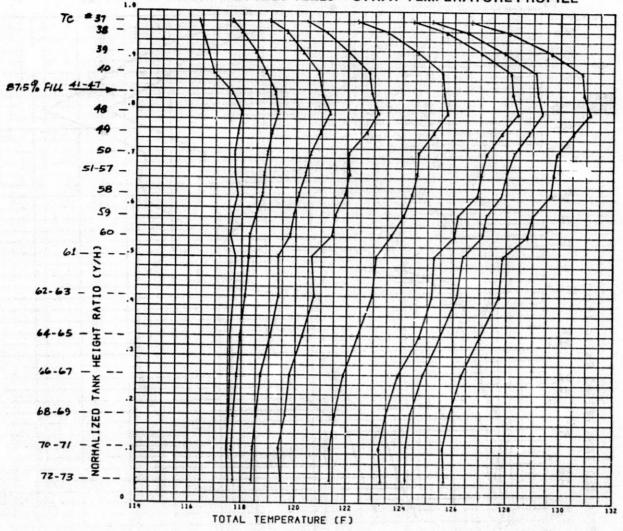


FIGURE 5.5-1c 6 IN. TNK TST8GESS STRAT TEMPERATURE PROFILE 60-NORMALIZED TANK HEIGHT RATIO (Y/H) TOTAL TEMPERATURE (F) Than) Timin) 0"= 600 BTU/ th ft 2 LIG HTG 12345

195

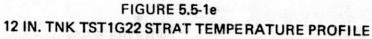
FIGURE 5.5-1d

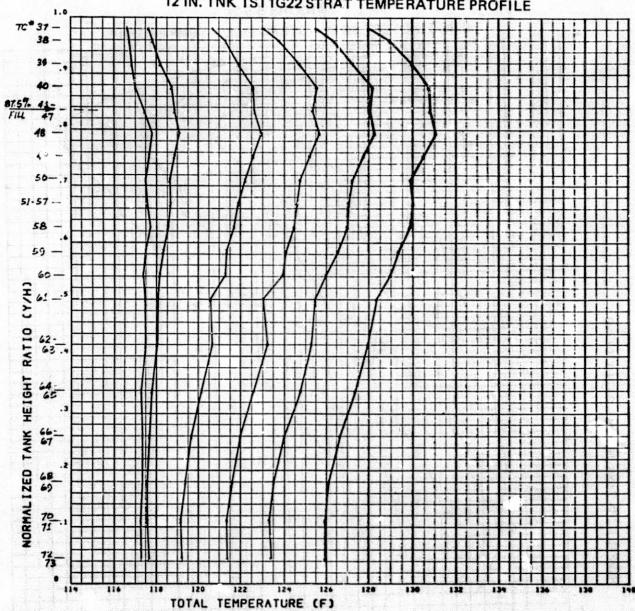
12 IN. TNK TEST 1GΣ20 — STRAT TEMPERATURE PROFILE



g" 300	BTU/ ft ft ²	
OH .	LIQ	HT'G CAVLY

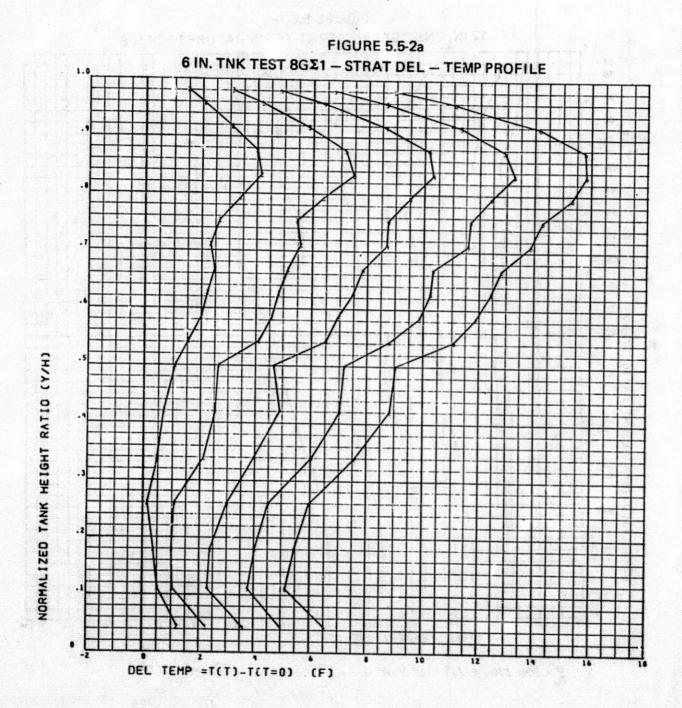
	T(min)	~ (TALL)
1	0.0	0.0
2	2.	./33
3	4.	.267
4	6.	.4
5	9.	.6
6	12.	.8
7	13.	.867
8	15.	1.0

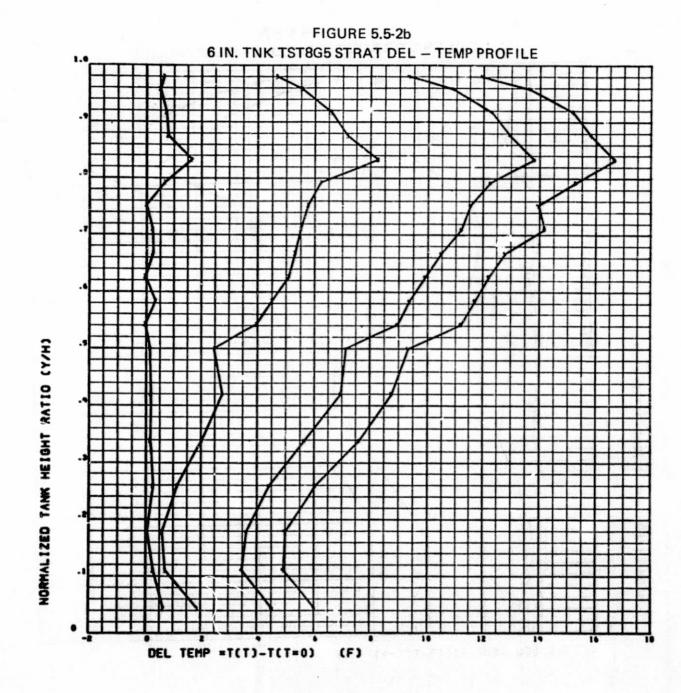




8 = 300 BTU/A, ft2	LIQ HT'G

	T(min)	T(TAU)
1	o.	0.
2	2.	. 133
3	6.	-4
4	9.	.6
5	12.	.8
6	15.	1.000





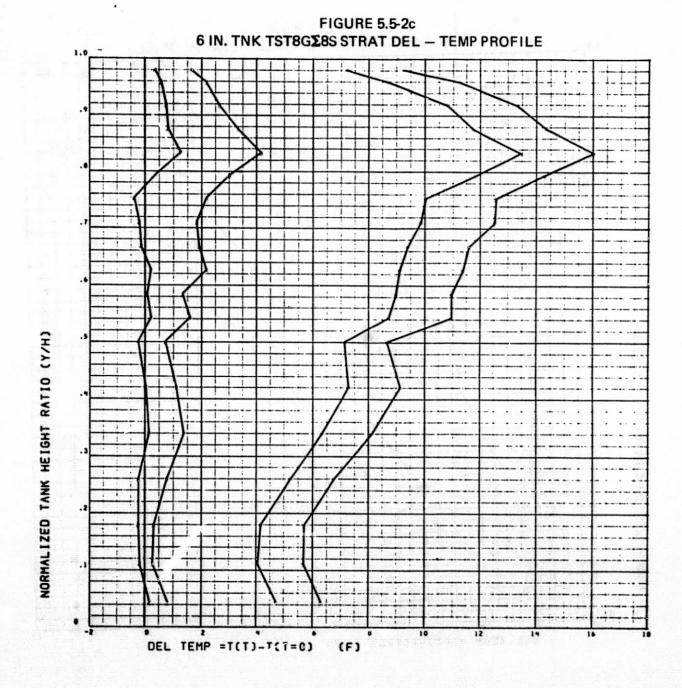
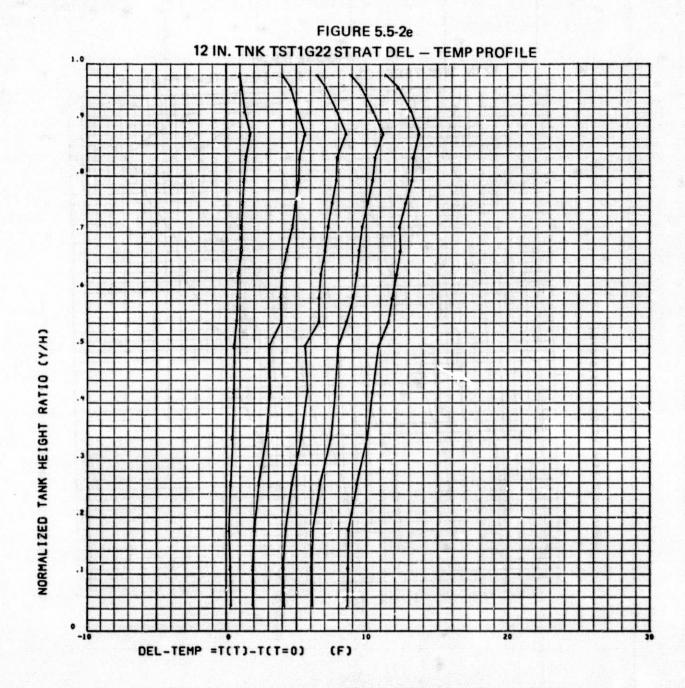
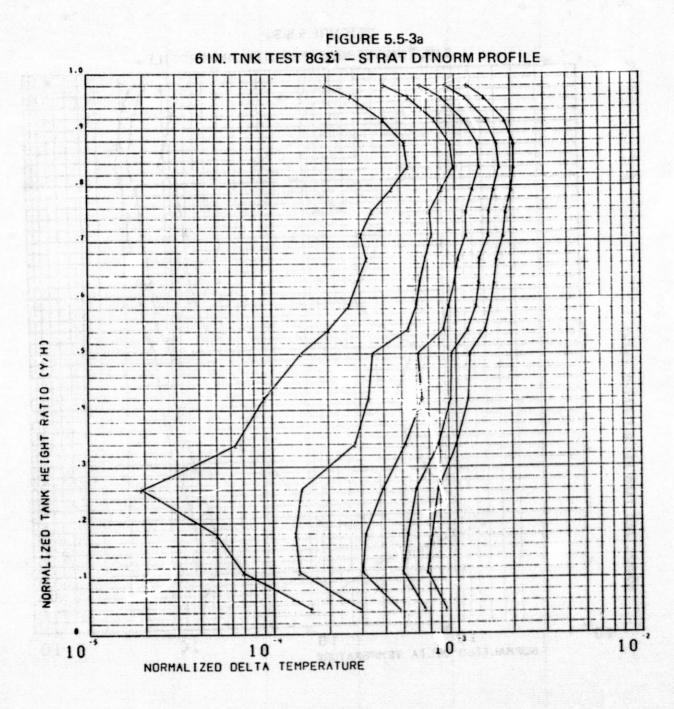
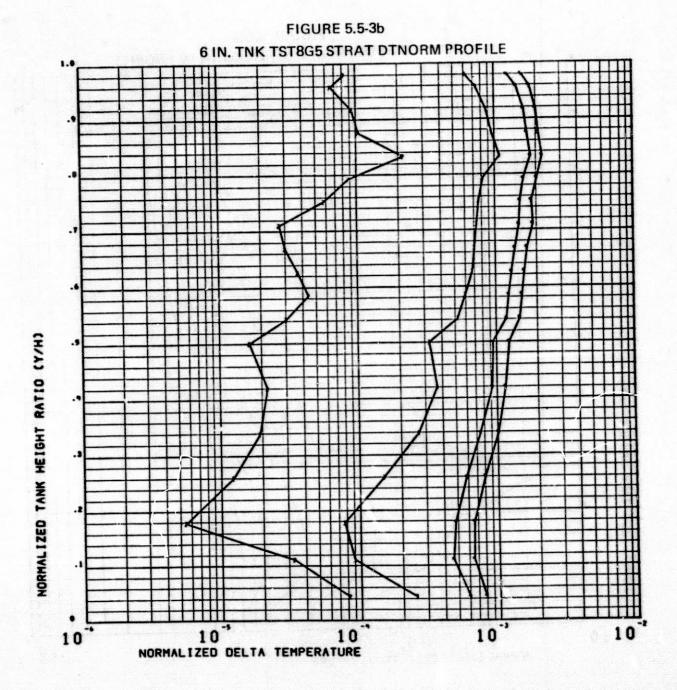


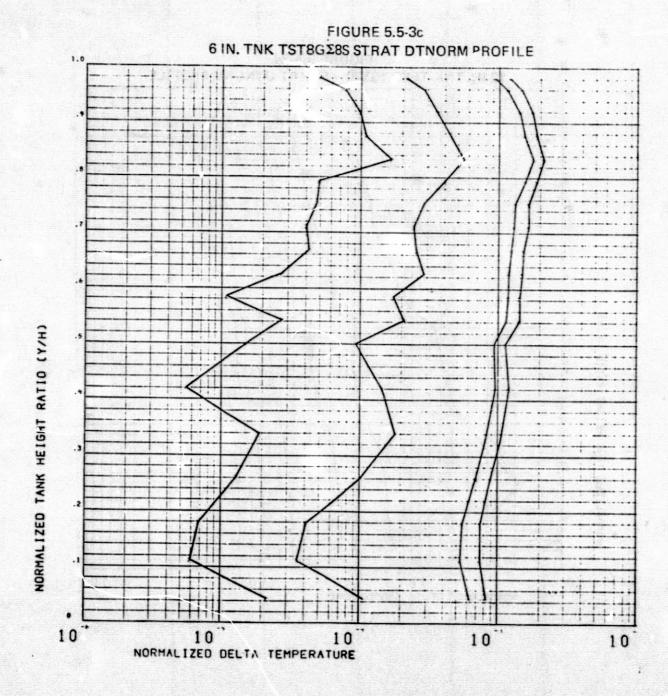
FIGURE 5.5-2d 12 IN. TNK TEST 1GΣ20 - STRAT DEL - TEMP PROFILE NORMALIZED TANK HEIGHT RATIO (Y/H) (F) DEL.TEMP =T(T)-T(T=0)

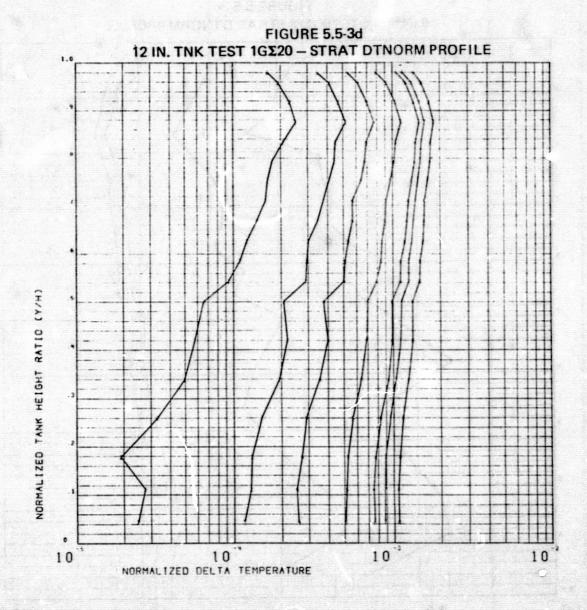
201

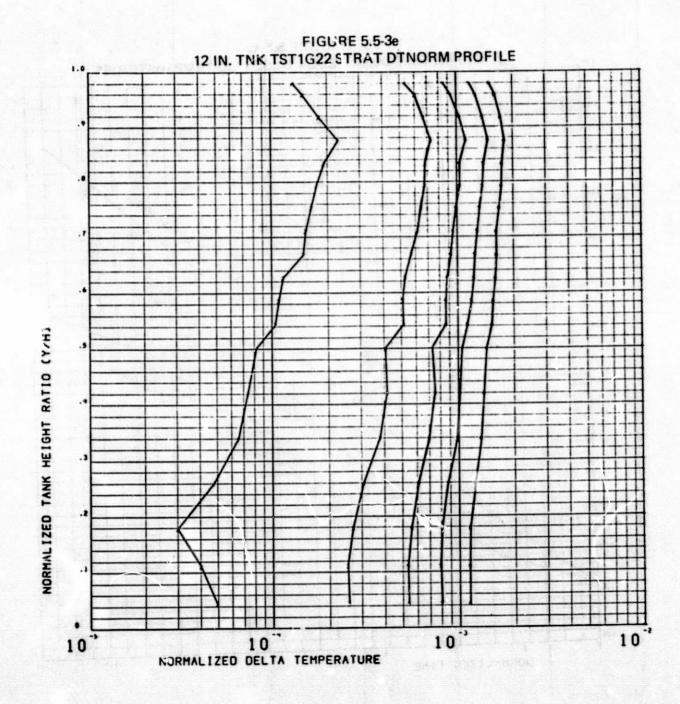


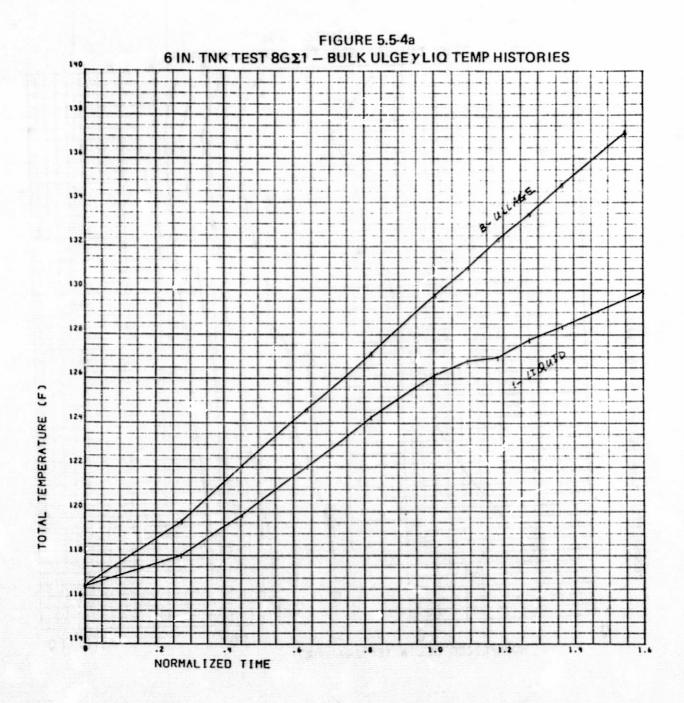












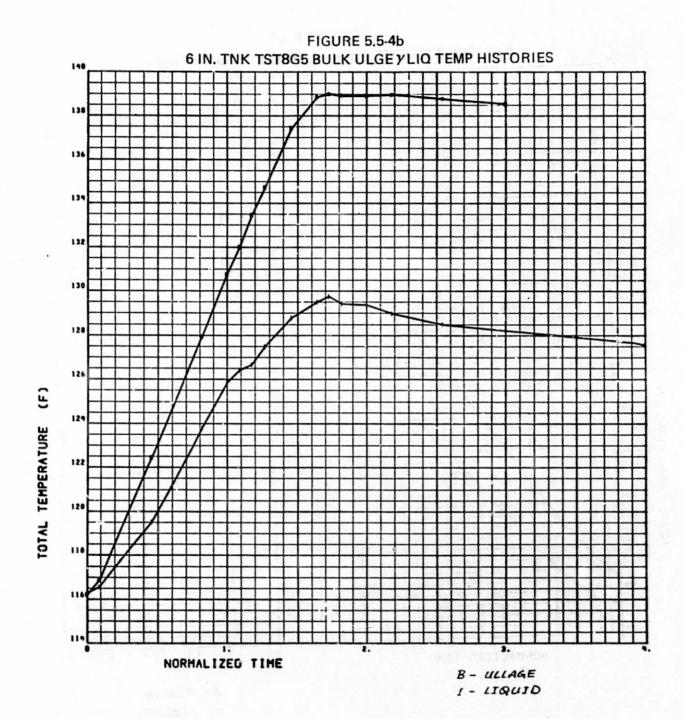


FIGURE 5.5-4c

8 - ULLAGE 1 - LIQUID

NORMALIZED TIME

E

TOTAL TEMPERATURE

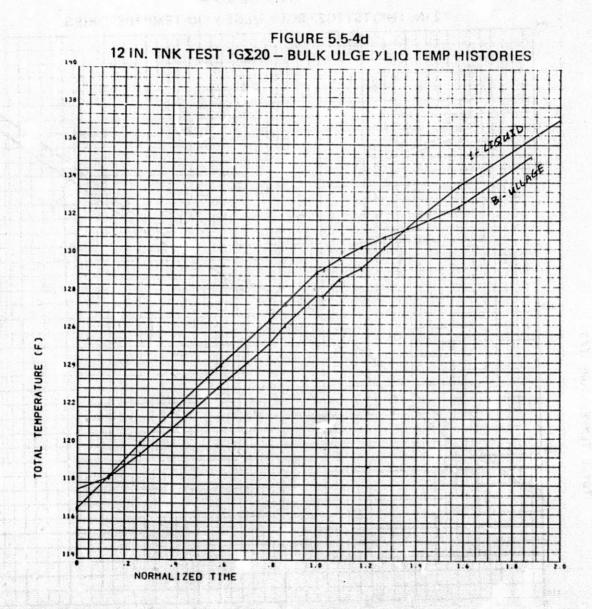
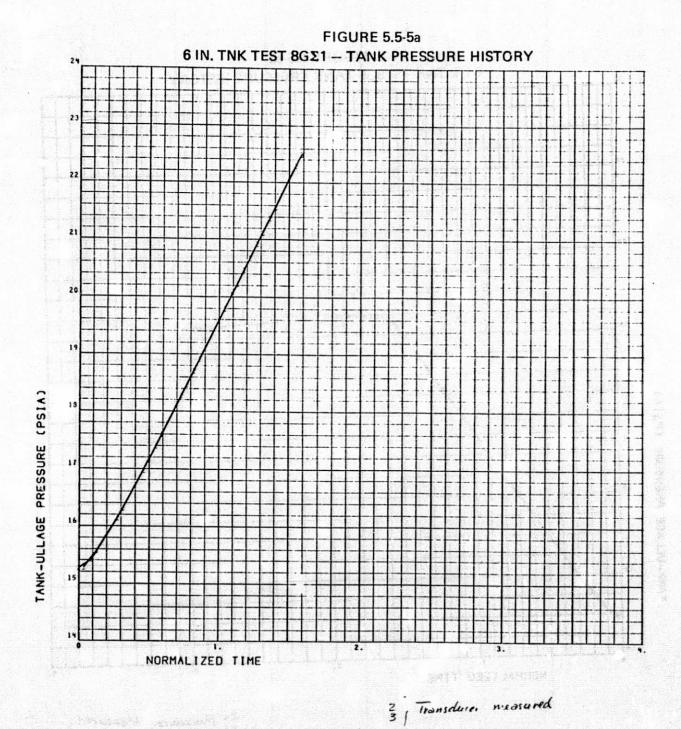
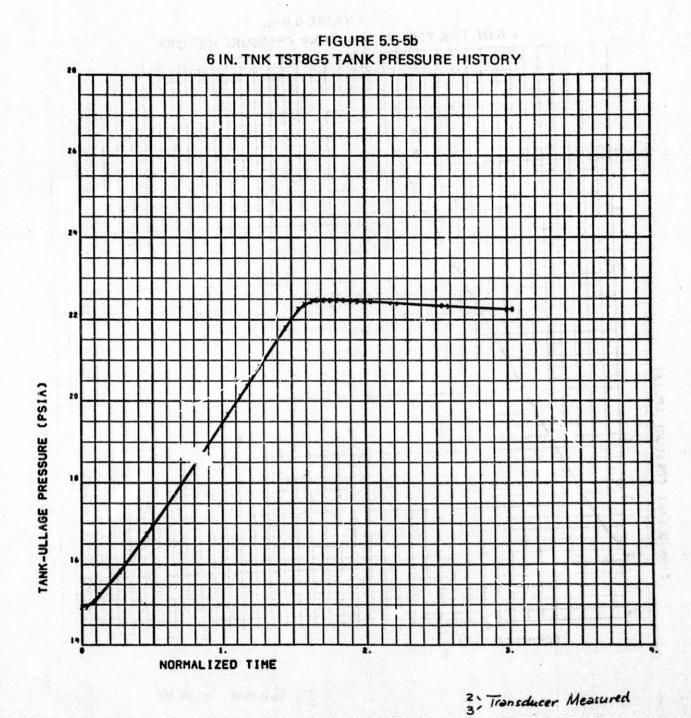


FIGURE 5.5-4e 12 IN. TNK TST1G22 BULK ULGEYLIQ TEMP HISTORIES TOTAL TEMPERATURE (F) NORMALIZED TIME

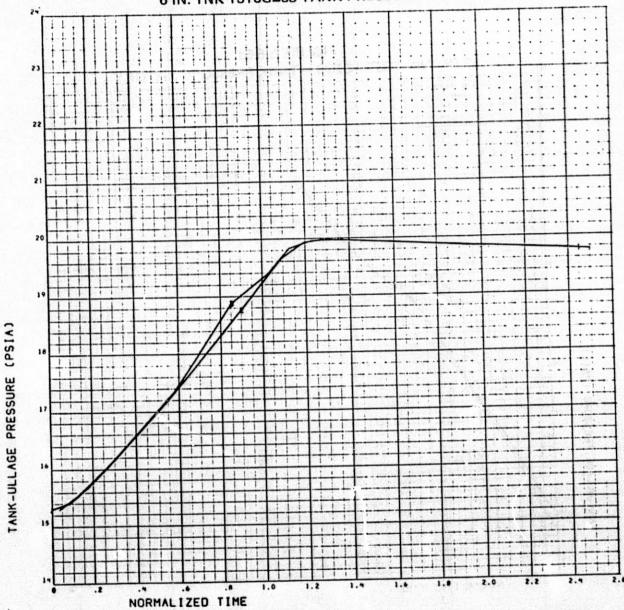
B - ULLAGE 1 - LIQUID



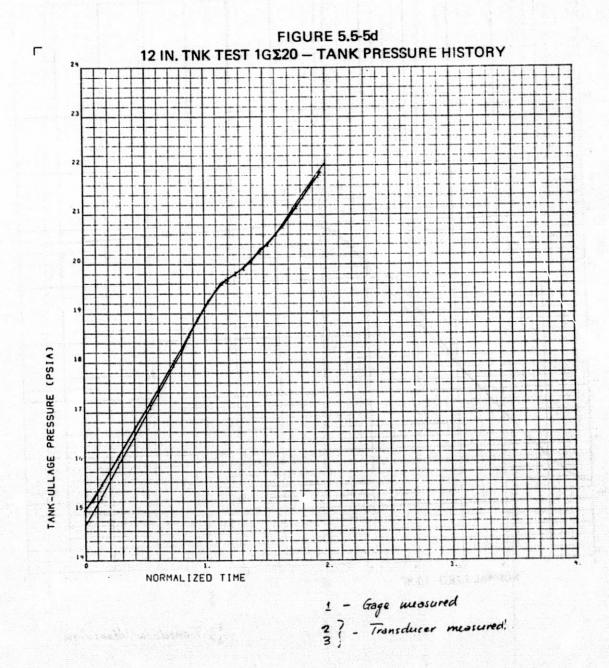


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FIGURE 5.5-5c
6 IN. TNK TST8GΣ8S TANK PRESSURE HISTORY



2; Transducer Measured

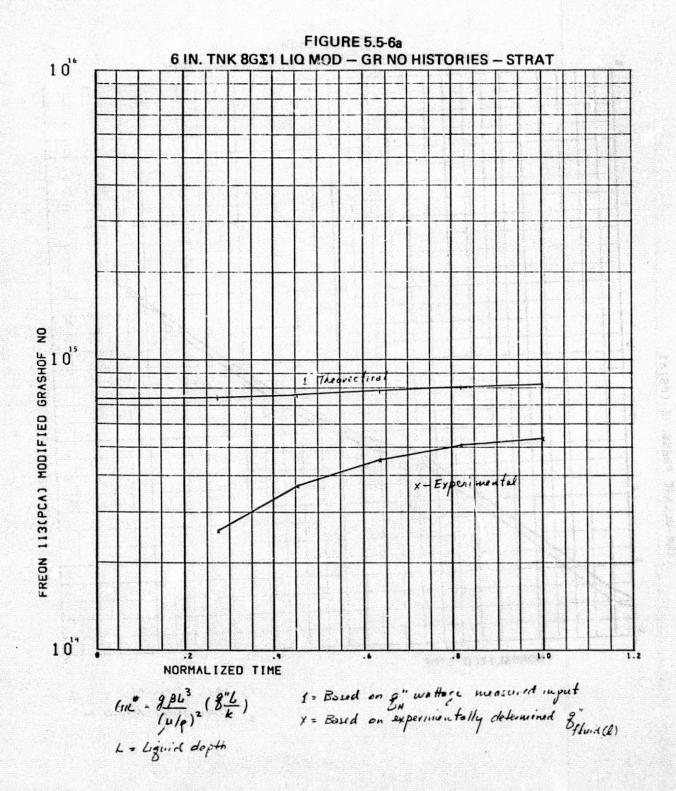


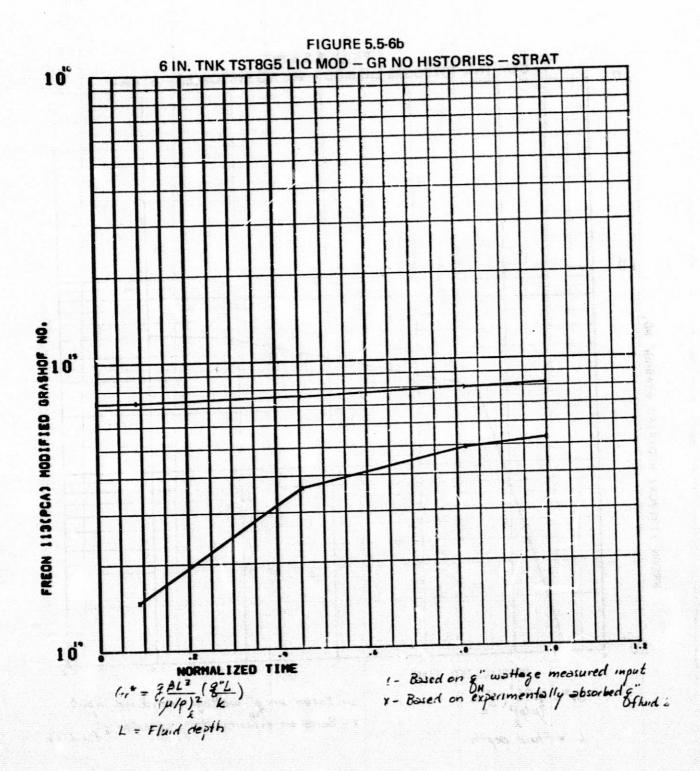
1- Gage Weasured

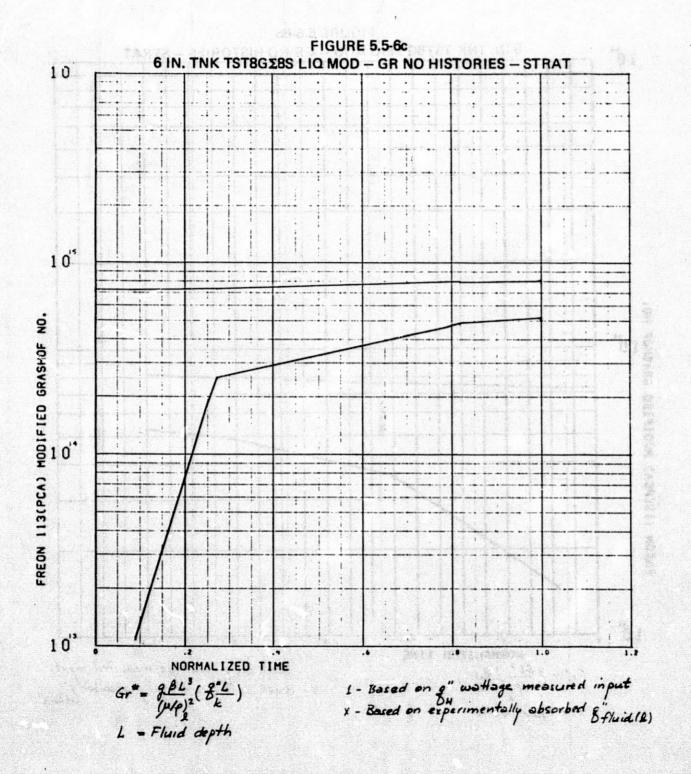
FIGURE 5.5-5e 12 IN. TNK TST1G22 TANK PRESSURE HISTORY TANK-ULLAGE PRESSURE (PSIA)

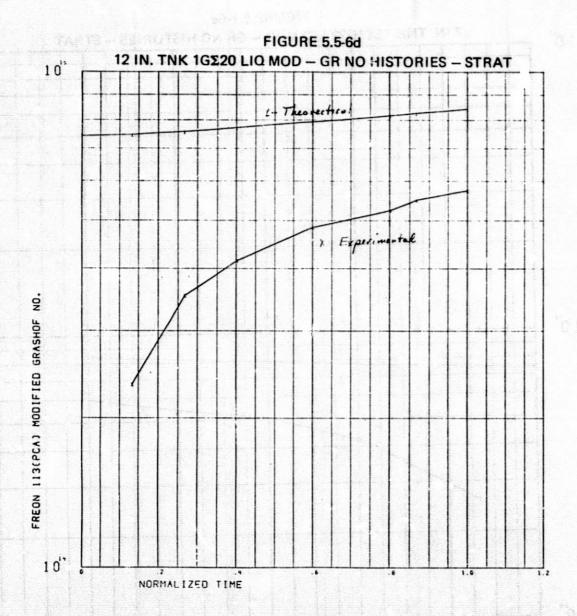
217

NORMALIZED TIME





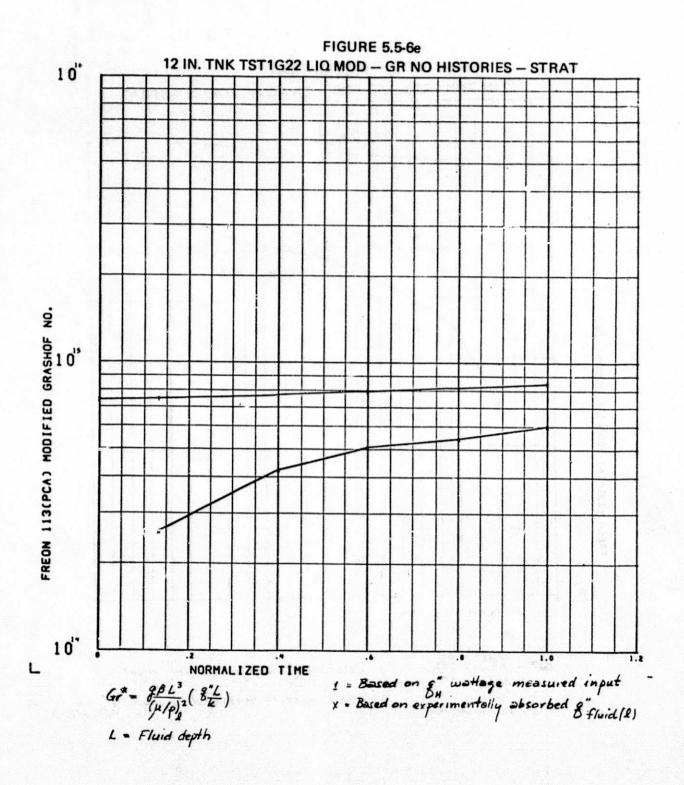


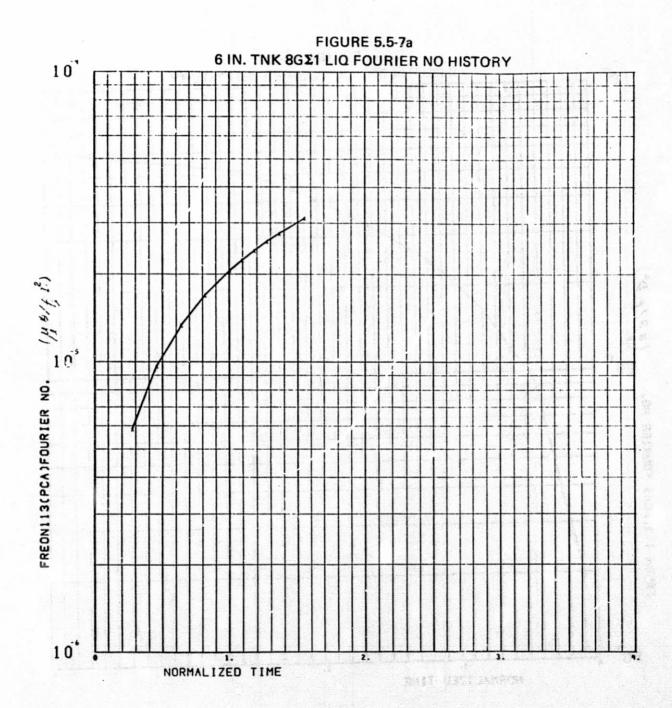


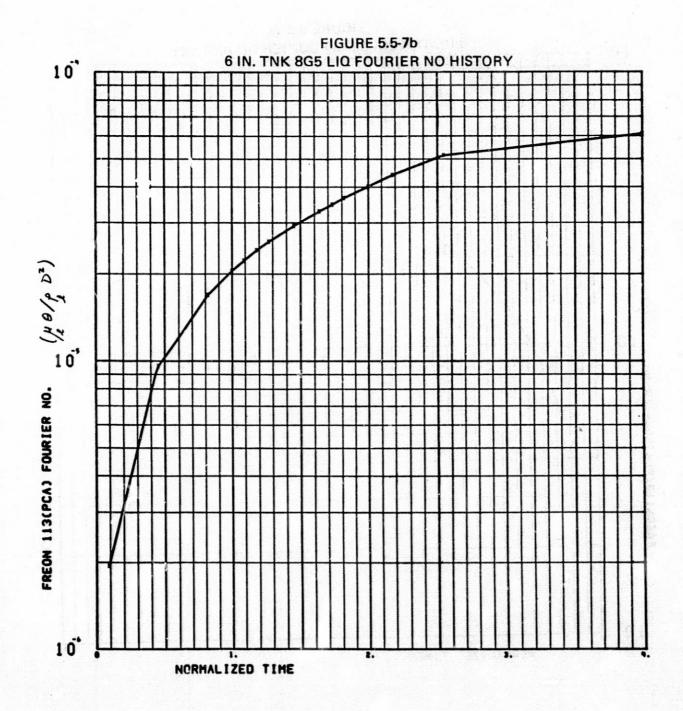
$$GR^* = \frac{g \beta L^3}{(\mu/\rho)^2} (\frac{g''L}{k})$$
 1 = Based on g'' wottage measured input

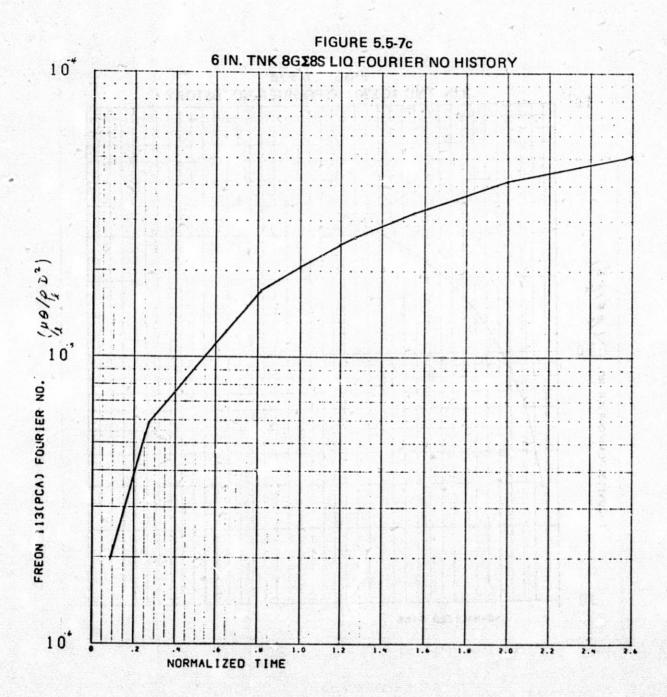
 $X = Based$ on experimentally determined g''

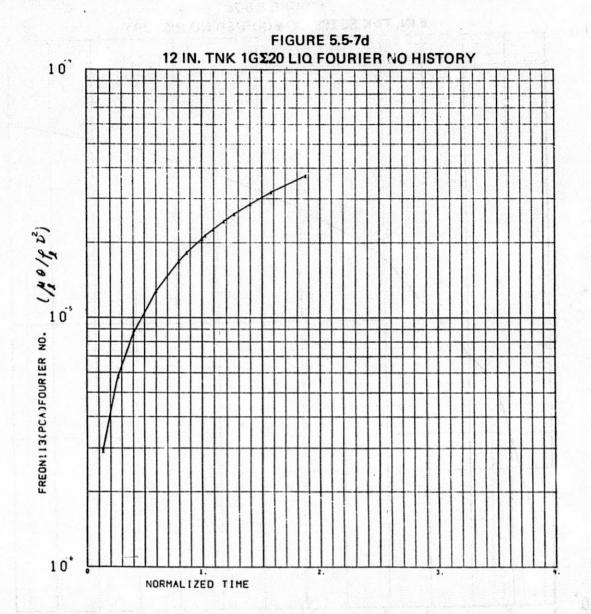
 $L = Fluid$ destin

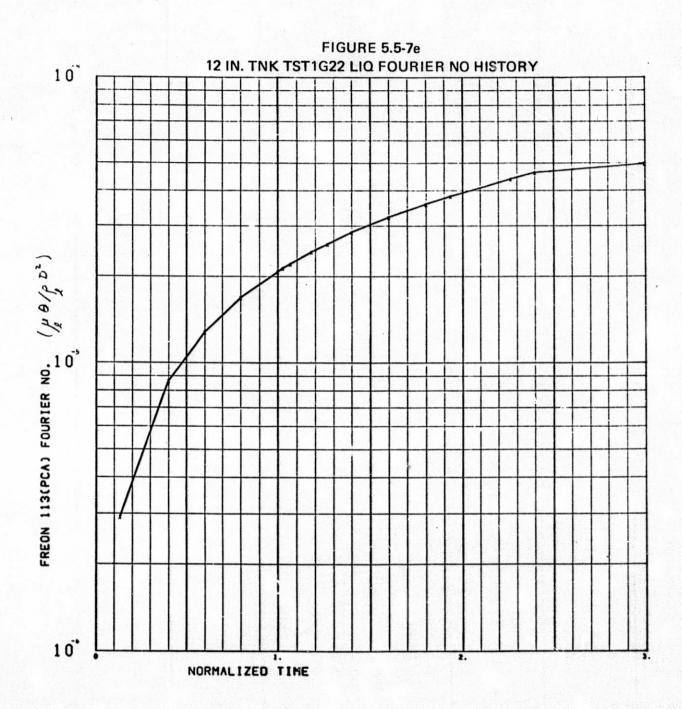












Section 5.6
SCALING SET

6-inDia Tank Tests	12-in Dia Tank Tests
8G	1G
Test #4	Test #23
Test #6	Test #28

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Table 5.6-la. 6 IN. DIA. TANK TEST 8G#4 (Page 1 of 3)

					- American
CTRICTURAL	GEOMETRIC	TANK	MISHATTHETER	MEAT FLUX	INPUTS
ALLIABIALIME	APALIP 1115A	1 -	M - DM - - -		

DOME AREA FT2# .3927 CYL AREA FT2# 1.5708 FLNGE A &A FT2# .056# DME HALL VOLFT3# .00164 FLNGE VOL FT3# DME MASS LBM# .65596 MASS 1/2 CYL LBM# .81996 FLANGE MASS# .3855#	.00076
LIG VOL FTS: ,22907 ULLAGE VOL FTS: ,03272	
INPUT HEAT FLUXES (BTU/HR-FT2), AND ABSORBED HEAT AND TEMPERATURE ESTIMATES	
H12= 600.8488 H34= 600.8488 H56# 600.8488 H910= 600.8488 H78# 600.8488	
EST, HT FLUX IN LIG (BTU/HR=FT2) = 600.8488 EST, HT FLUX IN ULLGE (BTU/HR=FT2) = 600.8488 EST, HT INPUT LIG(STRAT) BTU = 73.735 (STRAT+DESTRAT) BTU = 111.429 EST, LIG TEMP INCRSE(STRAT) = 15.1319F (STRAT+DESTRAT) = 22.8570F	
EST, HT INPUT ULLAGE (STRAT) BTU: 14:747 (STRAT DESTRAT) BTU: 22,286	
Table 5.6-1b. 6 IN. DIA. TANK TEST 8G#6 STRUCTURAL GEOMETRIC TANK WTS-WATTMETER HEAT FLUX INPUTS	
DOME AREA FT2= .3927 CYL AREA FT2= 1.5708 FLNGE AREA FT2= .0365 DME HALL VOL FT3= .00131 1/2 CYL WALL VOLFT3= .00164 FLNGE VOL FT3= DME MASS LBM= .65596 MASS 1/2 CYL LBM= .81996 FLANGE MASS= .38058	.00076
DOME AREA FT2= .3927 CYL AREA FT2= 1.5708 FLNGE AREA FT2= .0365 DME HALL VOL FT3= .00131 1/2 CYL WALL VOLFT3= .00164 FLNGE VOL FT3=	.00076
DOME AREA FT2= .3927 CYL AREA FT2= 1.5708 FLNGE AREA FT2= .0365 DME WALL VOL FT3= .00131 1/2 CYL WALL VOLFT3= .00164 FLNGE VOL FT3= DME MASS LBM= .65596 MASS 1/2 CYL LBM= .81996 FLANGE MASS= .38058	.00076
DOME AREA FT2= .3927	.00076

(STRAT+DESTRAT)BTU≂

EST.HT INPUT ULLAGE(STRAT)BTU= 14.944

1

52.434

Table 5.6-1c. 12 IN. DIA. TANK TEST 1G#23 (Page 2 of 3)
STRUCTURAL GEOMETRIC TANK WTS-WATTMETER HEAT FLUX INPUTS

ARTH BUT SERVE CONTRACTOR OF THE CONTRACTOR OF T

DOME AREA FT2= 1.5708 DME HALL VOL FT3= .01047 DME HASS L8M= 5.24772	CYL AREA FT2= 6.283 1/2 CYL WALL VOLFT MASS 1/2 CYL LBM= 6.5	3= .01309 FLNGE VOL FT3	,00608
LIO VOL FT3# 1.83260	ULLAGE VOL FT3# ,26	180	
INPUT HEAT FLUXES (STU/HR	FT2), AND APSORBED HEAT	AND TEMPERATURE ESTIMATES	
H12= 300,4244 H34= 300,42	244 H56# 299,5561 H	19107 300,4244 H78= 300,4244	
EST. HT FLUX IN LIG (STU/HR		·	
EST. HT FLUX IN ULLGE (BTU/) EST. HT INPUT LIG(STRAT)BTU: EST. LIG TEMP INCREE(STRAT)	= 589,200 (STRAT+D	ESTRAT)BTU= 1086,485 +DESTRAT)= 27.3279F	

Table 5. 6-1d. 12 IN. DIA. TANK TEST 1G#28 (Page 3 of 3) STRUCTURAL GEOMETRIC TANK WIS-WATTMETER HEAT FLUX INPUTS

경기 가장 보면 보다 되었다. 그는 것이 되었다는 것은 것이 되었다면 되었다면 되었다면 보다 되었다면 보다 되었다면 보다 되었다면 보다 되었다면 되었다면 되었다면 되었다면 되었다. 그렇게 되었다면 보다 되었다면	• • • • • • • • • • • • • • • • • • • •
DOME AREA FT2= 1.5708 CYL AREA FT2= 6.2832 FLNGE AREA FT2= .1458	
DME WALL VOL FT3= .01047 1/2 CYL WALL VOLFT3= .01309 FLNGE VOL FT3=	.00608
DHE MASS LBM= 5.24772 MASS 1/2 CYL LBM= 6.55965 FLANGE MASS= 3.04465	
LIQ VOL FT3= 1.83260 ULLAGE VOL FT3= .26180	
INPUT HEAT FLUXES (BTU/HR-FT2), AND ABSORBED HEAT AND TEMPERATURE ESTIMATES	
H12= 300.4244 H34= 300.4244 H56= 299.5561 H910= 300.4244 H78= 300.4244	
EST.HT FLUX IN LIQ (BTU/HR-FT2) = 300.0771	
EST. HT FLUX IN ULLGE (BTU/HR-FT2) = 300.4244	
EST.HT INPUT LIG(STRAT)BTU= 589.200 (STRAT+DESTRAT)BTU= 1139.120	
EST.LIQ TEMP_INCRSE(STRAT) = 15.1106F (STRAT+DESTRAT) = 29.1734F	
EST.HT INPUT ULLAGE(STRAT)BTU= 117.976 (STRAT+DESTRAT)BTU= 228.088	

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TEMPERATURE MATRIX-STRATIFICATION

TIME(M	IN) 0.000 1.000	1,667 2,33	0 3,000 3,750
TAU	C.000 .267	445 .621	.800 1.000
1	116,333 122,750 12	6.792 130.375	134,083 137,958
2		9,563 132,833	
3		2,333 135,292	
4	그리는 이번 보고 있는데 그렇게 보고 있는 전에 없고 있어 없는데 이번 때문에 되었다.	1,792 134,458	
5		,500 131,708	
6		.083 131,333	
7	그 그 그 그렇게 이번 그림 집에 그리고 모르고 있는 요리가 있고 있었다. 중에 보는 것이라면 되었다.	958 131,208	
8		.625 130.000	132,167 133.792
9		.833 122.333	124,125 125.792
10		.667 135.833	139.083 142.458
11		.292 135.167	137,833 140,583
12		.708 134.083	136,458 138,667
13		,583 130,958	[1] (1] [1] [1] [1] [1] [1] [1] [1] [1] [1] [
14		.792 130.375	132,625 134.375
15		708 132,917	134.083 137.958
16			136.417 139.583
17	아이는 아이는 것이 아이를 가고 있다면 그는 아이를 가게 되었다면 하고 있다면 하셨다면 하는데 아이를 하였다.		135,042 137.708
18	115 089 403 337 405	,583 128,500	130,958 133,083
19		,375 127,708	129,458 131.000
20		1542 122,417	124.125 125.917
21		.667 135,833	139.083 142.458
		,292 135,167	137,833 140,583
22		.708 134.083	136,458 138.667
23		,583 130,958	132.625 134.375
24		.708 186.250	200,583 213.333
25		.917 135.500	147,625 157.958
26		.417 130.583	135,167 139.833
27		.500 130.625	135,208 139,792
28	116,667 125,500 134	. CB3 144.00C	154.875 166.000
29		.750 156.792	167,917 178.792
30	116,667 159,042 181	.958 200.292	215.625 228.875
31	115,167 126,833 127		129,167 130.708
32	115,167 126,833 127	667 127.792	129,167 130,708
33		.833 121.667	122.750 124.125
34		,583 117.917	118,958 120,208

	Table 5.	6-2a. 6 II	N. DIA TA	ANK TEST	8G #4 (P	age 2 of 2	2)
	35	108,917	110,375		113.042		115.333
	36	115,167	126,833	127,667	127.792	129,167	130.708
•	37	117,000	126,458	137,917	151,000	165,167	178.500
	38	117,083	122,917	129,292	142.333	155,250	167.750
	39	117,083	123,458	129,542	138.792		158,542
		117,458	123,250	129,042	134.208	140,208	146.000
	40	117,417	121,292	124.708	128,542	131,917	136,000
	41		121,375	125.750	129.750	132.917	136,083
	42	117,375	121,667	125.250	128.542	132.542	136.500
	43	117.542	123,042	126,583	129.333	132,250	135,500
		117,458	121,417	124,583	128.375	131.875	135.833
	45		122,417	125.875	129.583	133,292	137.125
	46	117,417	122,958	126,292	129,292	133,250	137.250
	47	117,500		125,208	127,917	131,375	134.750
	48	118,000	121,833		126.042	128.875	131.500
	-49	116,542	119,500	122.750	125.542	128.625	131.375
	50	116,875		121.750	124.750	127 333	130.000
	51	116,458	118,917	122.417	125,188	128,063	130.521
	52	117,208	119,792	121,542	123.958	127,000	129.667
	53	116,333	119,500			128,792	131.042
	54	117,958	120,667	123.083	125.625		
-	55	117,708	120,875	123.375	126.250		131,708
	56	117.958	120,667		125,625	128.792	131.042
	57	117,708	120,875	123,375		129.250	128 876
	58	116,417	119,208	121,333	123.708		128.875
	59	117,417	119,667	122.083	124,456		129.792
	60	118,833	120,875	123,083	*** *** *** *** *** *** *** *** *** **	127,792	
	61	116.000	116,792	118,625	120.500	140,492	125,125
	62	115,833	116,792	118,333	120.417		124.583
	63	116,958	117,833	119,667	121.417	123.917	
	64	113,208	119,083	120,792	122.417		125.875
	65	115.917	116,125	117,333	118.708		
	66	116,042	116,125	116.917	118.667	120,292	121.708
	67	116.792	116,958	117,750	119.500		122.708
	68	117.750	118,000	118,625	119.792	121,500	123.125
	69	115,875	115,750		117.417	118,958	120.417
	70	115,958	116,000	116.500	117.458	119,125	120.417
	71	116,333	116,583	117.125	118.375	119.00/	121.375
	72	117.375	118,042	118,833	120.083	121,375	122.917
	73				117.750	119,00/	121,250
	74	107,125	108,417	109,750	111.500	113,833	116.042
	75	93,333	93,417	93,500	93.625	94,125	
	76	105,583	105,792	106,333	107.042	108,000	108.958
	77	91.750	91,417	91.042	90.792	90.958	90.958

.)

					7 147	7 800
TIME (MIN)	0.000	.833	1.500	2.500	3.167	000
TIME (MIN)	0 000	210	.395	658	.033	
1	117 125 1	27-542 1	20.500	330176 1	HISTON T	241
ż	7 /1 4 7 4	20 202 1	77.667	19-750 1	460176 1	
	117.417 1 -1-1-7.553-1	27-417-1	-31-+833-1	34.708-1	39.667-14	15433
4	117.875 1	27.250 1	31.458	35.700 1	20.3/2 1.	.0.730
5	117 354 1	25.417 1	29.500	33.458 1	35.875 1	58.125
6	-1-17-042-1	25.792-	29.125-	32.625-1	35.042-1	31.200-
7	117.417 1	26.375	28.667	132.333 1	34.333 1.	30.411
8	#50 4	26.125	26.167	132.625	34.500 1	36.500
		24-125-	1-21-192	1-24-250-1	26-125-1	27-66/-
10	117 147 1	28-125	132.158	137.250	40.303 1	43.130
11	7 775 4	28 625	171 -877	136-375	39.125 1	41.500
12	-1-17-708-1	29-458	131.583-	1-35-500-1	-37-833-1	59-108
13	117-000 1	27.833	129.625	132.042	135,000 1	33.430
i4	114 500	21 587	125.067	131.333	135.458 1	40.167
15	-116-607-1	-25-750-	124.750-	1-33-958-	137-3/5-1	40-625
16	117.167	26-167	130.125	133.625	132.012 1	37.046
17		NO DER	126.417	129.875	132.000 1	34.167
18	ALE OLB	22 917-	125-167-	128-542-	130-125-1	32-042
19	115 75A	118-433	120.583	123.292	125,200 1	50.033
20	117 167	28-125	132.458	137.250	140.583 1	45.750
21	117 775	L28-625-	1-31-833-	1-36-375-	139-1-25-1	41-500
55	117 708	129-458	131.583	135.500	137.835 1	34.700
23	117 000	27 833	129-625	132.042	133.503 1	35.450
24	414 RZZ	45-833	160-167-	191-208-	205-542-6	10.342
25	116 583	121-542	126.458	140.5/5	1200223	37.046
26	503	20 877	124.833	130.708	134.792 1	38.917
27	14 E 0 3	+30-H75-	1-24-875-	1-50-667-	134.833-1	38-75
28	117-000	123.792	132.125	147.042	12/6420 7	07.003
29	116 667	171 917	143-250	160.000	171.042 1	01.0/5
30	-117-000-	153-792	177.792-	206.125-	221.458 2	35.292
31	116 431	127-194	128.264	129.278	130.150 1	36.676
32	7 208	128 167	129.375	130.083	131.41/ 1	55.125
33	- A.F. ART	++B-833-	+20-500-	121-958-	123-167-1	24.585
34	111-125	112.708	114.458	116.583	117.917	19.125
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35		Table 5.6-2b. 6 IN. DIA FANK TEST 8G #6 (Page 2 of 2)
110.042 120.708 127.706 128.875 130.417 131.875 117.167 124.417 135.583 155.708 168.333 180.583 117.000 121.917 127.208 146.292 158.542 171.542 39 117.208 122.125 127.208 136.250 41.458 152.458 40 117.458 121.792 127.208 135.250 41.458 152.458 41 117.167 121.583 125.500 131.525 1.375 139.250 42 117.125 121.625 125.500 131.542 13.958 139.458 43 117.333 121.792 125.750 131.592 13.958 139.458 44 117.458 122.000 125.917 132.125 136.003 139.792 45 117.292 121.708 125.792 131.750 135.667 139.353 46 117.417 121.875 126.125 132.042 135.998 140.417 47 117.633 122.583 126.708 132.042 135.998 140.417 48 116.917 119.625 122.250 127.250 130.417 133.042 50 117.208 119.542 122.375 127.417 130.000 132.500 51 17.000 119.208 121.625 126.833 129.271 131.750 52 117.688 119.896 122.625 126.833 129.271 131.750 53 116.875 119.375 121.958 126.000 128.333 130.750 54 118.375 120.583 123.625 127.375 129.750 132.333 57 118.250 120.750 123.125 127.667 130.167 132.875 56 118.375 120.583 123.625 127.375 129.750 132.333 57 118.250 120.750 123.125 127.667 130.167 132.875 58 116.917 119.208 121.375 125.500 127.917 130.375 59 118.042 119.667 121.917 126.083 128.292 130.792 60 119.250 120.750 123.125 127.667 130.167 132.875 61 16.542 119.086 121.375 125.500 127.917 130.375 61 16.542 119.086 121.375 125.500 127.917 126.708 65 116.375 117.042 118.958 121.958 124.125 125.917 62 116.603 119.000 120.625 122.917 124.792 126.6708 65 116.375 116.292 117.542 120.083 121.708 123.417 66 116.500 117.958 119.025 122.910 121.875 126.708 67 117.167 117.125 117.928 129.958 124.125 123.375 68 116.803 118.083 118.417 120.458 121.625 123.625 70 116.803 118.083 118.417 120.458 121.625 123.625 71 116.708 116.998 117.417 119.002 120.858 121.625 123.857 72 117.500 117.958 117.417 119.002 120.858 121.625 123.857 73 115.417 116.917 117.167 119.002 120.858 121.625 123.855 61 16.708 116.998 117.417 119.002 120.858 121.625 123.855 61 16.167 116.002 117.958 117.417 119.002 120.858 121.625	35	106.625 107.583 108.708 110.625 111.917 112.958
117.167 124.417 135.583 155.708 168.333 180.583 117.000 121.917 127.208 146.292 158.542 171.542 171.542 171.542 171.542 171.542 171.542 171.542 171.542 171.542 171.542 171.542 171.542 171.542 171.542 171.545 121.792 127.208 135.250 41.458 152.458 41 117.167 121.583 125.500 131.542 13.958 139.458 42 117.125 121.625 125.500 131.542 13.958 139.458 43 117.333 121.792 125.750 131.500 135.917 139.583 44 117.458 122.000 125.917 132.125 136.083 139.792 45 117.292 121.708 125.792 131.750 135.697 139.667 137.691 171.693 122.563 126.708 132.042 135.792 139.667 117.693 122.548 122.375 124.633 129.667 133.083 139.667 133.083 139.667 137.688 119.542 122.375 127.417 130.000 132.500 117.008 119.542 122.375 127.417 130.000 132.500 117.008 119.542 122.375 127.417 130.000 132.500 117.608 119.542 122.375 126.67 130.167 132.675 136.375 120.583 123.625 126.833 129.271 131.750 136.875 136.375 120.583 123.625 126.833 129.750 132.333 159.675 136.375 120.583 123.625 127.375 129.750 132.333 159.675 136.375 120.583 123.625 127.375 129.750 132.333 159.675 136.375 120.583 123.625 127.375 129.750 132.333 159.675 136.375 120.583 123.625 127.375 129.750 132.333 159.675 136.671 139.208 121.375 127.375 129.750 132.333 130.750 136.575 136.550 120.750 123.375 125.500 127.917 130.375 136.675 136.671 137.675 136	36	116.042 126.708 127.708 128.875 130.417 131.875
117.000 121.917 127.208 146.292 158.542 171.542 39	37	117.167 124.417 135.583 155.708 168.333 180.583
117.208 122.125 127.75h 141.583 151.560 161.7h8 40 117.458 121.792 127.208 135.250 41.458 152.458 41 117.167 121.583 125.500 131.625 1.375 139.250 42 117.125 121.625 125.500 131.542 132.958 139.458 43 117.433 121.792 125.750 131.500 135.917 139.563 139.762 45 117.458 122.000 125.917 132.125 136.083 139.762 45 117.471 121.875 126.125 132.042 135.792 139.567 139.353 46 117.417 121.875 126.125 132.042 135.792 139.667 139.353 47 117.633 122.583 126.708 132.042 135.792 139.667 133.042 135.792 139.667 133.042 135.792 139.667 133.042 135.792 139.667 133.042 135.792 139.667 133.042 135.792 139.667 133.042 117.208 119.525 122.250 127.250 130.417 133.042 117.208 119.542 122.255 127.250 130.417 133.042 117.000 119.208 121.625 126.803 129.271 131.750 131.6875 119.375 121.958 126.600 128.333 130.750 136.875 116.875 119.375 121.958 126.600 128.333 130.750 138.250 120.750 123.125 127.667 130.167 132.875 118.250 120.750 123.125 127.667 130.167 132.833 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 132.333 16.375 129.750 123.333 129.271 130.375 129.250	ZA.	117.000 121.917 127.208 146.292 158.542 171.542
40		117.208 122 125 127 75. 1/1 587 454 550 144 7.0
41		117-458 121 702 127 208 175 250 44 450 412 450
#2 117.125 121.025 125.500 131.502 13.958 139.458 #3 117.333 121.792 125.750 131.500 135.917 139.583 #4 117.458 122.000 125.917 132.125 136.083 139.792 #5 117.292 121.708 125.792 131.750 135.667 139.333 #6 117.417 121.875 126.125 132.042 135.958 140.417 #7 117.833 122.583 126.708 132.042 135.958 140.417 #6 116.167 121.125 124.833 129.667 133.083 136.333 #9 116.917 119.625 122.250 127.250 130.417 133.042 50 117.208 119.542 122.375 127.417 130.000 132.500 117.000 119.542 122.375 127.417 130.000 132.500 51 117.000 119.542 122.375 127.417 130.000 132.500 51 117.000 119.542 122.625 126.292 128.792 131.167 52 117.688 119.896 122.625 126.833 129.271 131.750 53 116.875 119.375 121.958 126.000 128.333 130.750 54 118.375 120.583 123.625 127.375 129.750 132.333 57 118.250 120.750 123.125 127.667 130.167 132.875 58 116.917 119.208 121.375 125.500 127.917 130.375 58 116.917 119.208 121.375 125.500 127.917 130.375 60 119.250 120.750 123.125 127.667 130.167 132.875 61 116.542 117.042 118.958 121.958 124.125 125.917 62 116.792 117.083 118.708 121.958 124.125 125.917 62 116.500 117.042 118.958 121.958 124.125 125.917 63 116.500 117.042 118.958 121.958 124.125 125.917 64 116.500 117.058 119.625 123.008 124.958 126.083 65 116.375 116.292 117.592 123.508 124.125 125.917 66 116.375 116.292 117.592 120.500 121.875 123.3417 67 117.167 117.125 117.792 120.500 121.875 123.3417 68 118.083 118.083 118.417 120.0458 121.625 123.625 69 116.167-116.042-116.542-118.375-119.75.1-21.000 70 116.333 116.975 116.708 118.417 119.875 121.125 71 116.708 116.998 117.417 119.042 120.583 121.625 72 117.500-118.208 119.125-120.958 122.042 123.625 73 115.417 116.917 117.167 119.042 120.583 121.625 74 118.459 119.450 119.08 119.88 114.417 119.875 121.125 75 118.33 13.9500 106.792 107.958 108.750 109.542		117.167 121 587 125 500 171 425 175 177 178 278
43	도시 : [1] : [1] : [1] : [1] : [1] : [1] : [1] : [1] : [1] : [1] : [1] : [1] : [1] : [1] : [1] : [1] : [1] : [1]	117 125 121 125 125 126 126 127 127 127 127 127 127 127 127 127 127
44 117.458 122.000 125.917 132.125 136.083 139.792 45 117.292 121.708 125.792 131.750 135.667 139.333 46 117.417 121.875 126.125 132.042 135.798 140.417 47 117.833 122.583 126.708 132.042 135.792 139.667 48 118.167 121.125 124.833 129.667 133.083 136.333 49 116.917 119.625 122.250 127.250 130.417 133.042 50 117.208 119.542 122.375 127.417 130.000 132.500 51 117.000 119.208 121.625 126.292 128.792 131.167 52 117.688 119.896 122.625 126.833 129.271 131.750 53 116.875 119.375 121.958 126.000 128.333 130.750 54 118.375 120.583 123.625 127.375 129.750 132.333 55 118.250 120.750 123.125 127.667 130.167 132.875 56 118.375 120.583 123.625 127.667 130.167 132.875 57 118.250 120.750 123.125 127.667 130.167 132.875 58 116.917 119.208 121.375 125.500 127.917 130.375 59 118.042 119.667 121.917 126.083 128.292 130.792 60 119.250 120.750 123.125 127.667 130.167 132.875 61 16.542 117.042 118.958 121.958 124.125 125.917 62 116.792 117.083 118.708 122.042 123.583 125.583 63 117.500 117.958 119.625 122.917 124.792 126.708 65 116.375 116.292 117.542 120.083 121.708 123.417 66 116.500 116.417 117.000 119.542 120.917 122.208 67 117.167 117.125 117.792 120.500 121.875 123.375 68 116.375 16.292 117.542 120.083 121.708 123.417 69 118.500 119.000 120.625 122.917 124.792 126.708 60 116.333 116.875 116.708 118.417 119.875 121.25 60 116.600 116.417 117.000 119.542 120.917 122.208 61 116.500 116.417 117.125 117.792 120.500 121.875 123.375 62 116.407 116.918 117.417 119.045 121.075 121.833 63 117.600 117.958 117.542 120.083 121.708 123.417 64 116.500 116.417 117.125 117.792 120.500 121.875 123.375 65 116.335 116.958 117.417 119.095 121.833 67 116.408 119.608 119.608 119.608 121.005 121.875 121.825 68 116.408 118.808 118.417 120.458 121.025 121.825 69 116.407 116.908 119.608 119.608 120.608 121.708 123.417 60 116.500 116.417 117.105 118.417 119.875 121.225 61 116.500 116.417 117.105 118.417 119.042 120.875 121.833 62 116.500 116.608 119.608 119.608 119.608 120.608 120.608 120.608 120.608 120.608 120.608 120.608 120.608 120.608 120.608 120.608		117-333 121 702 125-500 131-542 133-958 139-458
45		117-458 132 000 135 917 173 135 177 007 170 700
117.417 121.875 126.125 132.042 135.958 140.417 117.833 122.583 126.708 132.042 135.792 139.667 118.167 121.125 124.833 129.667 133.083 136.333 49 116.917 119.625 122.250 127.250 130.417 133.042 50 117.208 119.542 122.375 127.417 130.000 132.5500 51 117.000 119.208 121.625 126.292 128.792 131.167 52 117.688 119.896 122.625 126.833 129.271 131.750 53 116.875 119.375 121.958 126.000 128.333 130.750 54 118.375 120.583 123.625 127.375 129.750 132.333 55 118.250 120.750 123.125 127.667 130.167 132.875 56 118.375 120.583 123.625 127.375 129.750 132.333 57 118.250 120.750 123.125 127.667 130.167 132.875 58 116.917 119.208 121.375 125.500 127.917 130.375 59 118.022 119.667 121.917 126.083 128.292 130.792 60 119.250 120.542 122.792 126.792 129.000 131.375 61 116.542 117.042 118.958 121.958 124.125 125.917 62 116.792 117.083 118.708 122.042 123.583 125.583 63 117.7500 117.958 119.625 123.208 124.958 126.603 64 118.500 119.000 120.625 122.917 124.792 126.708 65 116.375 116.292 117.542 120.083 121.708 123.417 66 116.500 116.417 117.000 119.542 120.917 122.208 67 117.167 117.125 117.792 120.500 121.875 123.375 68 118.083 118.083 118.417 120.458 121.625 123.625 70 116.708 116.958 117.417 119.292 120.875 121.83 72 117.500-118.208 119.125-120.958 122.042 123.583 73 115.417 116.917 117.167 119.042 120.583 121.625		117 303 122 000 125 717 132 125 136 083 139 792
117.833 122.583 126.708 132.042 135.792 139.667 48	그러워 맛이 없었다. 그는 이 아이를 하다.	117 /117 121 875 126 125 172 131 050 133 887 139 333
## 116.167 121.125 124.833 129.667 133.083 136.333 #9		117-877 122 587 126 708 172 042 135,938 140,417
116-917 119-625 122-250 127-250 130-417 133-042 117-208 119-542 122-375 127-417 130-000 132-500 117-000 119-208 121-625-126-292 128-792 131-167 117-688 119-896 122-625 126-292 128-792 131-167 116-875 119-375 121-958 126-000 128-333 130-750 118-375 120-583-123-625-127-375-129-750-132-333 16-875 120-583 123-625 127-375-129-750-132-333 18-250 120-750 123-125 127-667 130-167 132-875 18-375 120-583 123-625 127-375 129-750 132-333 16-917 119-208 121-375 125-500 127-917 130-375 18-250 120-750-123-125-127-667 130-167-132-875 18-042 119-667 121-917 126-083 128-292 130-792 18-042 119-667 121-917 126-083 128-292 130-792 118-042 119-667 121-917 126-083 128-292 130-792 118-042 117-042 118-958 121-958 124-125 125-583 116-917 119-208 121-375-129-000-131-375-128-128-128-128-128-128-128-128-128-128		118 147 121 125 124 977 120 (17 177 007 12)
117.208 119.542 122.375 127.417 130.000 132.500 117.000 119.208 121.625 126.292 128.792 131.167 52		116, 917 119 625 122 250 127 250 170 117 127
51		117 208 119 5/2 122 775 127 /17 172 000 173 500
117.688 119.896 122.625 126.833 129.271 131.750 116.875 119.375 121.958 126.000 128.333 130.750 116.875 119.375 121.958 126.000 128.333 130.750 118.375 120.583 123.625 127.375 129.750 132.333 118.250 120.750 123.125 127.667 130.167 132.875 118.250 120.750 123.125 127.667 130.167 132.875 118.250 120.750 123.125 127.667 130.167 132.875 118.250 120.750 123.125 127.667 130.167 132.875 118.250 120.750 123.125 127.667 130.167 132.875 118.042 119.268 121.375 125.500 127.917 130.375 118.042 119.667 121.917 126.083 128.292 130.792 60 119.250 120.542 122.792 126.792 129.000 131.375 61 116.542 117.042 118.958 121.958 124.125 125.917 62 116.792 117.083 118.708 122.042 123.583 125.583 63 117.500 117.083 118.708 122.042 123.583 125.583 64 118.500 119.000 120.625 122.917 124.992 126.708 65 116.375 116.292 117.542 120.083 121.708 123.417 66 116.500 116.417 117.000 119.542 120.917 122.208 67 117.167 117.125 117.792 120.500 121.875 123.375 68 118.083 118.083 118.417 120.458 121.625 123.625 69 116.167 116.042 116.542 118.375 119.75 1-121.000 70 116.333 116.375 116.708 118.417 119.875 121.125 71 116.708 116.958 117.417 119.292 120.875 121.833 72 117.500 118.208 119.125 120.958 122.042 123.417 73 115.417 116.917 117.167 119.042 120.583 121.625 74 108.458 109.458 111.083 114.417 116.917 119.708 75 94.833 95.000 95.208 95.875 96.292 96.833		117.200 117.342 122.373 127.417 130.000 132.500
116.875 119.375 121.958 126.000 128.333 130.750 118.375 120.583 123.625 127.375 129.750 132.333 55 118.250 120.750 123.125 127.667 130.167 132.875 56 118.375 120.583 123.625 127.375 129.750 132.333 57 118.250 120.750 123.125 127.667 130.167 132.875 58 116.917 119.208 121.375 125.500 127.917 130.375 59 118.042 119.667 121.917 126.083 128.292 130.792 60 119.250 120.542 122.792 126.792 129.000 131.375 61 116.542 117.042 118.958 121.958 124.125 125.917 62 116./92 117.083 118.708 122.042 123.583 125.583 63 117.500 117.958 119.625 123.208 124.958 126.833 64 118.500 119.000 120.625 122.917 124.792 126.708 65 116.375 116.292 117.542 120.083 121.708 123.417 66 116.500 116.417 117.000 119.542 120.093 121.875 123.375 68 118.083 118.083 118.417 120.458 121.625 123.625 69 116.167 116.042 116.542 118.375 119.75 123.375 68 118.083 118.083 118.417 120.458 121.625 123.625 71 116.708 116.998 117.417 119.292 120.875 121.833 72 117.500 118.208 117.417 119.292 120.875 121.833 73 115.417 116.917 117.125 120.958 122.042 123.417 73 115.417 116.917 117.167 119.042 120.583 121.625 74 108.458 109.458 111.083 114.417 116.917 119.708 75 94.833 95.000 95.208 95.875 96.292 96.833		117 688 119 896 123 625 124 927 128 274 127
54		116 875 449 775 424 959 426 833 129.271 131.750
118.250 120.750 123.125 127.667 130.167 132.835 118.250 120.583 123.625 127.375 129.750 132.333 57 118.250 120.750 123.125 127.667 130.167 132.875 58 116.917 119.208 121.375 125.500 127.917 130.375 59 118.042 119.667 121.917 126.083 128.292 130.792 60 119.250 120.542 122.792 126.792 129.000 131.375 61 116.542 117.042 118.958 121.958 124.125 125.917 62 116.792 117.083 118.708 122.042 123.583 125.583 63 117.500 117.958 119.625 123.208 124.958 126.833 64 118.500 119.000 120.625 122.917 124.792 126.708 65 116.375 116.292 117.542 120.083 121.708 123.417 66 116.500 116.417 117.000 119.542 120.917 122.208 67 117.167 117.125 117.792 120.500 121.875 123.375 68 118.083 118.083 118.417 120.458 121.625 123.625 70 116.333 116.375 116.708 118.417 119.875 121.125 71 116.708 116.958 117.417 119.292 120.875 121.125 71 116.708 116.958 117.417 119.292 120.875 121.833 72 117.500 118.208 119.125 120.958 122.042 123.417 73 115.417 116.917 117.167 119.042 120.583 121.625 74 108.458 109.458 111.083 114.417 116.917 119.708 75 94.833 95.000 95.208 95.875 96.292 96.833		118 775 120 597 127 425 127 775 128 333 130 750
118.375 120.583 123.625 127.375 129.750 132.333 57	경영, 성인 이번 보고 있어야 있네다. 하는데 얼굴 없었다.	118 250 120 750 123 125 127 177 177 177 177
57		110.230 120.730 123.123 127.667 130.167 132.875
116.917 119.208 121.375 125.500 127.917 130.375 118.042 119.667 121.917 126.083 128.292 130.792 60		110.375 120.303 123.025 127.375 129.750 132.333
118.042 119.667 121.917 126.083 128.292 130.792 119.250-120.542-122.792-126.792-129.000-131.375 116.542 117.042 118.958 121.958 124.125 125.917 116.792 117.083 118.708 122.042 123.583 125.583 117.500-117.958-119.625-123.208-124.958-126.833 118.500 119.000 120.625 122.917 124.792 126.708 116.375 116.292 117.542 120.083 121.708 123.417 116.500-116.417-117.000-119.542-120.917-122.208 117.167 117.125 117.792 120.500 121.875 123.375 118.083 118.083 118.417 120.458 121.625 123.625 116.167-116.042-116.542-118.375-119.75.3-121.000 70 116.333 116.375 116.708 118.417 119.875 121.125 71 116.708 116.958 117.417 119.292 120.875 121.833 72 117.500-118.208 119.125-120.958 122.042 123.417 73 115.417 116.917 117.167 119.042 120.583 121.625 74 108.458 109.458 111.083 114.417 116.917 119.708 75 94.833 95.000 95.208 95.875 96.292 96.833		116.250 120.750 125.125 127.667 130.167 132.875
60		110.717 117.200 121.375 125.500 127.917 130.375
61		110.042 117.007 121.417 126.083 128.292 130.792
116.792 117.083 118.708 122.042 123.583 125.583 117.500-117.958-119.625-123.208-124.958-126.833 64	얼마를 잃었다는 아이들이 없는 사람이 없었다면서	117 = 20 - 120 = 342 - 122 = 120 - 12
117.500-117.958-119.625-123.208-124.958-126.833-64 118.500 119.000 120.625 122.917 124.792 126.708 116.375 116.292 117.542 120.083 121.708 123.417 116.500-116.417-117.000-119.542-120.917-122.208-67 117.167 117.125 117.792 120.500 121.875 123.375 68 118.083 118.083 118.417 120.458 121.625 123.625 116.167-116.042-116.542-118.375-119.752-121.000-70 116.333 116.375 116.708 118.417 119.875 121.125 71 116.708 116.958 117.417 119.292 120.875 121.833 72 117.500-118.208 119.125-120.958 122.042 123.417-73 115.417 116.917 117.167 119.042 120.583 121.625 74 108.458 109.458 111.083 114.417 116.917 119.708 75 94.833-95.000-95.208-95.875-96.292-96.833-76 106.125 106.250 106.792 107.958 108.750 109.542		110.742 117.042 118.958 121.958 124.125 125.917
118.500 119.000 120.625 122.917 124.792 126.708 116.375 116.292 117.542 120.083 121.708 123.417 116.500—116.417—117.000—119.542—120.917—122.208—67 117.167 117.125 117.792 120.500 121.875 123.375 68 118.083 118.083 118.417 120.458 121.625 123.625 116.167—116.042—116.542—118.375—119.75—1-21.000—70 116.333 116.375 116.708 118.417 119.875 121.125 71 116.708 116.958 117.417 119.292 120.875 121.833 72 117.500—118.208 119.125—120.958 122.042 123.417 73 115.417 116.917 117.167 119.042 120.583 121.625 74 108.458 109.458 111.083 114.417 116.917 119.708 75 94.833—95.000—95.208—95.875—96.292—96.833—76 106.125 106.250 106.792 107.958 108.750 109.542		117.500 117.003 110.708 122.042 123.583 125.583
116.375 116.292 117.542 120.083 121.708 123.417 116.500—116.417—117.000—119.542—120.917—122.208— 67		119 500 119 000 129 025 125 208 124 958 126 833
116.500—116.417—117.000—119.542—120.917—122.208—67 117.167 117.125 117.792 120.500 121.875 123.375 68 118.083 118.083 118.417 120.458 121.625 123.625 69 116.167—116.042—116.542—118.375—119.753—121.000—70 116.333 116.375 116.708 118.417 119.875 121.125 71 116.708 116.958 117.417 119.292 120.875 121.833 72—117.500—118.208 119.125—120.958 122.042 123.417—73 115.417 116.917 117.167 119.042 120.583 121.625 74 108.458 109.458 111.083 114.417 116.917 119.708 75—94.833—95.000—95.208—95.875—96.292—96.833—76 106.125 106.250 106.792 107.958 108.750 109.542		110.500 119.000 120.625 122.917 124.792 126.708
117.167 117.125 117.792 120.500 121.875 123.375 118.083 118.083 118.417 120.458 121.625 123.625 116.167-116.042-116.542-118.375-119.753-121.000 116.333 116.375 116.708 118.417 119.875 121.125 116.708 116.958 117.417 119.292 120.875 121.833 72		110.373 110.292 117.542 120.083 121.708 123.417
118.083 118.083 118.417 120.458 121.625 123.625 69		110.500-110.41/-11/.000-119.542-120.917-122.208
70		11/-10/ 11/-125 11/-/92 120.500 121.875 123.375
70 116.333 116.375 116.708 118.417 119.875 121.125 71 116.708 116.958 117.417 119.292 120.875 121.833		110.003 110.003 118.417 120.458 121.625 123.625
71		110.10/-110.042-110.542-110.375-119.757-1-21.000
72		110.333 110.373 110.708 118.417 119.875 121.125
73		110.700 110.700 117.417 119.292 120.875 121.833
74 108.458 109.458 111.083 114.417 116.917 119.708 		117.500-110.200 117.125-120.958-122.042.123.417.
75 94.833 95.000 95.208 95.875 96.292 96.833 76 106.125 106.250 106.792 107.958 108.750 109.542		113.41/ 110.71/ 11/.16/ 119.042 120.583 121.625
76 106.125 106.250 106.792 107.958 108.750 109.542		
		104 125 144 250 144 702 147 000 200 700 146
77. 72.700 92.373 92.200 92.083 91.875 91.708		AA AAA AA WET AA AAA
	,,	72.100 92.313 92.200 92.083 91.875 91.708

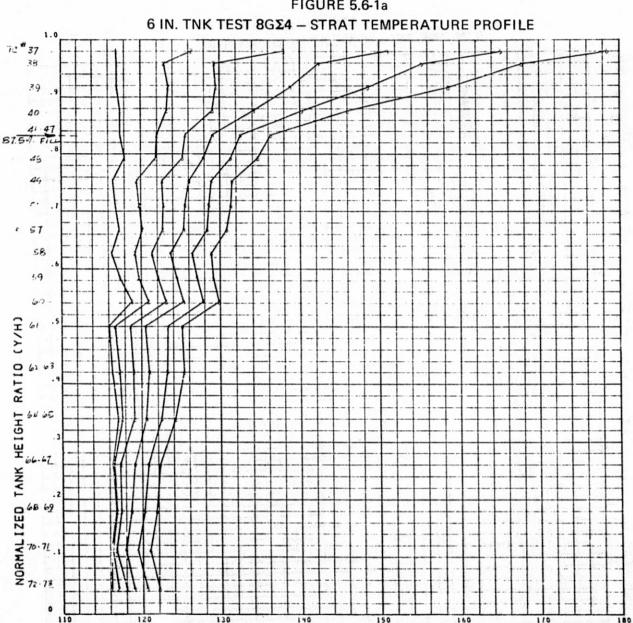
TIME (MIN))	0.00	0	3.00	0	6,00	0	9.00	0 12,0	0 15,000
TAU	0.0		,?			0.0	,	600	. 900	1,000
	116	875	122	.500	126	, 250	12	9,750		136,175
2				.375		.959	13	1,125	134,125	
3	117	167	125	458					134,458	
4						.275	13	0.750	-133.542	134,425
5	117	167	125	333	129	209	13	0.792	133,583	136,413
6		167								134,196
7		208			125	.667	-12	A . 292	130.748	133 242
ь		292				958	12	8.292	130.458	132,983
9				667		.333		5.708	127,917	130,304
10			120	252	133	167	13	. 777	430 417	142,600
11	117	125	129	625	132	792	1.31	5,542	130,3/5	141,342
12						125	43	7 050	136,458	139,196
13	117	DAR	120	458	1.51	417	137	1 250	136 05	138,425
14	116	542	123	450	126	007	4 20	1 1 2 2 3	-139,320	135,425
15	117	042	138	425	140	425	167	428	132,750	135,988
_16	117	208	127	277	130	11.40	13:	3 1 % U V	133,083	141,354
	117	000	4 2 7	E 9.2	430	700	-13.	4 50 6	-134,123	139,263
			12/	500	130	. 592	100	000	135,542	138,209
	110	925	120	ווטר	120	, 200	100	1792	133,083	135,675
	117	775	420	-10/-	12/	4-3-3-3	-144	1.792	-127-000	_120,458
20	11/1	3/3	130,	1183	103	, 292	136	458	139,458	142,796
21	11/	10/	130	n83	132	875	135	,70A	139,563	141,467
22	11/	042	144	792	131	125	134	1 unu	134,500	139,442
23	11/	083	129	083	130	. 833	132	958	135,375	137,965
24	110	792	136	458	150	958	159	8 . A75	166,125	171,408
_ 25	110	542	124	375	133	Q5A	-14.7	4625	152,583	-160,354
26	110	458	122,	167	129	,542	137	458	145,167	152,862
27	116,	500	122.	50E	129	.417	137	.375	149.167	152.858
28	116	792	135	163	157	1.67	180	1167	204,058	223.883
29	110	500	125.	708	143	.167	158	.292	173.333	190.456
30	116	583	145	750	169	. 167	184	. 333	199,292	210,517
	117	333_	124	458_	130	417	_1-32	A67-	134,717	137,413
32	117	125	127.	542	129	209	131	1292	133.500	135,963
_33	115	500	119.	750	121	292	123	חטח.	124.833	126,917
V34	115.	250	114.	950	115	292	115	.675	114.625	117,496

Τa	able 5.6-2c. 12 IN. DIA TANK TEST 1G #23 (Page 2 of 2)
35	115, 167 114, 083 113, 458 113, 125 112, 958 112, 800
36	117,708 128,708 130,667 132,750 135,167 137,638
37	117,208 129,708 151,417 174,750 194,458 214,237
38	117.125 125 083 138 750 453 075 444 075 403
39	117,125 125,083 138,750 150,875 164,875 180,412
- 40	117, 208 122,500 129,833 137,792 145,792 157,979
41	117,333 121,625 127,333 132,625 134,667 141,553
42	117,375 119,833 122,667 125,792 128,875 132,458
43	117,292 119,958 123,208 124,500 129,708 133,250
44	117,417 120,167 123,250 126,500 129,750 133,283
45	**/1/99 169.630 163.500 126.708 136.642 137 664
-46	117,375 119,792 123,292 126,500 129,667 133,296
47	** 1 2 10 16 1 7 10 1 123
48	117,500 120,167 123,417 126,708 129,917 133,504
49	44/199/ 16U.UBS 165.0B3 126.37B 120 117 170 020
50	
51	**' '''
52	++1 V(117 UUU 161 VDD 124 125 124 702 174 74
53	
54	44'1162 117,285 127,353 125,687 426 667 424 976
55	##' 1749 11749 167,200 167,200 125,417 100 000 174 747 .
56	68************************************
57	**'INYU 117.0/2 162.085 128.286 129 702 174 654
58	**'!**' ***,060 166,000 170,400 100 008 174 056
59	- 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1
60	+4'14U' 144,U42 121,417 124,527 107 105 176 775
61	**/ 1076 \$40.0/2 161.208 124.378 424.708 434 300
62	14' 14' 14' 14' 12' 12' 12' 12' 12' 12' 12' 12' 12' 12
63	44/19/2 110:020 120:708 123.500 128 017 100 149
-64	117,042 118,458 120,417 123,333 125,625 129,113
65	**************************************
66	+4'1076 1404'200 160.107 122.875 125.167 120 ATT
67	117,042 118,250 119,625 122,208 124,208 127,475
68	116,958 117,917 119,625 122,208 124,208 127,475
69	116,917 117,875 119,292 121,792 123,667 126,929
70	117,000 117,875 119,375 121,833 123,792 126,933
71	116,917 117,833 119,083 121,450 123,417 126,633 116,917 117,833 119,083 121,458 123,417 124,633
72	117, 117, 133 119, 183 121, 458 123, 417 126, 633
73	116 050 410 000 410 000 121,667 123,833 126,804
74	116,958 118,000 119,292 121,542 123,542 133,529
75	93,667 94,042 94,375 95,333 95,875 97,208
76	107,020 100,700 107,083 109,208 110,917 114,000
77	86,792 87,083 86,792 87,208 86,917 87,083
• • •	97,958 98,250 98,083 98,792 99,000 99,833

TIME (M	IIN) 0.000 3.00	00 6.000 9.000 12.000 15.000
UAT	0.000200	
1	117.000 122.708	8 126.500 129.875 133.208 136.708
5	116.958 124.500	0 128.167 131.125 134.125 137.042
. 3	117.333 125.375	5 128.625 131.458 134.208 137.042
4	117.500 125.125	5 127.958 130.583 133.333 136.208
5	117.292 125.250	0 128.208 130.792 133.292 136.250
6	117.250 123.667	7 126.250 128.667 131.125 133 833
7	117.333 123.542	2 125.833 128.167 130.417 133.000
8	117.417 123.708	8 126.000 128.000 130.292 132.583
9	116.833 120.667	7 123.333 125.458 127.583 130.042
10	117.167 129.875	133.292 136.250 139.208 142.292
11	117.292 129.792	132.667 135.458 138.042 140.917
12	117-375 128-667	7_131.208_133.542_136.125_138.917
13	117.167 129.708	131.375 133.458 135.542 137.958
14	116.792 122.917	126.625 129.833 132.958 136.292
15	117.083 128.458	132.208 135.333 138.042 141.000
16	117.333 127.792	2 130.958 133.417 136.125 139.042
17	117-125 127-542	129.958 132.542 135.042 137.708
18	117-000 126-292	128.583 130.375 132.708 134.958
19	116-583 120 0/2	123 503 134 503 132 708 134 958
20	117, 292 170 0/12	122.583 124.583 126.750 129.083
21	117 125 120 047	133.500 136.292 139.167 142.333
55	117 007 120 500	132.667 135.417 138.167 141.083
23	117 003 120 300	131.250 133.792 136.208 138.875
24	11/ 0003 120 075	130.917 132.917 134.958 137.375
25	116.075_130.292	150.625 158.917 165.458 170.292
26	116.625 124.083	133.375 142.750 151.500 158.875
27	110.500 121.792	129.042 136.625 144.167 151.083
	110.542 121.917	128.917_136.583_144.208_151.125
28	110.833 134.833	157.000 179.625 201.250 220.958
29	110.583 128.542	143.125 158.000 173.292 188.667
30	116.667_145.292_	169.750 187.750 201.583 212.750
31	117.042 128.333	130.583 132.458 134.583 136.917
32	116.875 127.375	129.333 131.250 133.208 135.667
33	115.375_119.708	121.458 122.875 124.500 126.458
34	115.083 114.875	115.333 115.583 115.917 116.708

	Table 5.6-2d. 12 IN. DIA TANK TEST 1G #28 (Page 2 of 2)
35	115-000 113 917 117 Foo 117 077 (Page 2 of 2)
₹ 36	115.000 113.917 113.500 112.833 112.458 112.333
37	117.375 128.750 130.708 132.750 134.792 137.208 117.167 130.208 152.250 174.958 195.083 313 587
38	130.200 132.200 1/4.938 195.083 212.583
39	
40	117.167 122.208 129.333 137.083 146.042 157.833
41	
42	117.500 119.625 122.833 125.917 128.958 132.250
43	117.500 120.083 123.542 126.667 129.708 132.958
44	117.583 120.250 123.542 126.708 129.708 132.917
45_	117.833 120.125 124.083 126.917 130.000 133.250
46	117.542 119.958 123.708 126.750 129.667 132.958
47	117.417 120.875 124.083 127.542 130.333 133.375
48	117.708 120.417 123.750 127.042 130.125 133.125
49	117.917 120.042 123.250 126.500 129.417 132.542
50	117-771 119-708 122-833 125-938 128-813 131-854
51_	117.625 119.375 122.417 125.375 128.208 131.167
52	117.667 119.125 121.583 124.250 126.917 129.708
53	117.625 119.417 122.375 125.375 128.000 130.958
54_	117.333 119.667 122.875 125.542 128.208 131.167
55	117.708 119.708 122.542 125.458 128.167 131.042
56	117.542 119.583 122.458 125.292 128.042 130.917 117.667 119.417 122.333 125.208 128.000 130.750
57	117.542 119.667 122.583 125.417 128.208 130.917
58	117.708 119.375 122.125 125.000 127.625 130.500
59	117.458 119.125 121.833 124.667 127.208 129.958
60	
61	**************************************
62	117.625 118.750 120.958 123.542 125.917 128.458
63	117.375 118.542 120.833 123.333 125.708 128.250
64	117.292 118.250 120.417 122.875 125.000 127.458
65	117.375 118.292 120.458 122.917 125.083 127.583
66	
67	**
68	***************************************
69	44/43/3 11/471/ 1174011 13t 703 437 07F 444
70	41'0604 11'0033 117.597 121.670 127 447 125 000
71	********* 11/4/76 117*342 121.5/13 137 5/13 438 438
72	11/0630 11/0033 1190503 121.625 127 647 125 702
73	117.292 117.917 119.500 121.708 123.500 126.000
74	70 147 YO 274 YO 958 97 708 98 500 90 500
75	106.125 107.042 108.833 110.833 112.833 115 200
76	87.792 87.875 87.958 88.042 87.917 87.050
77	98.375 98.375 98.750 99.125 99.417 99.958

FIGURE 5.6-1a



T(min) g"= 600 BTU/fo ft?
by LIQ+ULLAGE HT'G 0. 1. 1.667 123456 .B 3. 3.75

TOTAL TEMPERATURE (F)

FIGURE 5.6-1b 6 IN. TNK TST8G6 STRAT TEMPERATURE PROFILE 58---59 --NORMALIZED TANK HEIGHT RATIO (Y/H) 63.4 TOTAL TEMPERATURE (F) T(Min) T(TAU) g" = 600 BTU/for ft LIQ + ULGE HTG . .833 1.5 2.5 3.167 3.8 1.000

242

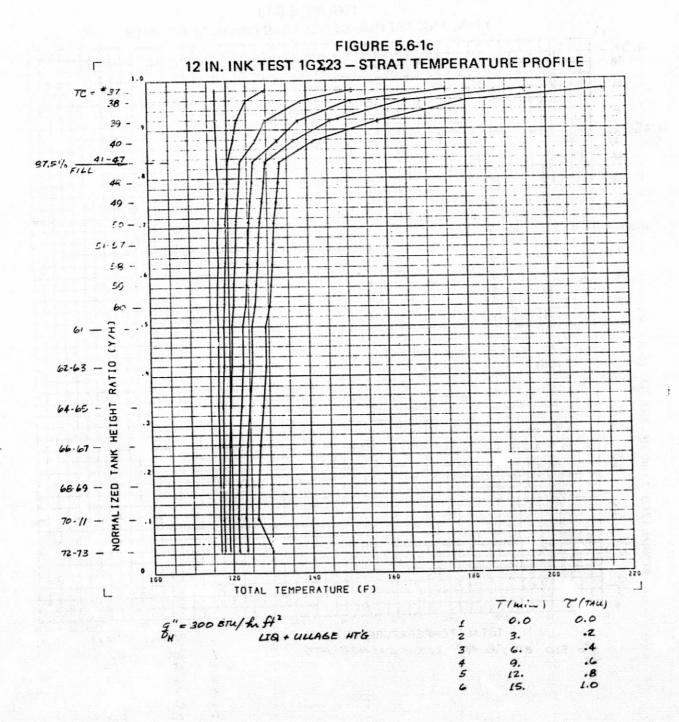
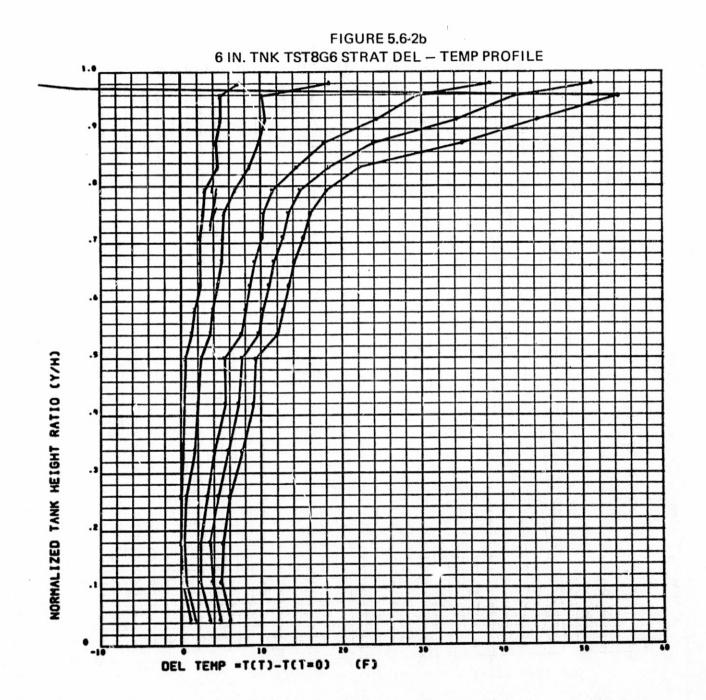


FIGURE 5.6-1d 12 IN. TNK TST1G28 STRAT TEMPERATURE PROFILE NORMALIZED TANK HEIGHT RATIO (Y/H) 62_ 63.4 66 68 TOTAL TEMPERATURE (F)

g"= 300 BTU/R. At 2 LIQ + ULLAGE HTG 7 (min.) C (TAU)

244

FIGURE 5.6-2a 6 1... TNK TEST 8GΣ4 - STRAT DEL - TEMP PROFILE NORMALIZED TANK HEIGHT RATIO (Y/H) DEL TEMP =T(T)-T(T=0) (F)



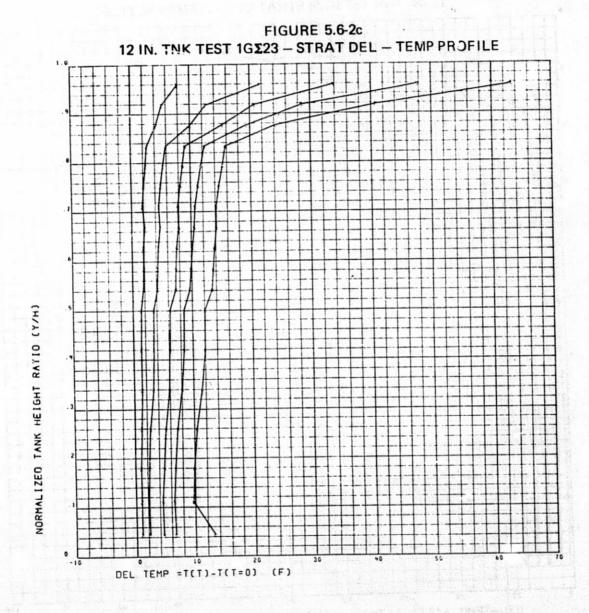
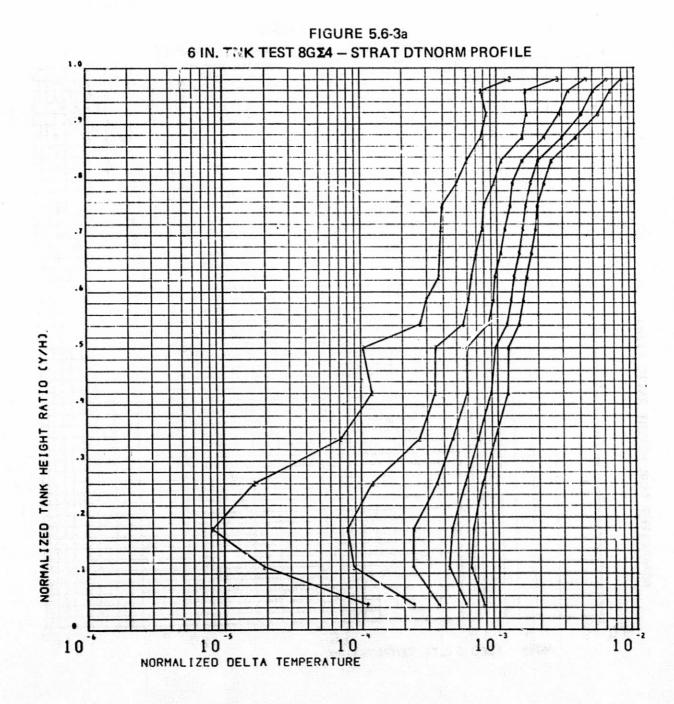
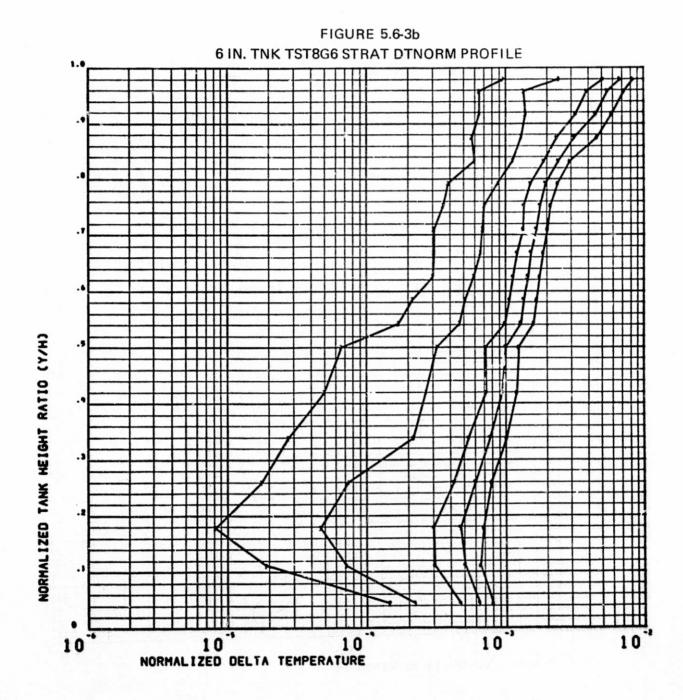
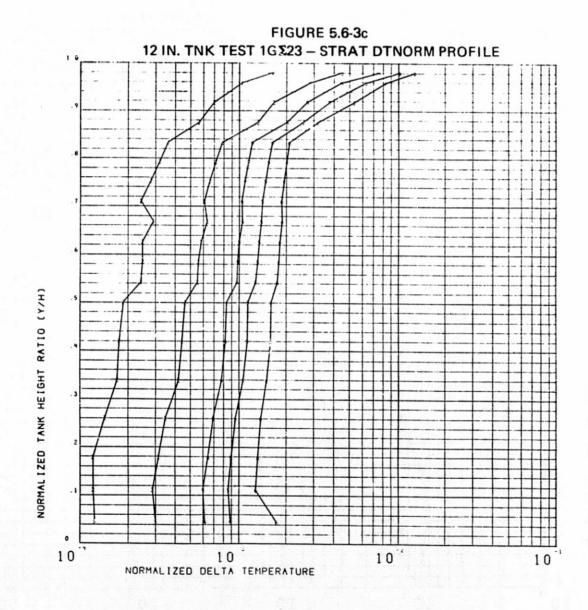
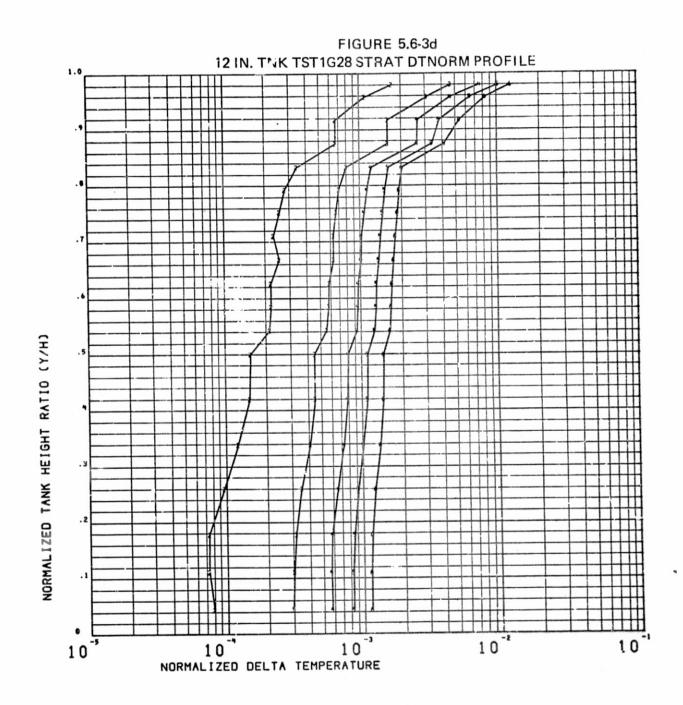


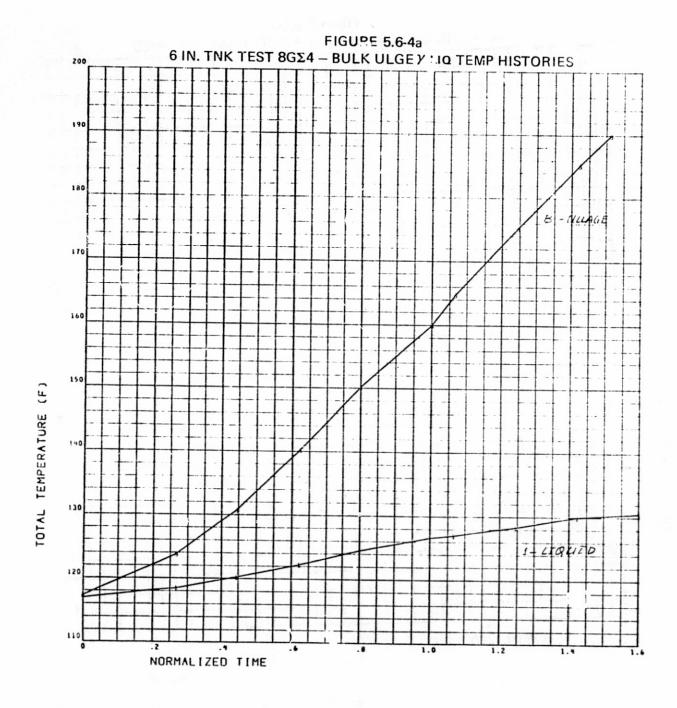
FIGURE 5.6-2d 12 IN' TNK TST1G28 STRAT DEL - TEMP PROFILE NORMALIZED TANK HEIGHT RATIO (Y/H) DEL-TEMP =T(T)-T(T=0) (F)

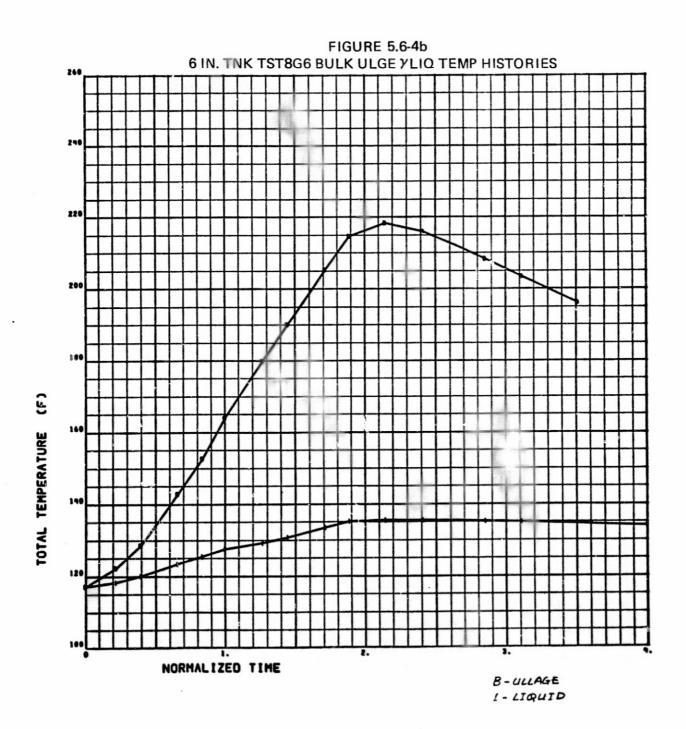


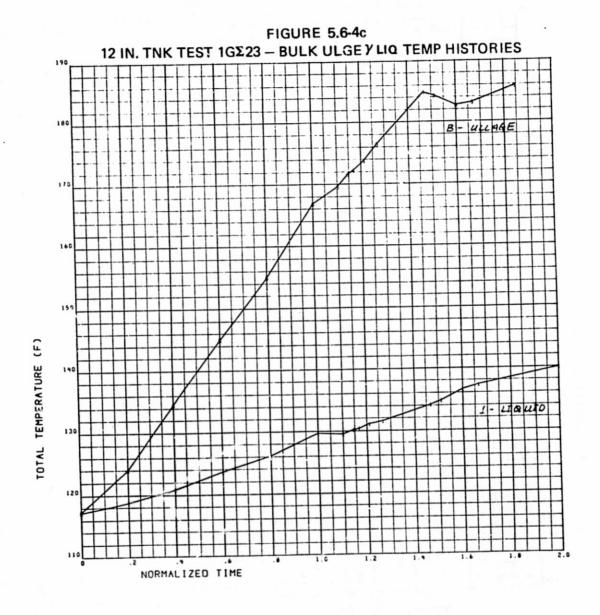


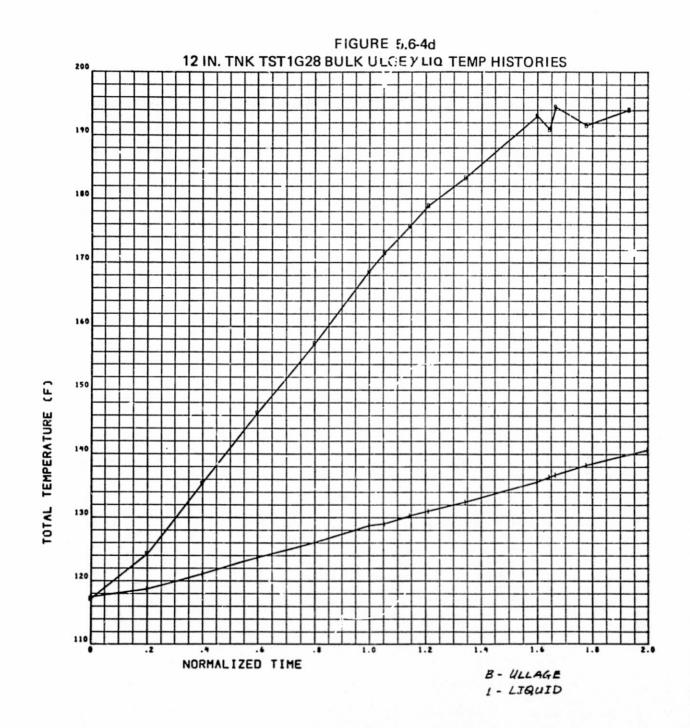


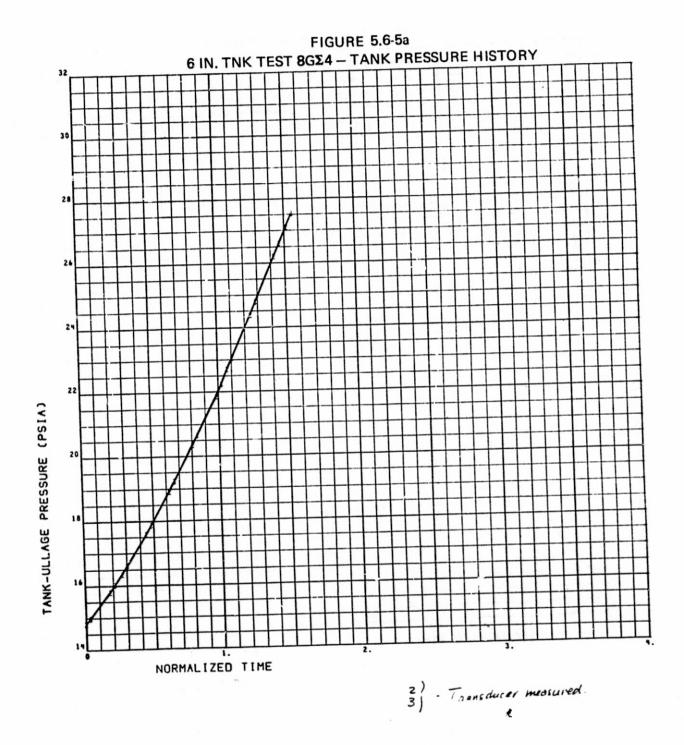


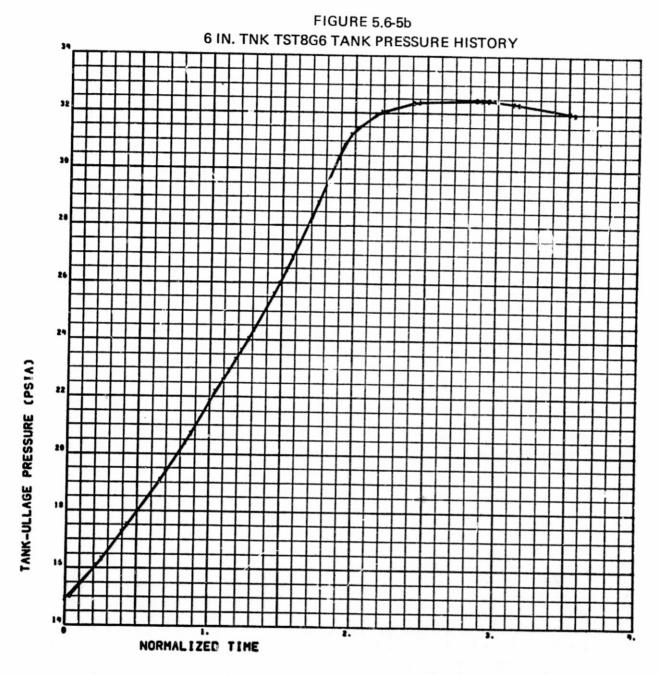




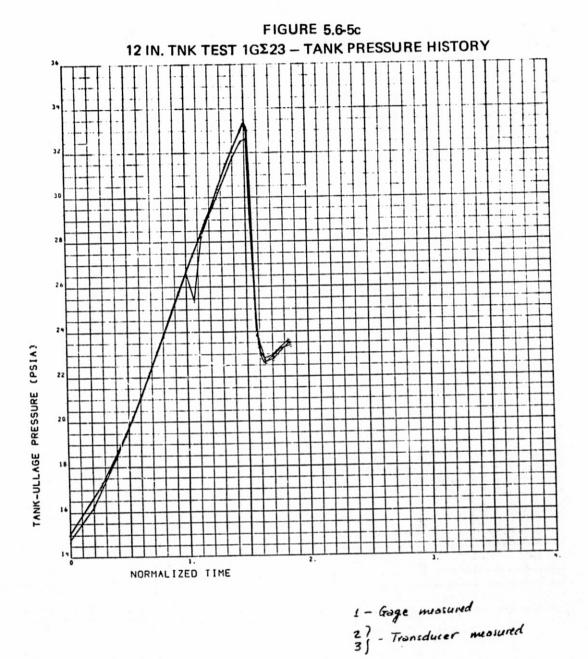




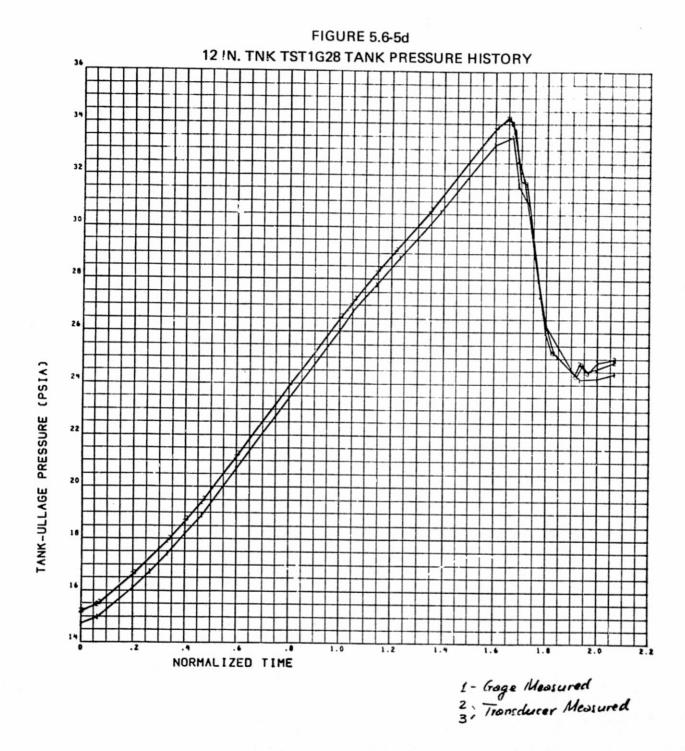




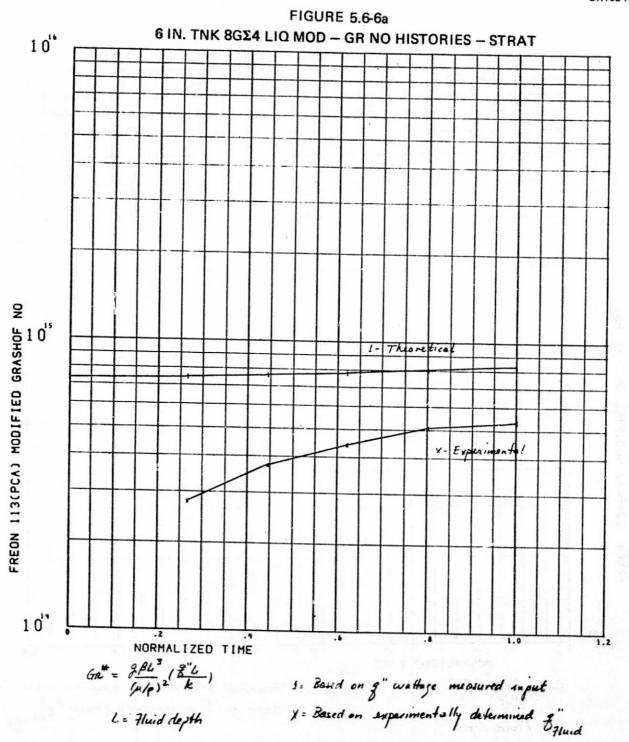
2) Transducer Measured



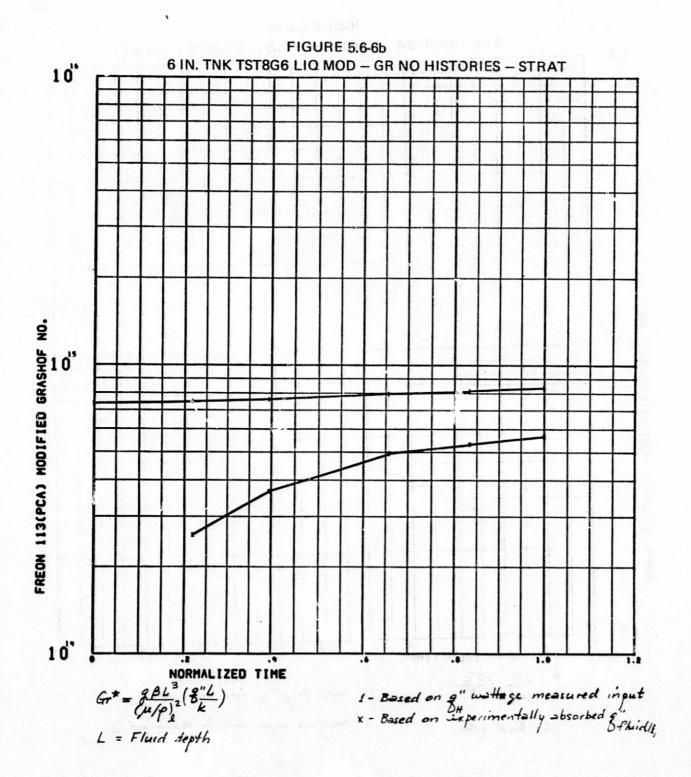
259



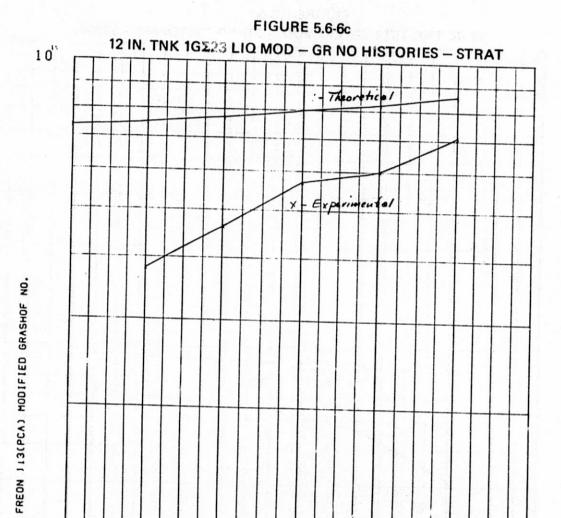
CR108-II



c."



CR108-II

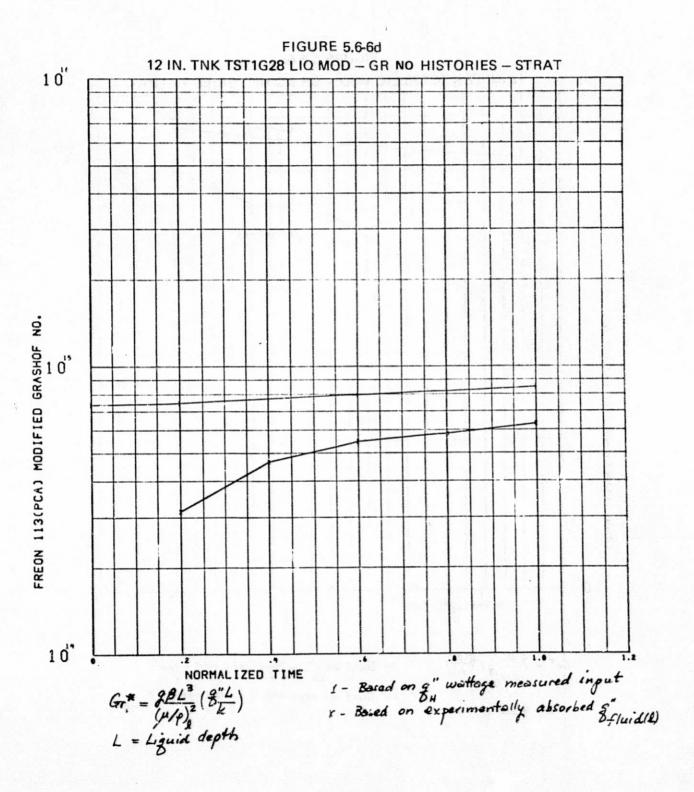


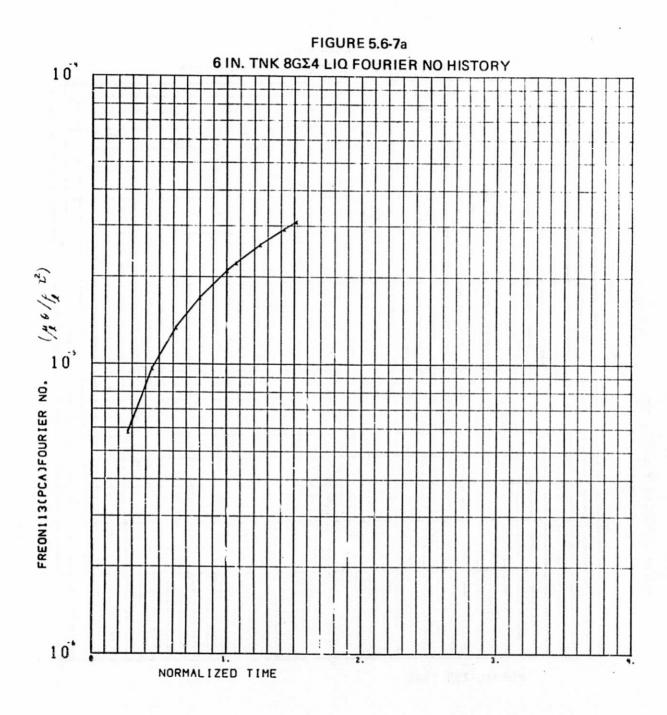
$$GR^* = \frac{9 \beta L^3}{(\mu/\rho)_2^2} (\frac{9^{\prime\prime} L}{k})$$

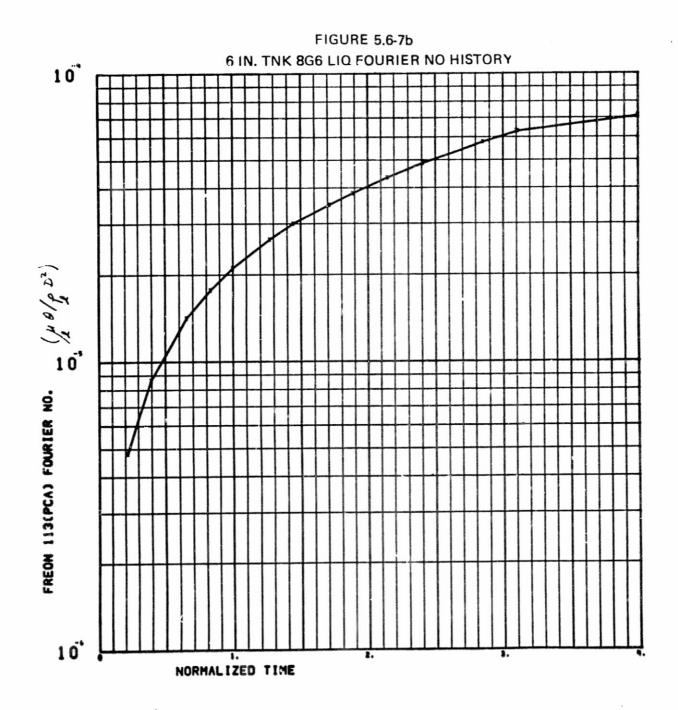
NORMALIZED TIME

10

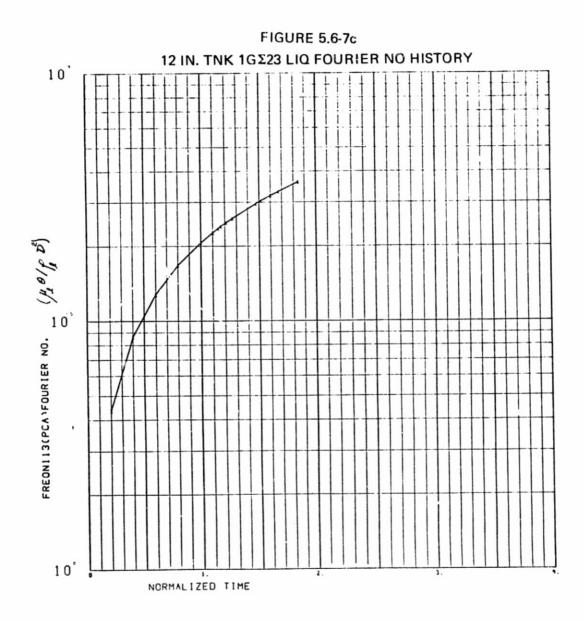
 $GR^* = \frac{q \beta L^3}{(\mu/q)_2} (\frac{g''L}{k})$ I = Bosed on g'' wottage invasured input $L = A | \mu | d$ depth X = B | d on experimentally determined $\frac{g''}{g}$

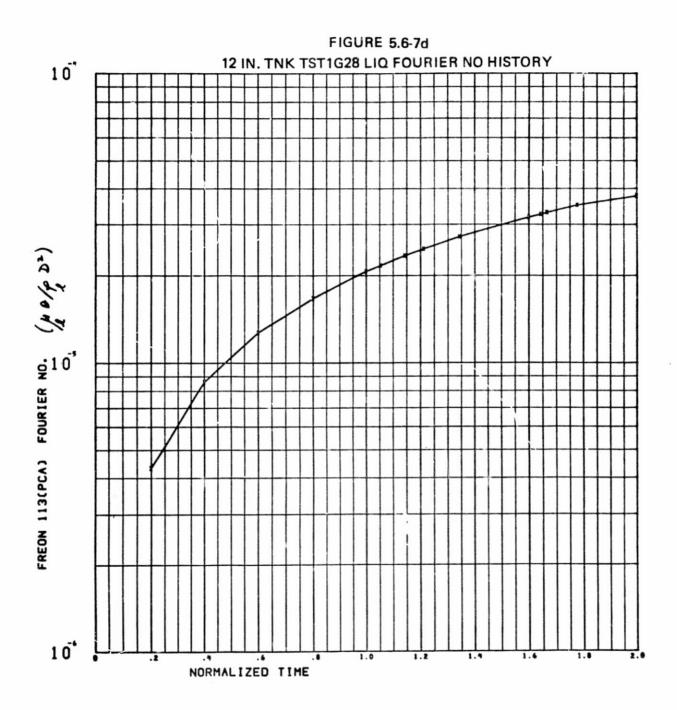






Cf





Section 5.7 SCALING SET

6-in Dia Tank Test	12-in Dia Tank Tests
8G	1G
Test #14	Test #26
1000 11 11	Test #15

Table 5.7-la. 6 IN. DIA. TANK TEST 8G#14 (Pag. 1 of 2)

STRUCTURAL GEOMETRIC TANK WISHWATTMETER HEAT PLUX INPUTS

```
DIME AREA FT2# .3927 CYL AREA FT2# 1.5708 FLNGE AREA FT2#
DHE WALL VOL FT3# .00131 1/2 CYL WALL VOLFT3# .00164 FLNGE VO
                                                                         .0365
                                                                 FLNGE VOL FT3=
 DME MASS LBME
                .65596
                           MASS 1/2 CYL LBH=
                                               .81996
                                                          FLANGE MASSE
                                                                        .38058...
 LTQ VOL FTS=
                .22907
                           ULLAGE VOL FT3=
                                              .03272
 INPUT HEAT FLUXES (BTU/HR-FT2) AND ABSORBED HEAT AND TEMPERATURE ESTIMATES
 H12= 90.1273
                H34= 90.1273 H56= 90.1273 H910= 90.1273
                                                                H78=
                                                                       0.0000
 EST. HT FLUX IN LIQ (BTU/HREFT2)= 90.1273
 EST. HT FLUX IN ULLGE (BTU/HR-FT2)= 0.0000
 EST. HT INPUT LIG(STRAT) BTUE 73.735 (STRAT+DESTRAT) BTUE
                                                              90.450
 EST.LIG TEMP INCRSE(STRAT) = 15.1332F
                                          (STRAT+DESTRAT)= 18.5683F
EST. HT INPUT ULLAGE (STRAT) BTUE 0.000
                                            (STRAT+DESTRAT)BYUM
                                                                  0.000
                         Table 5.7-1b. 12 IN. DIA. TANK TEST 1G#26
          STRUCTURAL GEOMETRIC TANK HTS+H4TTMETER HEAT FLUX INPUTS
 DGME APEA FT2= 1,5708. CYL AREA FT2= 6,2832. - FLNGE AREA FT2= ,1458
DME WALL VOL FT3= .01047
                              1/2 CYL MALL VOLFTS= .01309 FLNGE VOL FTS=
DME MASS LBM= 5.24772
                                                                                 .00603
                           MASS 1/2 CYL LBM= 6,55955
                                                       FLANGE MASS= 3,04465
 LIO VOL FT3= 1.83260
                           ULLAGE VOL FT3=
                                             .26180
-INPUT HEAT FLUXES (BTU/HR=FT2), AND APSORBED HEAT AND TEMPERATURE ESTIMATES
H12= 45,0637 H34= 45,0637 H56= 44,9334 H910= 45,0637 H78=
                                                                      0.0000
EST. HT FLUX IN LIG (BTU/HR-FT2)= 45.0116
EST. HT FLUX IN ULLGE (BTU/HR-FT2)= 0.0000
EST. HT_INPUT_LID(STRAT)BTU= -583,308 _____(STRAT+DESTRAT)BTU= -655,796
EST.LIQ TEMP INCHSE(STRAT)= 14.9611F (STRAT+DESTRAT)= 17.0779F
EST. HT INPUT ULLAGE (STRAT) BTU= 0.000 (STRAT+DESTRAT) RTUR 0.000
```

Table 5.7-1c. 12 IN. DIA. TANK TEST #15 (Page 2 of 2)	
DOME AREA FT2= 1.5708 CYL AREA FT2= 6.2832 FLNGE AREA FT2= .1458 DME AALL VOL FT3= .01047 1/2 CYL WALL VOLFT3= .01309 FLNGE VOL FT3= DME MASS LBM= 5.24772 MASS 1/2 CYL LBM= 6.55965 FLANGE MASS= 3.04465	.00608
LIQ VOL FT3= 1.83260 ULLAGE VOL FT3= .26180	
- INPUT HEAT-FLUXES (BTU/HR=FT2) AND ABSORBED HEAT-AND-TEMPERATURE ESTIMATES	
H12= 45.0637 H34= 45.0637 H56= 44.9334 H910= 45.0637 H78= 0.0000	
EST.HT FLUX IN LIQ (BTU/HR-FT2)= 45.0116	
EST.HT FLUX IN ULLGE (BTU/HR-FT2) = 0.0000	
-EST.HT-INPUT-LIQ(STRAT)BTU= -583.308(STRAT+DESTRAT)BTU=765.960	
EST.LIQ TEMP INCRSE(STRAT)= 14.9618F (STRAT+DESTRAT)= 19.6470F	
-EST.HT-INPUT ULLAGE (STRAT) BTU=	·

Table 5.7-2a. 6 IN. DIA TANK TEST 8G #14 (Page 1 of 2)

TEMPERATURE MATRIX-STRATIFICATION

				15.000	20.000 25.000
TIME (MIN)		5.000	10.000	.600	.800 1.000
TAU	0.000	.200	.400	127.708	130.292 132.417
1	117.208	122.208			132.250 134.375
5	117.417	124.250			131.667 133.833
3	117.708	123.833			130.958 133.125
4	117.875	123.542			129.208 131.333
5	117.208	122.333			128,375 130,375
6	117.208	122.000	123,958		127.354 129.104
7	117.354	121.750			126.333 127.833
8	117,500	121.500		120.792	122.542 124.000
9	116.125	118.208		128.292	130.750 133.083
10	117,333	122.542	125.542	127.292	129.792 132.083
11	117.417	122.333	124.792	126.042	128,250 130,500
12	117.833	121.500	123.750		125.167 126.542
13	117.083	120,667	121.917	123.417	128.083 130.208
14	116.000	120.583	123,250	128,083	130,667 132,833
15	116.667	122.750	125.583	120,003	129.917 131.958
16	117.250	122.708	125.042	127,542	127.250 128.917
17	116.688	121.313	123.229		124.583 125.875
18	116.125	119.917	121.417	122.750	121.917 123.250
19	115.583	117.833	119.083	120.333	130.750 133.083
20	117,333	122.542	125,542	128,292	129.792 132.083
21	117.417	122,333	124.792	127.292	
22	117.833	121.500	123.750	126.042	
23	117.083	120.667	121.917	123.417	
24	116.500	120.083	122.792	125.250	
25	116.292	119,956	122.583	125,125	
26	116,229	119,833	122.500	124.958	127,500 129.646
27	116.167	119,708	122.417	124.792	127.708 129.917
28	116.500	120.000	122,583	125.250	
29	116.167	119,375	122.083	124,667	
30	116.417	120.083	122,833	125,250	
31	116,333	120.354	121,313	122.708	
32	116,750	120.875	121.708	123,250	
33	115.333	117.792	118,583	119.750	
34	113.125	114.083	114.542	115,000	116,167 117,042

	Table 5.7-2a. 6	IN. DIA	TANK TE	ST 8G #14	(Page 2 o	of 2)	
35	109.958	109.667	109.167	109.167	109.792	110.417	
36	• • • • •	119.833	120,91/	122.167		125.083	
37		120.208	122,958			130.250	
38		120.292	123,000			130,333	
39	• • • • • • • • • • • • • • • • • • • •	120.458	123.292		128,250		
40		120.750	123,583	125,958	128.542	130,792	
41		120.583	123.500	126,083	128,625	130.792	
42		120.917	123,625	126,125	128,708	131.083	
43		120.875	123.708		128,750	131.042	
44		121,250	124.000	126.458	129.167		
45		120.750	123,583	126,250	128,750	131,042	
46		121.292	124.042	126,708	129.208	131.500	
47		121,417	123,792	126,333	128.792	131.167	
48		119.750	122.354	124,896	127,313	129,542	
49		118,917	121.208	123,708	126,000	128,292	
50			121.500	123,917	126.292	128,583	
51		118,833	121.042	123,500	125.667	127,875	
52		119.521	121.833	124.167	126.479	128,729	
53		118.000	120.542	122,833	125,208	127.542	
54		120.208	122,625	124,833	127.292	129,583	
55		120.000	122,500	125,000	127,208	129,583	
56				124.833	127,292	129,583	
57		120,000	122.500	125,000	127,208	129,583	
56		118,167	120.583	122.833	125.125	127,458	-
59		119.542	121.708	124.083	126,250	128.583	
60		120.792	123,083	125,250	127.458	129.917	
61		117.083	118.875	121.042	123,167	125,333	
62		116.792	118,583	120.542	122,500	124.750	
63		118,292	120.083	122,125	124.167	126.333	
64	V 200 200 200 200 200 200 200 200 200 20		121.208	123,167	125,208	127.208	
6	116,292	116.208		119.458	121,250	123.250	
66		116.250	117.458	118,958	120.708	122.292	
67	117,292	117.458	118,333	120.000	121.917	123.333	
66			117.250	118,646	120.250	121.750	
69	115,958	115.792	116,667	118.167	119,708	121.083	
70	116.042	116.083	117.042	118.333	119.792	121.208	
7		117.083	117.875	119.125	120.542	155.000	
7		118.333	119.333	120.583	122.042	123.458	
7:	_	116.042	116.708	117.958	119.458	120.792	_
7		112,500	115.292	117,750	120.083	122.208	_
7			101.833	163,708	105.292	106.917	
7		106.167	107.250	108.542	109.750	111.167	
7		90.375	90.417	90.875	91,458	92.083	

**																												
	TIME	(MIN))	i	Ο,	00	0	2	1	.00	0	4	1	. 00	00		61	(00		8	١.	000		9	9.00	0 0	
	TAU		0.	U	o o					2				4			61				P				. 01			
	1		4-1	ń	9	33	-1	50	-	500	- 4	21	,	000)	12	5	54	10	1	27	7	92	4	29	87	<u> </u>	
	2																									62		
	3		11	.7	5	46	1	21	(663	1	.24		000)	12	6.	50	0.0	1	2.2	8	75	1	30	83	5	
	4		11	.7	7	21	1	21		513	1	23	3	917	7 -	12	۸,	45	A-	1:	24	7	08_	1	39	792	2	
	5		11	.7	5	04	1	21		392	1	23	;	705	3	12	6.	12	25	12	23	4	17	13	30	458	3	
	_ 6		11	.7	4	54	1	21	. [325	1	22		375	5	12	5.	29	17	12	27	4	58	12	29	333	5	
3.7	₹ 7		11	.7	5	54	1	21	. 7	729	1	22		667	,	12	4.	95	8	12	27	0	42	12	28	875	j	
	8		11	.7	7	75	1	21		429	1	22	· ·	333	5	12	4.	29	2	17	24	2	92	12	28	000)	
	9		11	7	6	46	1	17		108	1	20		217	,	12	2:	87	15	12	4	6	67	12	26	333	5	
	-1n .		11	7_	3	75	-1	22	-4	444	-1	24		750	1	12	7.	33	3-	1	Q.	6	25_	13	31.	708	.	
	11		11	7	5	79	1	22	.:	363	1	24	÷	4 2	•	12	7:	12	3	12	0	4	17	13	31	458	}	
	12		11	7	6	75	1	22	. (150	1	24	. :	209	3	12	6:	54	2	13	6	7	0 6	13	50	750	,	
	-1-3		11	7	6	6.7	-1	21	-	134	-1	23	÷	0.0)_	12	5	08	3	12	7	(j	0.0	12	2.0	833		
	14		11	6	5	00	1	20		542	1	22		792	,	12	5.	33	3	12	7	7	8 0	12	9	667	•	
	15		11	7	2	50	1	23		121	1	24		750)	12	7.	29	2	12	9	7	50	13	51	708	}	
	16		11	7,	5	46	-1	22	÷	20	-1	24		459	3_	12	7	0.0	n-	4.2	9	2	50	13	34.	33.		
	17		11	7	3	11	1	21	. 7	158	1	23		750)	12	6:	20	2	12	A.	3	75	13	ñ.	375	,	
	18		11	7	3	30	1	20		000	1	22	Ċ	500)	12	4:	54	2	12	6	5	0.0	12	28	250	1	
	19		11	7	3	56	1	1	÷	75	1	20	÷	158	_	12	2	20	2	1	4	1	57_	12	5	833		
	50		11	7	8	67	1	22	. (46	1	24		17	,	12	7:	50	0	12	9	7	2	13	11.	833		
	21		11	7	8	17	1	22	. 3	113	1	24	្រ	583	,	12	7 :	04	2	12	0	3	75	13	1	333		
	22		-11	7	7	00	-1	21		33	1	23	÷	192	_	12	4	25	1	12	я.	5	0.0	13	n.	417		
	23		11	7.	8	54	1	21	. 3	142	1	22		158		12	5:	0 0	Ó	12	7.	0 (10	12	8.	709	,	
	24		11	6.	31	UB	1	19	. 6	88	1	21	۶	583	,	12	3.	91	7	1 2	٨.	01	0.0	12	8	042		
	25		11	5	8	71	1	1 %	-7	42	1	10	٠	133		12	•	33	7	4 2	2	2	8_	12	4	625		
	26																									375		
	27									58																875		
	-28		11	5.	9:	13	1	18	į.a	92	1	20	. 4	153	_	2:	2	37	5_	12	4.	3,	33			042		
	29		11	5.	72	29	1	18	. 7	46	1	20	.3	175	•	12	?	37	5	12	4:	37	15			167		
	30									58																750		
	31-																									875		
	32									50																375		
	33		11	5	54	16	1	16	្ន	13	1	17	. 3	92	1	118	3	12	4	11	ó.	12	5	12	n.	000		
	34		11	4,	55	6	1:	11	. 7	75	1	10	, 2	0.8	-1	-04	,	37	5	1-0	α,	Q	8	10	A.	917		
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Table	5.7-2b. 12 IN.	DIA TANK TE	EST 1G #26 (Page 2	of 2)
35	114.046 108	.721 105.542	103,459 103,529	101,125
36	115.305 121	.171 122.R33	124,708 126,583	124,250
	116,2/1 119	142 120 975	122,837, 124,917	124,750
38	116,417 119	.367 121,292	123,417 125,417	127,375
39	116,667 119	.739 121.975	124,083 126,375	125,250
40	-116.904-120	-192-122-583	-124, 917 127,37 5	_129,417
41	117,517 120	079 122,458	125,000 127,292	129,375
42	117,592 120	229 122,583	125,083 127,542	129,542
43	117,717 12C	-333-122-708	125,167 127,625	120,625
44	117,888 125	417 122,875	125,292 127,708	129,703
45	117,717 129	179 122,583	125,003 127,500	129,500
46	_117_567_120	,542-122,875	125,333-127,833	129,750
47	11/,81/ 120	,51/ 122,500 500 123 000	125,333 127,750	
48	118,022 120	378 122 700	125,417 127,792	
49	447 337 426	450 122 450	125,167 127,542 124,958 127,333	129,417
50	117,833 126	120 166,420	124,875 127,167	
51	117,825 126	460 423 EVS	125,000 127,292	
52	117,713 126		124,958 127,167	129,042
53	117 713 120	705 100 405	125,083 127,333	
54 ——55	117 788 120	175 122 458	125,000 127,107	120,125
56	117,796 120	200 122.459	125,125 127,292	129,208
57	117.750 120	179 122.500	125,042 127,167	129,083
58	117.850 120	200 122.500	125,000-127,167	
59	117,629 119	988 122 167	124 708 126 833	128,750
60		796 122,042		128,500
61	117,567 110	721 121 797	124,333 124,417	128,375
62	117.733 119	.758 121.933	3 124,167 126,294	124,167
63	117,496 119	.525 121.583	3 123,017 126,042	127,917
64	117.392 119	.246-121.n83	3 123,333 125,37	127,125
65	117.467 110	.333 121,208	123,500 125,417	127,167
66	117,467 119	,333 121,209	123,500 125,417	127,167
67	117,392 110	<u> 120 750 </u>	122,750 124,58	124,250
68	117,350 118	,842 120,375	122,417 124,042	125,625
69	117,458 118	,929 120,500	122,45R 124,208	124,700
70	117,458 11A	,229 120,417	122,333 124,208	125,700
71.	117,350 118			125,500
_72		771 120,292	122,292 123,950	125,458
V73			122,292 123,058	100.083
7.4		333 96,500		0 100,083 3 113,292
75		.533 109,209		87,417
76		.829 85.417 .638 96.792		3 100,458
77	94,233 95	,638 96,792		4001-20

Table 5.7-2c. 12 IN. DIA TANK TEST 1G #15 (Page 1 of 2)

TEMPERATURE MATRIX-STRATIFICATION

TIME (MI	N) 0.000 21.000 41.000 61.000 81.000 99.000
TAU	-0-000
1	117.042 120.583 122.958 125.250 127.375 129.417
Š	117.250 121.500 123.958 126.083 128.333 130.208
3	-117.958-121.750-124.167-126.417-128.542-130.500-
4	118.250 121.708 124.083 126.167 128.417 130.375
5	117.958 121.500 123.792 125.958 128.125 130.000
	-117 625 -120 - 958 - 123 - 167 - 125 - 250 - 127 - 250 - 129 - 167
7	117.708 120.792 122.792 124.792 126.708 128.500
8	117.667 120.625 122.375 124.167 125.875 127.583
9	117.000-119.292-120.917-122.542-124.167-125.667
10	117.583 122.417 124.833 127.042 129.208 131.167
11	118.000 122.542 124.958 127.167 129.333 131.292
-12	117.792 122.083 124.250 126.417 128.458 130.333
13	117.417 121.375 123.125 124.792 126.625 128.375
14	116.708 120.542 122.958 125.208 127.417 129.333
-15	117.583 122.625 125.083 127.333 129.542 131.417
16	118.167 121.958 124.292 126.625 128.750 130.708
17	117.500 121.625 123.750 125.675 127.958 129.875
18	117-292 120-667 122-458 124-292 126-000 127-667
19	116.542 118.792 120.375 122.125 123.708 125.250
20	117.583 122.583 125.000 127.250 129.375 131.375
-21	117-917 122-500 124-792-127-042-129-208-131-167
22	117.458 121.792 123.958 126.083 128.125 130.083
23 —24	117.417 121.125 122.917 124.750 126.583 128.250
25	116-875 119-875 122-208 124-417 126-542 128-500
26	116.458 119.375 121.542 123.500 125.458 127.208
27	116.208 118.875 120.000 119.208 119.250 119.958
28	116.125 117.958 114.042 110.625 109.500 109.583 116.875 119.458 121.708 123.875 125.958 127.833
29	110.073 117.430 121.700 123.073 125.730 127.833
30	116.750 119.208 121.458 123.667 125.708 127.708 116.667 119.667 122.000 124.250 126.333 128.333
31	117.250 120.792 122.417 124.125 125.750 127.167
32	117.083 120.417 121.917 123.500 124.958 126.375
33	114.917 115.500 115.875 116.542 117.417 118.417
34	114.708 110.458 108.667 108.042 108.000 108.292
J-	1144100 1104430 1004001 1004045 1004000 1004545

70 20 20 20 20 20 20 20 20 20 20 20 20 20	8 3 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6 7 6	0 - 1 0 - 1 - 1 0 0 0 0 0 0 0 0 0 0 0 0	
age 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	7. 400 7. 400 7. 400 7. 400 7. 400 6. 6. 6. 7	2000 2000 2000 2000 2000 2000 2000 200	23.417 23.500 23.500 23.500 23.250 23.250 23.250 23.250 23.250 23.250 23.250 24.250 24.250 25.250
T 1G #15 01.875 24.458 24.083 24.250 24.583 25.042 25.042 25.042 25.125	00000000000000000000000000000000000000	122 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	000 000 000 000 000 000 000 000 000 00
ANK TES 03.958 22.958 22.000 22.750 22.750		22 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	0.667 0.667 0.657 0.617 0.250 0.167 3.417 6.958
N. DIA 7	20 29 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	00000 0000 000 000 000 000 000 000 000	118 - 7 - 7 - 7 - 7 - 7 - 7 - 7 - 7 - 7 -
2c. 12 542 542 042 042 043 708 458	118.000 17.667 17.792 17.792 17.958 17.958 17.667 17.563	17.708 17.708 17.667 17.667 17.667 17.568 17.568 17.568	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
Table 5	25 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	100 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7
		•	

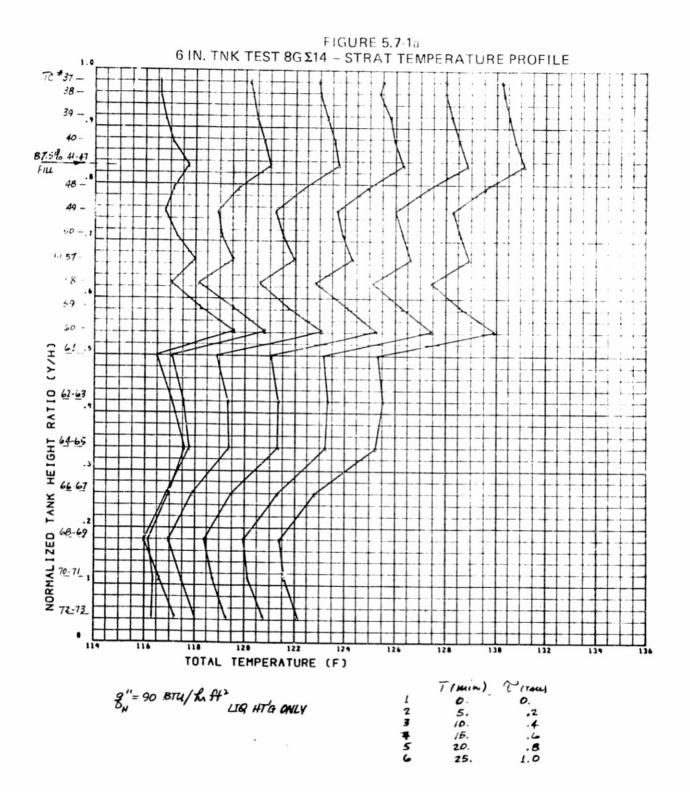
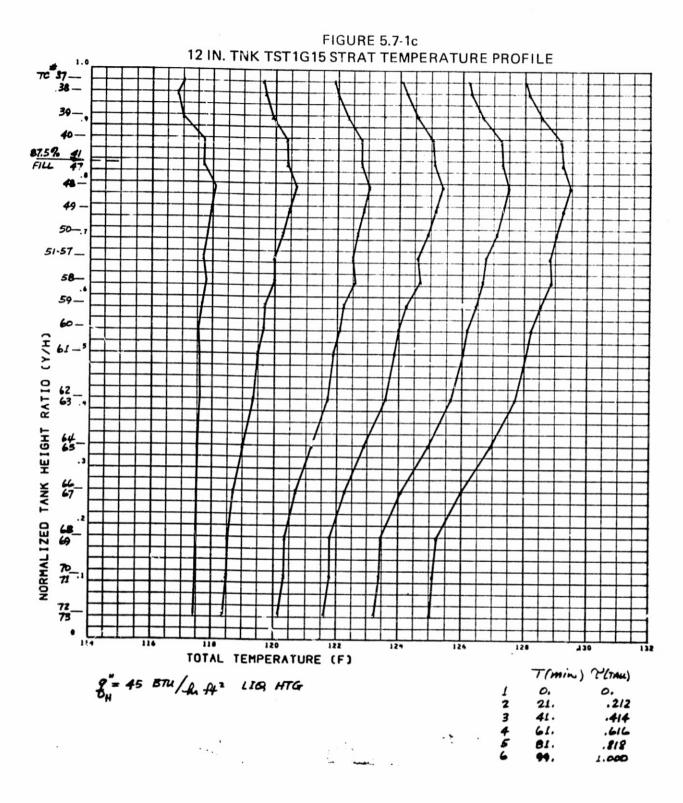


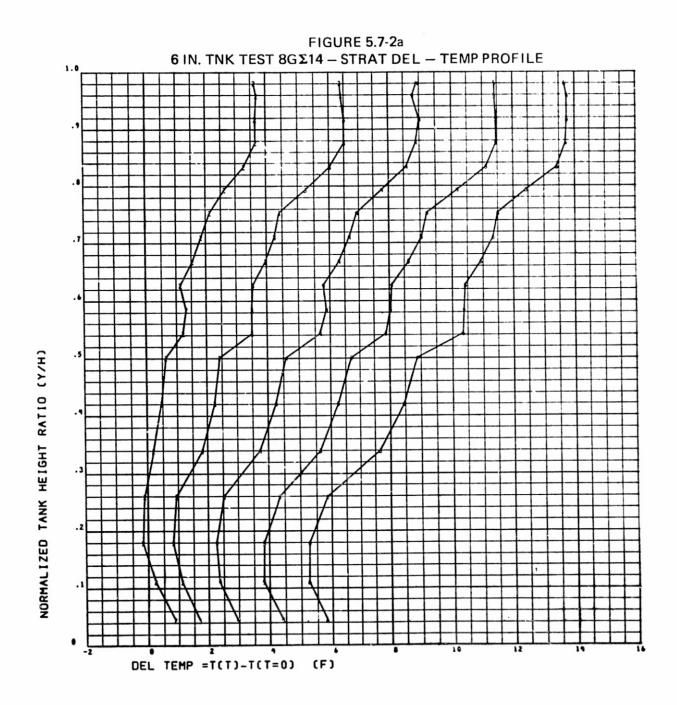
FIGURE 5.7-1b 12 IN. TNK TEST 1GΣ26 - START TEMPERATURE PROFILE 87.5% FILL 41-47 51-57 -62-63 -2ED - 69-89 70-71 -72.73 -TOTAL TEMPERATURE (F) T/min) T (TAU) EH LIQ HTG ONLY 0. 21. . 212 41. .616 61.

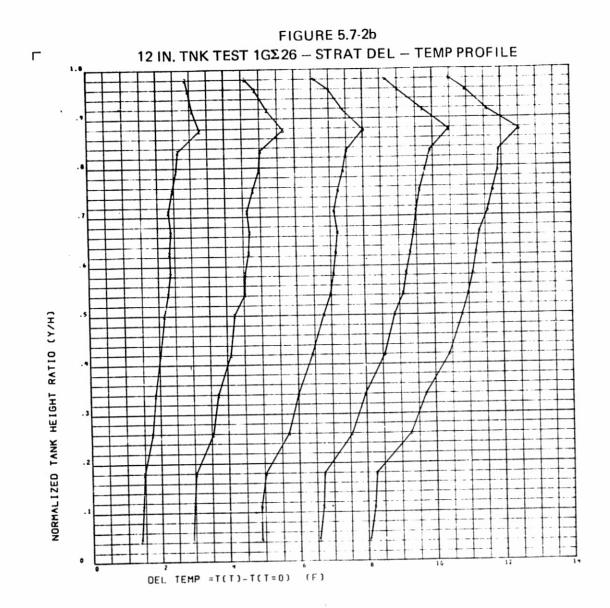
81.

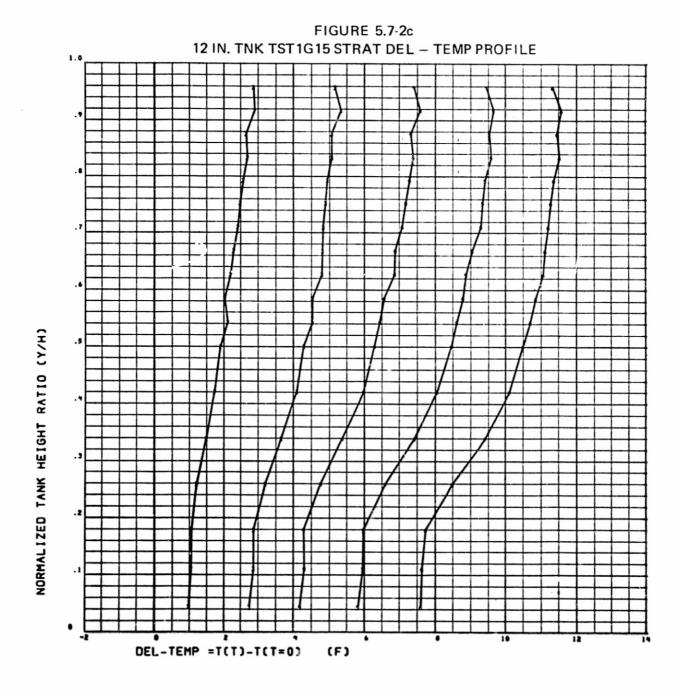
.318 1.0

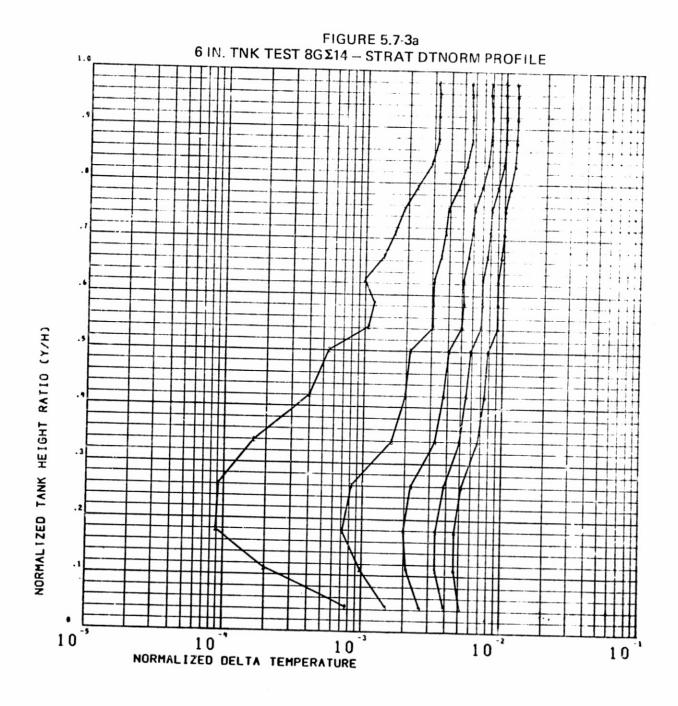


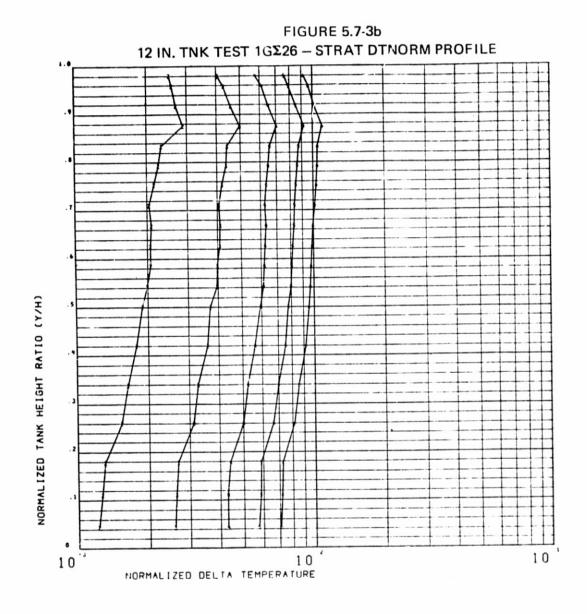
280

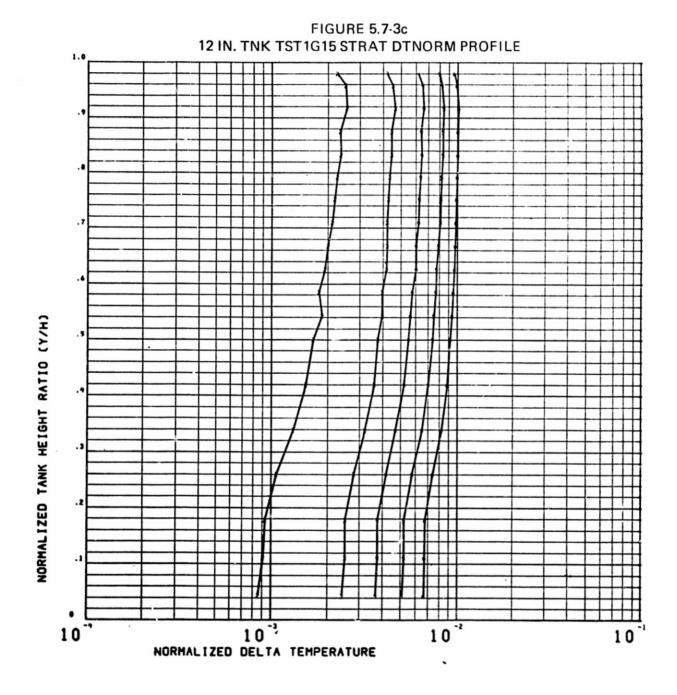


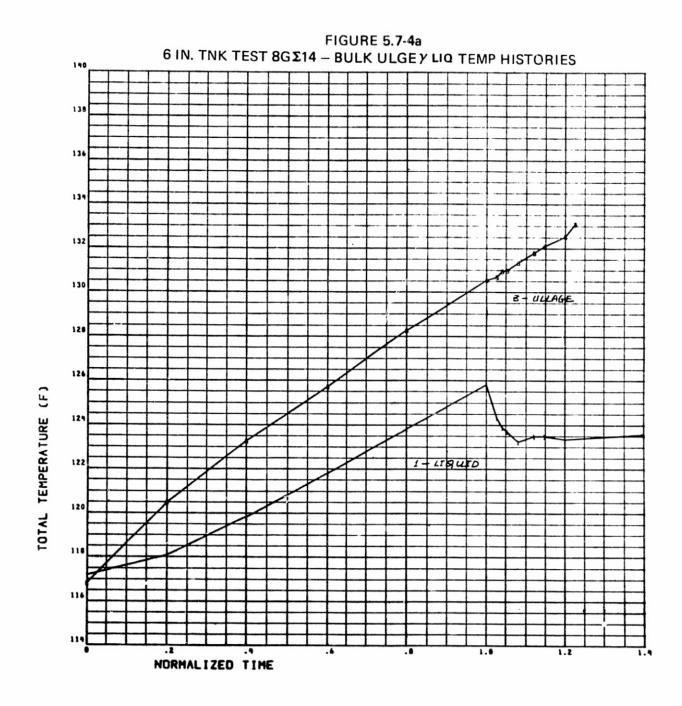












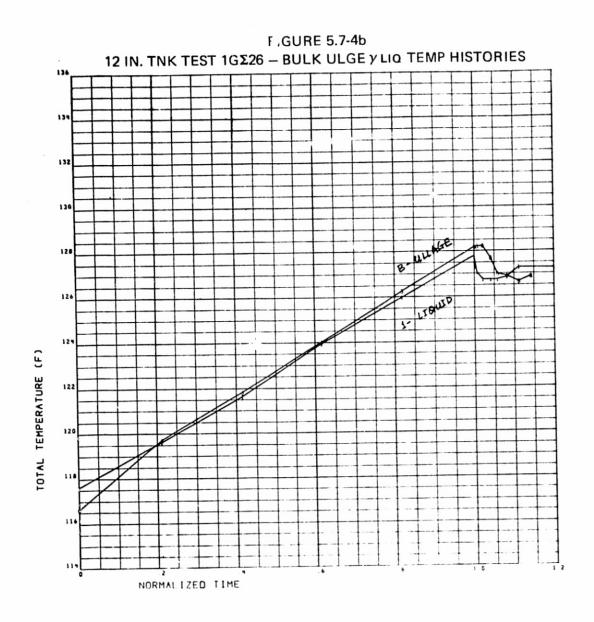
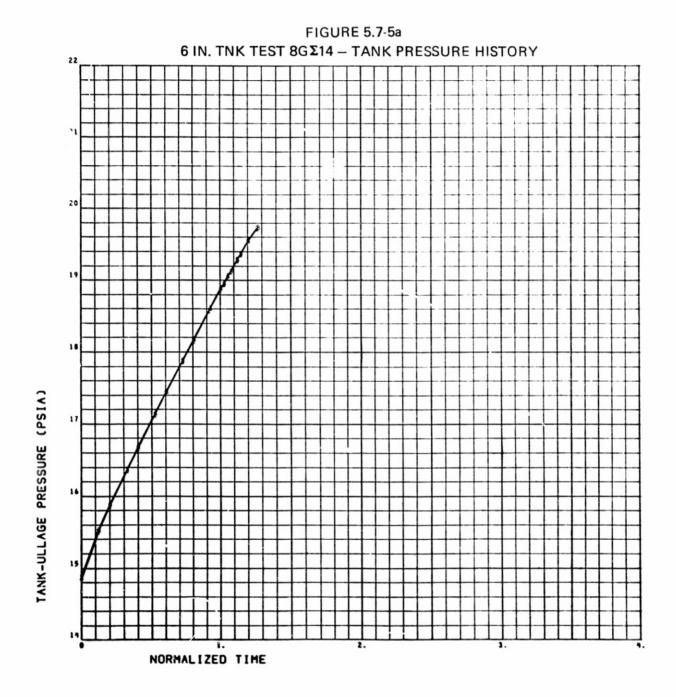
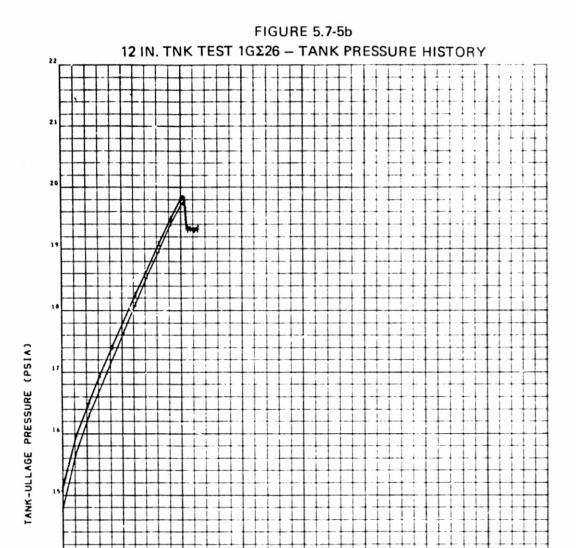


FIGURE 5.7-4c 12 IN. TNK TST1G15 BULK ULGEY LIQ TEMP HISTORIES 126 124 TOTAL TEMPERATURE (F) 122 120 116 NORMALIZED TIME

289

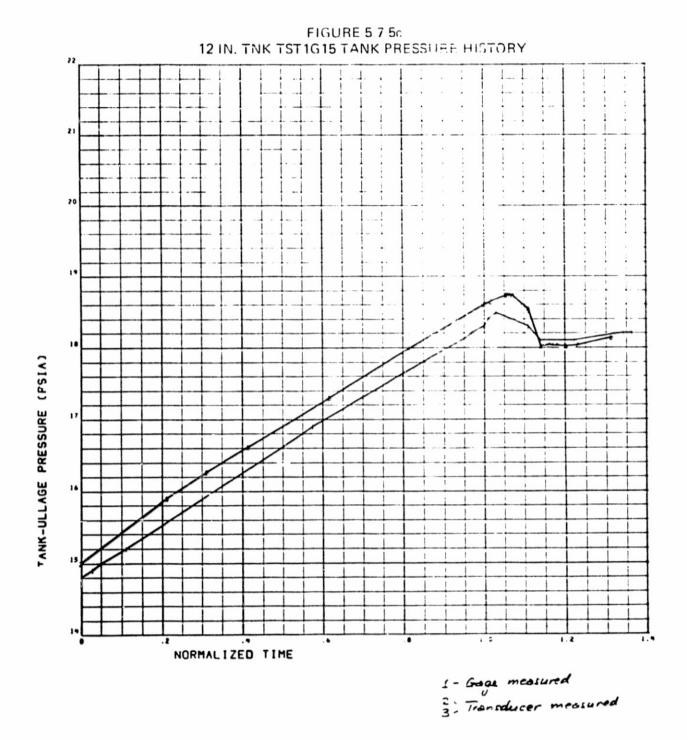
B - ULLAGE 1 - LIGUID

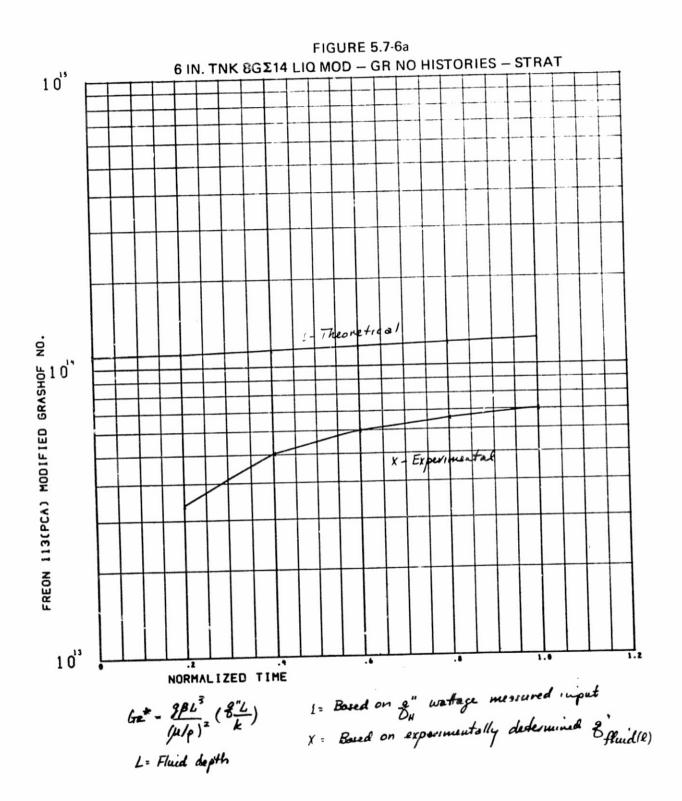


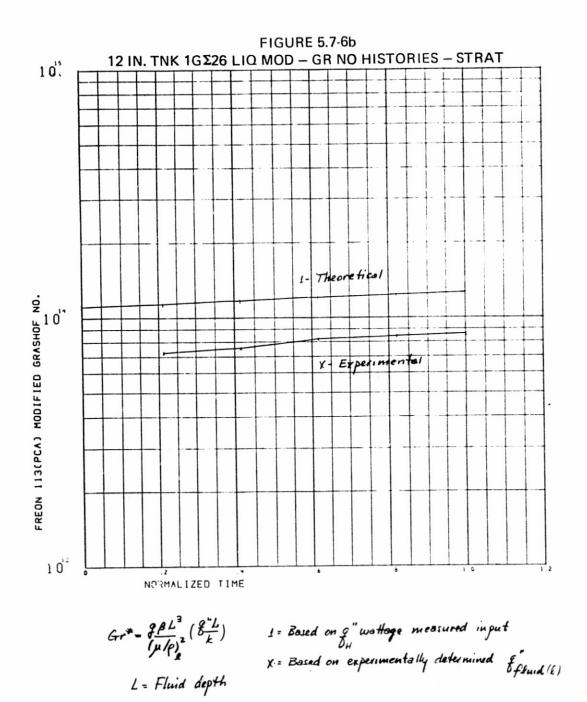


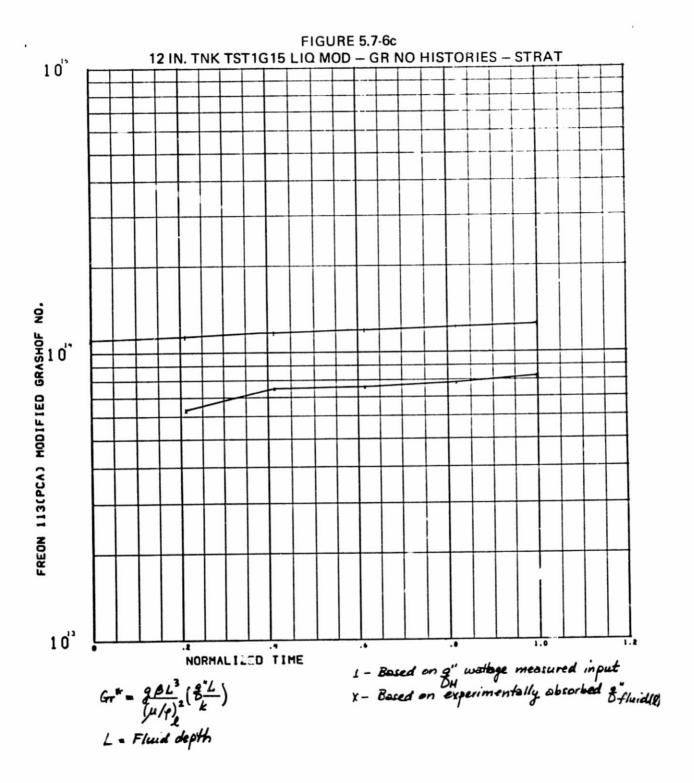
1 - Gage measured
27- Transclucer measured
35

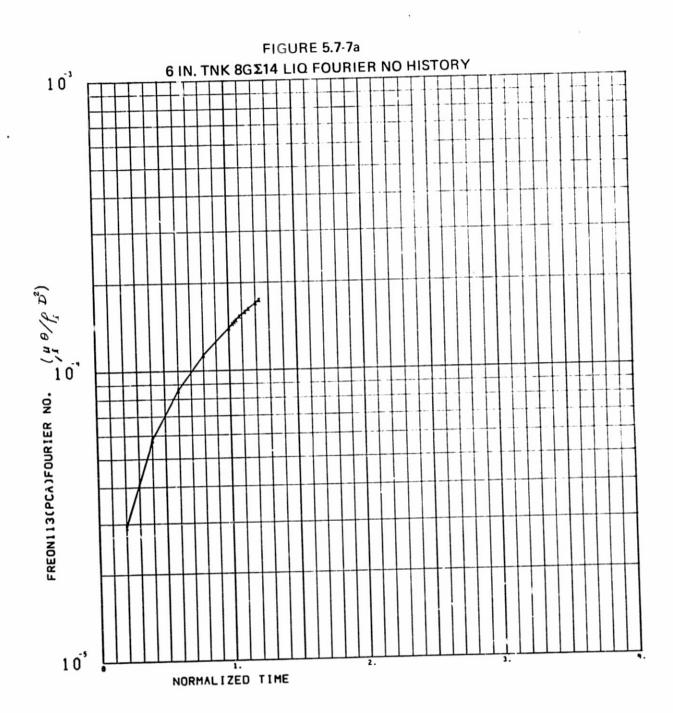
NORMALIZED TIME

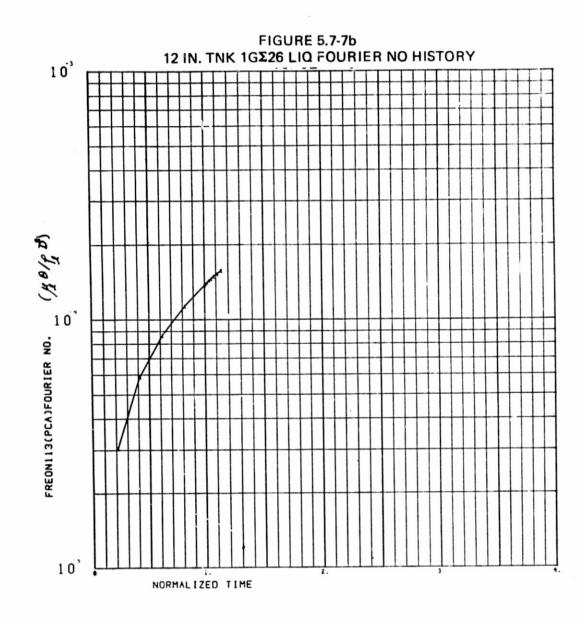


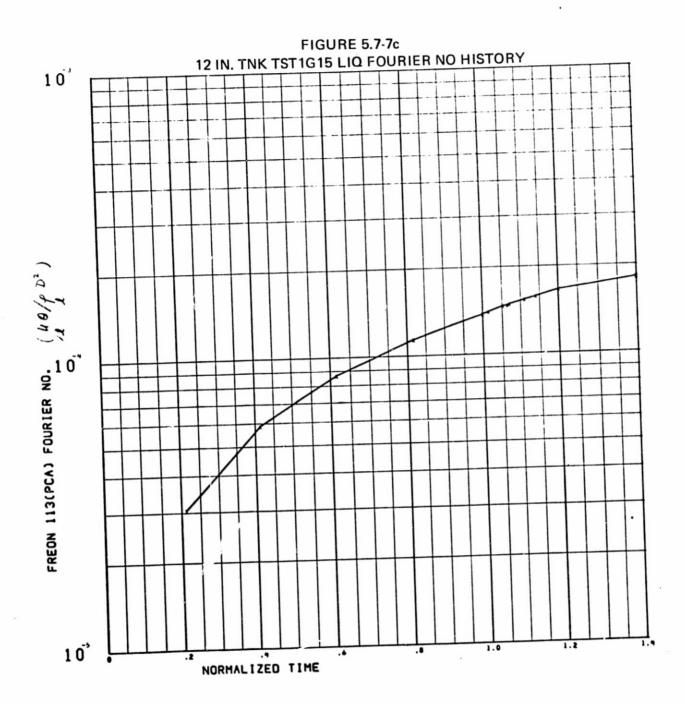












Section 5.8 SCALING SET

6-inDia Tank Test	12-in Dia Tank Test					
8G	1G					
Test #13	Test #27					

Table 5.8-la. 6 IN. DIA. TANK TEST 8G=13 STRUCTURAL GEOMETRIC TANK WIS-WATTMETER HEAT FLUX INPUTS

DME DME	MAL	LV	JL F	13P		001	31	MAS	1/	2 C	AL	WA	LL	VO	LF'	3=		. 0	016	4		FL MA	NGE	VÇ	L	FT	3 =	. 0	0076
LIG	VO	L F1	3=	, 2	290	7		UĻ	LAG	E V	OL	FT	3=		. 03	527	2			-									
_1NP	11	HEAT	LEL.	UXES	_ (8	TUZ	HR⊲	FT2) , A	ND_	AB:	SQR	BE)_ H	EA	P A	ND-	TE	HPE	RA	run.	E. E	STI	MAT	'ES				
H12=	9	0.12	73	нз	48	90	.12	73	H	56 s	(90.	127	3	ŀ	191	0 =	9	0,1	27	5	H7	8 =	90	.1	273	5 .		
EST,	HT	FLUX	IN	LIO	(B	TU/	HR=	F72) =	90	. 12	273																	
EST:	HI	INPL	T. L.	1015	TRA	I)B	TUS.		73.	735		-	151	'RA	T+L	ES	TRA	7)	BTU	#	8	5.5	33_						
EST.	L10	TEM	B I.	VCRS	E(S	TRA	T) =		15.	131	٥F		(ST	RAT	+1)	EST	RA') [17	55	57F						
EST.	HT	INPL	T U	LAG	ELS	IRA	ELT	TUE		4.	747	7		٤S	ĪRA	T.±1	DES	TR/	17)	BŤL	I	1	7.1	n 7					

Table 5.8-lb. 12 IN. DIA. TANK TEST 1G#27

STRUCTUPAL GEOMETRIC TANK WISHWATTHETER HEAT FLUX INPUTS

```
DU"L AREA FT2= 1,5708 CYL AREA FT2= 6,2832 FLNGE AREA FT2= ,1458
DEE 1 455 LEME 5,24772 MASS 1/2 CYL LIME 6,55965 FLANGE MASS = 3,04465
 INPUT HEAT FLUYES (STU/HO-FT2), AND ARSORRED HEAT AND TEMPERATURE ESTIMATES
H12= 45,0637 h34= 45,0637 H56= 44,9334 H9109 45,0637 H78= 45,0637
EST.HT FLUX.IN LIG (3TU/HR-FT2)= ..45,0116....
EST. HT FLUX IN PLLGE (BTU/HR-FT2)= 45.0637
ECT. HT TOPUT LIC(STRAT)BTH= 583,309 (STRAT+DESTRAT)BTH= 718,824
-EST, LIGHT TEMP INCRESE (STRAT) = 14,0503F (STRAT+DESTRAT) = 18,4319F
EST. HT INPUT ULLAGE (STEAT) BTU= 116.797 (STRAT+DESTRAT) BTU= 143.934
```

_____IEMPERATURE HATRIX-STRATIFICATION____

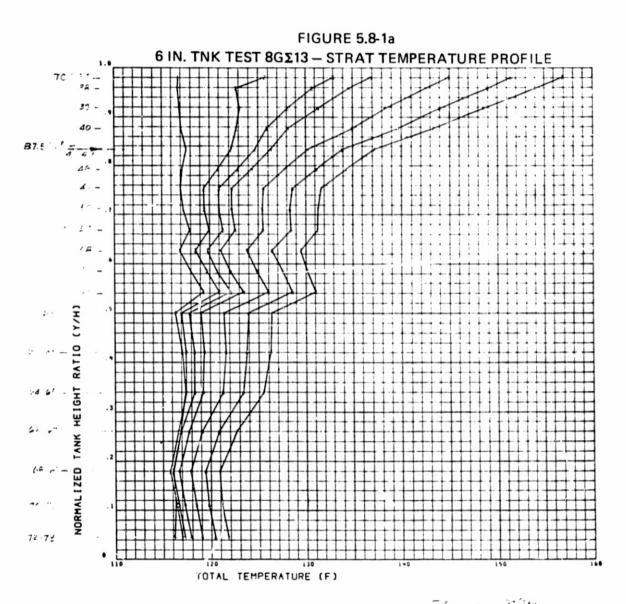
TINE (MIN)	0.000	5,00	0 8,300	10.000	15.000	20.000	25,000	
TAU	0.000	.200	.320		,600	,80C	1,000	
1 1	117.202		126.417					
2	117.375	124.625	176,772	128.083	131.667	134.750	137.675	
3	117 667	124.000	125,917	127.167	130.292	133.292	136.083	
4	117.875	123.768	125,438	126.500	129.417	132.643	134.708	
5	117,125	122.250	123,792	124.708	127.458	129.875	132,208	
6	117.208	121.058	123,375	124.208	126.500	128.750	130.875	
7			122,833					
t			122,272					
9			118,708					
10	117.290	122.708	125.033	126.250	130.042	133.232	136.417	
11	117 438	122,417	123,875	125.083	123.083	130.917	133.583	
12	117 583	121.375	122,958	123.958	126.375	128.722	131.083	
7 13			121.272					
1.4			123,958					
15	116.625	122.708	125,157	126.500	129.833	133.208	136.250	
16			124,417					
17			122,417					
1:			120,417					
12			_118,333					
20			125.033					
21			123,875					
22			122,958					
?3			121,292					
24			135,500					
25			125.010					
26			124.750					
27			124,570					
22			131.875					
29			133,230					
30			143,958					
31			120,657					
32			121,157					
			117.833					
34					115,200			

Table 5.8-2a. 6 IN. DIA TANK TEST 8G #13 (Page 2 of 2)	
35 106,500 108,125 108,500 108,792 109,458 110,500 111,4	17
36 115,750 119,625 120,167 120,500 121,792 123,292 124,7	
37 116,750 125,667 133,000 136,875 144,917 151,417 156,8	
38 116,708 122,792 130,750 134,625 142,625 149,042 154,0	
39 116,875 123,125 128,042 131,333 138,333 144,000 148,5	
40117,642-122,792 125,875 128,083 134,958 139,583-143,2	92
41 117,333 122,292 124,750 126,375 129,958 133,708 137,0	0.0
42 117,417 122,208 124,792 126,292 130,083 133,708 136,9	17
43 117,792 122,000 124,625 126,250 130,250 133,875 237,0	42
44 117,750 122,667 124,833 126,500 130,417 134,16 137,2	
45 117,625 121.875 124,208 125,792 129,917 133,708 437,1	
46117,375_122,083 124,750 126,583 130,750 134,125_437,6	
47 117,875 122,417 124,625 126,333 130,458 134,033 137,2	
48 117,146 120,854 122,875 124,333 127,750 131,146 134,3	
49 116,958 119,417 121,000 122,292 125,542 128,533 131,6	
50 117,250 119,458 121,000 122,292 125,417 128,333 131,3	33
51 117,000 119,042 120,375 121,833 124,625 127,533 130,4	38
_52	
53 116,667 118,542 119,708 121,167 123,917 126,917 129,7	
54 118,542 120,458 122,033 123,208 126,042 128,938 131,8	
55 118,375 120,667 122,000 123,292 126,083 129,083 131,9	38
56 118,542 120,458 122,093 123,208 126,042 128,958 131,8	15
57 118,375 120,667 122,000 123,292 126,083 129,033 131,9	56
58 116,875 118,542 119,730 121,167 123,833 126,417 129,4	38
59 118,042 119,708 120,730 122,125 124,792 127,542 130,1	. 7
60 119,333 120,958 122,208 123,458 126,000 128,542 131,0	13
61 116,375 117,042 117,875 119,083 121,453 123,917 126,3	53
62 116,625 116,958 117,792 118,750 121,083 123,125 125,6	5
63 117,593 118,042 118,958 120,042 122,203 124,375 126,8	33
64 118,542 119,083 120,167 120,917 123,333 125,238 127,50	10
65 116,333 115,917 116,533 117,542 119,333 121,542 123,49	7
66 116,458 116,042 116,272 117,208 118,542 120,250 122,13	5
67 117,230 117,292 117,542 118,250 119,667 121,458 123,21	18
68 116,250 116,042 116,229 116,958 118,292 119,750 121,4	9
69 116,000 115,542 115,833 116,417 117,542 119,125 120,3	15
70 116,042 116,042 116,167 116,708 118,042 119,250 120,83	13
71 116,583 116,875 117,167 117,833 118,875 120,292 121,50	0
72 117,208 118,083 118,533 119,292 120,417 121,750 123,29	2
73 115,167 115,833 115,875 116,542 117,667 119,125 120,29	2
74 108,375 112,417 114,833 116,750 120,458 123,875 126,95	8
75 94,250 97,750 99,333 100.917 103,625 106,167 108,25	0
76 103,750 104.667 105,033 105,792 107,292 108,667 110,29	2
77 88,333 87,833 87,667 68.125 88,667 89,333 90,29	2

TIME (•	0 10.00	0 20.00	0 30,000	40.000	50.000	60.000	30.000	99.000
TAL	C • () () J	.101	.202	.303	. 404	.505	.606	. 308	200
1 .	117,333	119.958	121.750	123.563	125.333 1	127.125	120.042	132,417 13	5 450
2	117,375	120,500	122.000	123.458	124.917	24.583	122.125	130,958 13	7 037
3	117,750	120.750	122.167	123.542	124.958	26.417	127.875	130,583 13	3,700
	11/,658	126.750	122 000	123 337	124,667 1	26.000	127 843	135,042_13	3,701
5	117.705	120.625	121.709	123.142	124.250	25.625	127 000	129,333 13	2 4 6 1 7 -
6	117.708	120.033	121.167	122.250	121.375 1	24.625	125 875	125,042 13	1,040
7	117,750	120,000	121.042	122.000	123,125 1	24.250	125 450	127,523 12	0.135
8	111.000	120.042	120.917	121.702	122 708 4	27.702	124 677	125,625 12	9,025
9	115.003	119.167	119.917	120.425	124 417 1	22.450	124 003	125,025 12	7,500
710	117.500	121 583	123 543	124 5.7	157847 7	27 426	121,496	132,123 13	1.4/5
11	1.1,70	121 468	122 750	124 147	127,796 1	2/10/2	127,704	137, 773 13	4,233
12		121 125	100 777	127 447	162/746 1	201/05	124,205	31,792 13:	3.208
13	117.503	120 703	124 475	123,417	184,700 1	25,8/5	127,203	29,333 13	1,563
14	117.042	110 017	151 607	122,042	125 41/ 1	24,456	125,542	27,417 12	7,292
15	117.583	121 626	127 007	124 535	125,125 1	26.875	124,833	32,167 13	5,125
-16	117 750	121 375	122 447	124,703	120 1046 L	2/12011	129,125	32,125 13	1,958
17	117.542	120 075	122 000	427 0-7	1211200-1	50-063-	24-045-	36,667 13	}
18	117 500	120 250	124 067	120,000	724,10/ 1	20,406	125,792	29,042 13	1.208
19	117 375	146 447	1410 777	121,426	155 400 1	23,833	125,083	25,875 125	1,750
20	117 7 .8	124 700	117,000	120,125	120,01/ 1	21,875	122,917	24,667 124	, 292
21	117,708	121,708	123,10/	124,007	126,167 1	27,705	129,333	32,208 134	1,95P
22	117,454	121,0/5	122,007	123,917	125,250 1	26,625	128,083 1	30,567 133	1,125
23	117 547	120 722	124 142	123-125	124-250-1	25,58.1.1	24-817-1	22,083-131	1565
24	110 625	124 000	141,625	122,375	123,208 1	24,292 1	25,417 1	27,375 123	1.25
25	110 060	124,000	125,833	133,142	134,333 1	39,792 1	42,667 1	47,500 150	375
26	116 747	143,10/-	125,500	129,792	32,500 1	35,542 1	33,417 1	43,042 147	,042
	110,000	120,625	124,583	128,107	131,292 1	34,250 1	37,000 1	41,625 143	.500
27	112,000	121 42	164,025	127,125	131 333 1	34.25C 1	37.083 4	41 708 445	E O O
-58	1191142	127,00	1301333	143 500	140,292 1	54,292 1	58,583 4	65,417 170	-667
29	110,/92	124,703	130.875	137.208	142.958 1	48.042 1	52.542 4	57 583 164	052
30	11/,125	129,333	136,000	140,792	144.792 1	46.292 1	51.542 1	55.667 160	708
31	11/1303	120,458	121,750	142.042	127.875 1	23.833 1	24.917 4	25 667 120	202
32	11/,41/	120,250	120.955	121.704 1	122.542 1	23,458 1	24.458 4	25 167 127	702
33	110,000	117,792	11/,3/5	117.425	117.917 1	18.333 1	13.875 4	17 702 120	100
34	115,583	114,375	113,125	112,167	11,375 1	10,875-1	10.708 4	10,208-114	167

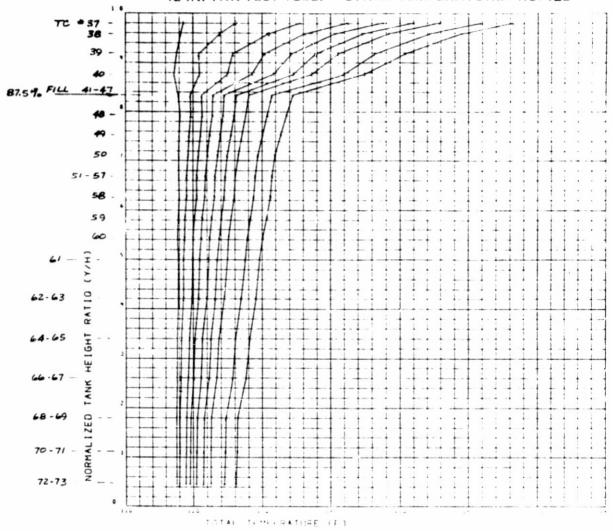
Table 5.8-2b. 12 IN. DIA TANK TEST 1G #27 (Page 2 of 2)

							.50 2 01 2,	
35								103,453 102,625
36	117,875	120,750	121,542	122,292	123,208	124,125	125,167	125,753 120,708
37	- 118,625	126,208	135.542	142.458	147.625	151,958	155,706	161,792 166,292
38								154,333 158,956
39								145,375 151,667
40	117 250	120 217	124 017	133 417	174 675	174 542	177 253	141,917,144,275
41								131,208 134,333
42								131,292 134,375
43	- 117,917	119,553-	121,250	122,875	124,542	126,206	124,167	131,417-134,500
44	116,083	119.433	121.459	122.958	124.708	126.417	129.250	131,500 134,583
45								131,458 134,455
46								131, 292 134, 333
47								131,625 134,708
48								130,708 133,583
40								
49								130,042 132,751
50	11/191/	110,545	140,750	142,083	123,542	124,917	126,542	129,375 131,917
51								128,833 131,292
52	-117,217	119,083	120,543	121,792	127,167	124,625	124,083	123,755-131,417
53	117,750	119,042	120,542	121,667	123,083	124,500	125,917	125,875 131,333
54								129,083 131,563
55								125,756 131,542
56	117.217	112.083	120.533	121.792	121,208	124.583	126.063	129,142 131,500
57								123, 258 131,500
58								123,703-131,208
59								
	117,000	110,000	120,705	121,000	12.7,007	124104.	127,417	125, 292 137, 625
60	11/1/20	114,/92	120,042	281,125	127,417	123,750	125,083	127,633 130,083
61	117,333	110,625	117,017	120,917	127,208	123,458	124,875	127,500 129,625
62	117,900	11º,750	119,917	120,028	127,125	123,292	124,542	127,342 129,208
63	117,750	119,458	119,750	120,503	121,475	123,042	124,333	125,792 124,917
-64	-111,667	114, 737	110 500	120,202	121,202	122,45	127,525	125,363 124,363
65	117,708	115.375	119.500	120,292	121,375	122,585	123.708	125, 763 129,125
66	117.7UP	110.375	119,500	120.292	121.375	122.583	123.703	125, 183 128,125
67	117.667	110.167	119.107	110.875	121.317	121.958	123,000	125,208 127,000
68	117 625	118 125	110 043	110 425	120 625	121 541	120 523	124,425 126,292
69	117 700	110 105	110 007	410 700	122 447	124 425	122 1303	124, 129 125, 476
	117,700	110,125	119,000	117,708	120,007	121,025	122,025	124,708 126,375
70	-1.7.4-1.211-	114152	114 Lug-	175-100	-15 UTVVV	121,025	122-623	124,703-124,375
71	11/,983	117,000	113,017	119,542	123,458	121,458	122,501	124,500 126,167
7?	11/,625	114,742	113,A75	119,542	120,458	121,454	122,454	124,458 124,204
75	117,667	11/1,042	117,717	110,542	120,417	121,500	122,542	124,500 12 ,125
74	97,583	97,45°	97,017	9A, 45A	30,520	100,297	101,375	105,458 105,783
_75	107,167	107,625	109,083	110,375	117,700	113.70%	115,375	113,500 120,958
▼ 76	67.575	00.375	82.333	89.042	80.042	89.167	49.535	87, 333 90,000
77	100.792	100.563	100.583	100.417	100.625	100.958	101.333	102,250 103,042
	,			,,				10-1-20 10010-2

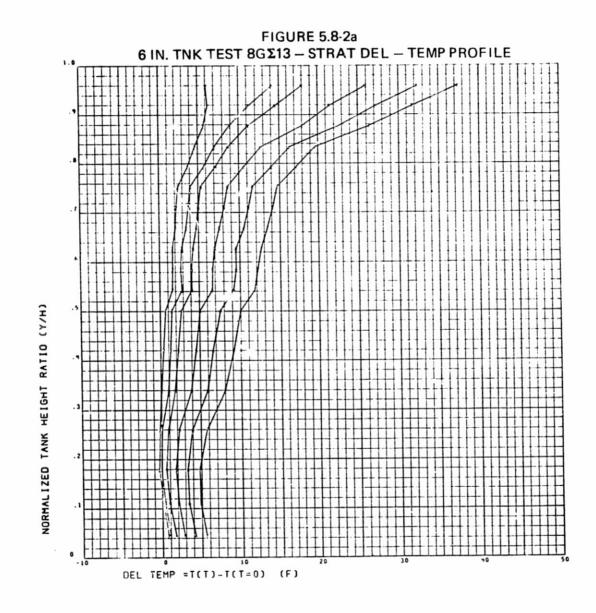


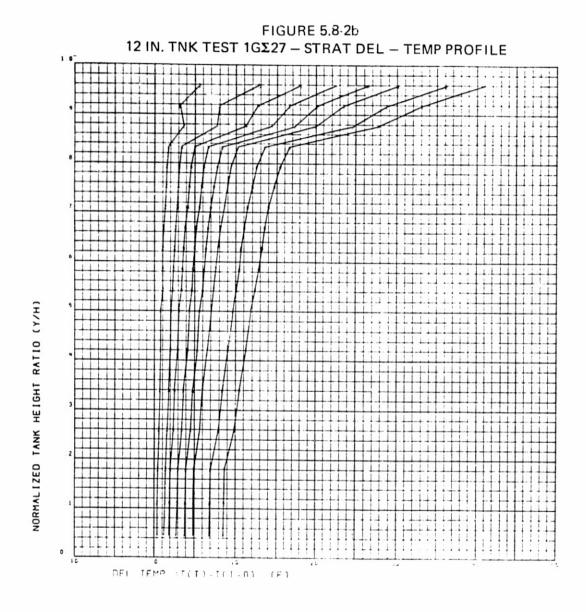
		1 (1411.)	C . 1211
9" = 90 ETU/An f72	1	0.	0.
LIQ + ULLAGE HTG	2	5.	. 2
LIN + ULLAGE HIG	3	8.	. 32
	4	:0.	. 4
	5	15.	. 6
	6	20.	.8
	7	25.	:.0

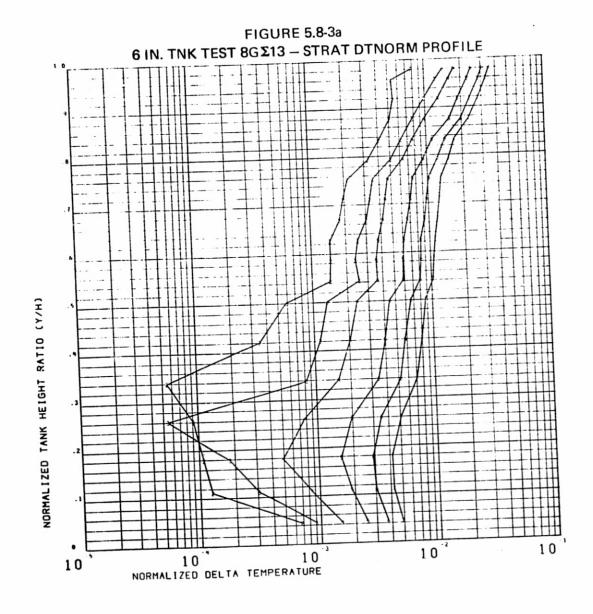
FIGURE 5.8-1b
12 IN. TNK TEST 1GΣ27 — STRAT TEMPERATURE PROFILE

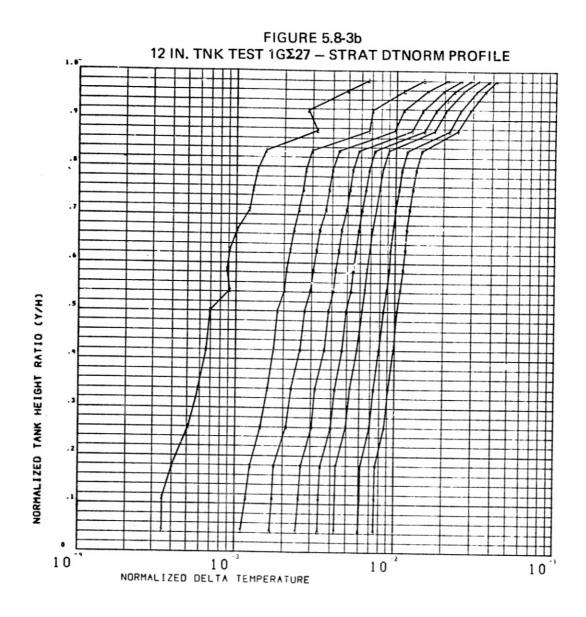


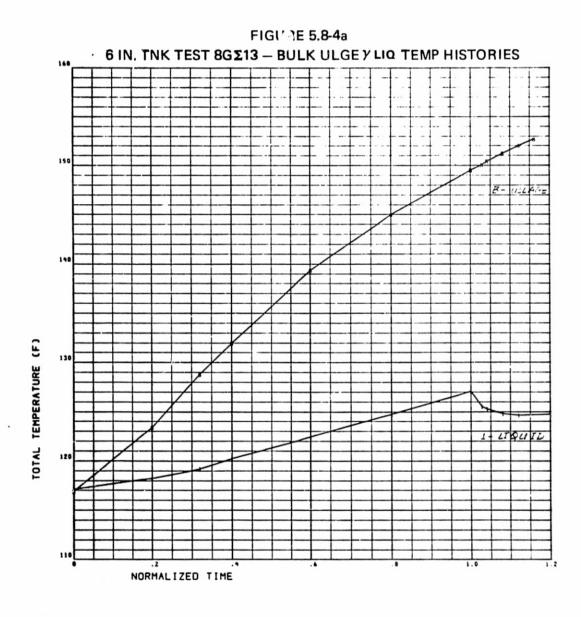
		7/4)	V/TAU)
2"= 45 BTU/kn ft 2	1	0.	0.
H L'SI + ULLAGE HTG	2	ic	01
L'DY + CALLEREE HILL	3	:0	.202
	4	3.0	. 303
	5	40	404
	6	50	.505
	7	60	. 606
	8	80.	.608
	_		

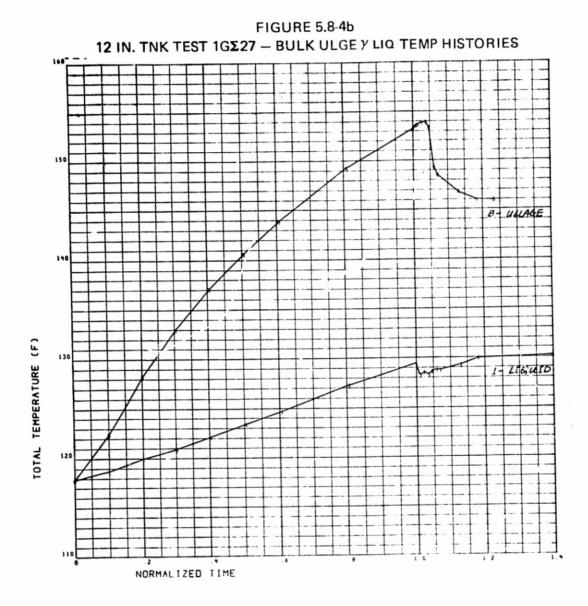












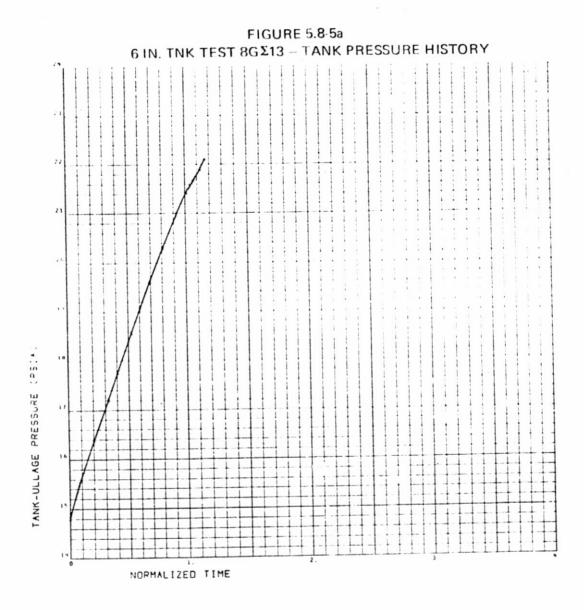
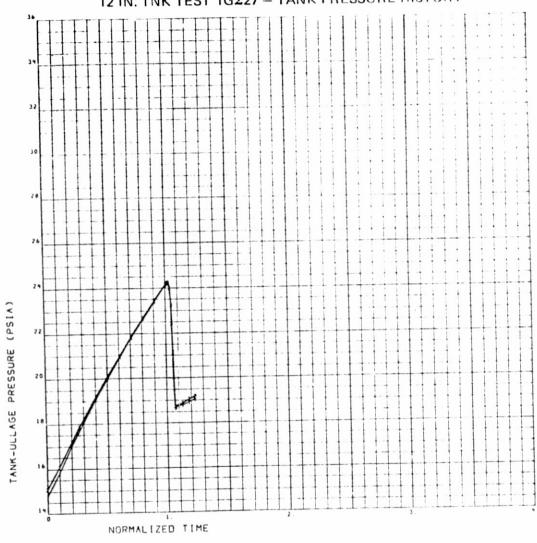
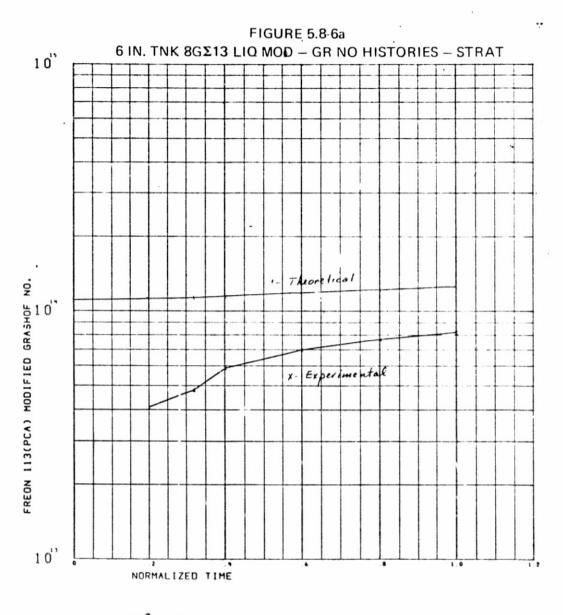


FIGURE 5.8-5b 12 IN. TNK TEST 1GΣ27 — TANK PRESSURE HISTORY





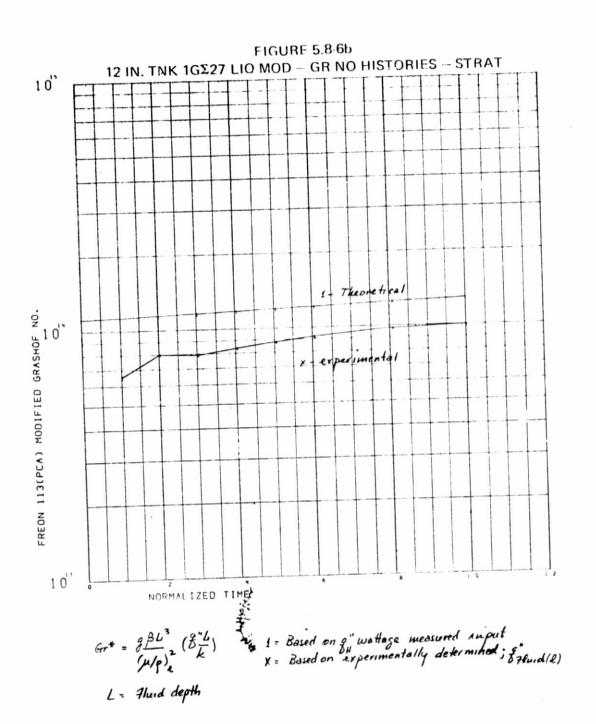
$$G_{T}^{*} = \frac{gBL^{3}}{(\mu/\rho)} \left(\frac{g''L}{k} \right)$$

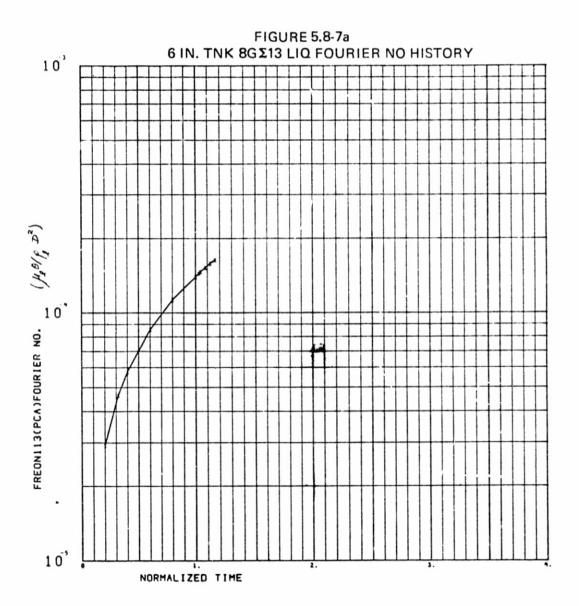
$$L = \text{Fluid depth}$$

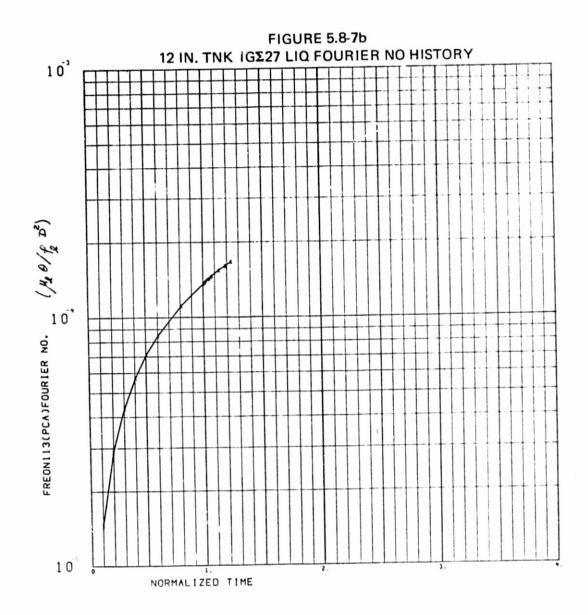
Grant = $\frac{gBL^3}{(\mu/p)^2}(\frac{g''L}{k})$ 1 - Based on g' wattage measured input

X - Based on experimentally determined; g''

L = Fluid depth







Section 5.9 SCALING SET

6-in Dia Tank Test	18-in Dia Tank Tests
2 7G	1G
Test #1S	Test #BS
= 557 11 10	Test #D

Table 5.9-1a. 6 IN. DIA. TANK TEST 27G#1S (Page 1 of 2) STRUCTURAL GEOMETRIC TANK WTS-WATTMETER HEAT FLUX INPUTS

DOME ARE DME WALL DME MASS	A FT2= VOL FT3 LBM=	.3927 = .0013 .65596	CYL AREA F 1 1/2 CYL MASS 1/2 CYL	T2≈ 1.5708 WALL VOLFT3≂ LBM=8199	FLNGE .00164	AREA FT2= FLNGE V GE MASS=	.0365 OL FT3=	.00076
			ULLAGE VOL I					
INPUT HE	AT FLUX	ES (BTU/H	R-FT2) AND ABS	ORBED HEAT AND	D TEMPERATI	JRE ESTIMA	TES	
H12= 0.	0000	H34= 0.0	0000 - H56=2236	6.6858 H910	=2236.6858	H78=	0.0000	
EDIONI FU	UX IN UL	LGE (BTIL	R=FT2)=2236.685 (HR=FT2)= 0.0	1000				
EST.LIQ TE	EMP INCR	RSE(STRAT)	0= 43.917 0= 15.7671F	(STRAT+DESTR (STRAT+DES	RAT)BTU= Strat)=	0.0000F	110000000000000000000000000000000000000	
EST.HT IN	PUT ULLA	GE (STRAT)	BTU= 0.000	(STRAT+DE	STRAT)BTU=	0.000		
No. or course a coupe from drop series.	STRUCTU	IRAL GEOME	able 5.9-1b. 18 TRIC TANK WTS=	IN. DIA. TANK WATTMETER HEA	EST IG#B	S PUTS		
DME MASS L	.Br= 16.	53031	CYL AREA FT 1/2 CYL W MASS 1/2 CYL	LBM= 22.13880		FLNGE VO E MASS= 10	L FT3=	.02051
			-FT2) AND 4850					
H12= 0.0	000 a	34= 0.0	000 H56= 753	.4729 H910=	752.5082	H78= 0	ES	
						.,,,,,,	. 0000	
EST.HT [1:P) EST.LIO (E)	UT LTQ(S	STRAT) BTU: SE(STRAT):	-Ff2)=-753.151: HR-Ff2)= 0.00 = 1197.835 = 15.9327F	000 (STRAT+DESTR (STRAT+DES	AT)RTU= TRAT)=	0.0000F		

Table 5.9-1c. 18 IN. DIA. TANK TEST #D (Page 2 of 2) STELCTORAL DEDMETRIC TANK WISHMATTHEIGH HEAT FLUX INFUTS

DOME AREA FIZE 3,5343 CYL APEA FIZE 14,1372 FLAGE AREA FIZE .3281

THE FALL VOL FIZE .03299 1/2 MYL FALL VOLFIZE .04418 FLACE VOL FIZE .02051

THE FASS LIME 16,53331 MASS 1/2 CYL LEME 28,13880 FLANGE MASS 10,275/1

LIO VOL FIZE 3,53429 ULLAGE VOL FIZE 3,53429

TYPUT HEAT FLUXES (BIU/HR-FIZ),AND AESCREED HEAT AND TEMPERATURE ESTIMATES

H12= 0,0000 H34= 0,0000 F56= 753,4729 H910= 752,5082 H78= 0,0000

EST, HT FLUX IN LIQ (BTU/HR=FT2)= 753.1513 EST, HT FLUX IN ULLRE (PTU/HR=FT2)= 0.0000 EST, HT INPUT LIG(STRAT)ETU= 1197.835 (STRAT+DESTRAT)FTU= 2928.042 EST, LIQ TERP INCRSE(STRAT)= 15.9339F (STRAT+DESTRAT)= 38.8666F

EST, HY INPUT ULLAGE (STRAT) PTU= 0,000 (STRAT+DESTRAT) BTU= 0,000

TI	ME(MIN)		.233			
TAU			233 4			
1			7.000 118		-	
2	1 1	6.625 11	7.125 118	875 121	.292 123.	625
3			7.625 119			
4			9.229 122			
5			0.833 126			
6			2.708_129			
7			3.208 129			
8			3.708 129			
9			8.083-120.			
10			6.833 118.			
11			6.917 118.			
			3691128.		-	
13			4.292 141.			
14			6.583 118.			
15			7.083 118.			
16			7.792 119.			
17			0.847 125.			
18			2.375 128.			
19			8.500 120.			
50			6.833 118.			
51			6.917-118.			
55			3.691 128.			
23			4.292 141.	-		
24			7.125-119.			
25			6.375 118.			
56			6.500 118.			
27			6.625 118.			
28			7.208 119.			
29			5.875 117.			
30-			6.542-118.			
31			2.611 135.			
32			3.167 136.			
- 33-			6.917-119.			
34	10	9.042 110	0.292 111.	563 112.	229 112.	833

99.625 100.292 101.167 101.958 102.917

108.875 109.417 109.958 110.750 111.583

94.000 94.333 94.458 94.833 95.208

Table 5.9-2a. 6 IN. DIA TANK TEST 27G #1S (Page 2 of 2)

104.042 103.667 103.708 103.625 103.667

-120-000-132-333-135-250-137-458-139-708

35

37

-36

75

76

77

TIME (MIN)	0.000	2.000	4.000	-		000
TALI	0.000		144 .66			
. 1	117.042-1	17.875-119	9.542 121	792 123	042 125.6	25
2	117.333 1	18.125 120	0.042 122	500 123	833 126.6	25
3	117.543 1	18.417 120	375 123	,000 124	333 126.9	17
4	-117.667-1	16-657-120	792-123	333-124	667-127-2	0.8
5	117.625 1	27.708 137	2.167 135	292 136	708 139.6	25
6	117.667 1	32.417 130	6.667 140	000 141	625 144.3	33
7	-117.875-1	34.042-130	8.125-141	000-142	167-145.0	42
8	118.125 1	30.625 13	3.708 136	708 137	792 140.4	1 /
9	117.750 1	25.520 15	4.583 127	125 128	458 130.9	56
10	117.292-1	18-000-11	958-122	458-123	853-124-5	0 0
11	117.375 1	18.208 12	0.500 123	.000 124	292 126.7	50
12	116.250 1	45.125 15	0.417 153	667 155	500 158.1	67
13	118.250 1	44.125-14	292-151	042-152	.000-154.7	92
14	117.042 1	17.875 119	9.542 121	792 123	.042 125.6	45
15	117.333 1	18.125 12	0.042 122	500 123	.833 126.6	45
16	117.458 1	18.333 12	0-542-1-23	107 124	417-126.9	17
17	117.542 1	26.333 13	0.625 133	917 135	.333 138.2	42
18	117.688 1	24.500 12	8.000 131	021 132	.458 135.3	
19		22.667-12	5.375-128	125-129	.583 132.3	33
50	117.292 1	18.000 11	9.958 122	.458 123	.833 126.5	
21	117.375 1	18.208 12	0.500 123	.000 124	.292 126.7	
55	118.625	46.053-15	0.625 155	917-153	417 158-2	92
23				.042 152	.000 154.7	92
24		17.875 11		875 123		
- 25		17.458 11		.042 122		-
26		17.250 11		.917 121		
2.7	113.792 1	16.833 11		.750 121		
58	116.750 1	17-125-11	8-125-119	245 150	-333-121-0	25
24		17.083 11			.875 122.6	
30	116.917 1	17.875 11		.000 123		
31	117.750-1	32.708-13	6.792-139	607-141	.125 143.3	5.5
32	118.500 1	37.700 14	1.750 144	.500 145	.875 148.4	20
33	113.708 1	20.917 12	4.625 127	.083 128	.292 130.6	6/
34	111.333 1	14.854-11	6-771-118	187-118	833-120.1	46

Table 5. 9-2b. 18 IN, DIA TANK TEST IG #BS (Page 2 of 2) 108,958 108,792 109,917 109,253 139,375 109,525 35 116,625 136,530 110,263 121,205 122,000 123,633 36 117,125 117,750 119,530 121,525 122,000 123,633 37 117,125 119,125 119,375 122,510 125,776 126,000 38 117,125 119,125 119,375 122,510 123,776 126,000 39 117,229 118,129 120,125 122,510 123,776 126,000 43 117,232 118,129 120,125 122,510 123,750 126,375 44 117,232 118,232 120,125 122,510 123,750 126,375 45 117,232 118,232 120,125 122,510 124,233 126,417 45 117,232 118,510 120,417 122,917 124,117 127 126,117 46 117,232 118,510 120,417 122,917 124,117 127 126,117 51 17,500 118,375 120,417 122,917 124,117 127 127 52 117,500 118,375 120,250 124,417 127 127 127 53 117,500 118,375 120,20 128,517 124,417 127 127 54 117,500 118,522 120,250 124,417 127 127 127 55 117,500 118,522 120,250 124,417 127 127 127 50 117,500 118,522 120,22 123,000 124,417 127 127 127 51 117,500 118,522 120,22 123,000 124,417 127 127 127 51 117,500 118,522 120,22 123,000 124,417 127 127 127 51 117,500 118,522 120,000 124,543 127,127 51 117,500 118,524 120,234 120,245 120,245 127 120,000 124,543 127 127 51 117,500 118,524 120,22 121,500 124,417 127 127 127 51 117,500 118,524 120,22 121,500 124,417 127 127 127 51 117,500 118,524 120,22 121,500 124,417 127 127 127 51 117,500 118,524 120,22 121,500 124,417 127 127 127 51 117,500 118,524 120,224 120,225 120,000 124,543 120,200 124,575 51 117,500 118,524 120,22 121,500 124,417 127 127 127 127 127 127 127 127 127 1				
Table 5.9-2b. 18 IN. DIA TANK TEST IG #85 (Page 2 of 108.972 109.875 109.375 109.375 109.16.526 136.50 110.292 143.125 144.542 141.16.526 115.00 121.625 122.833 123.458 120.117.125 118.17.18 375 162.292 122.500 121.625 123.470 121.625 118.17.125 118.17.18 375 162.292 122.500 123.750 120.117.250 118.75 162.292 122.500 123.750 120.117.250 118.75 162.292 122.625 123.750 120.117.252 118.292 120.250 122.625 123.750 120.117.252 118.292 120.250 122.625 123.750 120.117.252 118.292 120.250 122.625 123.750 120.292 120.200 120.292	000 000 000 000 000 000 000 000			WIL WORDE
Table 5, 9-2b. 18 IN. DIA TANK TEST 1G #BS (Page 116, 625 136, 500 140, 292 143, 125 144, 54 116, 625 136, 500 140, 292 143, 125 144, 54 116, 750 117, 750 119, 500 121, 625 122, 833 117, 125 118, 177, 125 119, 177, 126, 119, 177, 126, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 127, 117, 11				2000
Table 5, 9-2b. 18 IN. DIA TANK TEST 1G #BS 118, 625 136, 570 140, 292 143, 125 116, 790 121, 525 141, 125 118, 127, 119, 119, 570 121, 525 119, 570 121, 525 117, 125 118, 125 119, 570 121, 525 117, 125 118, 125 119, 375 122, 520 121, 525 117, 525 118, 127, 120, 342 122, 520 117, 250 118, 127, 120, 342 122, 520 117, 250 118, 127, 120, 342 122, 520 117, 292 118, 292 120, 112 122, 317 117, 292 118, 292 120, 417 122, 127 117, 292 118, 292 120, 417 122, 127 117, 292 118, 292 120, 417 122, 293 117, 292 118, 292 120, 417 123, 292 117, 293 117, 293 118, 292 120, 293 123, 300 117, 292 118, 292 120, 293 123, 300 117, 292 118, 292 120, 293 123, 293 117, 292 118, 292 120, 293 123, 293 117, 292 118, 292 120, 293 123, 293 117, 292 118, 292 120, 293 123, 293 117, 293 118, 292 120, 293 121,	age 31			25 E 5 E 5 E 5 E 5 E 5 E 5 E 5 E 5 E 5 E
Table 5. 9-2b. 18 IN. DIA TANK TEST 1G 1108.625 136.500 140.292 143.1 116.708-117.625-119.063-121.0 116.750 117.708 119.500 121.0 117.125 118.125 119.375 122.5 117.417 118.375 120.345 122.5 117.822 118.375 120.345 122.5 117.822 118.375 120.345 122.5 117.822 118.375 120.345 122.5 117.822 118.375 120.345 122.5 117.822 118.375 120.345 122.5 117.822 118.375 120.417 122.7 117.822 118.375 120.417 122.7 117.822 118.375 120.417 122.7 117.822 118.375 120.417 122.7 117.822 118.375 120.417 122.7 117.822 118.375 120.438 122.7 117.822 118.375 120.333 122.7 117.825 118.375 120.333 122.7 117.825 118.375 120.333 122.7 117.825 118.375 120.333 122.7 117.825 118.375 120.333 122.7 117.825 118.375 120.375 122.7 117.825 118.375 120.375 122.7 117.825 118.325 120.625 120.	BS 11 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	200 200 200 200 200 200 200 200 200 200		33.5
Table 5. 9-2b. 18 IN. DIA TANK TES 108.958 136.550 140.292 116.756 117.750 119.563 117.125 118.125 119.563 117.417 118.375 120.392 117.542 118.375 120.302 117.542 118.592 120.303 117.542 118.592 120.303 117.542 118.592 120.417 117.542 118.375 120.417 117.542 118.542 120.417 117.542 118.375 120.417 117.542 118.375 120.417 117.542 118.375 120.417 117.542 118.375 120.333 117.542 118.375 120.333 117.542 118.375 120.333 117.550 118.375 120.333 117.550 118.375 120.353 117.550 118.375 120.353 117.551 119.375 120.375 117.551 119.375 120.375 118.000 117.875 119.083 117.875 118.500 119.292 117.875 118.500 119.292 117.875 118.500 119.292 118.000 117.875 118.555 120.000 117.875 118.18.507 118.100 117.875 118.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 117.875 118.18.507 118.875 118.875 118.875 118.875 118.875	P water water out to it.	~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~ ~		0 C 01 M W 3 W 1
Table 5. 9-2b. 18 IN. DIA TAN 108.958 108.792 109 118.625 136.500 140 116.706 117.625 118.125 119 117.250 118.125 119 117.250 118.292 120 117.250 118.592 120 117.250 118.592 120 117.250 118.592 120 117.250 118.592 120 117.250 118.592 120 117.251 118.592 120 117.251 118.592 120 117.251 118.292 120 117.252 118.292 120 117.251 118.292 120 117.251 118.292 120 117.251 118.292 120 117.251 118.292 120 117.251 118.292 120 117.251 118.292 120 117.251 118.292 120 117.251 118.292 120 117.251 118.292 120 117.251 118.292 120 117.251 118.292 120 117.252 118.251 120 118.125 118.125 120 117.253 117.254 120 118.125 118.125 120 117.253 120 117.254 117.255 118 118.125 118.125 120 117.255 118.125 120 117.257 118.125 120 117.257 118.125 120 117.257 118.125 120 117.257 118.125 120 117.257 120 117.257 120 117.257 120 117.257 120 117.257 120 117.257 120 117.257 120 117.257 120 118.127 120 120 120 120 120 120 120 120	TE 2000 200 200 200 200 200 200 200 200 2	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		9958 9958 125 9942 9942 9942
Table 5. 9-2b. 18 IN. DIL 108.958 108.79 118.625 136.50 117.125 118.17 117.125 118.17 117.250 118.29 117.292 118.29 117.292 118.29 117.292 118.29 117.625 118.50 117.625 118.50 117.657 118.65 117.657 118.65 117.657 118.67 117.657 118.67 117.657 118.67 118.063 119.67 118.063 119.67 118.063 119.67 117.958 118.97 118.063 119.67 118.063 119.67 117.958 118.97 118.165 118.97 117.958 118.97 117.958 118.97 117.958 118.97 117.958 118.97 117.958 118.97 117.958 117.958 117.958 117.958 117.958 117.958 117.958 117.958 117.958 118.18.18 94.333 94.33	109 1199 1199 1199 1199 1199 1199			111111111111111111111111111111111111111
Table 5.9-2b. 18 IN 108.958 10 118.625 13 117.125 11 117.125 11 117.125 11 117.125 11 117.125 11 117.125 11 117.125 11 117.129 11 117.129 11 117.129 11 117.129 11 117.129 11 117.129 11 117.129 11 117.129 11 117.129 11 117.129 11 117.129 11 117.129 11 117.129 11 117.129 11 117.129 11 118.000 11 118.000 11 117.917 11 117.917 11 117.917 11 117.917 11 117.917 11 117.917 11 117.917 11 117.917 11 117.917 11 117.917 11	10 10 10 10 10 10 10 10 10 10 10 10 10 1			2 C C C C C C C C C C C C C C C C C C C
Table 5. 9-2b. 108.95 1108.95 1117.75 1117.85 1117.85 1117.85 1117.85 1117.85 1117.85 1117.85 1117.85 1117.85 1117.85 1117.85 1117.85 1117.85 1117.85 1117.85 1117.85 1118.06 1117.85 1118.06 1117.85 1117.85 1118.06 1117.85 1117.85 1117.85	N amilianian			0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Table 5.9	2b	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	$\frac{1}{1}$	4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4
40 T T T T T T T T T T T T T T T T T T T	6			
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; >	WWWWagaa	3 3 3 3 3 0 0 0 0 0 0 0 0 0 0	N:0 c 0 c 0 c c c c	01111111

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Table 5.9-2c. 18 IN. DIA TANK TEST 1G #D (Page 2 of 2)
           113,875 113,593 113,542 113,583 113,833
  36
           -118,042-136,250-139,792-143,625-146,542
  37
           113,042 113,125 113,625 114,705 115,625
  38
           113,375 113,542 114,250 116,083 117 333
  39
         --113,833 114,042 115,375 117,875 119,583
  4 C
           114,208 114,708 116,167 118,833 121,000
  41
           114,333 114,675 116,458 119,625 122,333
           -114,375-115,167-116,792-120,333-123,250
  43
           114,542 115,208 116,958 120,333 123,208
  44
           114,542 115,417 117,083 120,625 123,375
  45
           114,292 115,083 116,675 120,417 123,250
  46
           114,292 115,250 117,042 120,667 123,583
  47
           114,417 115,542 117,417 121,203 124,25C
           -115,2>0-116,333-116,333-122,750-126,250
  48
  49
          / 115.542 116.667 118.833 123.250 126.833
  50
           116,042 117,292 119,375 124,083 127,292
           116,417 117,625 119,833 124,583 127,333
  51
  52
           116,250 120,458 119,750 124,667 127,375
  53
           116,250 117,333 119,708 124,583 127,417
           116,319-119,542 119,819-124,667 127,431
  55
           116,375 117,542 119,750 124,583 127,458
 56
           116,458 117,768 119,958 124,667 127,542
  57
           116,303 117,625 119,875 124,708 127,417
  58
           116,917 117,958 120,375 124,542 127,333
  59
           116,792 116,083 120,583 124,583 127,417
           116,750-118,333-120,458-124,208-126,875
 61
           117,167 119,268 121,256 124,208 127,642
 62
           117,408 119,125 121,458 125,542 128,333
 53
           117,167 118,875 121,208 125,208 126,C42
 64
           117,347 118,389 120,222 124,028 126,764
 65
           117,167 118,125 120,000 124,000 126,792
 66
           117,417 117,917 119,208 122,542 125,167
 67
           117,250 117,500 118,500 121,625 124,083
 68
           117,125 117,375 116,500 121,875 124,542
          117,200 117,542 118,750 122,207 124,958
 69
 70
           117,375 117,542 116,417 121,167 123,667
 71
           117,208 117,292 118,125 121,333 123,750
 72
          117,042 116,042 119,542 123,125 126,083
          117,125 118,042 119,792 123,333 126,458
 73
 74
            66.107
                   86,292
                            86,042
                                     86.083
                                             86,167
 75
            94,042
                   94,167
                            93,958
                                     94.042
                                             94.250
 76
            84,958
                    84,958
                            84,792
                                     84,917
                                             84.917
 77
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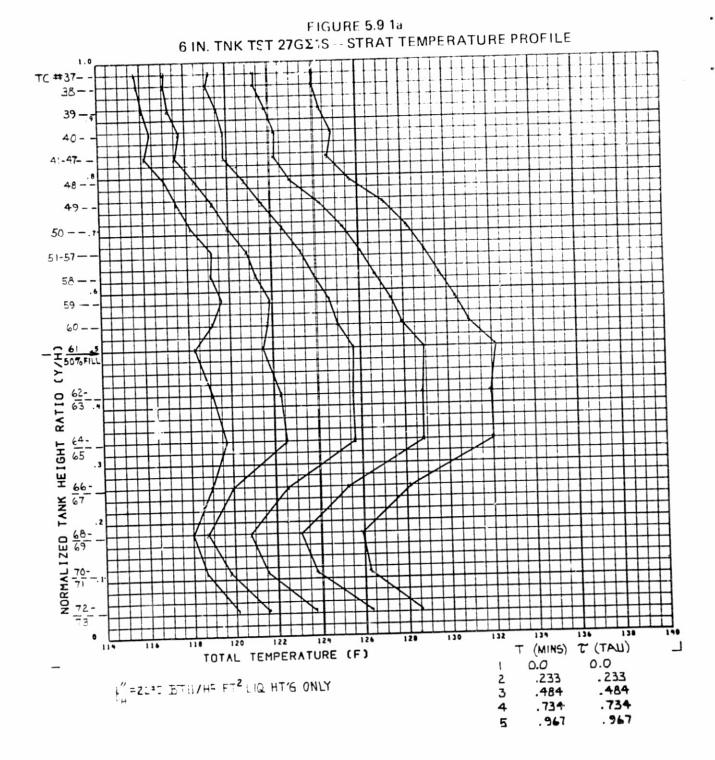
95.625

95.667

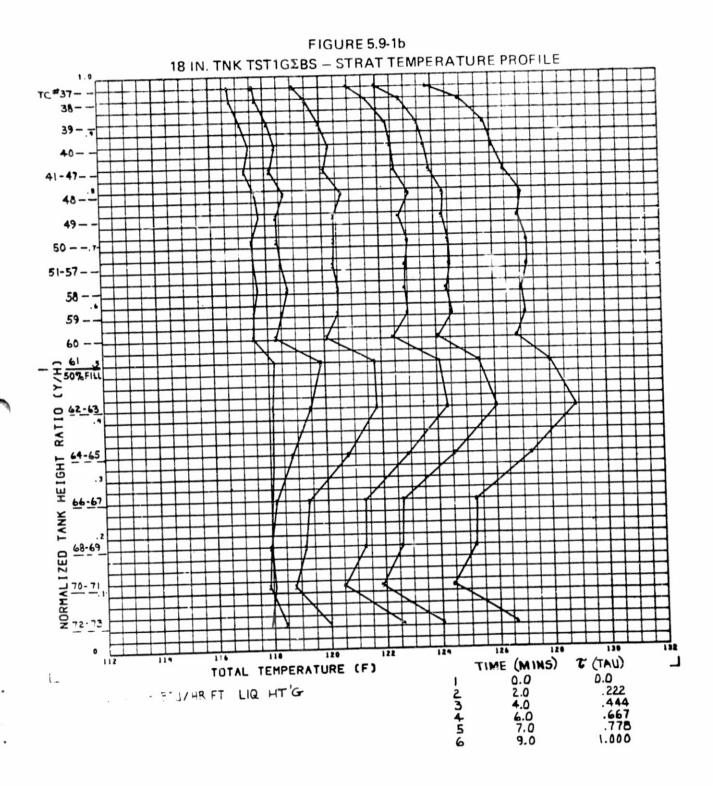
95.500

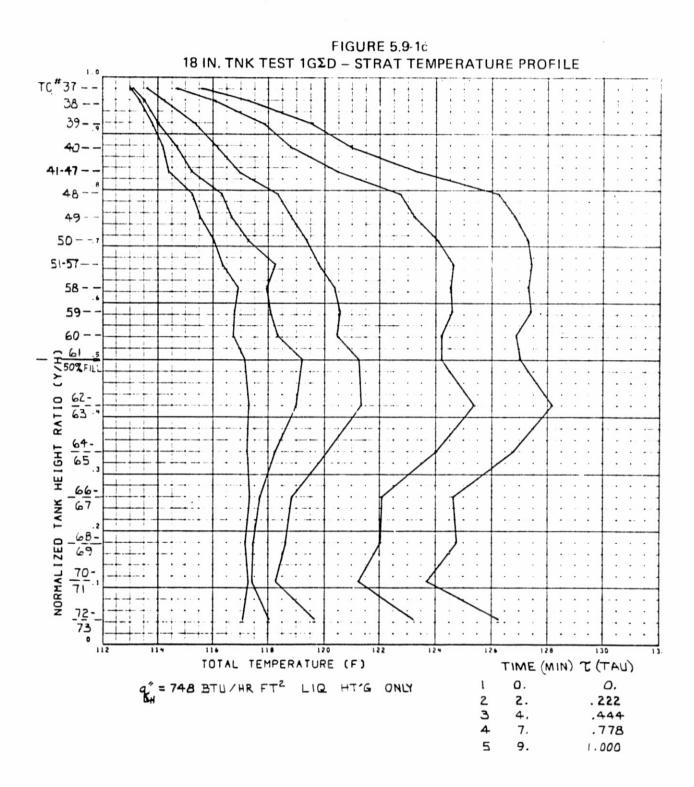
95.583

95,667

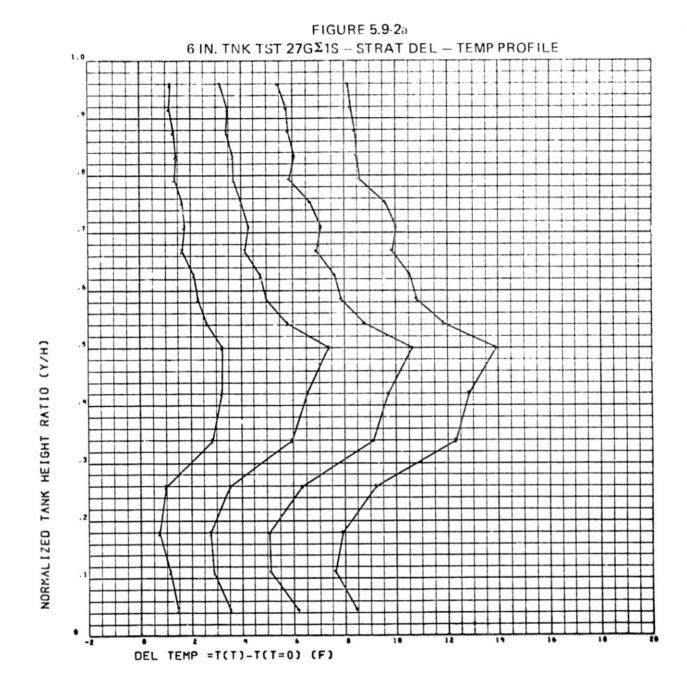


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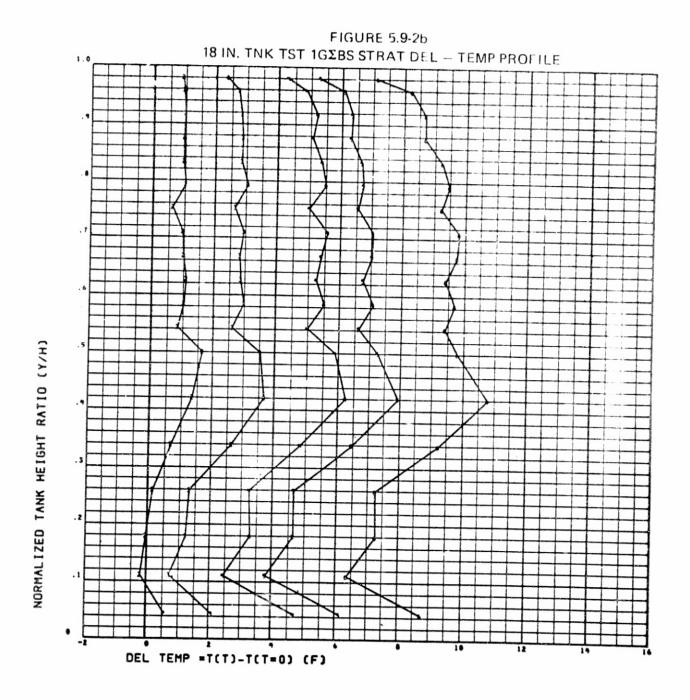


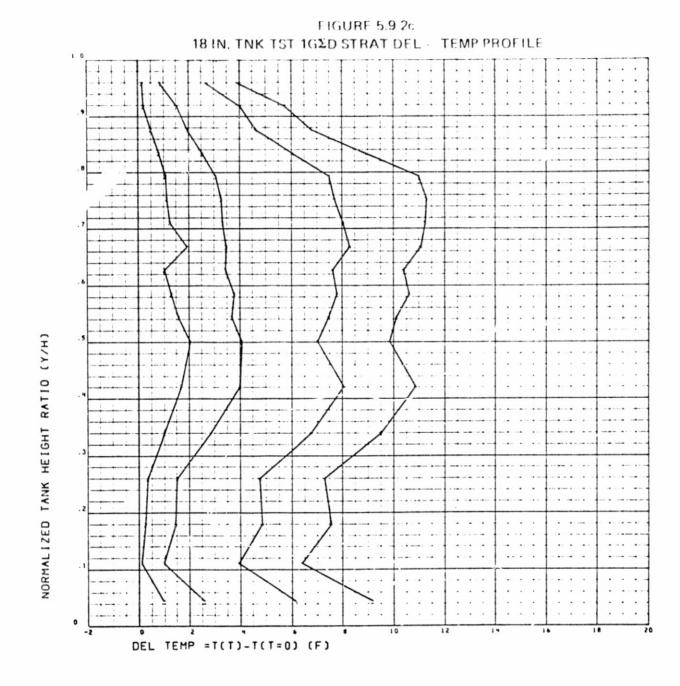


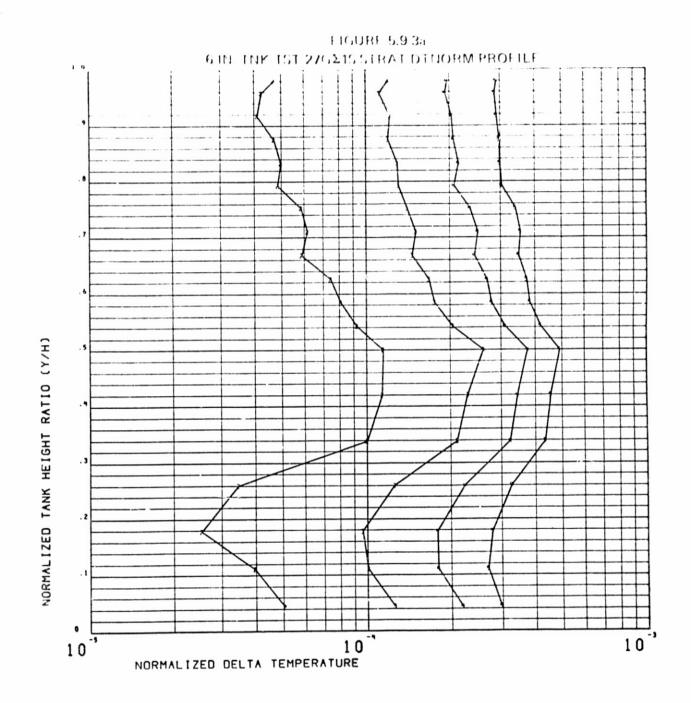
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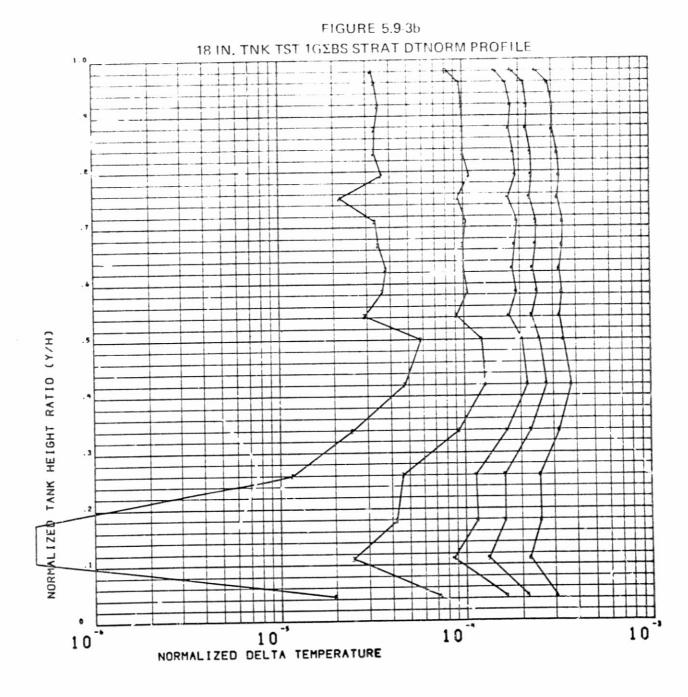


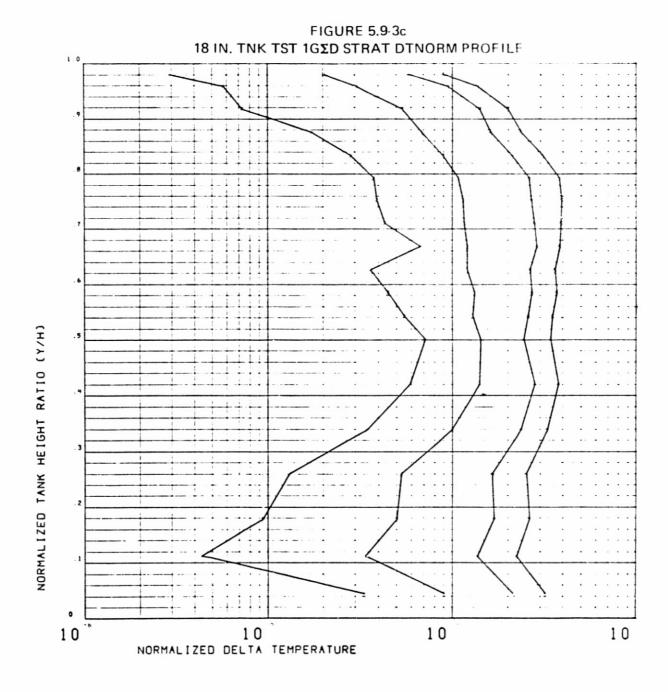
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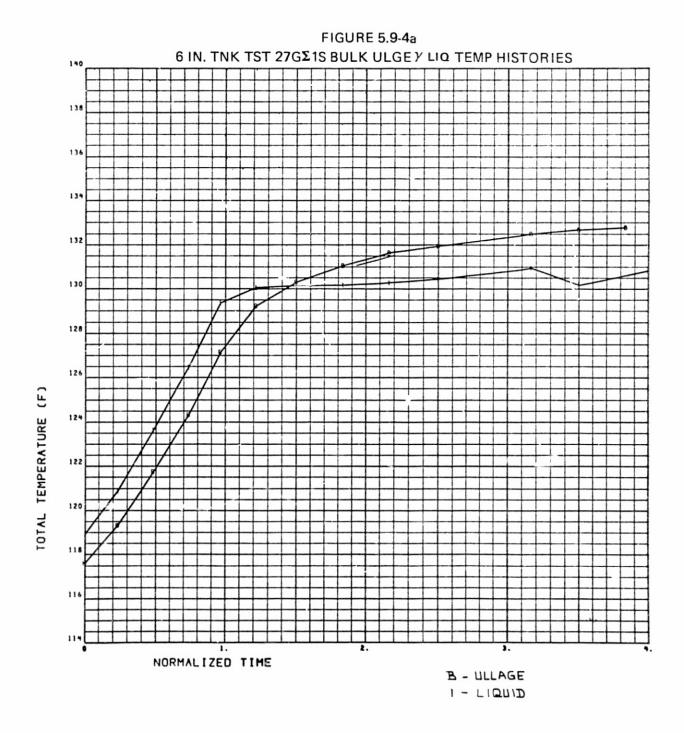


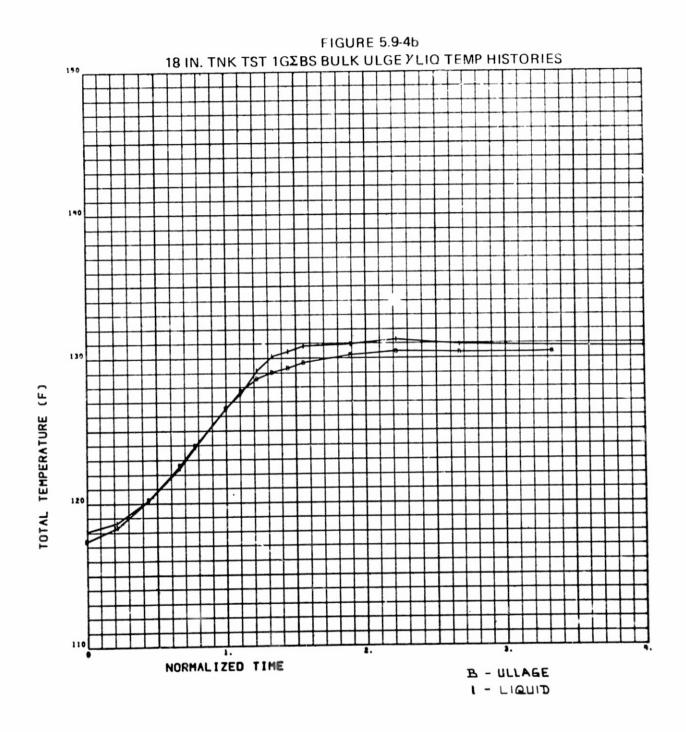


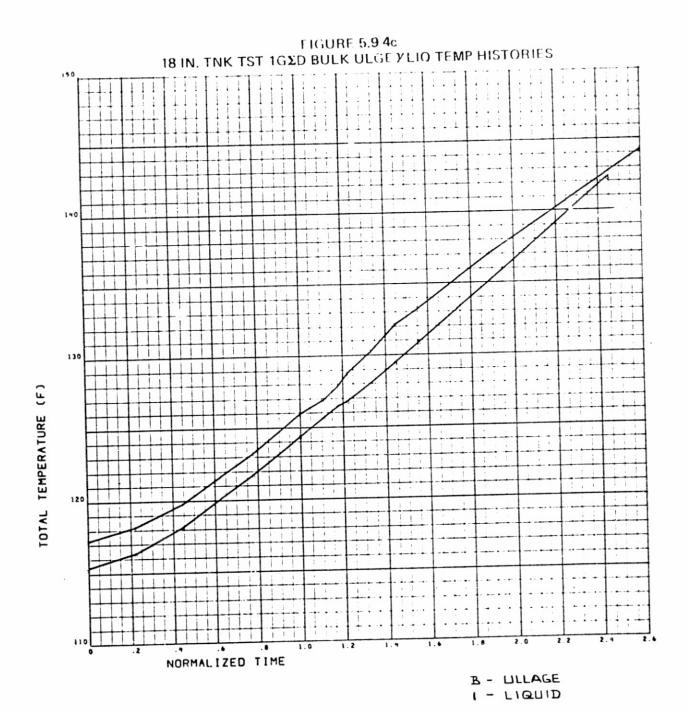


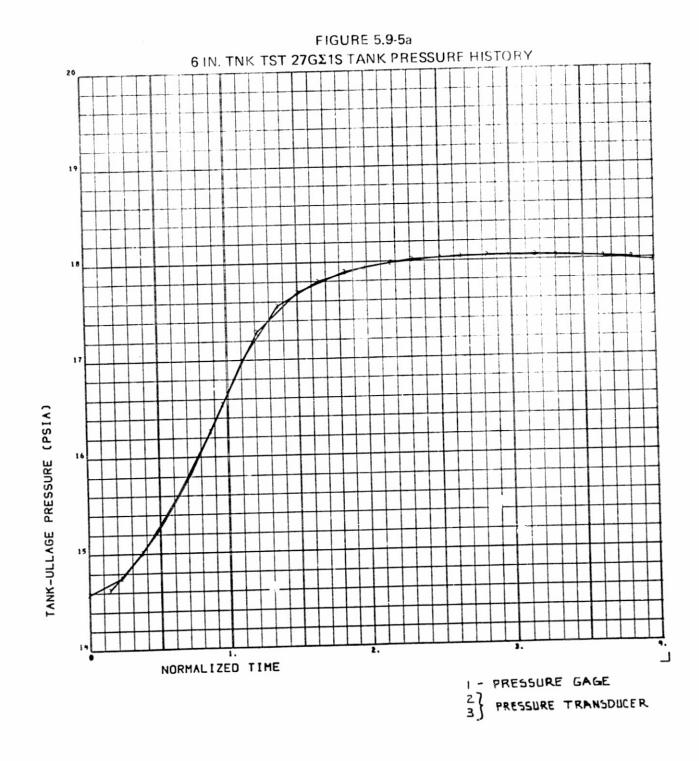


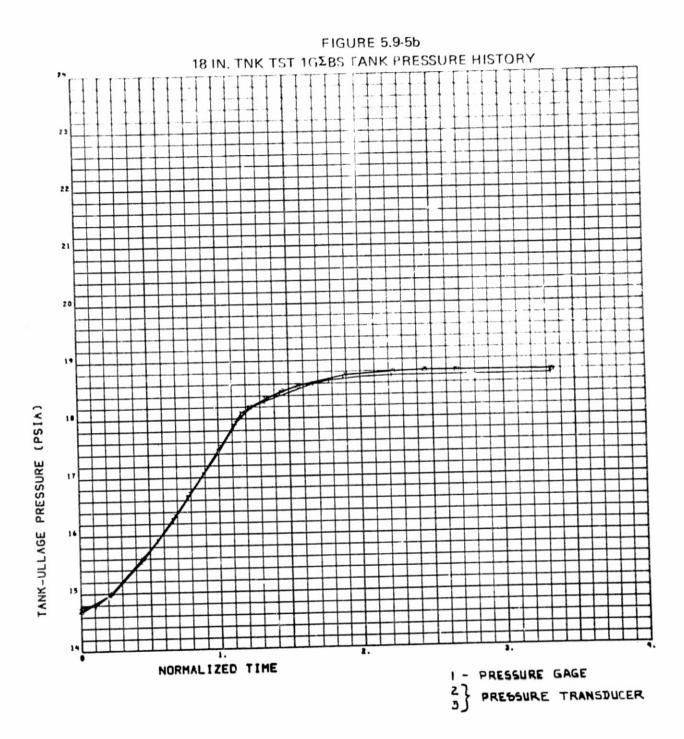








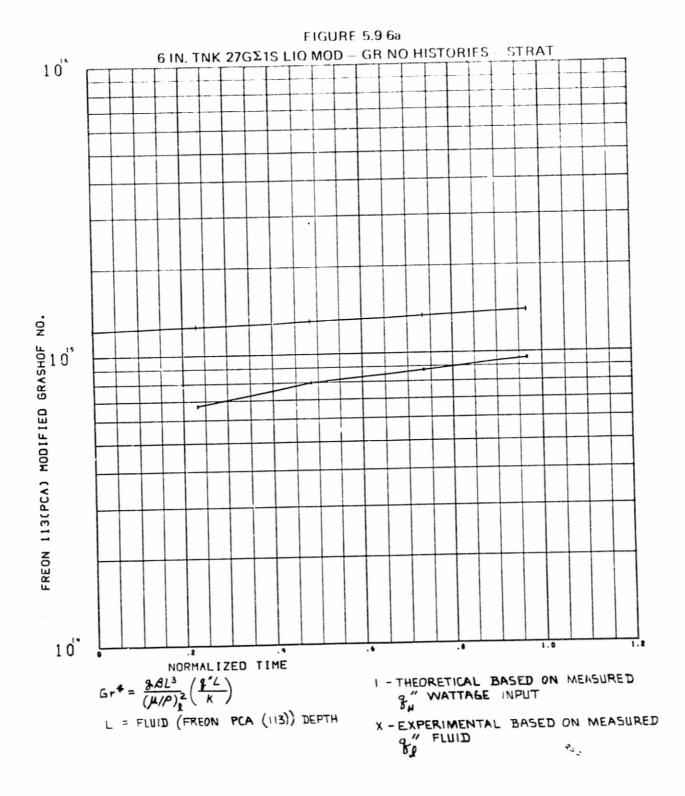


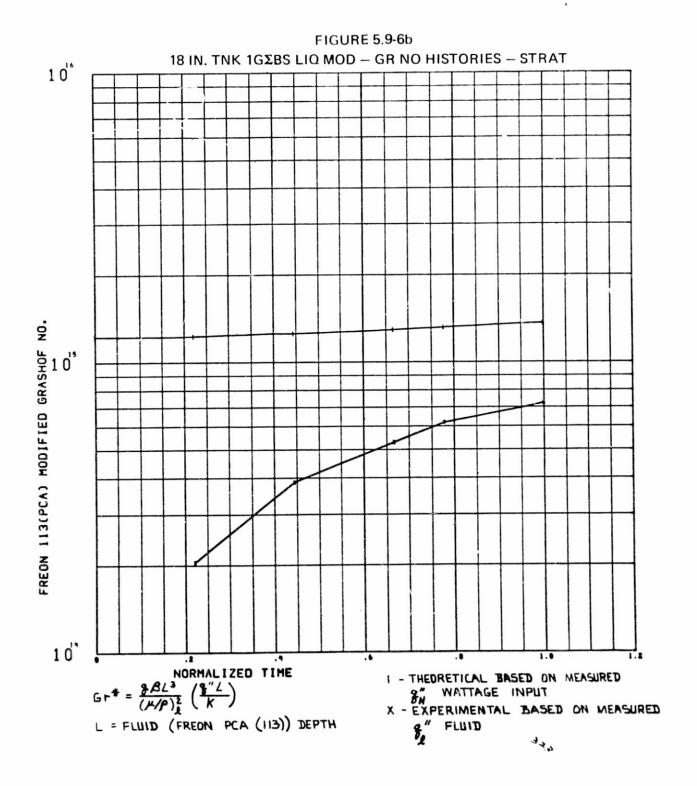


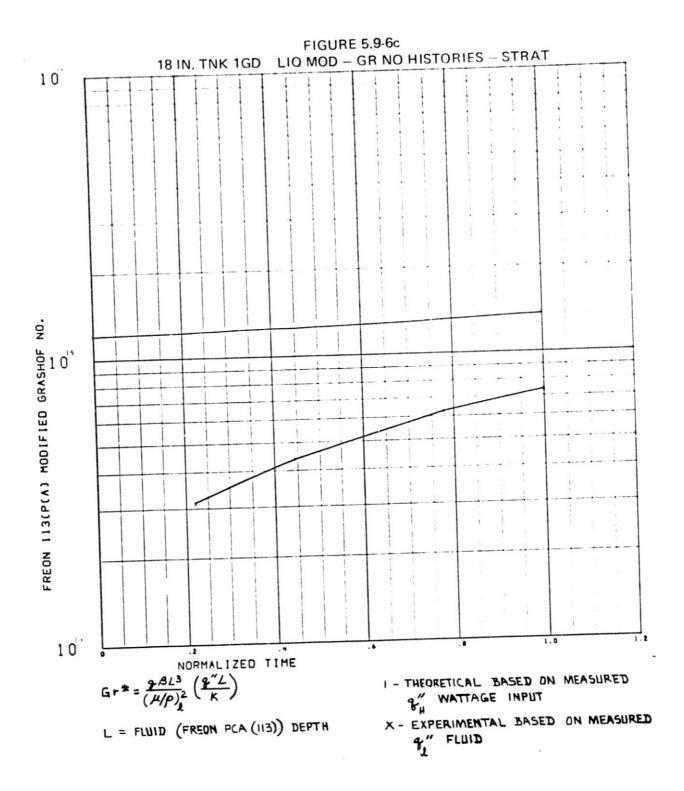
PRESSURE TRANSDUCER

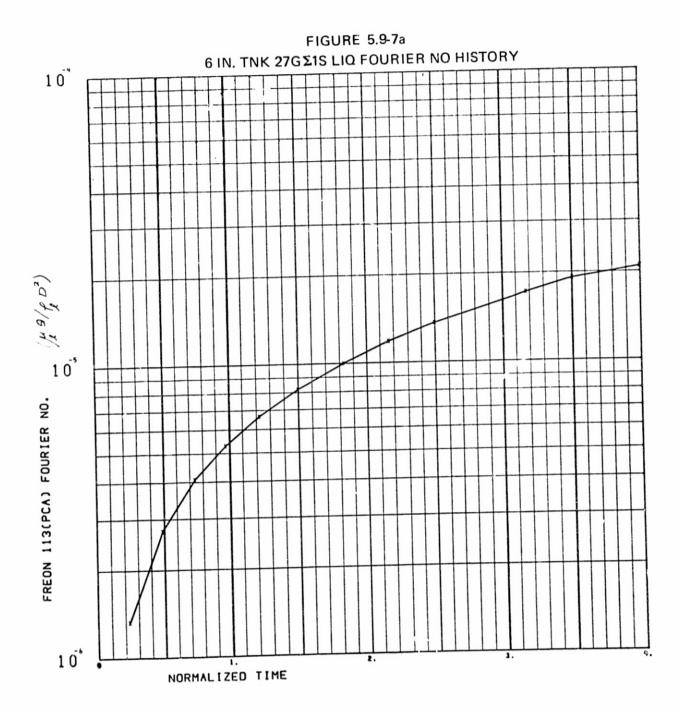
FIGURE 5.9-5c 18 IN. TNK TST $1G\Sigma D$ TANK PRESSURE HISTORY TANK-ULLAGE PRESSURE (PSIA) NORMALIZED TIME PRESSURE GAGE

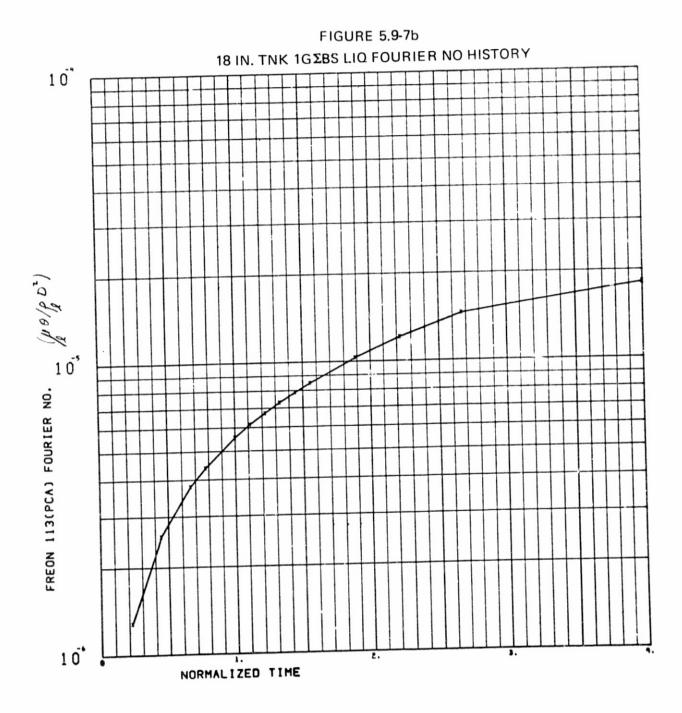
342

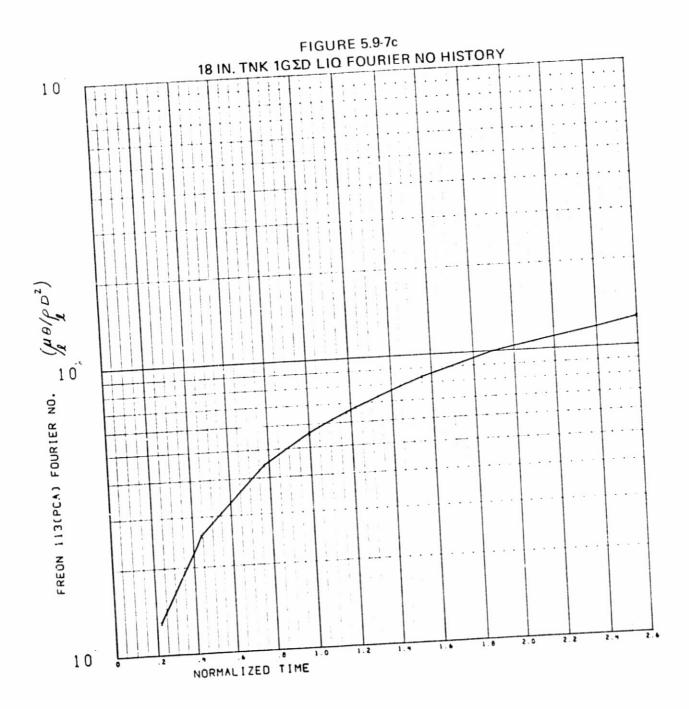












Section 5.10 SCALING SET

6-in Dia Tank Test	18-in Dia Tank Test
27G	1G
Test #3S	Test #IS

Table 5.10-la. 6 IN. DIA. TANK TEST 27G#3S STRUCTURAL GEOMETRIC TANK WTS-WATTMETER HEAT FLUX INPUTS

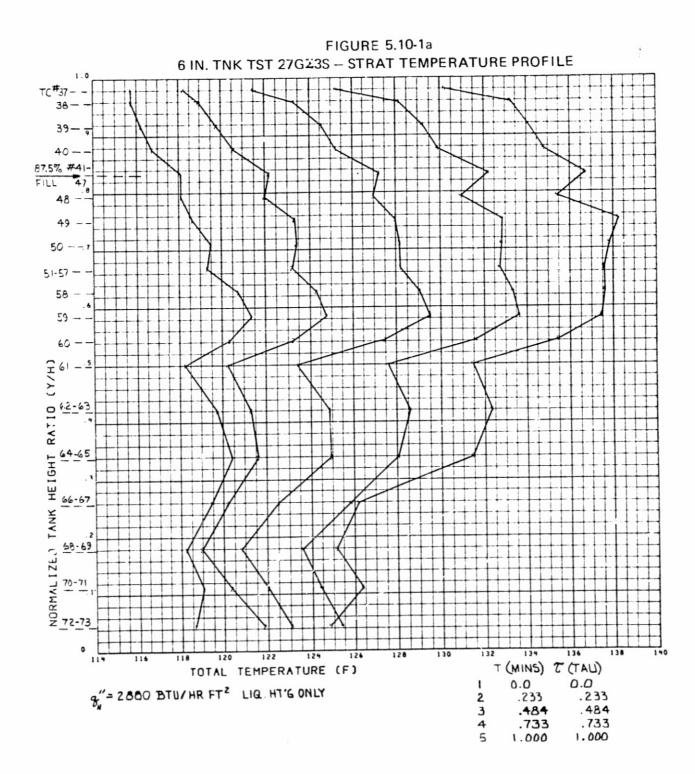
DOME AREA FT2= .3927 CYL AREA FT2= 1.5708 FLNGE AREA FT2= .0365 DME WALL VOL FT3= .00131 1/2 CYL WALL VOLFT3= .00164 FLNGE VOL FT3= .000 DME MASS LBM= .65596 MASS 1/2 CYL LBM= .81996 FLANGE MASS= .38058	76.
LIQ VOL-FT3= .22907 ULLAGE-VOL FT3= .03272	
INPUT HEAT FLUXES (STU/HR=FT2)+AND ABSORBED HEAT AND TEMPERATURE ESTIMATES	
H12=2884.4216 H34=2884.4216 H56=2884.4216 H910=2884.4216 H78= 0.0000	
EST.HT FLUX IN LIQ (BTU/HR=FT2)=2884.4216 EST.HT FLUX IN ULLGE (BTU/HR=FT2)= 0.0000 EST.HT INPUT LIQ(STRAT)BTU= 94.392 (STRAT+DESTRAT)BTU= 0.000 EST.LIQ TEMP_INCRSE(STRAT)= 19.3591F (STRAT+DESTRAT)= 0.0000F	
EST.HT INPUT ULLAGE(STRAT)BTU= 0.000 (STRAT+DESTRAT)BTU= 0.000	
Table 5. 10-1b. 18 IN. DIA. TANK TEST 1G#15	
STRUCTURAL GEOMETRIC TANK WISHWATTMETER HEAT FLUX INPUTS	
DOME AREA FT2= 3,5343 CYL ARFA FT2= 14,1372 FLNGE AREA FT2= .3281 DME WALL VOL FT3= .03299 1/2 CYL WALL VOLFT3= .04418 FLNGE VOL FT3= .020! DME MASS LBM= 16,53031 MASS 1/2 CYL LBM= 22,13880 FLANGE MASS= 10,27571	51
LIG VOL FT3= 6,18501 ULLAGE VOL FT3= ,88357	
INPUT HEAT FLUXES (BTU/FR#FT2), AND ABSORBED HEAT AND TEMPERATURE ESTIMATES	
H12= 966,6835 H34= 966,6835 H56= 964,7540 H910= 962,3422 H78= 0,0000	
EST, HT FLUX IN LIG (BTU/FR=FT2) = 965,0435 EST, HT FLUX IN ULLGE (BTU/FR=FT2) = 0,0000 EST, HT INPUT LIGISTRAT) BTU = 2558,057 (STRAT+DESTRAT) ETU = 0,000 EST, LIG TEMP INCRSE(STRAT) = 19,4362F (STRAT+DESTRAT) = 0,000F EST, HT INPUT ULLAGE(STRAT) RTU = 0,000 (STRAT+DESTRAT) BTU = 0,000	erados

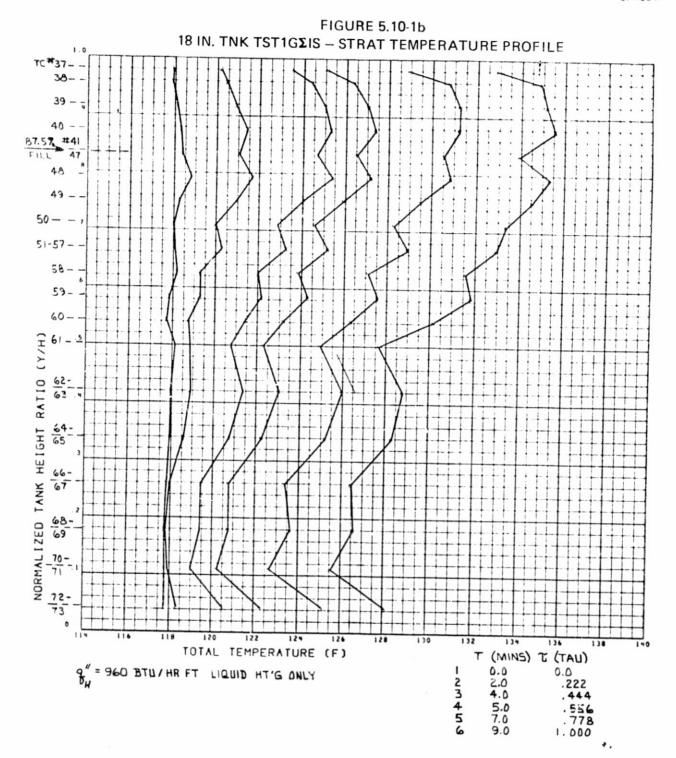
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	5 · ·		11	7 .	25	125	• 5	42-	135	5 . /	08	-14	• 0	24		45	• '	20.		
	3		11	7.	792	124	• 4	58	132	2 • 1	25	1.	88.	25	0 1	44	• 4	1/		
	4		11	7 . 7	292	123	• 5	42	131		908	13	37.	12	5 1	42	د .	40		
	5		110	6.	792	122	.6	25	130	• 6	92	13	56.	00	0 - 1	40	٤.	15		
	6		116	6 . 1	333	123	. 0	42	130	. 1	67	13	55,	25	0 1	39	د ،	42		
	7		11	7 . :	292	123	. 8	33	130	• (21	13	34.	64	6 1	39	• 1	88		
	8		-11	7 .	750-	124	.6	25-	-1-29). <u>.</u> .{	375	-1:	34.	-04	2-1	38	-8	55		
	9		111	5.	208	118	. 2	92	121	1 . 5	542	12	23.	87	5 1	27	• 6	25		
	10				583		. 8	33	147	7 . 1	67	15	53.	70	8 1	59	. 9	58		
	_		::	7	625	1 Z A	. 0	00	147	7.7	792	-15	56.	12	5 1	61	. 6	25		-
	11		11		000	1/10	- 1	67	150	1 . 8	3 3 3	1	58.	91	7 1	64	. 1	25		
	12		111	4	625	177	- 4	25	144	5 . 1	117					47				
	13		11		375-	131	. 6	67_	42/		75	-4-	31.	50	0-4	-36	. 7	50		
	14		11	,	333	120	. 0	51	17	. .	567	•	38.	41	ž ;	43	9	17		
	15		11	•	333	120	• 2	30	130	2 0 0	. o F	. :	20	58	7	45	. n	8 7		
	16		11	! •	333	121	• 4	1/	13.	•	122	4	370 75	45	5 - i	70	. 3	33		
_	17		11	٥.	111	124	• [10	13		775		77	70	3	34	• //	58		
	18		11	5 ,	500	123	• 4	58	150	•	3/3	1.	320	17	2	30	• 7	0 (,		
	19		11	5.	625	118	. 4	58	12	Ō•,	958	1	23,	/4	2	150	• /	00		_
	50		11	7.	583	-137	. 8	33-	14	7 :	67	-1-	53	-70	8-	154	• 7	סכי		
	21		11	7.	625	138	. 0	00	14	7.	792	1	56,	12	5	161	. 6	25		
	5.5		11	8.	000	140	0 1	67	15	0.	833	1	58,	91	7	164	. 1	25		
	23		11	6 -	625	137	. 6	25	14	6.	417	-1	50,	79	2 - :	47	• 2	92		
	24		11	5.	792	3.3.6	0 6	25	12	3.	375	1	28,	.20	8	133	. 4	58		
	25		11	5.	000	14	. 4	58	12	1.	125	1	25,	, 29	2	130	• 4	11/		
-	26		-1-1	4 .	042	-1-1-7	-3	75-	-1.2	0 .	958	1-	257	-16	7-	<u>-</u> 30	y-1	67		
	27		10	6.	805	117	. 3	33	12	0.	958	1	24.	91	7	130	. 0	83		
	28				917			92	11	9.	167	1	21	54	2	124	. 6	67		
NSST45	29		• • • •	<i>/</i> .	958	116	. 0	42	-11	8.	292	-1	21	58	3	25	. 8	33		
				5	333	115	1.4	17	12	3.	042	1	27	83	3	133	. 0	83		
	30		11	, ,	847	174	7	89	13	8 -	250	1	39	58	3	140		67		
	31		11	3	875-	17/	/I	17	1.7	A_	587	_1-	39	41	7_	40	_ 8	333		
	- 32		-11		958	-134		17	11	A	717	1	20	0.4	2	122	Ċ	15A		
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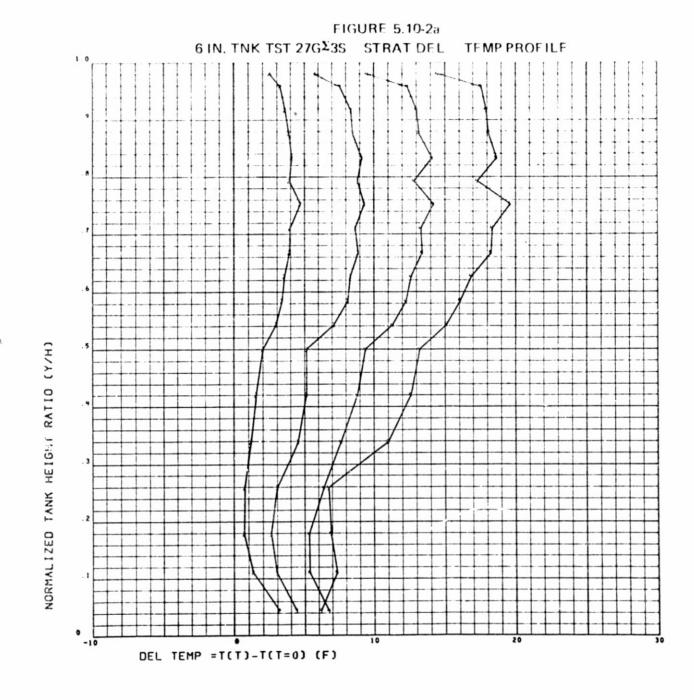
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Table 5. 10-2a. 6 IN. DIA TANK TEST 27G #3S (Page 2 of 2)
         --100.875-100.500-100.208-99.917-112.167
           118.833 134.375 138.083 139.667 140.583
 36
 37
           115.750 118.250 121.458 125.250 130.250
           115.750-119.000-123.292-128.125-133.292
 -38
 39
           116.208 119.792 124.542 129.208 134.125
           116.750 120.583 125.208 129.917 134.833
 40
           -117.750--121.542--126.625--131.917--136.250
 41
           117.292 121.333 126.375 131.333 135.750
 42
 43
           118,458 122,458 127,542 132,375 136,875
           -1-17--500--1-21--479--1-26--333--1-31--458--1-36--333
           118.792 123.042 128.250 132.417 136.750
 45
           117.708 121.625 126.292 131.583 13e.917
 46
          -119.208-123.833--129.250--134.458--138.167-
 47
          118.125 122.000 126.958 130.958 135.417
 48
 49
          118.667 123.333 127.968 132.875 138.250 *
 50
          119.500 123.417 128.167 132.833 137.833
          120.125 123.861 128.611 133.097 137.708
 51
 52
          119.333 123.222 128.201 132.757 137.503
 53
          -118.542-122.583-127.792-132.417-137.417-
 54
          119.333 123.222 128.201 132.757 137.563
 55
          119.333 123.222 128.201 132.757 137.563
 56
          -119-333--123-222--128-201--132-757--1-37-563-
 57
          119.333 123.222 128.201 132.757 137.563
 58
          120.750 124.306 129.056 133.361 137.583
 59
          -121.375-124.750--129.500--133.625--137.458
 60
          120.333 123.250 127.458 131.625 135.458
 61
          118.250 120.250 123.375 127.625 131.458
 62
          -118-756-120-458-123-958-127-167-131-458
 63
          120.750 122.125 125.792 130.000 133.250
          122,583 124,208 127,792 130,917 134,875
 64
 65
          118,250 119.000 122.042-125.167 128.000 --
          118.625 119.333 121.875 125.417 126.542
 66
 67
          120.292 121.083 123.125 126.250 125.875
 68
          118.361-119.347-121.250-124.014-125.639
 69
          118.167 118.625 120.417 123.125 124.667
 70
          118.292 120.083 121.458 123.500 125.708
 71
          119.792 120.667 122.583 125.292 127.042
 72
          118.667 121.833 123.042 125.375 124.833
 73
          118.667 121.833 123.042 125.375 124.833
 74
          -112-125-113-917-116-000-118-583-121-125
 75
           99.750 100.958 102.458 103.833 105.417
 76
          107.750 108.125 108.792 109.667 110.667
 77
           90.417 90.750 91.250 91.625 92.042
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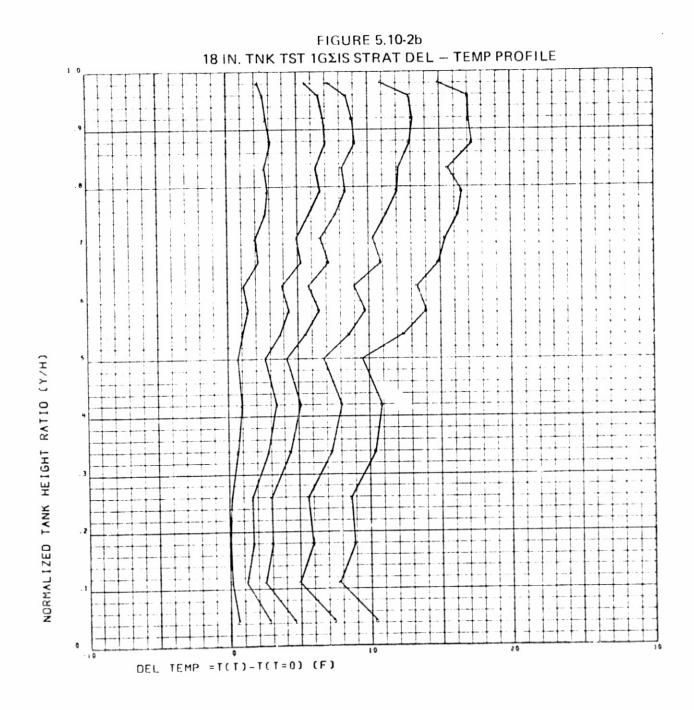
TEMPERATURE MATRIX-STRATIFICATION

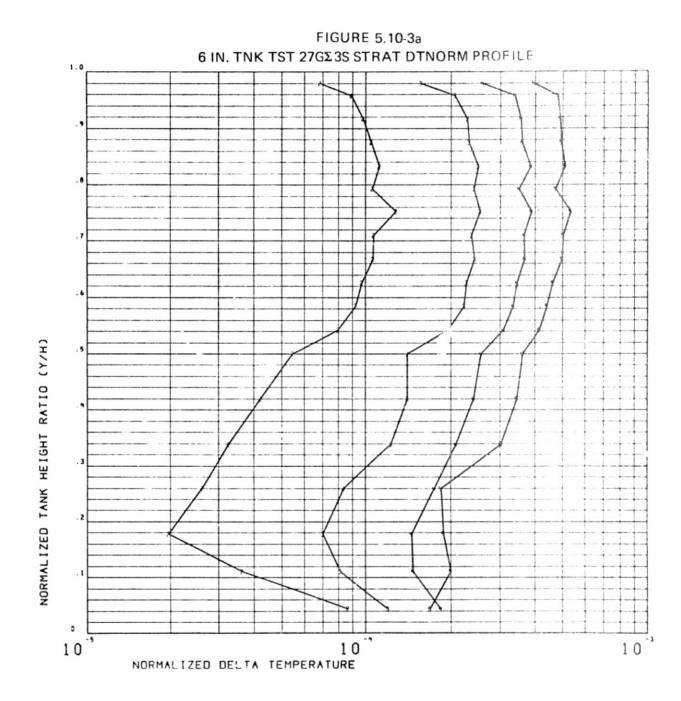
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	6							6		13	3	75	n	1	3 A		0		13							83		76	17	58		
	7							3		13.	3	01	ž						14	0	7	75								25		
	8						-	3			0			1	35	1 5	7	,								08		40	13	33		
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	10							0 (9,6					15	~ .	•	12	41	Ö	4 2				58		32	1/	80	٠	-
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	13										7 1 5			1:	2	. 0	83		15	3,	0	4 2				75		59	12	08		
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	6							42			,,9			1	31	٤,	33		13				1	37	, 3	75	1	41	. 0	00		
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	9				11	.7	, 7	08	1	23	1,2	08	3	12	26	, 2	08		12							83	1.	34	2	60		
	0 2				12	4	5	00	1	49	, 6	25				7			15							67		53	. 1	67		
2	1 -				12	8	4	58	-1	57	16	67	-	16	2	. 6	25									25	-17	71	5.	42	-	
2	2				11	8	2	υ8	1	48	4	58	3	15	3	3	33		15	5:	50	0				33						
2	3								1	47	, 5	83	3	15	2	. 0	83									75						
2	4				11	8	0	00	1	20	3	75	;	12	4	: 3	75		12	ί.	41	7				17		54				
2	5				11	7	7	92	1	20	.0	0 0)	12	3	5	0.0		12							57		33	4	5.2		
2	6										. 0			12	3	5	0.0		2		20	2	12				1.3	33	7	7		
2	7-				11	7	7	08	-1	19	, 9	17	_	12	3	. 7	3.3						12	2	7	92-	.13	3	. ה	37		
2	8				11	7	7	92	1	19	,1	25		1 2	1	2	50		121	;'	77	5	12	4	0	58	1 2	, ,	70			_
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	3										;5			4 2	71	7	- 0		148				15	1,	5 /	2	13	4,	0	3		
3					4 4	٦,	B.	75	1	10	19	70		4 2	1	7	9 0		2		9					7		41	0.8		tin about	-
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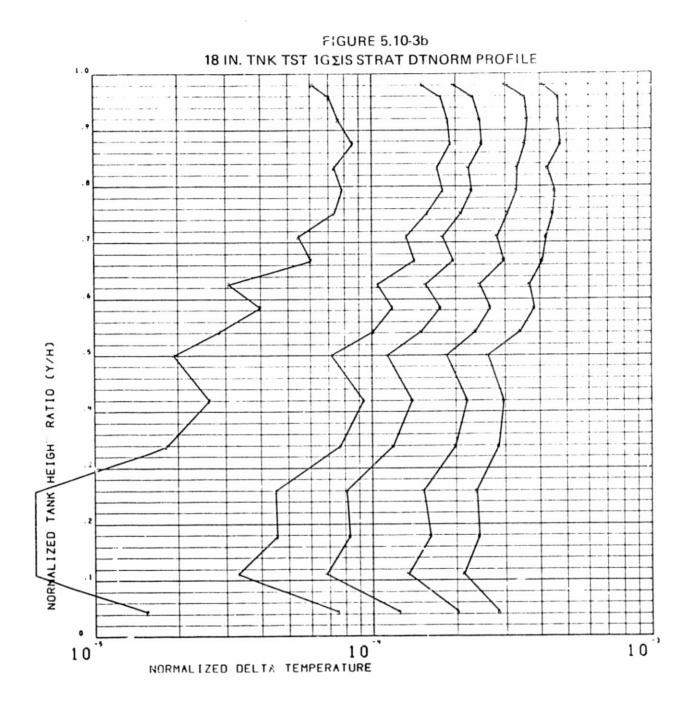


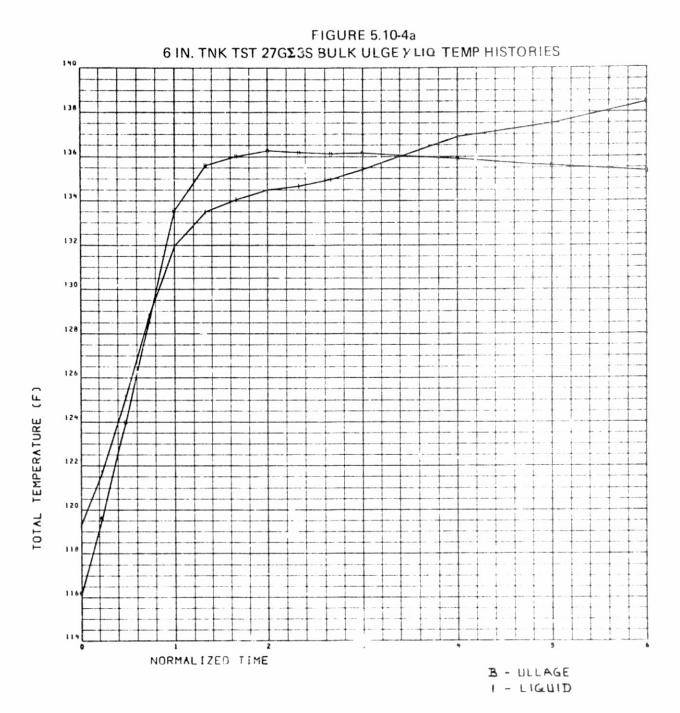


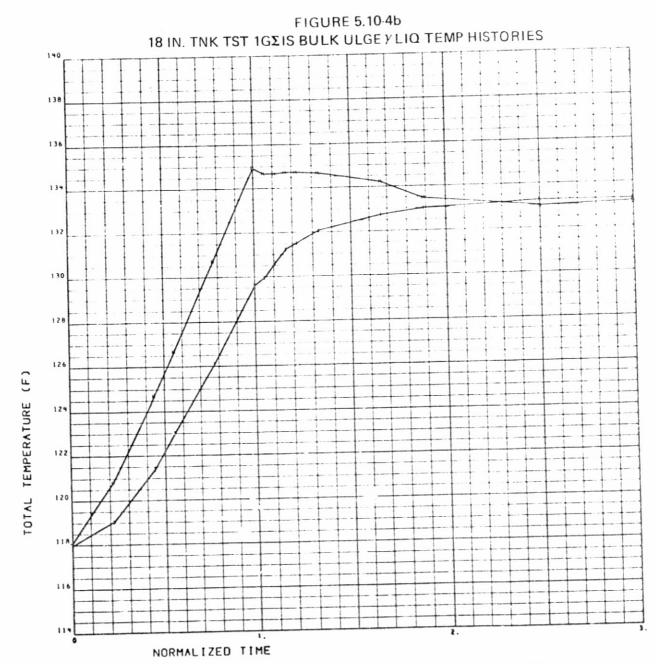




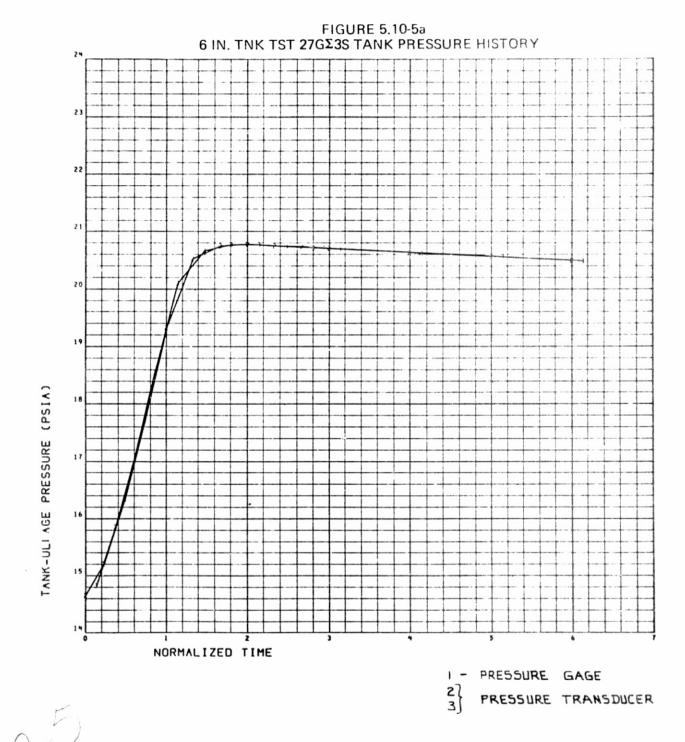








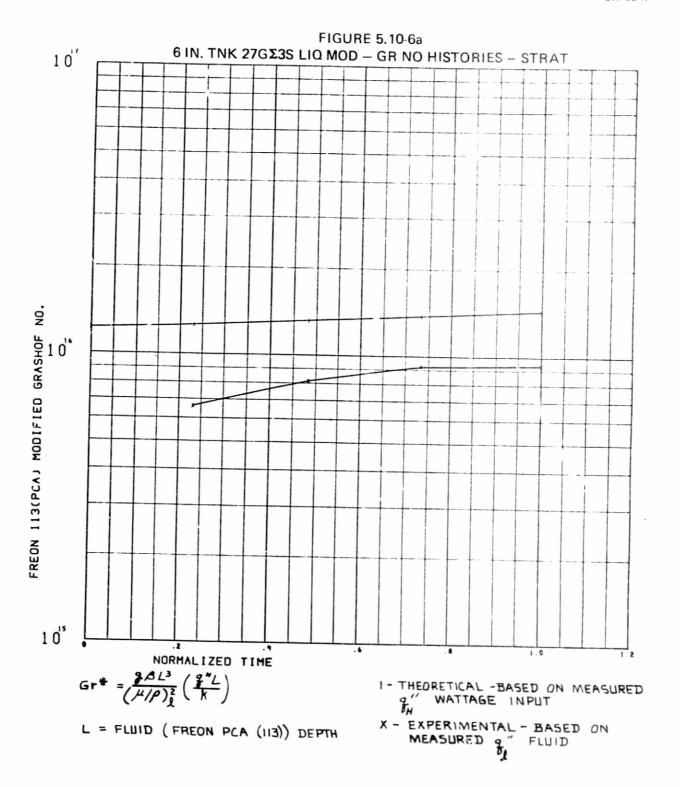
B - ULLAGE

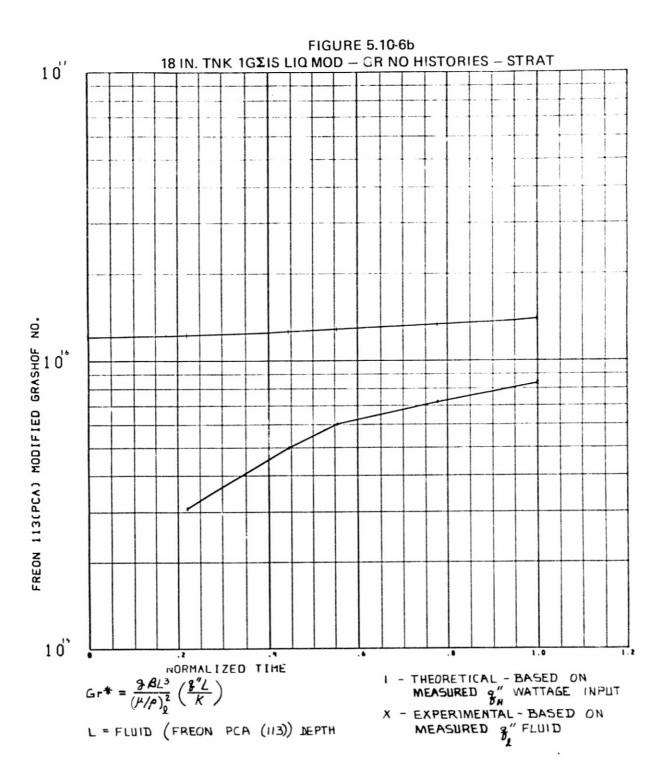


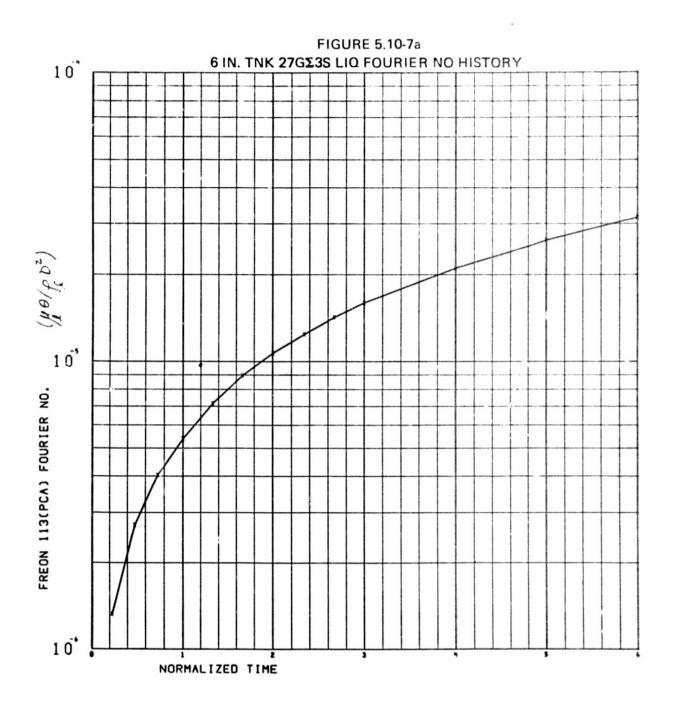
PRESSURE TRANSDUCER

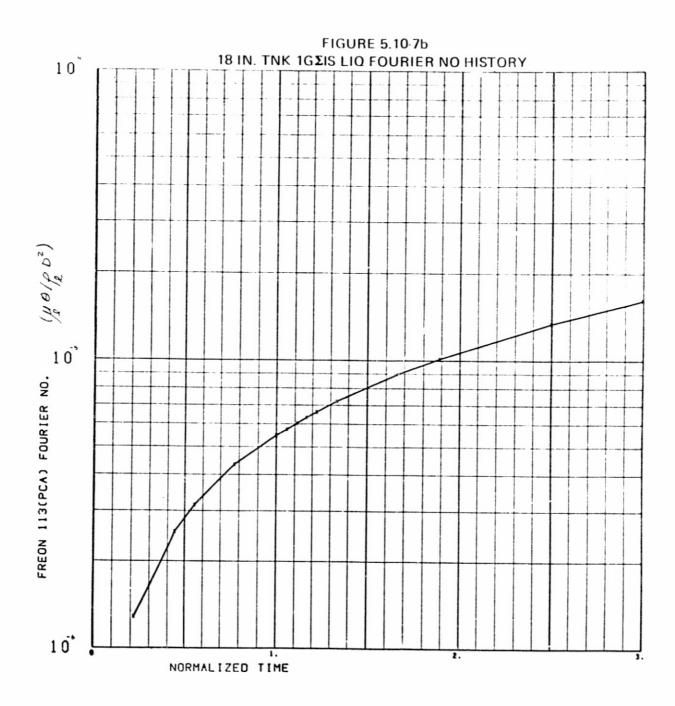
FIGURE 5.10-5b 18 IN. TNK TST $1G\Sigma$ IS TANK PRESSURE HISTORY TANK-ULLAGE PRESSURE (PSIA) NORMALIZED TIME 1 - PRESSURE GAGE
27
PRESSURE TRAN

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Section 5.11
CONSTANT WALL HEATER HEAT FLUX TESTS

 $q_{H}^{"}$ = 600 Btu/hr ft²

6-in Dia	Tank Tests						
1	G						
Test #1							
Test #2							

Note: c.f. 6-in.-Dia Tank Test 8G #1 (Section 5.5)

Table 5.11-1a. 6 IN. DIA. TANK TEST 1G#1 STRUCTURAL GEOMETRIC TANK MIS-MATTMETER HEAT FLUX INPUTS

DME MASS	AOP E.	73= ,	00131	1/	2 CYL W	ALL VOL	F73=	FLNGE AR 100164 FLANGE	FLNGE	VOL FT3=	.00076
LIG VOL	FT3=	.2290	7	ULLAG	E VOL F	T3# ,	03272				
INPUT HE	AT FL	IXES (8	IU/ER=	F121,A	ND ABSO	RBED_HE	AT AND	TEMPERATUR	E ESTIM	ATES	
H12= 600,	8488	H34#	600.84	88 H	56= 600	,8488	H910=	600,8458	H78=	0,0000 ~	
EST, HT FL	UX IN	LIG (B	TII/HR=	FT21=	600:848	8					
EST HT FL	UX IN	ULLGE	(BTU/H	Ref [2]	. 0.0	000					
EST HI IN	PUT L	LILSTRA	TIBIUE	72+	752	-4STRAT	*DESTRA	TJBTUR 13	7,439		
EST, LIQ T	EMP I	VCRSE(S	TRATI	14.	9311F	(STR	ATODEST	RAT)# 28	, 2232F		
EST.HT IN	PUT_U	LAGE (S	TRAT.) B	TUs	0.000	(ST	RATODES	TRATIBIU=_	0.00	0	
			Тa	ble 5. 1	1-1b. 6	IN. DIA	. TANK	TEST 1G#2			-
	STRUC	TURAL						FLUX INP			*****
DOME ARE	A FT2	. ,39	27	CYL	AREA FT	2= 1,5	708	FLNGE AR	EA FT2=	.0365	
TIME WALL	VOL F	3= .	00131	1/	2 CYL K	ALL VÓL	F73=	.00164	FLNGE		.00076
				MACC 4	10 CVI	LLM-					
			6	MASS I	/2 CTL	Pous	<u>. 51996</u>	FLANGE	MASSE	,38058	•
	raw:	6559					. <u>5</u> 1996	FLANGE	MASSE	,38058	
TIO AOF I	LBW=	,6559 _,2290	7	ULLAG	E VOL F	T3= ,	03272	FLANGE TEMPERATUR			
TIO AOF I	LUM# FT3# AT FLL	,6559 ,2290 JXES (B	7 TU/FR=	ULLAG	E VOL F	T3= . RBED HE	03272 AI AND				
LIG VOL I INFUT HEA	LUM# FT3# AT FLL 8488	,6559 ,2290 JXES (B	7 TU/FR= 600,84	ULLAG F72),A	E VOL F NC ABSC 56# 600	73≈ . RBED HE .8488	03272 AI AND	TEMPERATUR	E EST;	ATES	
LIG VOL I LIG VOL I INFUT HEA H12= 00010	LUM# FT3# AT FLL B488 UX IN	,6559 ,2290 JXES (B H34# L10 (B	7 TU/IR= 600,84 TU/IR=	ULLAG F72),A 88 H F72)=	E VOL F NC ABSC 56# 600 600.848	T3= , R6ED HE ,8488	03272 AI AND	TEMPERATUR	E EST;	ATES	
LIQ VOL I LIQ VOL I INFUT HEA H12= 00018 EST, HT FLE	LUM# FT3# AT FLL 8488 UX IN UX IN	,6559 ,2290 JXES (B H34# L10 (B ULLGE	7 TU/IR= 600,84 TU/IR= (8TL/H	ULLAG FT2),A 88 H FT2)= R=FT2)	E VOL F NC ABSC 56# 600 600.848	T3= , REED HE ,8488	03272 AI AND H910#	TEMPERATUR	E EST;A	ATES	
LIQ VOL I INFUT HEA 12= 600,0 ST, HT FLU ST, HT FLU ST, HT INF	LUM# FT3# AT FLL 8488 UX IN UX IN PUT LI	,6559 ,2290 JXES (B H34= LIQ (B ULLGE Q(STRA	7 TU/IR= 600,84 TU/IR= (8TL/H T)8TU=	ULLAG F72),A 88 H F72)= R=F72)	E VOL F NC ABSC 565 600 600.848 F 0.0	RBED HE .8488 8 000 (STRAT	03272 AI AND H910=	TEMPERATUR 600,8468 T)ETU= 13	E EST;#	ATES	
INFUT HEAT THE STATE OF THE STA	LUM# FT3# AT FLL 8488 UX IN PUT LI	,6559 ,2290 JXES (B H34# LIQ (B ULLGE Q(STRA	7 TU/FR= 600,84 TU/FR= (BTL/H T)BTU= TRAT)=	ULLAG F72),A 88 H F72)= R=F72) 72, 14.	E VOL F NC ABSC 56# 600 600.848 0.0 752 9301F	T3# , RBED HE .8488 8 000 (STRAT (STR	03272 AI AND H910# +DESTRA	TEMPERATUR	H78=	ATES	

TINE (MIN)	0	.000	1,000	2,000	3.000	3,700
TAU	0.00		.270	.541	7811 1	.000
	115.	Á19	123.625			36,083
2			130.750	136, 375	141.208	43,625
3	116	467	128.750	134.250	138.667	
4	116	750	129.333			40,833
5	116	375	127.000		135,500	
6			128.000	132.375	135,875	37.917
7	116	500	120-500-	133.208	134.375	38.333
8	116	542	128.375	131,792	134.667	36,417
	110	058	121.458	124.875	127.958	29,750
9	115	733	133.792	139.167	143.447	46.250
10	110	581	134.458	130.458	142.956	45,792
11	110	047	133.583	137.667		
12	110	727	132,500	135.792	138.708	40,375
. 13	110	708	122.456	127.458	132.147	34,917
14	115	700	125.958	174.333		
15	110	072	126.167_	131,003	435.280	37.437
16	110	917	120-101-	131,303	434.498	34,000
17	110	220	124.125	1201147	430 780	32,792
18	112,	/00	124.375	1271700	1001/90	27 475
19	112,	777	119.5A3	1231003	447 447	44 250
20	110	333	133.792	139,107	173,717	146,250
21	110,	203	134,458	139,420	145,400	42 053
22	110,	917	133,583	13/ 100/	170 700	40 378
23	110	379	132,500	139,772	130,700	170,375
24	115	426	117.250	120,0/2	124,797	127,458
25	113	,125	115,958	117, 728	150-400	22,083
26	105	875	109.875	113,772	115,250	116,292
27	99	583	100.958	104,107		107,125
28	114	958	115.750	117,208	119.042	20,025
29	115	042	115.875	117,333	119.708	121,500
30	115	,542	117.583	121,200	125,375	120,042
31	115	681	129.861	132,528	134,744	130+730
32	116	292	130.333	133,000	135,333	130,917
33	112	,790	117.500	120,438	122.900	123,833
34	108	583	198.625	100,230	110,208	110.917

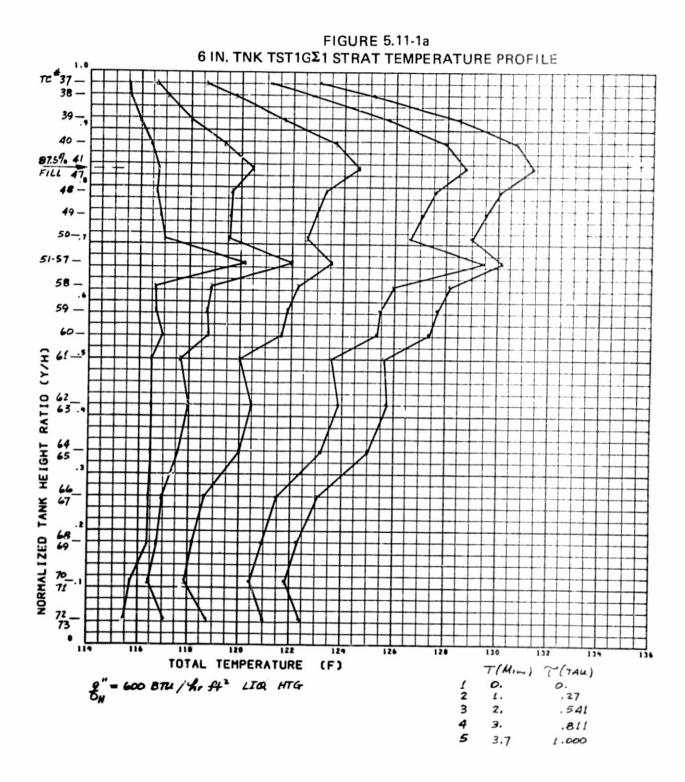
Table 5.	11-2a. 6 IN. DIA TANK TEST 1G #1 (Page 2 of 2)
35	104,375 103,708 103,250 103,208 103,292
36	115,375 129.625 132,292 134,750 136,667
37	115,542 \16.667 118,625 121,167 123,125
38	115,583 117,125 119,792 122,875 125,167
39	115,958 118.042 121,667 125,750 128,500
40	116,417 119.375 123,708 127,958 130,708
41	116,500 119.708 123,607 128,042 130,625
42	116,708 119,917 124,708 128,917 131,458
43	116,792 120.417 125,083 129,292 131,792
44	116,958 120.542 124,417 128,375 130,875
45	116,667 120.458 124,625 128,958 131,583
46	116,750 120.750 124,458 128,542 131,417
47	116,750 121,458 125,250 129,083 131,792
48	116,667 119,667 123,306 127,569 130,083
49	416,833 119,625 122,944 127,097 129,542
50	117,000 119.583 122,583 126,625 129,000
51	116,625 119.042 122,647 126,500 128,667
52	140,792 139,042 129,792 146,792 139,125
53	116,750 119,167 122,667 126,958 129,042
54	116,917 119,000 121,833 126,000 128,208
55	116,708 119,458 123,042 126,917 129,042
56	116,917 119,000 121,833 126,000 128,208
57	116,708 119,458 123,042 126,917 129,042
58	116,646 118,875 122,250 125,979 128,188
59	116,667 118,708 121,833 125,458 127,708
60	116,917 118,750 121,625 125,333 127,375
61	<u> 116,500 117,667 120,000 123,583 125,625</u>
62	116,500 117,917 120,375 123,917 125,750
63	116,500 118,042 120,542 123,833 125,750
64	116,667 117.958 120,583 123,708 125,708
65	116,292 117,250 119,458 122,667 124,333
66	116,333 116,958 118,583 121,375 122,958
67	
68	116,500 116,875 118,208 120,917 122,292
69	116,290 116,667 118,167 120,958 122,333
70	115,750 116.458 117,792 120,500 121,833
71	115,625 116.375 118,000 120,417 121,833
72	115,542 116,750 118,375 120,958 122,292
- 73	115,333-117-375-119,167-121,042-122,542
74	105,875 107.083 108,750 111,208 112,333
75	90,500 90,833 90,543 91,268 91,125
76	103,000 103.458 104,458 106,083 106,792
77	89,750 90,042 89,750 90,125 89,833

Table 5.11-2b. 6 IN. DIA TANK TEST 1G #2 (Page 1 of 2)

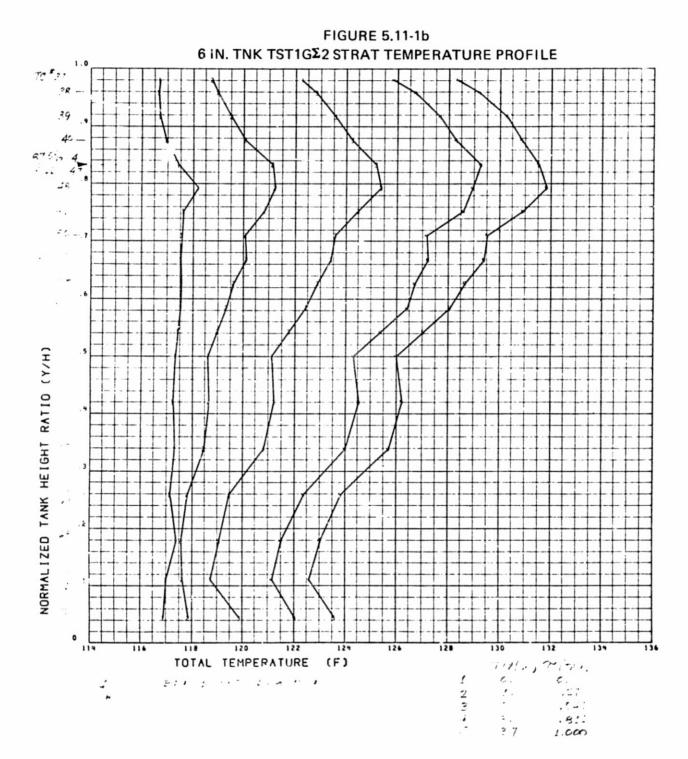
TEMPERATURE MATRIX-STRATIFICATION

			-								
TIME (MIN	,	0.00	0	1 00			^	• ••			
TAU	0.0			1,00 70	-	2.00		3,00		3,700	
1		750			129	125	;;	11,75	1.0		
2		333	130	500	136	167	140			958	
3			120	708	134	877	438	500	142	,917	
 4	117	375	128	958	133	771	137	125	130	500	
5		250		208		708	136	.083			
6		208			133	000	136			.292 .417_	
 7		333		875	132	ROA	135	833		771	
8		458		000	132	792	135	458	137	125	
9		375		000		583	128	500		208	
10		333		333		708	143	500		500	
11		500		250	140	292	144	208		292	
12	117	667	134		138	125	144	375	143	500	
13	117	167	132	875	136	083	138	708	140	542	
14	116	542	123	167	128	125	132	708	135	208	
 15	116	917	126	458	131	958	136	292	138	675	
16	117	417	126	750	132	000	135	833	138	167	
17		021		-	130	458		667			
 18				125	128	917	131	500	133	292	
19	116	125	120	333	123	708	126	708	128	500	
20	117	333	134	333	139	708	143		146		
21	117	500	135	250	140	292	144	208	146	292	
22	117	667	134	250	136	125	141.	375	143	500	
2 3	117	167	132	875	136	083		708			
24	116	708	119	000	123	125	127	125	129	500	
2 5	116	333	118,	500	122	000	125,	625	128	208	
26	116	250	118,	396	121,	792	125.	333	127	813	
 27	116	167	118,	292	121	583	125	042	127	417	
28	110	242	110,	292	121,	208	124.	542	126	583	
2 9	116,	250	117,	583	120	333	123.	708	125	875	
 30	116,	542	119,	125	123,	167	127.	208	129	792	
31	116,	792	130	889	133,	500	135.	819	137	347	
32	117,	458	131,	417	134,	000	136,	042	137.	625	
 33	115	458	120,	083	122.	375	124.	167	125.	333	
34	113,	167	113,	208	113.	792	114.	417	114.	833	

Table 5. 11-2b. 6 IN. DIA TANK TEST 1G #2 (Page 2 of 2) 110,958 110,250 109,833 109,625 109,458 35 116,458 130,625 133,250 135,708 137,208 36 3.7 116,708 118,750 122,250 125,875 128,375 116,667 119,000 122,833 126,708 129,208 38 116,708 119,542 123,583 127,667 130,292 39 116,958 120,083 124,250 128,292 130,875 40 117,417 119,958 124,250 128,042 130,375 41 117,333 120,575 125,083 129,292 131,708 42 117,375 120,956 125,208 129,250 131,750 43 117,667 120,958 125,458 129,333 131,625 44 117,333 121,292 125,333 129,458 131,750 117,458 121,958 125,542 129,458 131,708 46 117,375 122,083 125,417 130,042 131,792 47 118,208 121,250 125,375 128,958 131,833 117,625 120,833 124,500 128,583 130,917 49 117,583 120,083 123,583 127,167 129,542 50 117,575 119,933 123,350 127,017 129,250 117,558 120,029 123,404 127,133 129,333 52 117,417 120,458 123,208 127,375 129,583 53 117,542 120,125 123,458 127,250 129,417 54 117,542 120,125 123,458 127,250 129,417 55 117,542 120,125 123,458 127,253 129,417 56 117,542 120,125 123,458 127,250 129,417 57 117,558 119,633 122,883 126,717 128,667 58 117,542 119,333 122,417 126,417 128,083 59 117,438 118,979 121,771 125,375 127,042 60 117,333 118,625 121,125 124,333 126,000 61 117,125 118,583 121,208 124,542 126,000 62 117,375 118,750 121,208 124,542 126,458 63 117,417 118,875 121,458 124,583 126,417 64 117,208 118,083 120,208 123,417 125,042 65 117,083 117,750 119,500 122,375 123,792 66 117,208 117,875 119,458 122,375 123,875 67 117,625 117,667 119,000 121,292 122,917 68 69 117,125 117,500 119,167 121,708 123,125 117,083 117,542 118,792 121,292 122,750 70 116,917 117,708 118,667 121,042 122,417 71 117,083 117,917 119,375 121,792 123,292 72 116,708 117,833 120,417 122,292 123,917 73 105,792 106,917 108,333 110,625 111,625 74 89,625 90,208 90,125 75 89,667 89.375 102,708 103,125 104,208 105,875 106,667 76 88,125 88,417 88,250 77 87,917 88,167

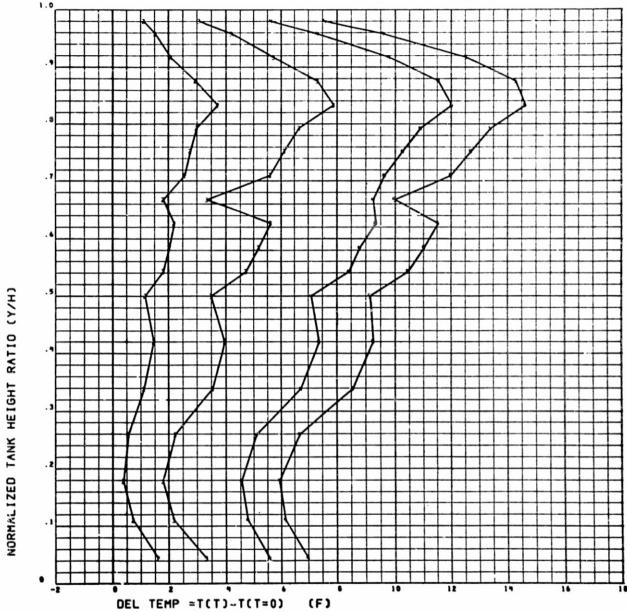


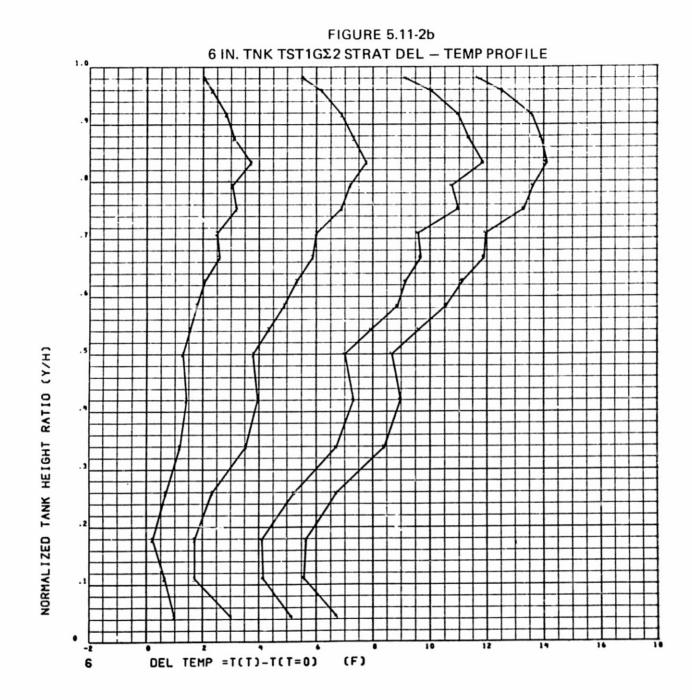
375



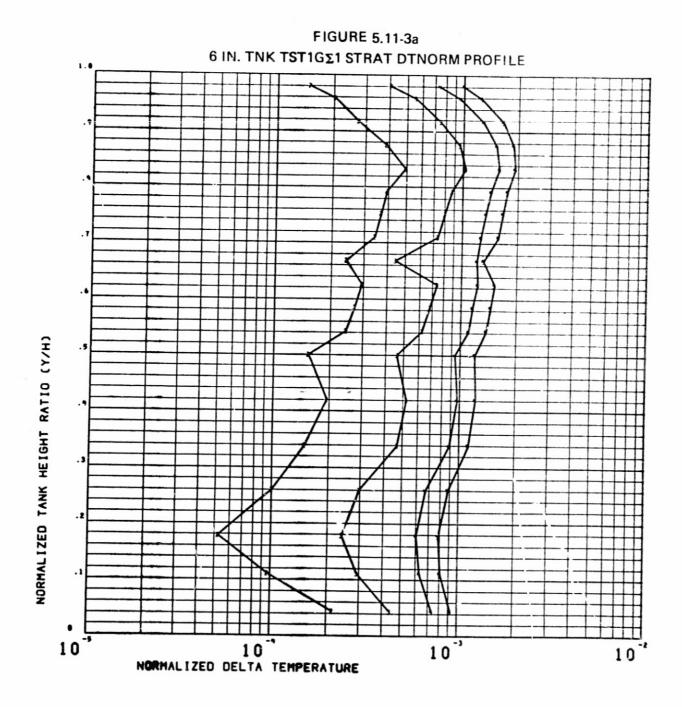
376

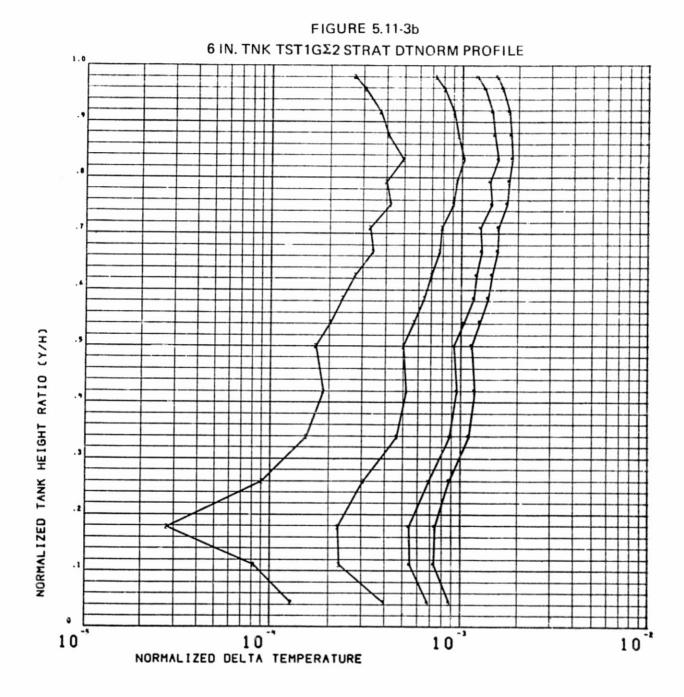
FIGURE 5.11-2a 6 IN. TNK TST1G Σ 1 STRAT DEL — TEMP PROFILE





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The Samuel Street In-

FIGURE 5.11-4a 6 IN. TNK TST1GΣ1 BULK ULGE YLIQ TEMP HISTORIES 126 TOTAL TEMPERATURE 122 NORMALIZED TIME B - ULLAGE 1 - LIQUID

381



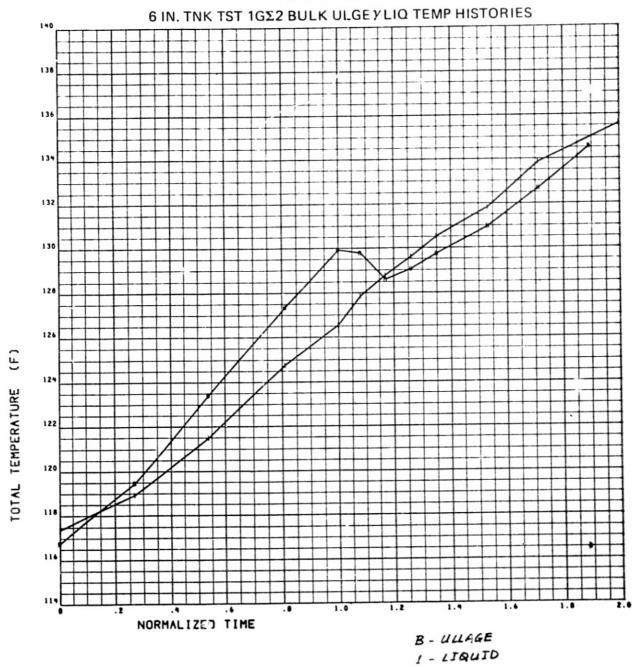


FIGURE 5.11-5a 6 IN. TNK TST1GΣ1 TANK PRESSURE HISTORY TANK-ULLAGE PRESSURE (PSIA) NORMALIZED TIME 2: Transducer Measured

FIGURE 5.11-5b 6 IN. TNK TST1GΣ2 TANK PRESSURE HISTORY TANK-ULLAGE PRESSURE (PSIA) NORMALIZED TIME

2; Transducer Heasund

